



City of Columbia, Missouri Water and Light
Department
McBaine Water Treatment Plant

2017-2018 Drinking Water Planning
Work Group Recommendations
Update to 2011 Preliminary Design
Report

FINAL | March 2018





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Abbreviations

AACE	American Association of Cost Estimators
CaCO ₃	calcium carbonate
Carollo	Carollo Engineers, Inc.
CDP	Criterion Decision Plus
CEC	Contaminants of Emerging Concern
City	City of Columbia
DBP	Disinfection By-Product
D/DBPR	Disinfectants/Disinfection By-Products Rule
DWPWG	Drinking Water Planning Work Group
ft	feet
GAC	Granular Activated Carbon
gpm/sf	gallons per minute per square foot
GWUDI	groundwater under the direct influence
IDSE	Initial Distribution System Evaluation
IWRP	Integrated Water Resource Plan
<i>LRWSS</i>	<i>Long Range Water System Study (Jacobs, 2015)</i>
µg/L	micrograms per liter
MG	million gallons
µg/L	micrograms per liter
mg/L	milligrams per liter
mgd	million gallons per day
MIEX	Magnetic Ion Exchange
NTU	nephelometric turbidity unit
PDR	2012 Preliminary Design Report for the McBaine WTP
ppd	pounds per day
RO	reverse osmosis
SDA	Structured Decision Analysis
S.U.	Standard Units
TTHM	Total Trihalomethane
UF	Ultrafiltration
UV	ultraviolet
WTP	water treatment plant

EXECUTIVE SUMMARY

Goals

The main goal of this project is to update the recommendations of the 2012 Preliminary Design Report (PDR) for the McBaine WTP. This update is based on the conclusions and recommendations of the 2016 Condition Assessment Report and the updated demand projections from the 2017 Integrated Water Resources Plan (IWRP).

Mission of Drinking Water Planning Workgroup

Provide planning recommendations to the Water and Light Advisory Board and the City Council regarding the expansion of the water treatment system by establishing water quality goals, determining assessment criteria; and, conducting a thorough, objective, assessment of industry accepted treatment technologies to determine the process or processes that best meet these criteria.

Methodology

Similar to the 2012 PDR, the Drinking Water Planning Workgroup (DWPWG) utilized a series of workshops, facilitated by Carollo Engineers, Inc., (Carollo), in which a structured decision analysis (See Figure ES-1) was employed to provide these planning recommendations. A total of eight (8) workshops were held between May 2017 and February 26, 2018.

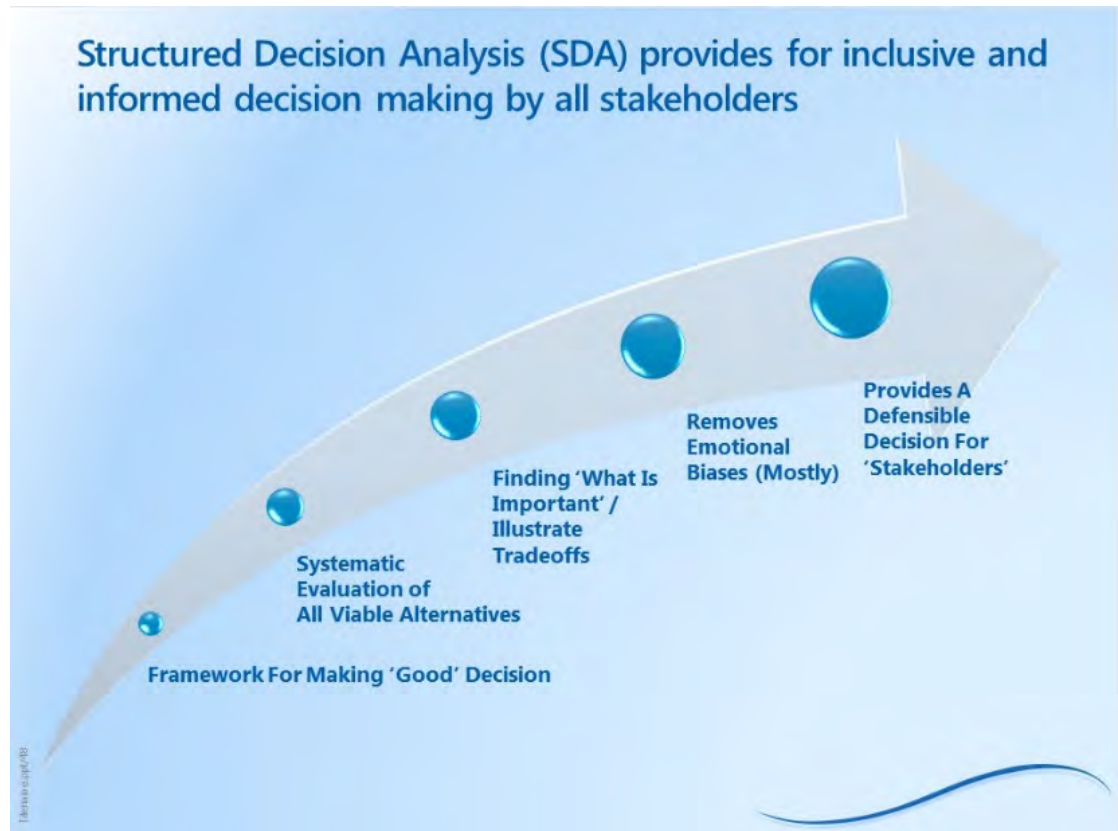


Figure ES-1 Structured Decision Analysis Benefits

The major steps associated with the structured decision analysis are as follows:

- **Project Visioning:** A process in which the framework and boundaries for the decision are established. A fatal flaw list is developed.
- **Alternatives Identification and Screening:** A process in which potential alternatives are identified and screened. Any alternatives with fatal flaws are eliminated from further consideration.
- **Criteria Selection and Ranking:** A process in which the criteria upon which particular alternatives associated with the decision process are to be evaluated and the relative importance of these criteria to the decision are established through a “pairwise” comparison.
- **Alternative Development and Shortlist:** A process in which potential alternatives are sufficiently developed to eliminate those that provide the lowest benefit (non-economic scores): i Cost (Economic scores) ratio when examined with the weighted criteria.
- **Alternative Re-Ranking and Sensitivity Analysis:** A process in which data gaps identified as relevant to the decision process are identified and resolved; the alternatives reranked with respect to the evaluation criteria; a sensitivity analysis conducted to determine the robustness of a potential decision; and a final decision statement and recommendation statement is generated.

Cost Development

Table 5 presents the cost classification system as applied in Engineering, Procurement, and construction for the Process Industries as developed by the American Association of Cost Estimators (AACE). It is important to note that the level of estimates (Class 4) provided in the alternatives development and selection process are utilized to provide a relative comparison between alternatives and **should not be utilized for budgetary purposes.**

Table ES-1 **AACE Cost Classification System**

Estimate Class	Primary Characteristic	Secondary Characteristic		
	Maturity Level of Project Definition Deliverables (as % of definition)	End Usage – Typical Purpose of Estimate	Methodology – Typical Estimating Method	Expected Range of Accuracy Typical variation in low to high
Class 5	0% to 2%	Concept Screening	Capacity factored Parametric models Judgement or analogy	L: -20% to +50% H: +30% to +100%
Class 4	1% to 15%	Study or Feasibility	Equipment factored Parametric models	L: -15% to +30% H: +20% to +50%
Class 3	10% to 40%	Budget Authorization or Control	Semi-detailed unit costs with assembly level line items	L: -10% to -20% H: +10% to +30%
Class 2	30% to 70%	Control or bid/tender	Detailed unit costs with forced detail take-off	L: -5% to -15% H: +5% to +20%
Class 1	65% to 100%	Check estimate or bid/tender	Detailed unit costs with detailed take-off	L: -3% to -10% H: +3% to +15%

Notes:

(1) Taken from 18R-97 Cost Estimate Classification System Published by AACE.

Final Recommendations

The findings and recommendations of the DWPWG are as follows:

1. DWPWG Findings:
 - a. The McBaine WTP should consider processes that meet the requirements for a GWUDI Facility.
 - b. The McBaine WTP should utilize treatment technologies to achieve Disinfection By Products (DBP) compliance without the need for chloramines and to also assist in removal of Contaminants of Emerging Concern (CEC's).
2. DWPWG Recommendations:
 - a. Priority should be given to first restoring the plant to its 32 MGD capacity prior to increasing capacity to 48 MGD.
 - b. The base alternatives of B1.1, B1.2, and B2 should be evaluated with the supplemental processes to achieve improved water quality through a phased approach.
 - c. The design on the selected alternative should begin no later than 2020, as indicated in Carollo's analysis, to be in operation no later than 2024, unless design and construction are able to be accomplished sooner.
 - d. In order to improve water quality while the new process train is in design, and construction, repair and/or enhancement of the current filters and pilot testing done to make every effort to return to free chlorine disinfection.
 - e. The rehabilitation and/or enhancement initiatives outlined in the Condition Assessment will address deficiencies in the facility and system and request an updated timeline for these initiatives be produced by Water and Light.

Section 1

INTRODUCTION

1.1 Background

The City of Columbia (City) owns and operates a municipal water treatment utility that supplies water to domestic, commercial, institutional, and industrial customers in and around the City. The water supply and treatment system consists of a 15 well ground water well field, one water treatment plant rated for 24 million gallons per day (mgd) capacity, a transmission network, and several water storage tanks/reservoirs. Originally constructed in 1970, the facility has gone through a number of upgrades and expansions with the latest occurring in 2008.

1.1.1 2012 McBaine Water Treatment Plant (WTP) Expansion Preliminary Design Report

Following the last plant expansion, the City completed the *McBaine WTP Expansion Preliminary Design Report* (Carollo, 2012). The purpose of this report was to provide recommendations to expand the existing facilities in order to meet future demands and achieve compliance with current and anticipated future regulatory requirements. The decision making process that was established considered three (3) primary criteria, thirteen (13) sub-criteria, and incorporated relative cost comparisons.

The recommended treatment alternative from this report involved rehabilitation of the existing filters to increase filtration rate to 6 gallons per minute per square foot (gpm/sf) along with installation of high rate deep bed rapid rate multimedia filters as part of any filtration expansion. This recommendation resulted in a treatment alternative that not only met future demands, but also provided a facility that was groundwater under direct influence compliant. It should be noted that treatment alternatives that provided removal of contaminants of emerging concern (CECs) were also evaluated. Although these higher cost alternatives resulted in a lower benefit/cost ratio, the decision to implement these is a matter of public policy rather than determination through any engineering evaluation.

1.1.2 2016 Condition Assessment Report

In 2016, the City worked with Black & Veatch to complete a condition assessment of the McBaine WTP, as well as the Well Field and West Ash Booster Pump Station. The goal of the condition assessment was to assess the condition of the existing equipment to determine which components need to be replaced to meet current critical demands and water quality, identify potential improvements that will enhance performance and reliability, and address future capacity increases.

Because the ultimate capacity of the plant was uncertain at the time of the condition assessment, the report that was developed evaluated alternatives for expanding the plant to 45 or 60 mgd. In addition, the associated impact if the groundwater is reclassified as groundwater under the direct influence (GWUDI) was also considered in some of the alternatives. All in all, three (3) 45 mgd alternatives were considered, three (3) 60 mgd alternatives were considered, and two (2) of the 60 mgd alternatives were evaluated considering the impact of GWUDI.

Selection of the recommended alternatives was based on a number of factors, including capital costs, operation costs, constructability, regulatory, and operational. Based on this evaluation, the initial expansion alternative (45 mgd expansion) that was recommended in the Condition Assessment Report was construction of a new process train. This alternative consists of building an additional treatment train on the north side of the plant that includes two new aerators, one solids contact unit, one recarbonation basin, and a new filter complex. Although the costs associated with this alternative were higher than re-rating the existing plant, it was selected due to its ease of constructability and regulatory approval.

Another notable result of the condition assessment that should be mentioned here was the derating of plant capacity. As previously mentioned, the last plant expansion occurred in 2008 and included, among other things, a fourth Primary Basin and a fourth Secondary Basin. The four sets of basins each provided a capacity of 8 mgd, for a total plant capacity of 32 mgd. Because of the age and condition of the equipment in Primary Basins No. 1 and 2, these basins were derated to 4 mgd each, resulting in a total plant capacity of 24 mgd. It should be noted that the replacement of equipment in Primary Basins No. 1 and 2 should occur regardless of any expansion alternative recommended in this report.

1.1.3 2017 Integrated Water Resource Plan

In 2017, the City completed their *Integrated Water Resource Plan (Black & Veatch, 2017)*. This report focused on a number of issues associated with managing water resources and included the following:

- The City's current water source and supply capacity.
- Projected population growth and water needs.
- Potential future sources of water.
- Development of water alternatives considering:
 - Water Demand Trends.
 - Water Conservation.
 - Potable Water Supply.
 - Non-Potable Water Supply.
 - Regulatory Requirements.
 - Community Involvement.

There were multiple notable recommendations from the Integrated Water Resource Plan (IWRP) that directly affect the development of recommendations in this report. The IWRP established specific demand projections by user class, which included residential, commercial, large commercial, and irrigation users to better understand the impact if alternative water supply or conservation measures were implemented. This evaluation included a review of known historical data along with expected growths typical of this type of community to establish supply requirements to year 2040. The demand projections derived from the evaluation were also compared to previous projections from the *Long Range Water System Study (LRWSS) (Jacobs, 2015)* and are presented in Figure 1.

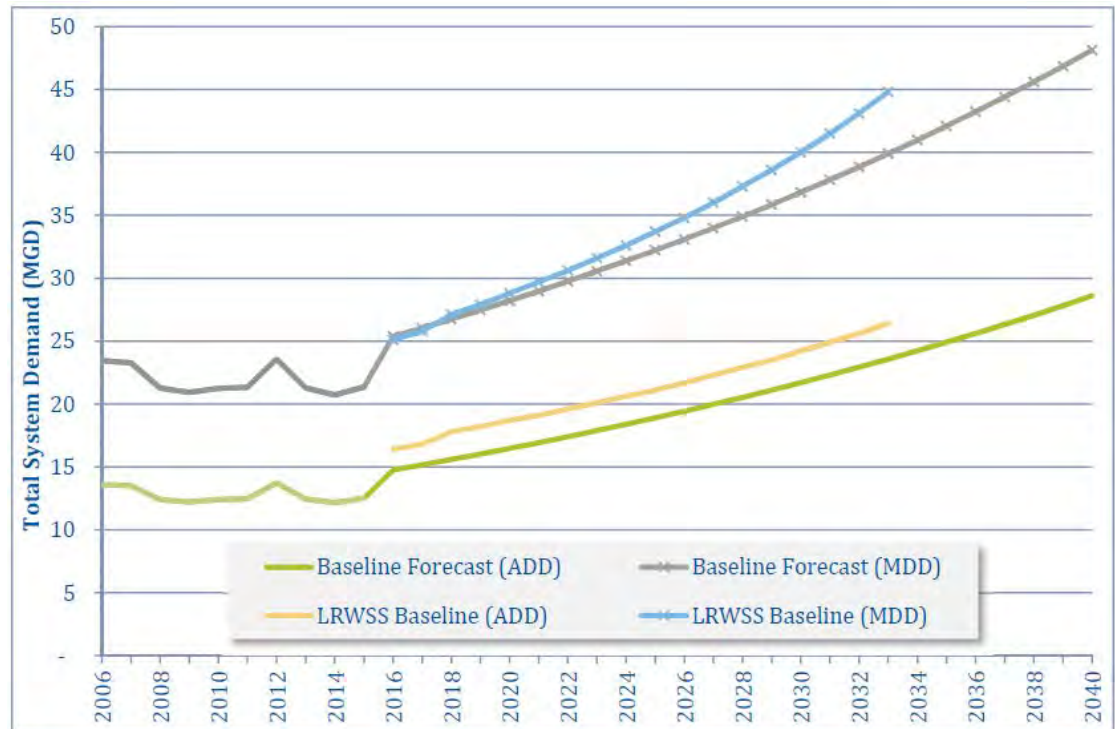


Figure 1 Average Daily and Maximum Daily Demand Forecasts from the Integrated Water Resource Plan (Black & Veatch, 2017)

In addition to the updated demand projections, the IWRP also evaluated current and potential future water supply sources. The alternatives that were evaluated included the continued use of the McBaine Bottoms Aquifer using vertical wells, installation of horizontal collector wells along the Missouri River bank, and the potential use of the Missouri River as a supply source. The evaluation did not include potable water supplies beyond the general area of the plant due to the requirement for a new treatment facility and additional transmission piping. A conceptual model indicated that the aquifer could yield a total of 65 mgd with 32 wells for 30 days with groundwater levels at each well approaching, but not dropping below the tops of the well screens. In summary, the evaluation concluded that the McBaine Bottoms Aquifer could produce the desired demands for the planning period.

1.2 Scope

The main goal of this project is to update the recommendations of the 2012 Preliminary Design Report (PDR) for the McBaine WTP. This update is based on the conclusions and recommendations of the 2016 Condition Assessment and the updated demand projections from the 2017 IWRP.

In order to facilitate the process of updating the Water Treatment Plant Expansion PDR, the City Council established the Drinking Water Planning Work Group (DWPWG). The group consists of seven (7) voting members and three (3) non-voting members. The voting members include one (1) member from the City Council and six (6) members appointed by City Utilities from several drinking water customer user groups. The resolution signed by the Mayor is provided in Appendix A.

A series of workshops were conducted that included direct input and participation from the DWPWG. These workshops utilized a decision analysis model to identify and screen potential alternatives and ultimately come up with a recommendation. By using the decision analysis model, the team was able to provide a defensible decision for stakeholders by providing a systematic approach for evaluation of all viable alternatives.

Project visioning was utilized to review existing information, discuss the results of previous studies, and discuss potential boundaries for the project. Input was solicited from the DWPWG to establish a set of water quality goals as well as any additional goals for the project. These goals were then used to develop a set of viable base and supplemental alternatives for the project. Following project visioning, a potential set of viable base and supplemental alternatives were developed.

Similar to what was done in the 2012 PDR, the decision making process considered several primary criteria along with sub-criteria. The primary criteria that were agreed upon included constructability, water quality, operability, project cost, and GWUDI facility. Each of the primary criteria and sub-criteria were assigned weighted values based on input from the DWPWG. Using computer based software, the viable alternatives were then scored against the criteria, and a preliminary ranking of alternatives was developed. The rankings were reviewed with the DWPWG and a shortlisted set of alternatives was created.

To further refine the alternatives, data gaps were identified, layouts were created, and costs were refined. The shortlisted alternatives were then re-ranked and a sensitivity analysis was conducted on the results. Using these results, along with input from the DWPWG, a final recommendation was developed.

Section 2

PROJECT VISIONING

2.1 Purpose

The purpose of the project visioning phase of the project was to establish the boundaries or framework for the decision. This included the following:

- Establish/refine the mission statement and goals for the project.
- Development of questionnaire to assess preferences of DWPWG.
- Determine the water quality goals for the treatment plant effluent.

2.2 Meetings and Workshops

The following public meetings were held during the project visioning phase of the project:

- Visioning Workshop I – July 10, 2017.
- Visioning Workshop II – August 14, 2017.
- Water Quality Goals Workshop – September 11, 2017.

2.3 Mission and Goals Statement

The DWPWG met over the three visioning meetings and developed the following mission statement:

"Provide planning recommendations to the Water and Light Advisory Board and the City Council regarding the expansion of the water treatment system by establishing water quality goals, determining assessment criteria; and, conducting a thorough, objective, assessment of industry accepted treatment technologies to determine the process or processes that best meet these criteria."

The **Goals** of the DWPWG are as follows:

- Review current planning strategies for water supply and verify current goals and planning horizon for water treatment capacity expansion.
- Considering current regulations, potential future regulations, and potential enhancements; review and recommend potential long term water quality goals.
- Assess the state of the industry and shortlist potential treatment strategies that meet or exceed some or all of the potential long term water quality goals based upon industry acceptance and long term (present worth) costs.
- Formulate a set of criteria upon which potential treatment strategies to meet or exceed potential goals will be evaluated.
- Objectively evaluate and rank potential treatment strategies that meet planning horizon goals using a structured decision analysis model.
- Conduct a sensitivity analysis of decisions to review robustness and defensibility of decisions to potential changes in criterion assessments.

- Through this objective process, develop planning recommendations to guide the Water and Light Advisory Board and City Council regarding the water treatment system.

2.4 Visioning Questionnaire and Results

Appendix C presents the questionnaire and a summary of the results. The questionnaire was issued as a vehicle to allow the group to provide feedback on the development of the direction for the planning group.

2.5 Establishing Project Boundaries

The following boundaries were established by the DWPWG for the investigations:

1. Retain/Expand Current Well Field per IWRP: The DWPWG accepts all of the recommendations of the IWRP. This includes retaining the existing groundwater wells and well field as the water supply source for the Citizens of Columbia.
2. Retain Existing WTP infrastructure: The existing plant infrastructure and plant site will be retained. As a result, the investigations into the treatment strategies to be employed will be limited to expansion and integration of processes at the existing WTP site.
3. Water Treatment Expansion Needs/Timeline: Figure 2 presents a summary of the projected demands and the WTP expansion capacity and timeline recommended by the IWRP reviewed and accepted by the DWPWG. The IWRP recommended an expansion of the water treatment plant capacity from 32 mgd to 48 mgd by the planning year 2024.

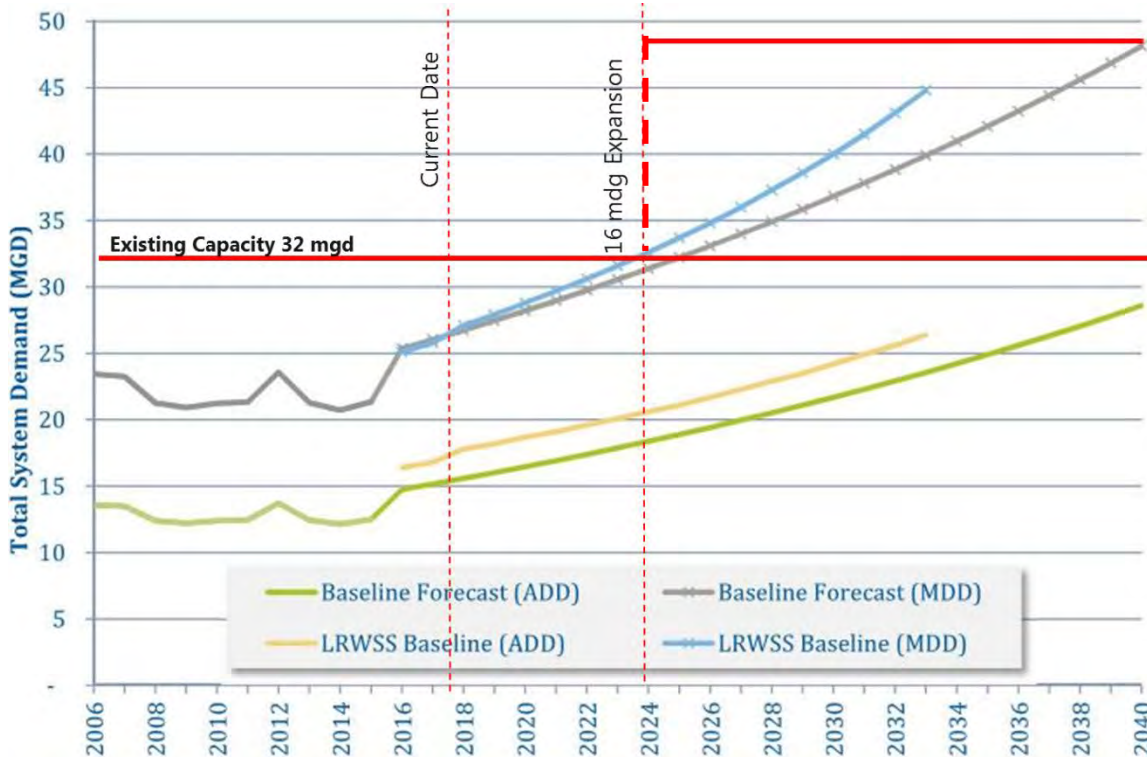


Figure 2 WTP Expansion Recommendations of IWRP

4. Accept WTP Capacity Restoration Project: Figure 3 presents a summary of the recommendations of the 2017 *Condition Assessment Report Well Field, McBaine Water Treatment Plant, and West Ash Booster Pump Station*. The findings and recommendations of these report to conduct a project to restore the capacity of the existing plant 32 mgd from its current derated capacity of 24 mgd in 2018-2019.
5. Softening: Following an examination of the benefits and drawbacks of the softening process in water treatment, the DWPWG concluded that softening would be continued with the targeted plant expansion project.

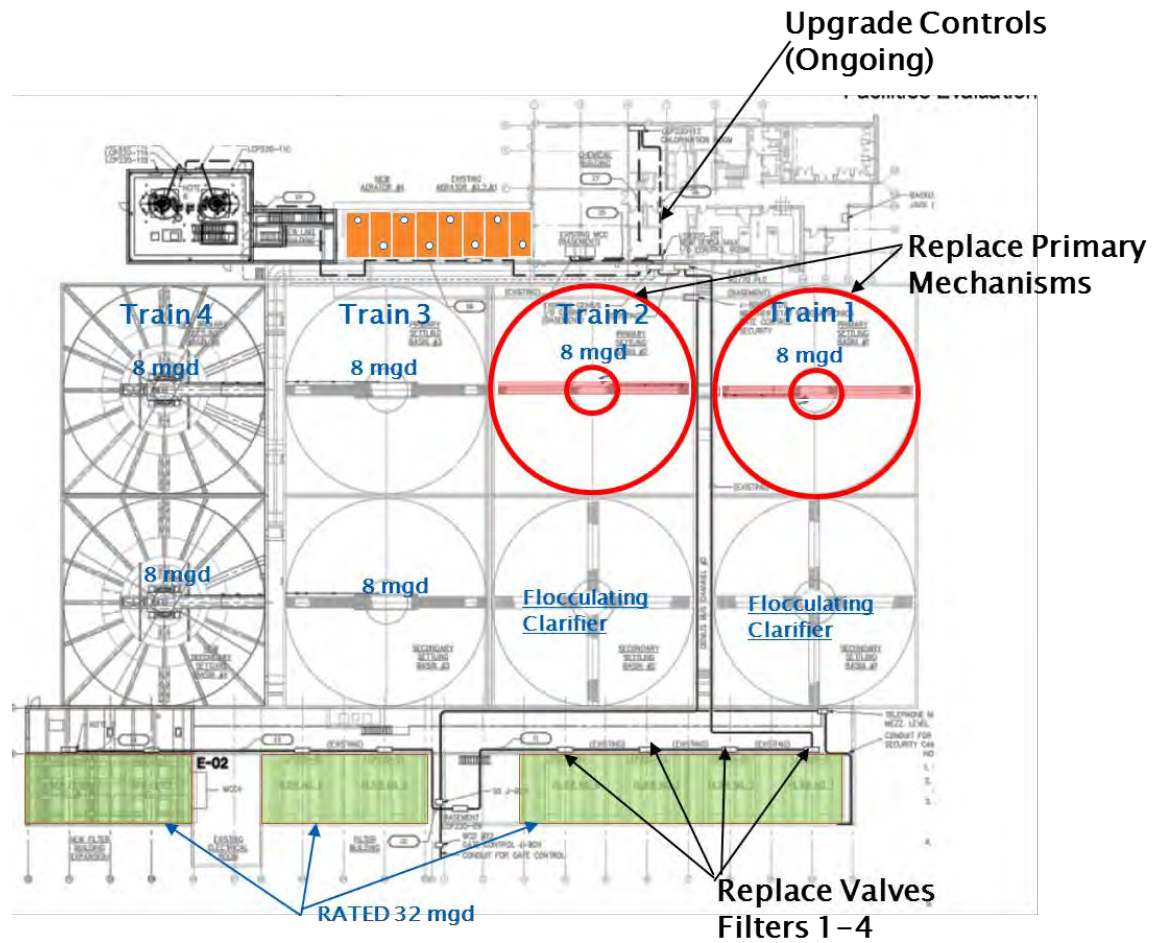


Figure 3 Summary of Capacity Restoration Project as Recommended by 2017 Condition Assessment Report Well Field, McBaine Water Treatment Plant, and West Ash Booster Pump Station

2.6 Regulatory Review and Water Quality Goals

The visioning process included an assessment of the current and anticipated future drinking water regulations. A differentiation was made between the primary drinking water regulations which establish strict compliance levels for certain health related parameters and secondary standards which provide treatment goals for mainly Aesthetic reasons (i.e. taste and odor, salinity, manganese, etc.). From this discussion a tiered water quality goal sheet presented in Table 1 was compiled that provided the following tiered levels of water quality goals:

Groundwater Only: The first tier of water quality goals were related to the current primary and secondary standards achieved by the existing WTP facility.

Groundwater Under the Direct Influence: The next tier of water quality goals were related to achieving compliance with a facility supply source classified by the state as a Groundwater Under the Direct Influence of a Surface Water (GWUDI).

Enhanced WQ Goal: The final tier of water quality goals were related to achieve additional level of treatment not required by the regulations but included levels of treatment to achieve specific water quality goals based upon the results of the survey. This final tier specifically includes the best available technologies to maximize removal of CEC and additional treatment requirements to maintain a free chlorine residual within the distribution system while maintaining water quality goals for disinfection by-products.

Table 1 DWPWG – Summary of Tiered Finished Water Quality Goals

Regulation	Tier 1 Goal Groundwater Only	Tier 2 Goal GWUDI Facility	Tier 3 Goal Enhanced WQ Goal	Regulatory Limit	
				GW	GWUDI
Microbial Removal/Inactivation Performance					
Filter Effluent Turbidity	≤ 1 NTU of 95% of CFE ≤ 5 NTU of CFE	≤ 0.3 NTU for 95% of individual Filter Readings ≤ 1.0 NTU in 100% of individual Filter Readings	≤ 0.1 NTU for 95% of individual Filter Readings ≤ 0.3 NTU in 100% of individual Filter Readings	<u>None</u>	≤ 0.3 NTU for 95% of individual Filter Readings ≤ 1.0 NTU in 100% of individual Filter Readings
<i>Giardia</i> Inactivation	<u>None</u>	≥ 2.5 log removal through filters ≥ 0.5 log inactivation through Disinfection ≥ 3.0 total	<u>None</u>	<u>None</u>	3-log removal/inactivation

Table 1 DWPWG – Summary of Tiered Finished Water Quality Goals (cont.)

Regulation	Tier 1 Goal Groundwater Only	Tier 2 Goal GWUDI Facility	Tier 3 Goal Enhanced WQ Goal	Regulatory Limit	
				GW	GWUDI
Virus Inactivation	4 log removal/inactivation	≥2.0 log removal through filters ≥ 2.0 log inactivation through Disinfection ≥ 4.0 log removal (total)	<u>None</u>	4-log Removal/Inactivation	4 log removal/inactivation
Cryptosporidium Inactivation	<u>None</u>	2-log removal/inactivation	<u>None</u>	none	None- Bin 0
TOC Removal Through Process	None	25% Removal	25% Removal	As necessary to achieve goals	25%
Disinfection By-Products					
TTHM ⁽¹⁾	≤64 µg/L	≤64 µg/L	≤50 µg/L	≤80 µg/L	≤80 µg/L
HAA5 ⁽¹⁾	≤48 µg/L	≤48 µg/L	≤50 µg/L	≤60 µg/L	≤60 µg/L
Total Chlorine	1.2-1.5 mg/L	1.2-1.5 mg/L	< 4.0 mg/L	>0.2 mg/L and < 4.0 mg/L	> 0.2 mg/L and < 4.0 mg/L
Bromate (BrO ₃ ⁻)	≤10 µg/L	≤10 µg/L	≤5 µg/L	≤10 µg/L	≤10 µg/L
Chlorite (ClO ₂ ⁻)	<0.4 mg/L	< 0.4 mg/L	≤1.0 mg/L	≤1.0 mg/L	≤1.0 mg/L
Finished Water Stability					
pH	8.5 to 9.0 S.U.	8.5 to 9.0 S.U.	7.5 to 8.5 S.U.		Sufficient to retain effectiveness of disinfectant and high enough to limit nitrification.
Total Hardness	150 mg/L as CaCO ₃	150 mg/L as CaCO ₃	NA	NA- Internal Goal	NA- Internal Goal

Notes:

- (1) Running annual average of locations selected in accordance with IDSE (typically long duration time) required by Stage II D/DBPR.
- (2) California became the first state in the nation in 2014 to issue a drinking water standard for chrome 6, setting a maximum concentration of 10 parts per billion. However, in August 2017, the State Water Resources Control Board removed the cap in response to a Sacramento judge’s ruling that said the regulation was invalid. Based upon current research, a national standard of 20 ppd is much more likely in the distant future.

The workshops conducted as part of the visioning process included a comprehensive review and discussion of the potential regulations and anticipated impacts (if any) on any potential decisions regarding treatment process. The workshops associated with the visioning portion of the project are provided in Appendix D. The DWPWG provided this tiered approach to aid in evaluating the benefit:cost ratios associated with progressively higher levels of treatment than required by current regulations.

2.7 Treatment Concept Development

Based upon the visioning process, the DWPWG developed a list distinguishing the “must have” with the “may have” for the treatment alternatives development and evaluation. These are presented in Table 2.

Table 2 Summary of Must Haves and May Haves for Treatment Plant Expansion Alternatives

Element	Definition	Components
Must Include	Elements that must be included in the development of the treatment plant expansion alternative that satisfy the Tier 1 water quality goals.	<ol style="list-style-type: none"> Expansion must be performed on existing site. Continued use and expansion of the existing wellfield per the recommendations of the IWRP. Meets all current regulations for a Groundwater Treatment facility. Continue satisfying secondary standard MCLG’s and soften to a finished water hardness of 150 mg/L as CaCO₃.
May Include	Elements that contribute to enhancements of the treatment process to achieve advancement of the process to satisfy one or more of the goals specifically to achieve one or more of the Tier 2 or Tier 3 water quality goals.	<ol style="list-style-type: none"> Allow entire facility (existing and expanded capacity) to satisfy the regulatory requirements of a GWUDI facility. Will enable the City of Columbia to utilize free chlorine as a secondary disinfectant in the distribution system during the entire year.⁽¹⁾ Will include technologies and operational techniques that include the best available control technologies for contaminants of emerging concern (CEC).

Notes:

(1) Currently the city utilizes a periodic “free chlorine burn” to control nitrification within the distribution system. However, this is performed at lower temperatures to ensure compliance with the stage II Disinfection by Product rule.

Figure 4 presents a summary of the concept for examination of treatment alternatives by the DWPWG. The concept is to provide a “base” treatment alternative which, at a minimum, is designed to satisfy all of the “must have” criteria provided in Table 2. Other unit processes or groups of processes would be provided as a “supplement” to provide all or some of the tiered water quality goals associated with the “may have” criteria provided in Table 2.

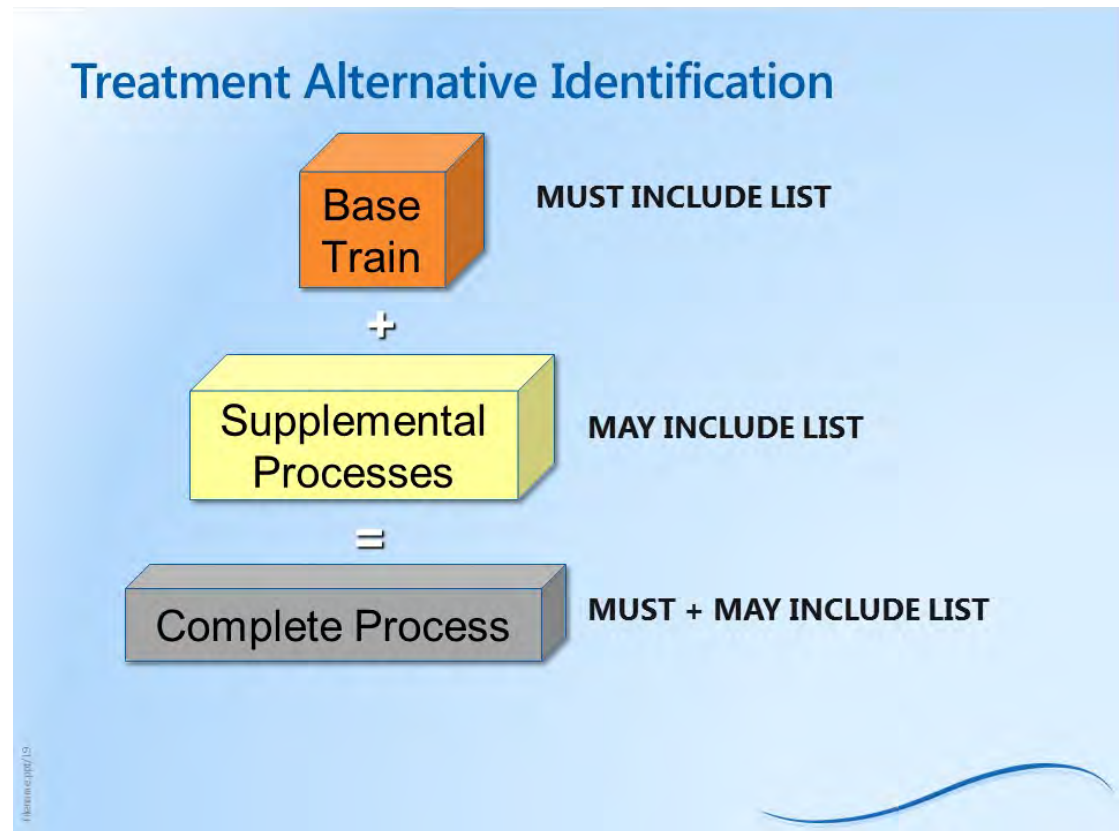


Figure 4 Summary of Treatment Train Alternative Development

2.8 Treatment Train Identification and Fatal Flaw Analysis

Once the boundaries and goals for the treatment process have been established, the final phase of the visioning process is to examine the suite of potential “base” and “alternative” treatment processes that potentially be included as part of a treatment alternative and examine each of these potential processes for a “fatal flaw” that would eliminate this process from further consideration. In this manner, the visioning process can take an almost unlimited combination of treatment alternatives into a shortlist of those that, in the opinion of the DWPWG, are suitable for further examination and evaluation as part of the structured decision analysis approach described in the next section.

2.8.1 Treatment Technology Identification

Figure 5 below summarizes the potential technologies examined for the base and supplemental unit processes for the McBaine WTP. These were grouped based upon the following characteristics:

1. Softening Treatment Technologies: The implementation of these technologies will, among other elements, enable the McBaine WTP to satisfy the base treatment goal of providing a finished water hardness of 150 mg/L. In addition if paired with the appropriate technologies will allow the continued use of the well field and provide treatment that would, at a minimum, satisfy the requirements of a groundwater treatment facility.

2. Filtration Technologies: The implementation of these technologies will enable the McBaine WTP to provide a physical filtration element as part of the base or supplemental alternative. This is particularly important for a facility to meet the requirements of a groundwater under direct influence of a surface water.
3. Oxidation/Disinfection Technologies: The implementation of these technologies either by themselves or as part of another system will provide disinfection and/or oxidation within the treatment process. This becomes increasingly important as the tier levels of water quality increase. The lowest tier, only requires disinfection/oxidation to remove viruses and iron/manganese, respectively. The second tier or GWUDI tier, will require a higher level of disinfection to satisfy these standards. The third tier may require a much stronger level of disinfection/oxidation involving the generation of a hydroxyl radical to provide sufficient oxidation to satisfy the goal of providing a technology that maximizes the reduction of CEC compounds.
4. DBP/DBP Precursor Removal Technologies: The implementation of these technologies either by themselves or in combination with another treatment technologies will provide removal of either disinfection by-products (DBPs) themselves or DBP precursors to provide the enhanced level of treatment required to eliminate the need of chloramines as a secondary disinfectant.

Hardness Removal Technology	
Fatal Flaw	Treatment Technology
	Conventional Softening
	High Rate Softening
	Enhanced Softening
	Softening with Caustic
	Anion Exchange
	Split Treatment
	Nanofiltration/RO
	Pelletized Lime Reactor
	Electromagnetic
	Home POU devices

CEC Removal/Oxidation Technology	
Fatal Flaw	Treatment Technology
	Ferrate
	Free Chlorine
	Chlorine Dioxide
	Ozone or Ozone/Peroxide
	Wet Air Oxidation
	UV/Peroxide
	UV/Titanium Dioxide
	UV/Peracetic Acid
	Permanganate
	Peracetic Acid

Filtration Technology	
Fatal Flaw	Treatment Technology
	Conventional Filtration – Constant Rate
	Ultrafiltration Membranes
	Deep bed filtration – Constant Rate
	Alternative (Slow Sand Diatomaceous Earth)
	MnO2 Coated Media Filtration
	Manganese Greensand
	Nanofiltration/RO
	Cartridge Filtration
	Declining Rate Filtration

DBP Precursor Removal Technology	
Fatal Flaw	Treatment Technology
	GAC Filter Contactors
	PAC Contactors (Actiflow CARBtm)
	Post Filter GAC Contactors
	NanoFiltration/RO
	Enhanced Coagulation
	Ozone Biofiltration
	Chlorine Dose Control
	Anion Exchange Beds
	Chloramination (w/ Nitrification Action Plan)
	MIEX (magnetic Ion Exchange)
	Air Stripping
	Electrodialysis

Figure 5 Potential Treatment Technologies Identified for Fatal Flaw Analysis

2.8.2 Fatal Flaw Analysis

The final step in the visioning process is to select for a group of technologies that have a high potential of being incorporated as part of the “Base” or “Base+Supplemental” treatment alternatives. The selection is based upon a “fatal flaw” analysis to eliminate the process or processes that possess one or more of these fatal flaws.

Table 3 presents a summary of the fatal flaws applied to the treatment technologies.

Table 3 Summary of Fatal Flaws

Fatal Flaw	Description	Comment
Scale	Technology has never been constructed at this scale. This can either be measured by mgd or by another parameter such as ppd or other capacity element.	Historically there have been significant issues with trying to apply a higher scale for some treatment technologies.
Inappropriate Technology	Technology will not be capable of achieving the goals either by itself or as part of a treatment ensemble.	
Extremely Inflated Costs	Technology is appropriate and can achieve goals but because of specific conditions (geographical, energy costs, operational costs, etc.) the costs to install, operate and maintain can be magnitudes higher than other technologies.	Because of antidegradation issues with the Missouri River and the inability to locate a diffuser in the river, disposal of reject becomes an issue with RO systems.
Not Acceptable to the Community	This relates to the acceptance of the technologies by the community. For example, there are some communities that have taken the stance that anything that contributes significantly to increasing the carbon footprint of the utility will not be allowed.	The DWPWG was expected to provide guidance during the fatal flaw analysis.

Figure 6 below presents a summary of the fatal flaw analysis for the softening processes to be evaluated as part of the “base” treatment train. It evaluating this it was understood that these were to be incorporated or integrated as part of the existing infrastructure at the treatment facility and that that infrastructure was modified to the extent recommended by the 2017 Condition Assessment Report.

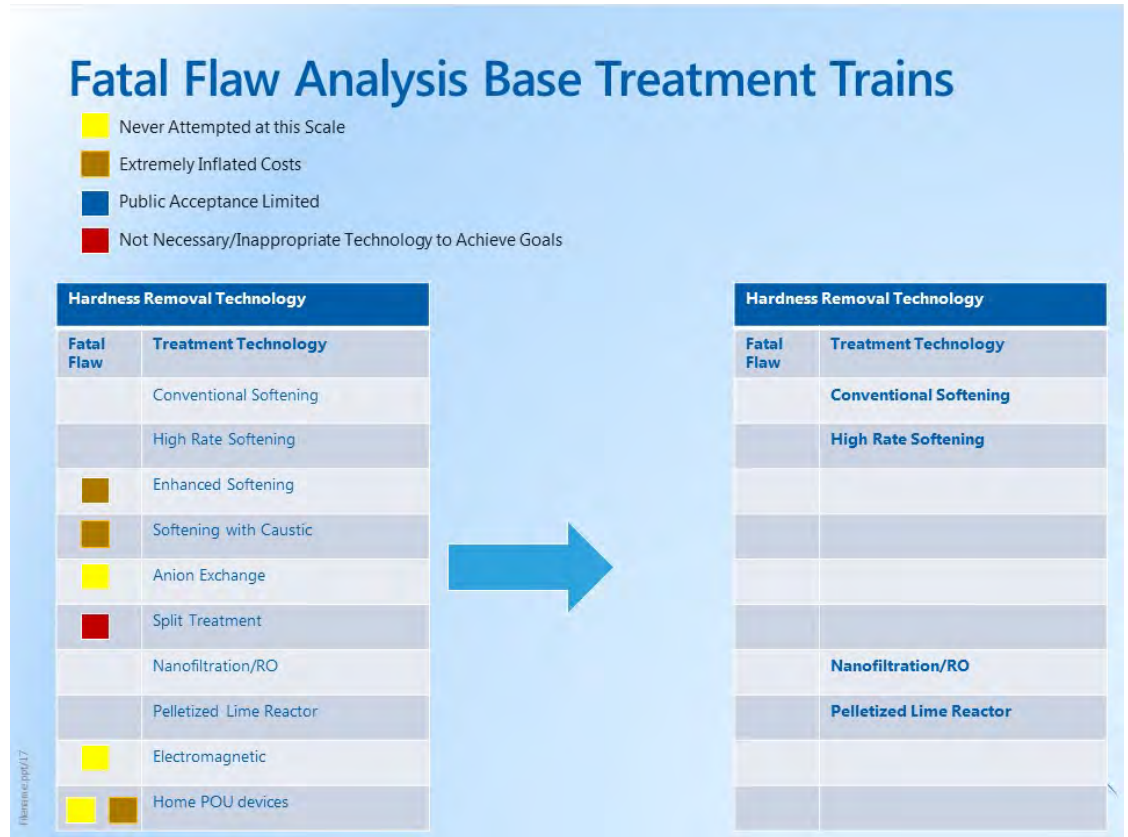


Figure 6 Fatal Flaw Analysis – Hardness Removal Technologies

Figure 7 presents the fatal flaw analysis for the filtration technologies to be employed as part of the base or as part of an advanced treatment technology. Normally, in these cases it would be appropriate to eliminate reverse osmosis because of its typically high cost. However, because reverse osmosis (RO) offers potential significant benefits to all of the tiered water supply goals, it will be evaluated further as a base alternative.

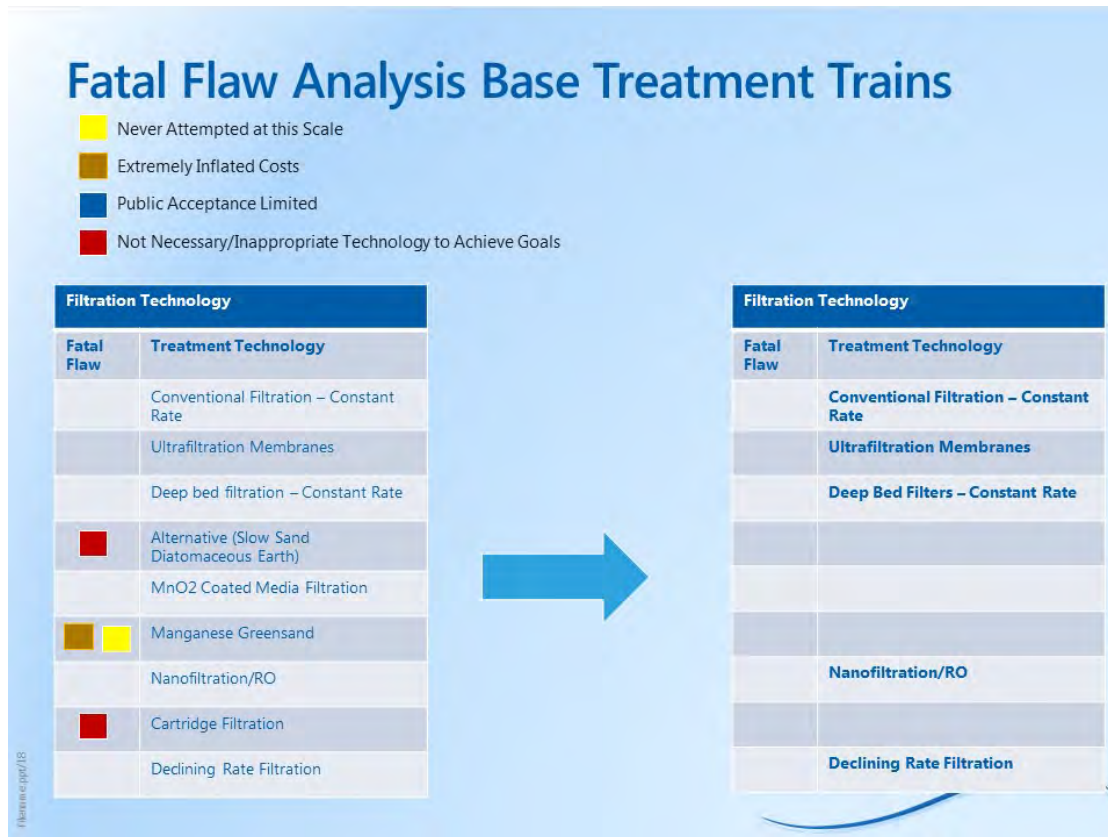


Figure 7 Fatal Flaw Analysis – Filtration Technologies

Figure 8 presents the fatal flaw analysis of the advanced oxidation and disinfection technologies. The technologies were selected based upon historical performance as part of a multi-barrier process involving oxidation to form hydroxyl radicals followed by biofiltration commonly employed in drinking water for disinfection and oxidation, as in the case of ozone or ultraviolet (UV); or advanced oxidation processes (UV peroxide) employed in wastewater reuse applications specifically for the reduction of contaminants of emerging concern.

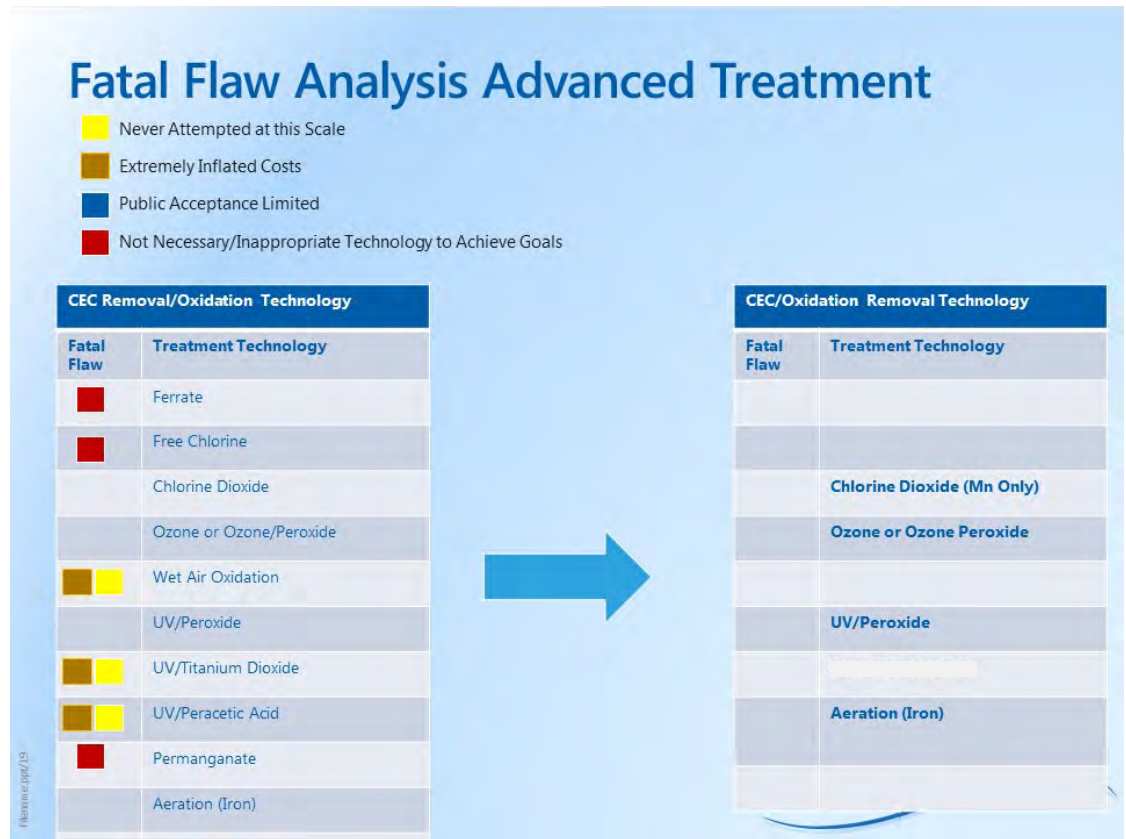


Figure 8 Fatal Flaw Analysis – CEC Removal/Oxidation Technologies

Figure 9 provides a summary of the fatal flaw analysis for the DBP/DBP by-product precursor removal technologies for the advanced treatment processes as part of the supplemental treatment process. These have been shortlisted to technologies and processes commonly employed in the drinking water field to reduce the potential for disinfection by product formation when using free chlorine by removing the precursors that react to form disinfection byproducts (total organic carbon) due to the nature of the disinfection by products formed, it was found during the previous studies that removal of disinfection by-products after formation by physical unit processes (such as air stripping) were impractical because some of the compounds formed required a sufficiently high number of aerators that it became too costly to employ with in the distribution system.

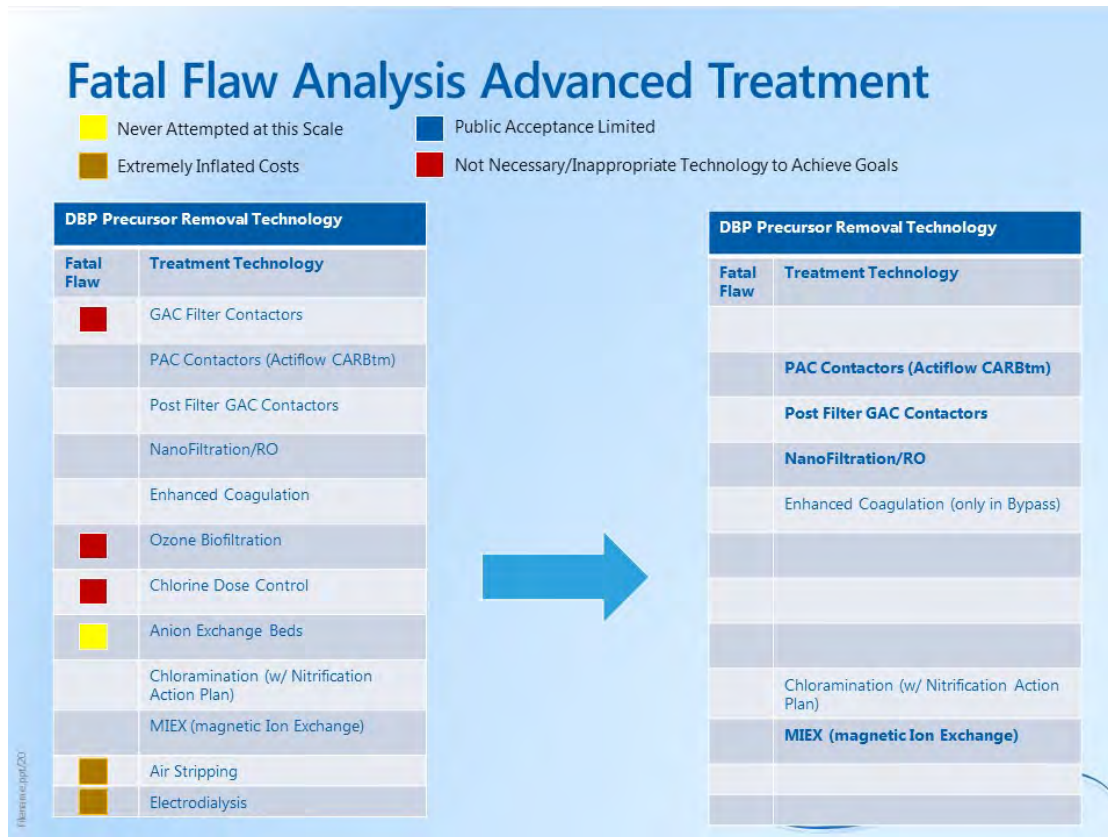


Figure 9 Fatal Flaw Analysis – DBP/DBP precursor Removal Technologies

The development of a shortlist of treatment technologies within the framework of the established boundaries completed the visioning phase of the DWPWG process. The next phase involves the assembly of viable alternatives that includes a base treatment process with and without the supplemental processes to achieve a particular tiered water quality goal and the incorporation of the structured decision analysis process to shortlist, analyze, and select the recommended treatment alternative from this suite of viable alternatives.

Section 3

ALTERNATIVE EVALUATION

3.1 Purpose

The purpose of the evaluation phase of the project was to establish a shortlisted set of viable base and supplemental alternatives that could be evaluated in additional detail. This included the following:

- Establish a set of viable base and supplemental alternatives.
- Screen the alternatives using a level 5 cost estimate.
- Select criteria that will be used to evaluate the alternatives.
- Establish weighting of the criteria and assign scores for each alternative.
- Rank the alternatives with respect to the criteria weighting and scoring and establish a shortlist of alternatives for further evaluation.

3.2 Meetings and Workshops

The following public meetings were held during the evaluation phase of the project:

- Criteria Selection Workshop –October 11, 2017.
- Pairwise Comparison and Ranking Workshop I –November 13, 2017.
- Pairwise Comparison and Ranking Workshop II –January 8, 2018.

A summary of the workshop materials are provided in Appendix E.

3.3 Establish Viable Set of Treatment (Base and Supplemental) Alternatives

3.3.1 Establish Potential Combination of Base and Supplemental Alternatives to Achieve Treatment Goals

At the completion of the visioning process, the boundaries of the investigations were established and potentially viable Treatment Technologies were identified following a fatal flaw analysis. The next step in the process employed by the DWPWG was to assemble a viable set of base and supplemental alternatives from these treatment technologies. As previously discussed these would consist of a base treatment alternative that accomplished, at a minimum the first tier of water quality goals with supplemental alternatives that would permit achievement of all or some of the advanced tier water quality goals. Table 4 provides a summary of the preliminary alternatives assembled for the “base and Supplemental” treatment technologies established from the visioning process.

Table 4 Summary of Preliminary Alternatives

Tier 1 Water Quality Goals: Base Alternatives	Tier 2 – GWUDI Compliance	Tier 3 Water Quality Goals	
		DBP Control	CEC Removal
B1.1 - Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○ Add S2.1, S2.2, S2.3, or S2.4	○ Add S3.1, or S3.2
B1.2 - Expand Existing Plant w/Conventional Softening (New 15 mgd Filter Train)	○ Add S1.1	○ Add S2.1, S2.2, S2.3, or S2.4	○ Add S3.1, or S3.2
B2 - New 15 mgd Treatment Train	○ Add S1.1	○ Add S2.1, S2.2, S2.3, or S2.4	○ Add S3.1, or S3.2
B3 - Replace Filters w/UF Membranes	●	○ Add S2.1, S2.2, S2.3, or S2.4	○ Add S3.1, or S3.2
B4 - Replace Plant w/RO Facility	●	● Add S2.1, S2.2, S2.3, or S2.4	● Add S3.1, or S3.2
B5 - Replace Conventional Softening w/Pellet Softening	●	○ Add S2.1, S2.2, S2.3, or S2.4	○ Add S3.1, or S3.2

Key:

- Yes ● Partial ○ No
- S1.1 - Expansion to GWUDI
- S2.1 - Granular Activated Carbon (GAC)
- S2.2 - Magnetic Ion Exchange (MIEX)
- S2.3 - Actiflo™ CARB
- S2.4 - Ozone/Biofiltration
- S3.1 - UV Disinfection/Peroxide
- S3.2 - Ozone/Biofiltration

3.3.2 Screen Base Alternatives

Table 5 presents the cost classification system as applied in Engineering, Procurement, and construction for the Process Industries as developed by the American Association of Cost Estimators (AACE). To conduct further screening of these alternatives, level 5 cost estimates were prepared of each of the alternatives to determine if the anticipated cost range of one or more of these alternatives was substantially higher.

Table 5 AACE Cost Classification System

Estimate Class	Primary Characteristic	Secondary Characteristic		
	Maturity Level of Project Definition Deliverables (as % of definition)	End Usage – Typical Purpose of Estimate	Methodology – Typical Estimating Method	Expected Range of Accuracy Typical variation in low to high
Class 5	0% to 2%	Concept Screening	Capacity factored Parametric models Judgement or analogy	L: -20% to +50% H: +30% to +100%
Class 4	1% to 15%	Study or Feasibility	Equipment factored Parametric models	L: -15% to +30% H: +20% to +50%
Class 3	10% to 40%	Budget Authorization or Control	Semi-detailed unit costs with assembly level line items	L: -10% to -20% H: +10% to +30%
Class 2	30% to 70%	Control or bid/tender	Detailed unit costs with forced detail take-off	L: -5% to -15% H: +5% to +20%
Class 1	65% to 100%	Check estimate or bid/tender	Detailed unit costs with detailed take-off	L: -3% to -10% H: +3% to +15%

Notes:

(1) Taken from 18R-97 Cost Estimate Classification System Published by AACE.

Based upon the comparison of the level 5 estimates for the capital and life cycle costs associated with each of the base alternatives, the following conclusions were made:

1. Eliminate Base Alternative B4 Replace Plant with RO facility: This alternative was eliminated due to a higher capital and life cycle cost of the alternative with respect to other combination of base and supplemental alternatives that accomplished the same water quality goals.
2. Eliminate Base Alternative B5 Pellet Softeners: this alternative was eliminated due to a higher life cycle cost of the alternative with respect to other base alternatives that accomplished the same water quality goals.

3.3.3 Screen Supplemental Alternatives

Similar to the base alternatives, the supplemental alternatives were screened for excessive costs (capital and/or life cycle) using a level 5 estimate. The conclusions of this screening process were as follows:

1. Eliminate Supplemental Alternative S2.2 (MIEX Carb) from consideration due to high operating costs (higher life cycle) than other viable DBP precursor removal technologies. Bench scale testing indicating an extremely low amount of bed volumes (number of volumes processed before resin becomes ineffective) leading to high operating costs due to resin loss during regeneration.

2. Eliminate Supplemental Alternative S2.4: An advanced oxidation process (ozone, Ozone peroxide, UV-peroxide, etc.) followed by biofiltration as a means to reduced disinfection by product precursors as results from other installations indicate this will not be sufficient to reduce disinfection by product precursors to allow complete use of free chlorine as a disinfectant in the distribution system. These options will remain, however, due to excellent ability to reduce CEC compounds.
3. Eliminate Supplemental Alternative S3.1 UV Disinfection: This alternative was eliminated due to the high costs of maintaining UV disinfection systems employing advanced oxidation facility downstream of a softening process.

Table 6 below presents a summary of the remaining viable alternatives following the preliminary screening process.

Table 6 Summary of Remaining Viable Alternatives Following Initial Screening Using AACE Level 5 Cost Estimates

Tier 1 Water Quality Goals: Base Alternatives	Tier 2 – GWUDI Compliance	Tier 3 Water Quality Goals	
		DBP Control	CEC Removal
B1.1 - Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○ Add S2.1, S2.2 , S2.3, or S2.4	○ Add S3.1 , or S3.2
B1.2 - Expand Existing Plant w/Conventional Softening (New 15 mgd Filter Train)	○ Add S1.1	○ Add S2.1, S2.2 , S2.3 , or S2.4	○ Add S3.1 , or S3.2
B2 - New 15 mgd Treatment Train	○ Add S1.1	○ Add S2.1, S2.2 , S2.3 , or S2.4	○ Add S3.1 , or S3.2
B3 - Replace Filters w/UF Membranes	●	○ Add S2.1, S2.2 , S2.3, or S2.4	○ Add S3.1 , or S3.2
B4 - Replace Plant w/RO Facility	●	○ Add S2.1, S2.2, S2.3, or S2.4	○ Add S3.1, or S3.2
B5 - Replace Conventional Softening w/Pellet Softening	●	○ Add S2.1, S2.2, S2.3, or S2.4	○ Add S3.1, or S3.2

Key:

- Yes ○ Partial ○ No
- S1.1 - Expansion to GWUDI
- S2.1 - Granular Activated Carbon (GAC)
- ~~➤ S2.2 - Magnetic Ion Exchange (MIEX)~~
- S2.3 - Actiflo™ CARB
- ~~➤ S2.4 - Ozone/Biofiltration~~
- ~~➤ S3.1 - UV Disinfection/Peroxide~~
- S3.2 - Ozone/Biofiltration

3.4 Evaluation Criteria

The Criteria Selection Workshop was held with the DWPWG on October 11, 2017. As part of this workshop, potential evaluation criteria and sub-criteria for the various alternatives were presented and discussed. In addition, the Structured Decision Analysis process was presented.

3.4.1 Structured Decision Analysis

The Structured Decision Analysis (SDA) that was used for the evaluation process is an effective way of making an informed decision for a complex problem. The primary benefit of using SDA is that it's designed to deal explicitly with uncertainty, and responding transparently to public preferences or values in the decision making process. This process can be divided into three simple phases each containing helpful steps for problem solving as seen below:

- Structured Decision Analysis - Phase I:
 - Define the decision makers and a simple and clear decision statement.
 - Define a potential set of viable alternatives.
 - Select the criteria that will be used to differentiate the alternatives.
 - Assign weights to the criteria and assure there is no redundancy nor 'must haves' (pass/fail criteria).
- Structured Decision Analysis - Phase II:
 - Score each alternative against each criterion (without "weight").
 - Identify 'data gaps' or 'knowledge gaps' as a part of the scoring.
 - Fill 'data and knowledge gaps'.
 - Combine the scores and weights to rank the alternatives.
- Structured Decision Analysis - Phase III:
 - Complete final ranking of each alternative.
 - Select 'best' alternative.
 - Test sensitivity of 'best' (the gut check analysis).
 - Assign the 'devil's advocate' to assure a robust decision.

In general, the SDA model receives input from the group making the decisions (DWPWG) regarding the selection and weighting of criterion. Each alternative is then scored against the criterion. The scores and weights are then combined to develop a ranking of the alternatives. This concept is illustrated in Figure 10.

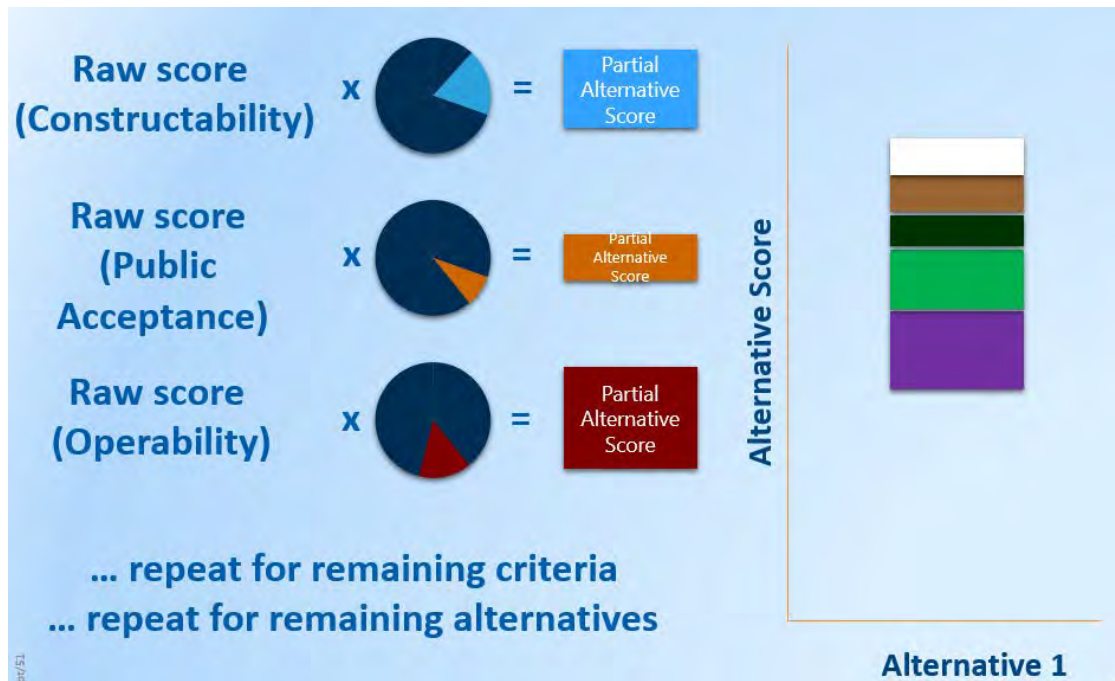


Figure 10 Alternative Weighted Scoring Process

Following the ranking of alternatives, the model can then be used to test the sensitivity of the top alternatives. Criteria weightings that were previously determined can be adjusted to determine their effect on the alternative. This concept is illustrated in Figure 11. It can be seen, that as the importance of operation and maintenance costs is adjusted, the top alternative can change.

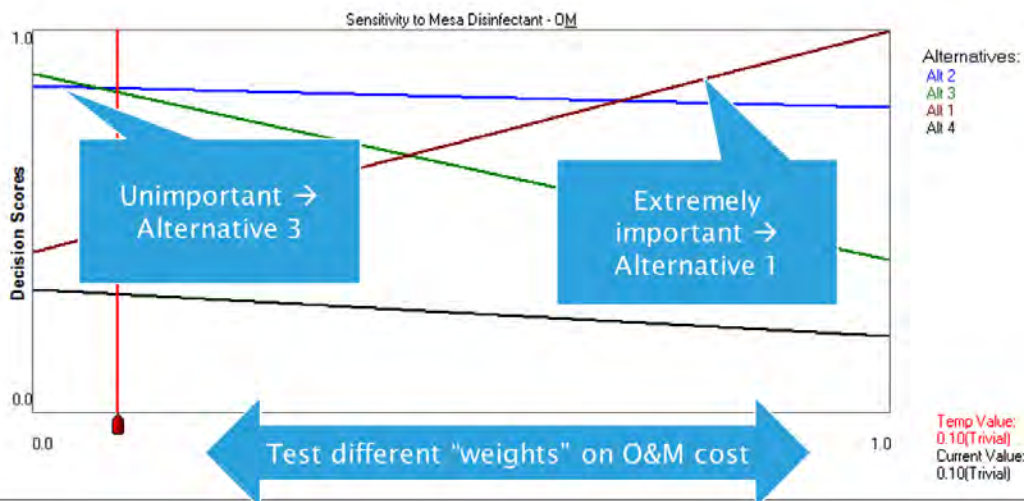


Figure 11 Sensitivity Analysis Example

3.4.2 Criteria Selection and Ranking

During the Criteria Selection Workshop, the DWPWG identified the criteria from which to base the alternatives screening process. Following this, the criteria were grouped into primary criteria and sub-criteria. The primary criteria that were agreed upon included constructability, water quality, operability, project cost, and GWUDI facility.

The relative importance of each primary criterion was determined by pair-wise comparison by the DWPWG members. Sixteen sub-criteria were identified and grouped with one of the five primary criteria by the DWPWG members. The relative importance of the sub-criteria associated with each primary criterion was similarly determined by pair-wise comparison by each of the DWPWG members and submitted to Carollo for analysis. A summary of the submitted criteria evaluation forms is provided in Figure 12.

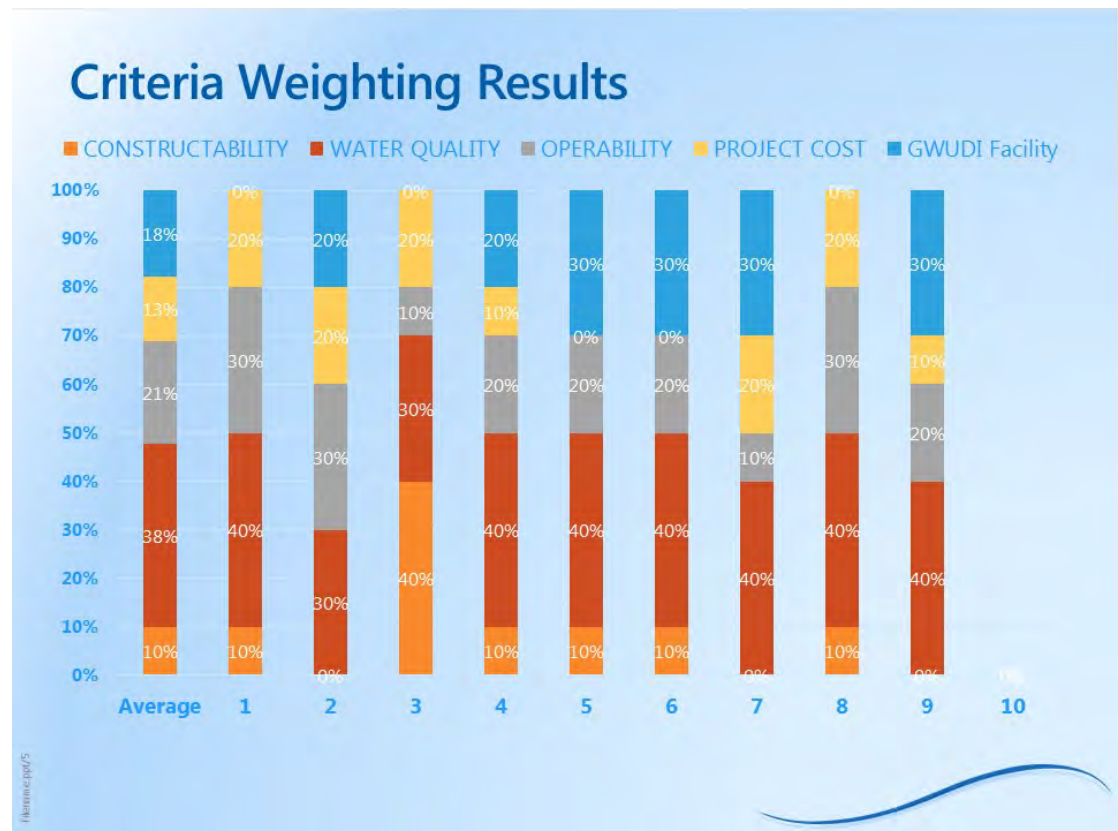


Figure 12 Summary of Pairwise Comparison from DWPWG Worksheets

Criterion Decision Plus (CDP) was used to facilitate assigning a numerical weighting (percent contribution to the total decision) to each primary and sub-criteria based on the results of the pair-wise comparisons. The ultimate numerical weighting assigned to each primary and sub-criteria was defined through an iterative process of reviewing and refining the relative weighting of each criteria. The resultant criteria, sub criteria, and associated weighting are detailed in Table 7. Water quality goals for total trihalomethanes (TTHMs) was the largest contributor to the decision with sustainability and water quality goals for CECs also determined to be significant factors.

Table 7 Summary of Primary and Sub-Criteria Ranking

0.10	Constructability
0.043	Maintain Plant Operations
0.006	Schedule
0.028	Space Requirements
0.024	Permitting
0.38E	Water Quality
E	Water Quality Goals - TTHMs
0.098	Sustainability
0.105	Water Quality Goals - CECs
0.000	Communication
0.21	Operability
0.028	Residuals Production
0.040	Staffing Requirements
0.056	Proven Technology
0.028	Maintenance Complexity
0.059	Source Water Quality
0.13	Project Cost
0.022	Capital Cost
0.052	Operational Cost
0.037	Maintenance Cost
0.022	Life Cycle Cost
0.18	GWUDI Facility

3.4.3 Establish Criteria Scores:

Table 8 details the primary and sub-criteria used to screen alternatives. It also summarizes the associated goal/measurement and scale applied for scoring of alternatives based on each sub-criteria. A scale range of 0-5 was used in all cases, including intermediate values of 1, 2, 3, and 4. Table 8 also details the rationale associated with establishing the upper boundary (i.e., score of 5) and the lower boundary (i.e., score of 0) for each sub-criteria. Intermediate scores were assigned by relative comparison of each sub-criteria amongst alternatives. The sub-criteria scores were then multiplied by their associated weighting and totaled to result in a total score for each alternative for direct comparison.

Table 8 Evaluation Sub-Criterion for McBaine WTP Expansion

Primary Criteria	Sub-Criteria	Goal/Measurement	Scale Range
Constructability	Maintain Plant Operations	Plant must be able to produce finished water during construction activities.	0 - Unable to phase process with multiple plant shutdowns. 5 - Many options for phasing process alternative with minimal disruption to existing plant operations.
	Schedule	Construction duration in months, shorter duration is desired.	0 - Very long construction period. 5 - Short construction period.
	Space Requirements	Square feet, Smaller footprint is better.	0 - Largest footprint required to accommodate WTP structures (not including residuals handling). 5 - Smallest footprint required to accommodate WTP structures (not including residuals handling).
	Permitting	Number of permits required and difficulty to obtain.	0 - Numerous permits needed requiring significant involvement from multiple stakeholders. 5 - Minimal permitting requirements with limited stakeholder involvement.
Water Quality	Water Quality Goals - TTHMs	A process that can remove TTHMs and other DBPs.	0 - No removal of TTHMs or DBPs. 5 - Highest removal of TTHMs and DBPs based upon Best Available Control Technology.
	Sustainability	Minimize carbon footprint. Minimize chemical usage. Maximize energy efficiency. Opportunities for reuse.	0 - Process is not energy efficient and uses large quantities of chemicals for treatment. No opportunities for reusing waste materials. 5 - Process is efficient and uses small quantities of chemicals, uses less energy, and offers opportunities for reusing waste materials.
	Water Quality Goals - CECs	A process that can remove CECs.	0 - No removal of CECs. 5 - Highest removal of CECs based upon Best Available Control Technology.
	Communication	A process that is easily communicated to and accepted by the public and the decision makers is good.	0 - Process alternative is difficult to demonstrate to stakeholders and is difficult to obtain stakeholder and general public buy-in. 5 - Process alternative is easy to explain and widely acceptable to stakeholders and general public.

Table 8 Evaluation Sub-Criterion for McBaine WTP Expansion (cont.)

Primary Criteria	Sub-Criteria	Goal/Measurement	Scale Range
Operability	Residuals Production	Tons per year. Smaller quantities of residuals are desired.	0 - High residuals production. 5 - Low residuals production.
	Staffing Requirements	Alternatives that do not require intensive training and large numbers of operators are desirable.	0 - Extensive training is required and the process requires several operators at any given time. 5 - Training requirements are less complicated and fewer operators are required to operate the process.
	Proven Technology	Alternatives including processes with a proven track record score higher than newer, less proven technologies.	0 - No full-scale installations. 5 - Extensive full-scale experience both in number of installations and number of years in service.
	Maintenance Complexity	Mechanical Intensity. Alternatives with more processes and/or a higher degree of sophistication are less desirable.	0 - Numerous processes with extensive short- and long-term maintenance needs. 5 - Fewer processes with low level of sophistication resulting in easier maintenance.
	Source Water Quality	Alternatives include processes that can handle large variability in source water quality without impact to finished water quality is good.	0 - Many processes sensitive to water quality changes requiring frequent operator intervention. 5 - Fewer processes sensitive to water quality changes requiring less operator intervention.

Table 8 Evaluation Sub-Criterion for McBaine WTP Expansion (cont.)

Primary Criteria	Sub-Criteria	Goal/Measurement	Scale Range
Project Cost	Capital Cost	Initial capital investment necessary to design, procure, construct, and place into successful working operation improvements or process modifications recommended by a particular alternative.	0 – Highest Capital Cost (H) 5 – lowest Capital Cost (L) Other costs (A) will be calculated: $A=(10-0)*(H-A)/(H-L)$
	Operational Cost	The operational costs over the anticipated life cycle of the process equipment recommended including labor and consumables presented in an annualized basis for assessing impact on rates.	0 – Highest Annual Operational Cost (H) 5 – lowest Operational Cost (L) Other costs (A) will be calculated: $A=(10-0)*(H-A)/(H-L)$
	Maintenance Cost	The maintenance costs over the anticipated life cycle of the process equipment recommended including labor and consumables (oil, grease, etc.) presented in an annualized basis for assessing impact on rates.	0 – Highest Annual Maintenance Cost (H) 5 – Lowest Maintenance Cost (L) Other costs (A) will be calculated: $A=(10-0)*(H-A)/(H-L)$
	Life Cycle Cost	The total present worth costs representing a summary of the initial capital costs, annualized maintenance costs, and annualized operational costs over a 20 year period presented in “today’s dollars” using a discount rate reflective of the time value of money.	0 – Highest Life Cycle Cost (H) 5 – Lowest Life Cycle Cost (L) Other costs (A) will be calculated: $A=(10-0)*(H-A)/(H-L)$
GWUDI Facility	The assessment of the capability of the facility to maintain full compliance with the water quality goals and regulations associated with a source water classified by the state as a “Groundwater Under the Direct Influence of Surface Water.”	0 – Significant capital and operational/maintenance investment will be required to enable GWUDI compliance. 3 - Relatively minor capital investments (i.e. tweaks in process arrangement) will be required for GWUDI compliance. 4 – Minor operational changes will be required for GWUDI compliance. 5- Facilities are fully compliant with GWUDI regulations and water quality goals associated with at GWUDI facility.	

3.4.4 Further Screening Utilizing CDP Software – Base Alternatives

Similar to the original 2012 PDR, CDP software was used to perform the ranking and evaluation of the preliminary alternatives. Each of the remaining base alternatives were further screened with respect to the other base alternatives with respect to the established weighted criteria. Figure 13 presents a summary of the results of the preliminary screening of the base alternatives with respect to the weighted criteria using the CDP platform.

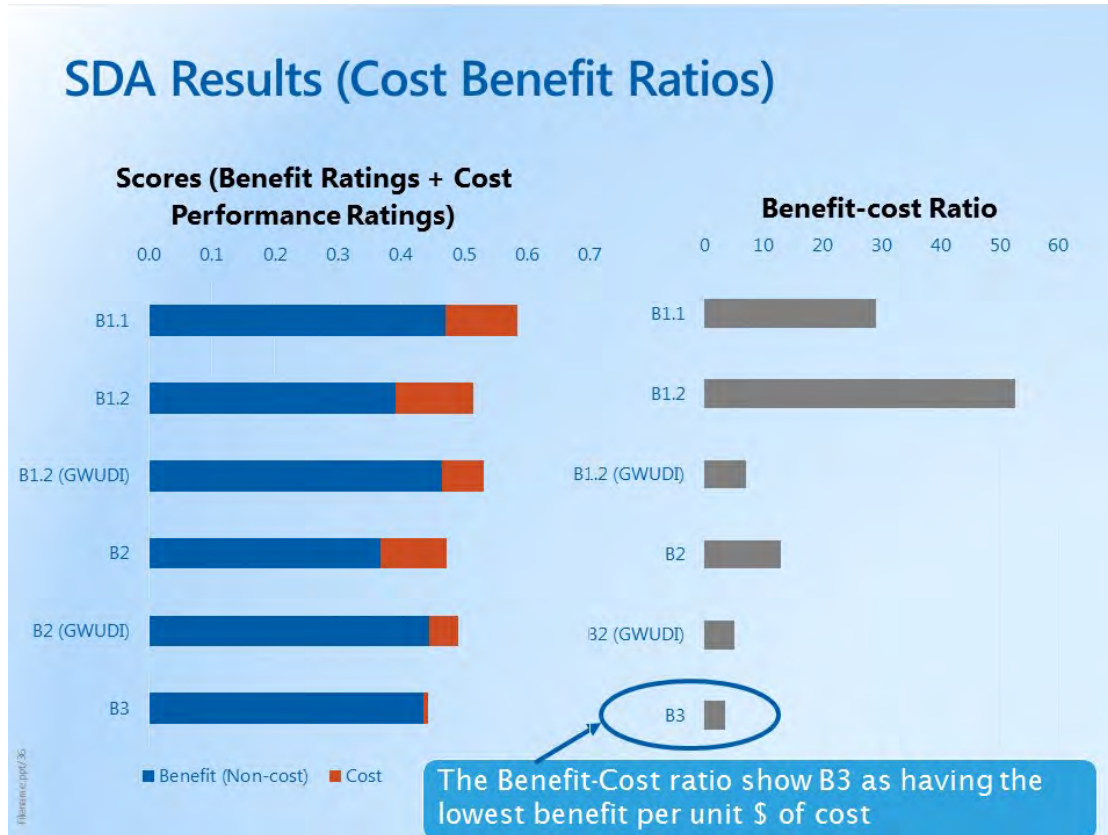


Figure 13 Summary of Base Alternative Evaluation – CDP Analysis

Figure 13 illustrates the low benefit: cost ratio of alternative B3- Ultrafiltration Membranes based upon the evaluation criteria and level 5 cost estimates. Further sensitivity analysis indicated the robustness of the evaluation and the decision to exclude Alternative B3 from further evaluation.

Table 9 presents the updated summary of viable alternatives based upon the results of the screening of the alternatives.

Table 9 Summary of Remaining Viable Alternatives Following Final Screening Using CDP Model

Tier 1 Water Quality Goals: Base Alternatives	Tier 2 – GWUDI Compliance	Tier 3 Water Quality Goals	
		DBP Control	CEC Removal
B1.1 - Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○ Add S2.1, S2.2 , S2.3, or S2.4	○ Add S3.1 , or S3.2
B1.2 - Expand Existing Plant w/Conventional Softening (New 15 mgd Filter Train)	○ Add S1.1	○ Add S2.1, S2.2 , S2.3, or S2.4	○ Add S3.1 , or S3.2
B2 - New 15 mgd Treatment Train	○ Add S1.1	○ Add S2.1, S2.2 , S2.3, or S2.4	○ Add S3.1 , or S3.2
B3 - Replace Filters w/UF Membranes	●	⊖ Add S2.1, S2.2, S2.3, or S2.4	⊖ Add S3.1, or S3.2
B4 - Replace Plant w/RO Facility	●	● Add S2.1, S2.2, S2.3, or S2.4	● Add S3.1, or S3.2
B5 - Replace Conventional Softening w/Pellet Softening	●	⊖ Add S2.1, S2.2, S2.3, or S2.4	⊖ Add S3.1, or S3.2

Key:

- Yes ○ Partial ○ No
- S1.1 - Expansion to GWUDI
- S2.1 - Granular Activated Carbon (GAC)
- ~~➤ S2.2 - Magnetic Ion Exchange (MIEX)~~
- S2.3 - Actiflo™ CARB
- ~~➤ S2.4 - Ozone/Biofiltration~~
- ~~➤ S3.1 - UV Disinfection/Peroxide~~
- S3.2 - Ozone/Biofiltration

Figure 14 presents a summary of the treatment alternatives considered for detailed ranking and evaluation using the CDP model.

Treatment Alternatives

Base	Supplement	Description	Comments
B1.1	No Supplement	Only Upgrade Existing	GWUDI Compliant, Requires Chloramines
B1.1	S2.1	Upgrade Existing With GAC Contactors	GWUDI Compliant Permits use of Free Chlorine
B1.1	S2.1, S3.2	Upgrade Existing with Ozone/BAF and GAC Contactors	GWUDI Compliant Permits use of Free Chlorine
B1.2	No Supplement	New Filters (15mgd)	Not fully GWUDI Compliant Requires Chloramines
B1.2	S1.1	New Filters (15 mgd) with plant upgraded	GWUDI Compliant Requires Chloramines
B1.2	S1.1, S2.1	New Filters (15 mgd) with GAC Contactors	GWUDI Compliant Permits use of Free Chlorine
B1.2	S1.1, S2.1, S3.2	New Filter (15 mgdd) with Ozone/BAF and GAC Contactors	GWUDI Compliant Permits use of Free Chlorine Adds CEC's
B2	No Supplement	New Treatment Train (15 mgd)	Not fully GWUDI Compliant Requires Chloramines
B2	S1.1	New Treatment Train (15 mgd) with plant upgraded.	GWUDI Compliant Requires Chloramines
B2	S1.1, S.2.1	New Treatment Train (15 mgd) and GAC Contactors	GWUDI Compliant Permits use of Free Chlorine
B2	S1.1, S2.1, S3.2	New Treatment Train (15 mgd) with Ozone/BAF and GAC Contactors	GWUDI Compliant Permits use of Free Chlorine Adds CEC's

Figure 14 Summary of Preliminary Alternatives

3.5 Ranking of Preliminary Alternatives

Similar to the original 2012 PDR, CDP software was used to perform the ranking and evaluation of the preliminary alternatives. Figure 15 presents a summary of the rankings that were established with respect to the non-economic and economic criterion previously indicated. The relative weight of each criterion is represented by a particular color band within the total band for each alternative. The higher the value, the stronger that particular alternative satisfies the criteria. The alternatives that best satisfy the relatively ranked criteria are represented with the highest overall bands.

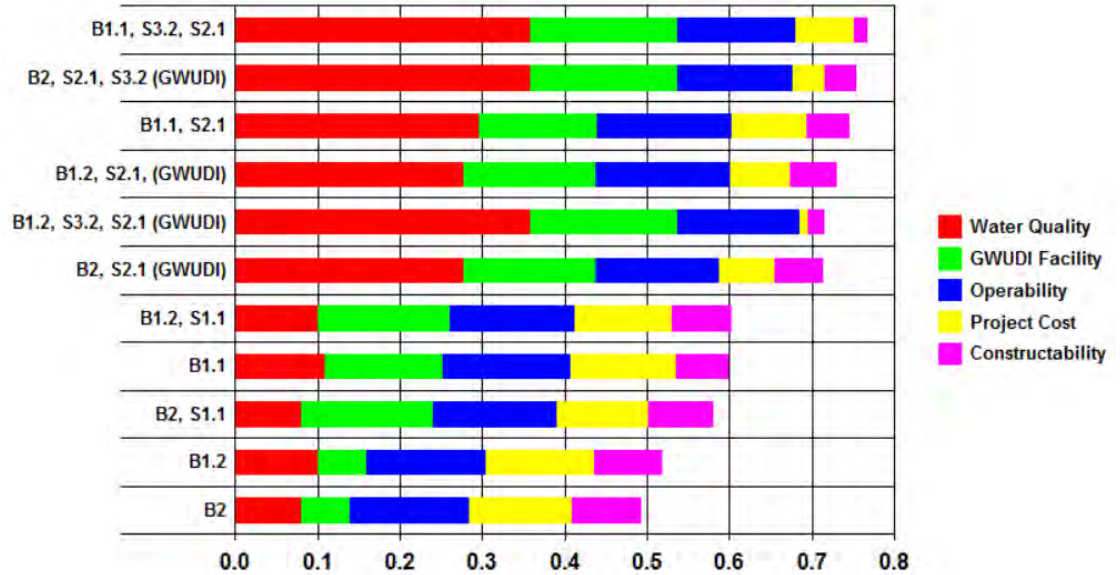


Figure 15 Results of Preliminary Alternatives Screening

On January 8, 2018, the Pairwise Comparison and Preliminary Ranking Workshop was held to discuss the results of the preliminary screening process and to develop a shortlisted set of alternatives. It can be noted from Figure 15, that because of the high weight given to Water Quality and GWUDI, it was the higher cost alternatives that scored highest and provided the most benefit. Based on the results, the team decided to eliminate the two alternatives that didn't include a GWUDI compliant facility (B1.2 and B2). In addition, it was decided to eliminate Alternative B1.2, S3.2, S2.1, S1.1 (GWUDI) due to the moderate overall score, low constructability rating, and high cost.

Further analysis of the alternatives was done by compiling the benefit/cost ratios for each alternative. This analysis indicated that some alternatives offered little additional benefit at high incremental costs. A summary of the overall ratings and benefit/cost ratios is presented in Figure 16.

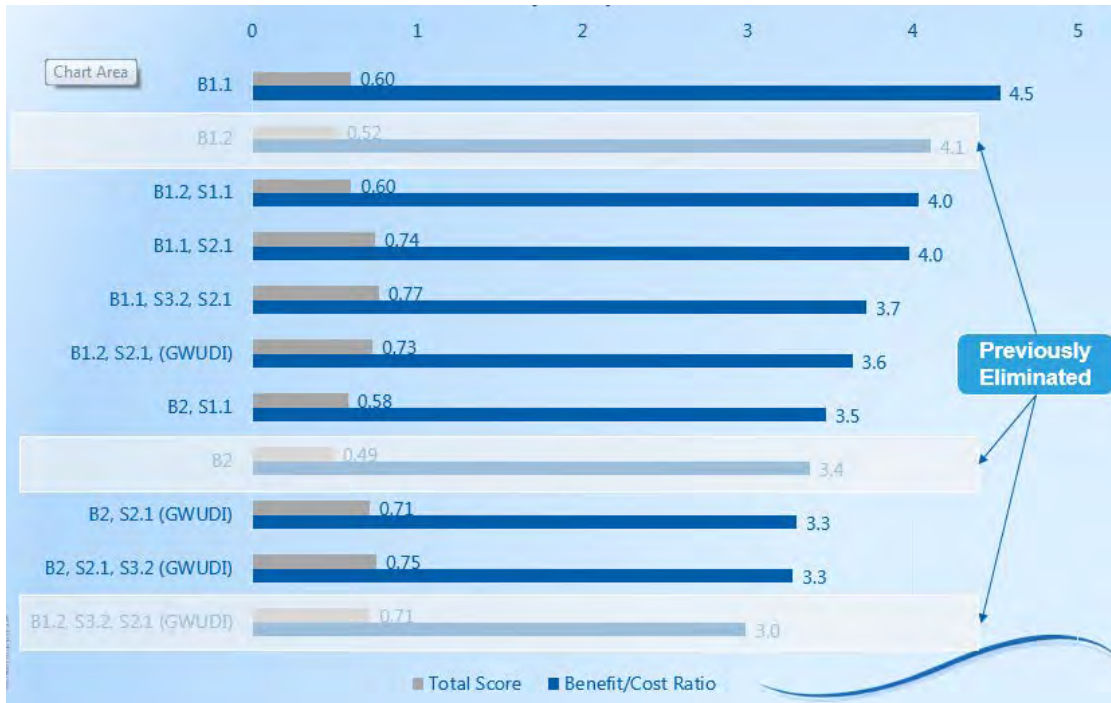


Figure 16 Total Scores and Benefit/Cost Ratios

Due to the low benefit/cost ratios presented in Figure 16, it was decided to eliminate Alternative B2, S2.1, S1.1 (GWUDI) and Alternative B2, S1.1 (GWUDI). In addition, upon further evaluation of the remaining alternatives, it was determined that due to space constraints on the site, the only viable base alternative that could implement S3.2 (Ozone/Biofiltration) in the future was B2. Because of this, regardless of benefit/cost ratio, it was decided to keep Alternative B2, S2.1, S3.2, S1.1 (GWUDI) and eliminate Alternative B1.1, S3.2, S2.1. In summary, the following alternatives were shortlisted for further evaluation:

- B1.1 - Expand existing plant (rerate existing filters).
- B1.1, S2.1 - Expand existing plant (rerate existing filters) and add post filter GAC contactors.
- B1.2, S1.1 - Expand existing plant (new filter train).
- B1.2, S1.1, S2.1 - Expand existing plant (new filter train) and add post filter GAC contactors.
- B2, S1.1, S2.1, S3.2 - Expand existing plant (new treatment train), post treatment ozone/Biofiltration and post filter GAC contactors.

Section 4

FINAL RANKING AND RECOMMENDATIONS

4.1 Purpose

The purpose of the final ranking phase of the project was to further define the shortlisted alternatives and develop final rankings that can be used to establish a recommendation. This included the following:

- Identify data gaps, develop layouts, and refine cost opinions.
- Update scores and re-rank shortlisted alternatives.
- Develop final rankings and recommendations.

4.2 Meetings and Workshops

The following public meeting was held during the final ranking phase of the project:

- Final Ranking Workshop –January 29, 2018.

4.3 Data Gap Analysis

The purpose of the data gap analysis that was performed was to identify any missing information in order to further refine scores for the shortlisted alternatives. This may include modifying alternatives to address potential operability or permitting issues. Some of the concerns identified during the data gap analysis include the following:

- Due to the hydraulic capacity of existing facilities, improvements to rerate the existing filters may lead to potential problems. Alternatives that include rerating the filters should conservatively consider adding a pump station to address the concern.
- The useful life of the media in GAC contactors is unknown. Alternatives that include GAC contactors should conservatively assume a carbon life of 3 years. Pilot testing is recommended to determine useful life for DBP management.

By identifying these data gaps, the team was able to update scores for each alternative to reflect the results of the data gap analysis providing a more refined ranking.

4.4 Level 4 Cost Estimates

In addition to the data gap analysis, layouts and refined costs were developed for the shortlisted alternatives in order to update scores. This section presents a summary of each shortlisted alternative, along with the defined layouts and process flow diagrams. It should be noted that the cost estimates prepared for the analysis are considered Level 4 estimates by the AACE (see Figure 17) and contain a +50% to -30% level of accuracy. **The cost estimates developed for the final rankings are meant to be for relative comparison of the alternatives and are NOT to be used for budgetary purposes due to insufficient detail and lack of elements common to all alternatives (i.e. raw water pipeline, wellfield expansion, etc.).**

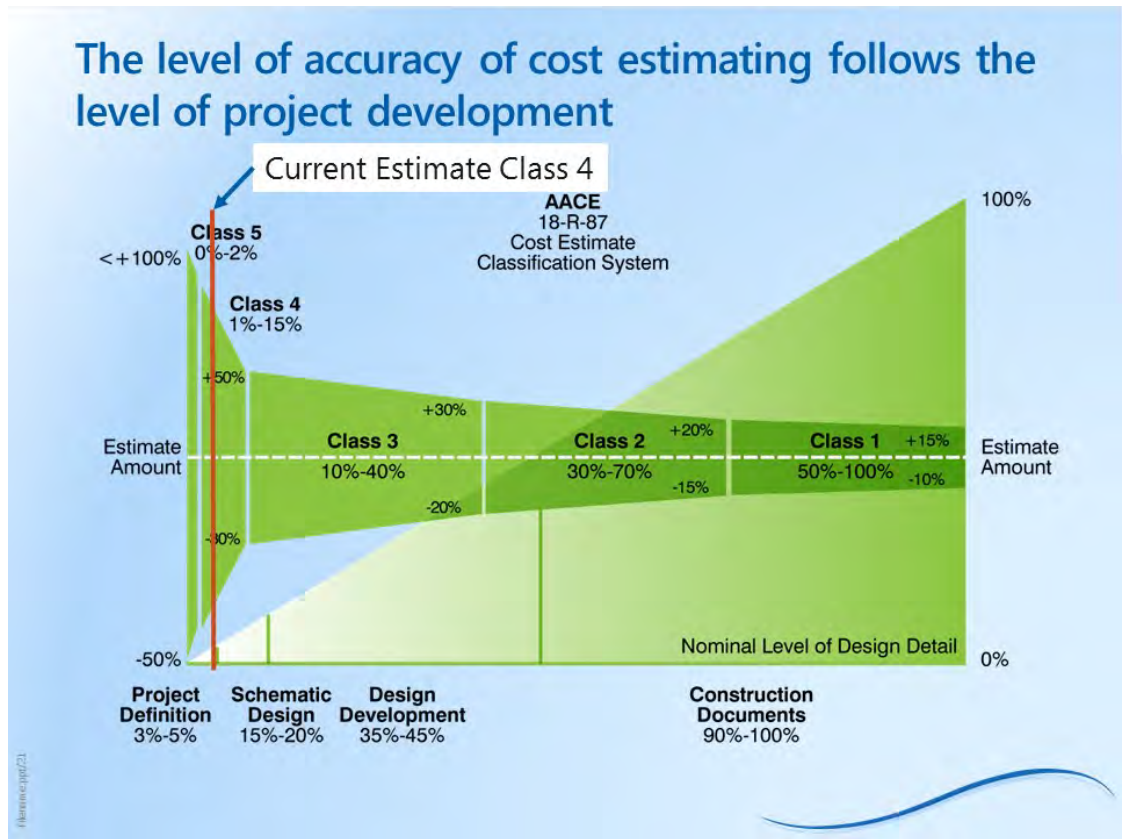


Figure 17 Level 4 Cost Estimates for Final Alternatives Ranking

4.5 Summary of Shortlisted Alternatives

4.5.1 Alternative B1.1 - Expand Existing Plant (Rerate Existing Filters)

This alternative includes construction of two new aerators, modifications to the primary basins, multiple new low lift pump stations, modifications to rerate the existing filters, new clearwells, and a new high service pump station for delivery of finished water to the distribution system. A summary of the highlights included with this alternative are presented below. An overall layout along with a process flow diagram for this alternative is presented in Figure 18 and Figure 19, respectively.

- Water Quality:
 - Likely requires chloramines to satisfy current Disinfection By-Product regulations.
 - Potential future regulatory concerns (CEC's) will need additional processes.
 - No significant improvement in overall water quality (except for GWUDI compliance).
- Operability:
 - Increased maintenance (new pumps).
 - Low lift pumps required to control filtration process and pump to clearwells, increasing complexity.
 - Most efficient use of space (easier phasing).

- Constructability:
 - Large disruption to plant operations (work on existing filters).
 - Minimal footprint of new facilities.
 - Rerating filters requires permitting variance.
- GWUDI Facility:
 - Improved filtration.
 - Disinfection to meet SWTR requirements.
- Project Costs:
 - Capital = \$106 million.
 - O&M = \$3.6 million.
 - Life Cycle = \$160 million.

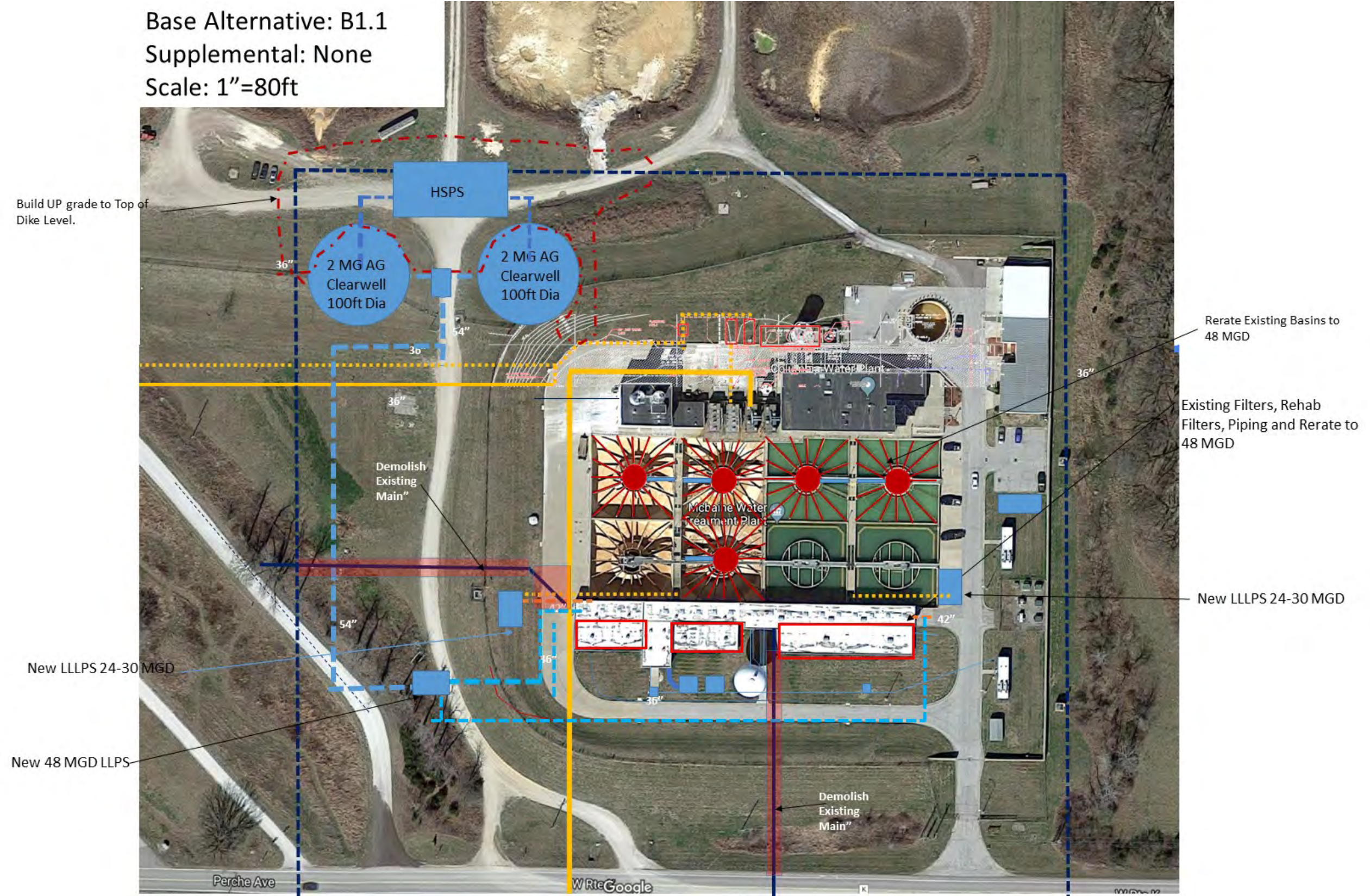


Figure 18 Alternative B1.1 Layout

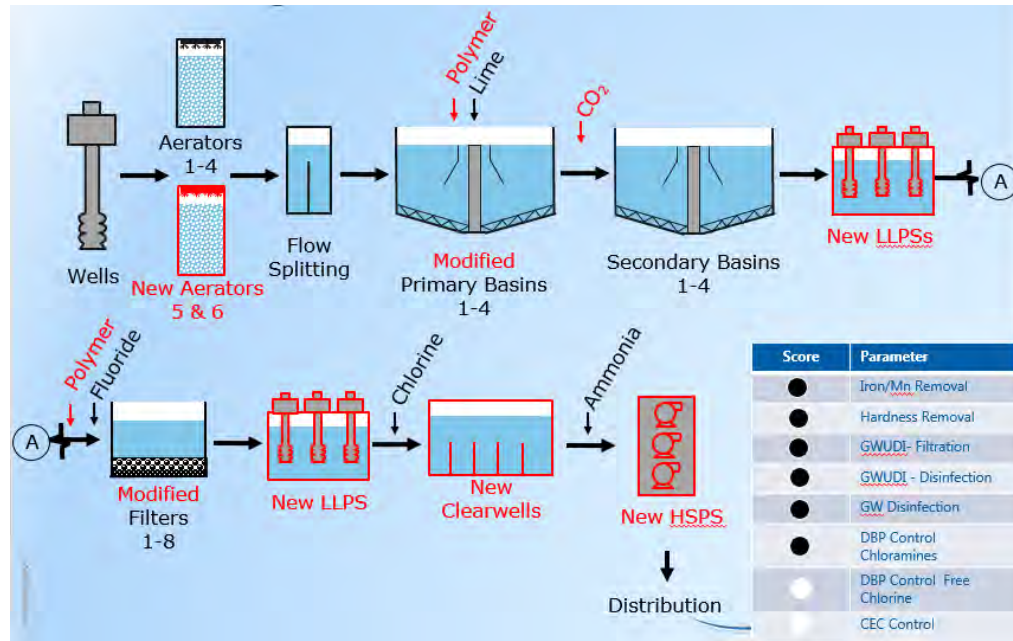


Figure 19 Alternative B1.1 Process Flow Schematic

4.5.2 Alternative B1.1, S2.1 - Expand Existing Plant (Rerate Existing Filters) and Add Post Filter GAC Contactors

This alternative includes the same improvements included in Alternative B1.1 with the addition of construction of GAC contactors. A summary of the highlights included with this alternative are presented below. An overall layout along with a process flow diagram for this alternative is presented in Figure 20 and Figure 21, respectively.

- Water Quality:
 - Ability to design finished water quality to meet DBP regulations without relying on chloramines.
 - Robust process that will remove some CECs. Operating cost may be impacted by future regulations due to process inefficiencies.
- Operability:
 - Additional staffing.
 - Staffing education for new processes (DBP control).
 - Increased maintenance (new pumps and process).
 - Moderate complexity.
- Constructability:
 - Large disruption to plant operations (work on existing filters).
 - Large space requirements will require some use of lagoon space.
 - Rerating filters requires permitting variance.
- GWUDI Facility:
 - Fully compliant.
- Project Costs:
 - Capital = \$152 million.
 - O&M = \$4.7 million.
 - Life Cycle = \$221 million.

Base Alternative: B1.1
Supplemental: S2.1
Scale: 1"=80ft

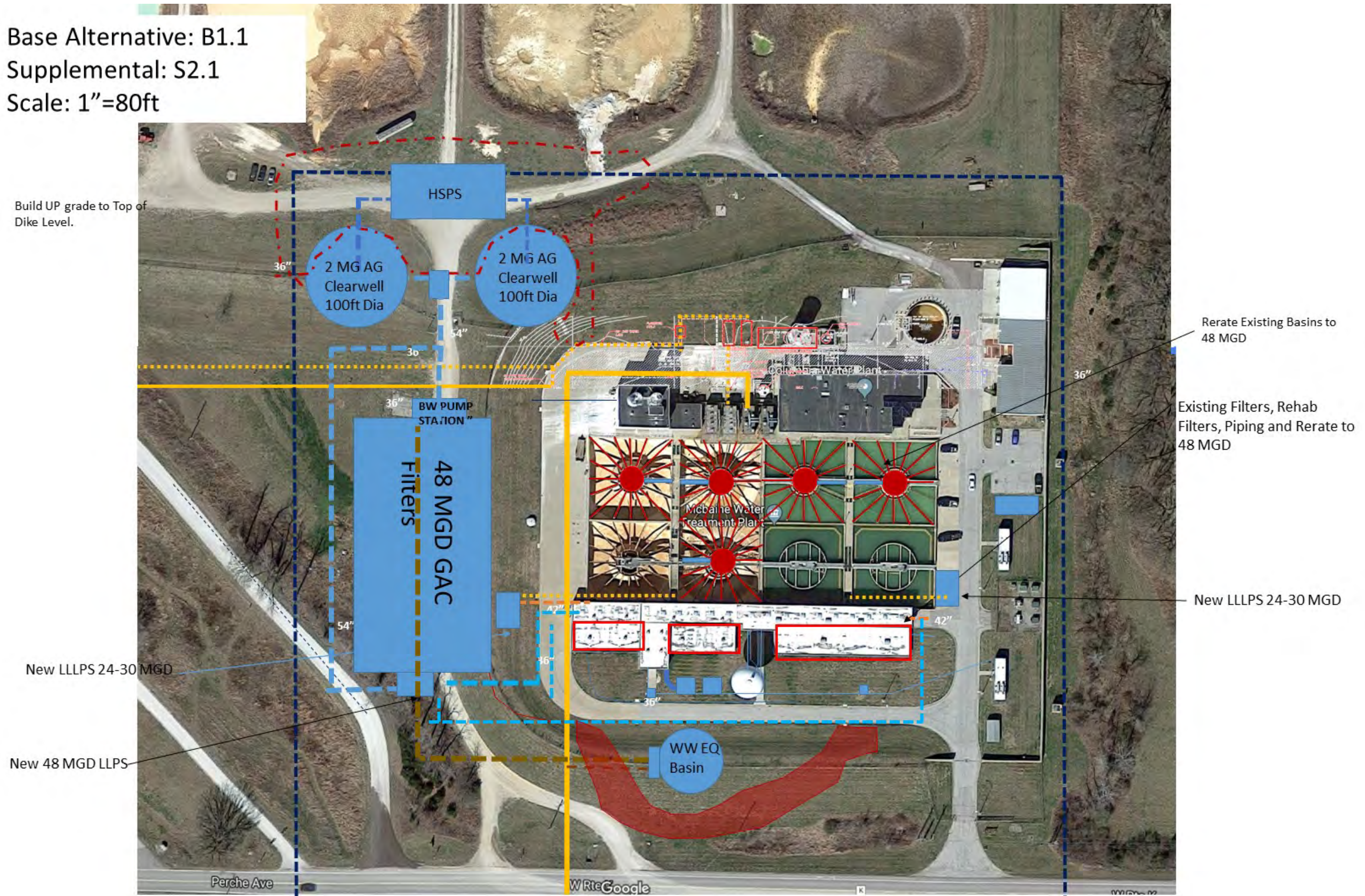


Figure 20 Alternative B1.1, S2.1 Layout

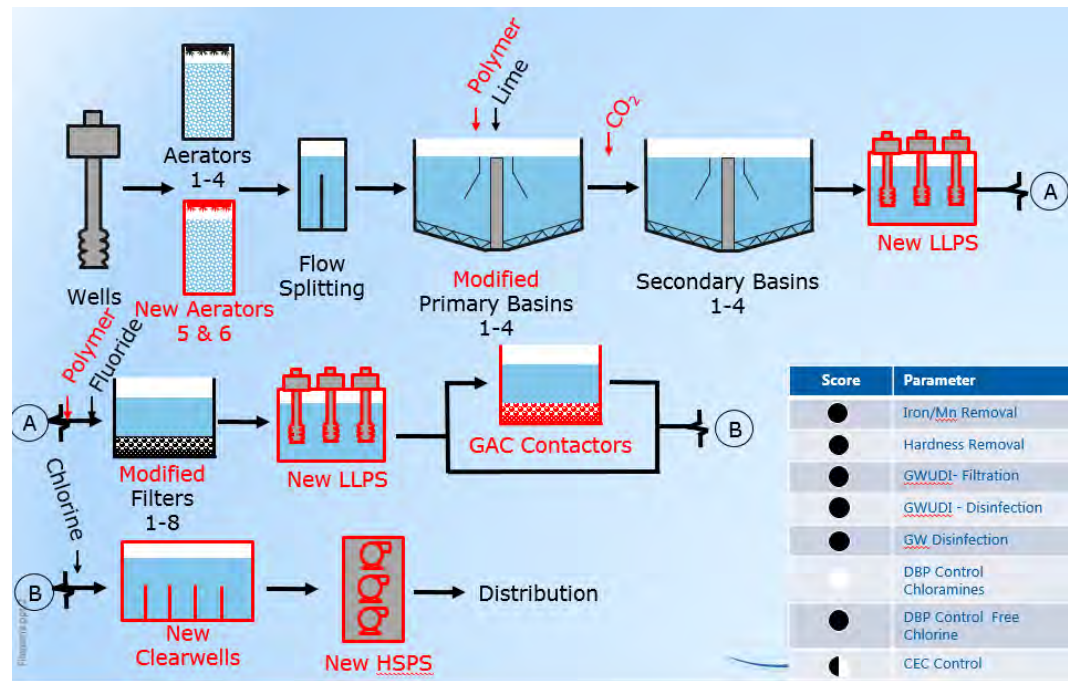


Figure 21 Alternative B1.1, S2.1 Process Flow Schematic

4.5.3 Alternative B1.2, S1.1 - Expand Existing Plant (New Filter Train)

This alternative includes construction of two new aerators, modifications to the primary basins, construction of a new filter train, modifications to existing filters for GWUDI compliance, multiple new low lift pump stations, new clearwells, and a new high service pump station for delivery of finished water to the distribution system. A summary of the highlights included with this alternative are presented below. An overall layout along with a process flow diagram for this alternative is presented in Figure 22 and Figure 23, respectively.

- Water Quality:
 - Likely requires chloramines to satisfy current Disinfection By-Product regulations.
 - Potential future regulatory concerns (CEC's) will need additional processes.
 - No significant improvement in overall water quality (except for GWUDI compliance).
- Operability:
 - Increased maintenance (new pumps and filters).
 - Minimal complexity.
 - Low lift pumps required for phasing and to minimize future construction costs.
 - A little more difficult to phase.
- Constructability:
 - Moderate disruption to plant operations.
 - Moderate space requirements.
- GWUDI Facility:
 - Fully compliant.
- Project Costs:
 - Capital = \$124 million.
 - O&M = \$3.6 million.
 - Life Cycle = \$178 million.

Base Alternative: B1.2
 Supplemental: S1.1
 Scale: 1"=80ft

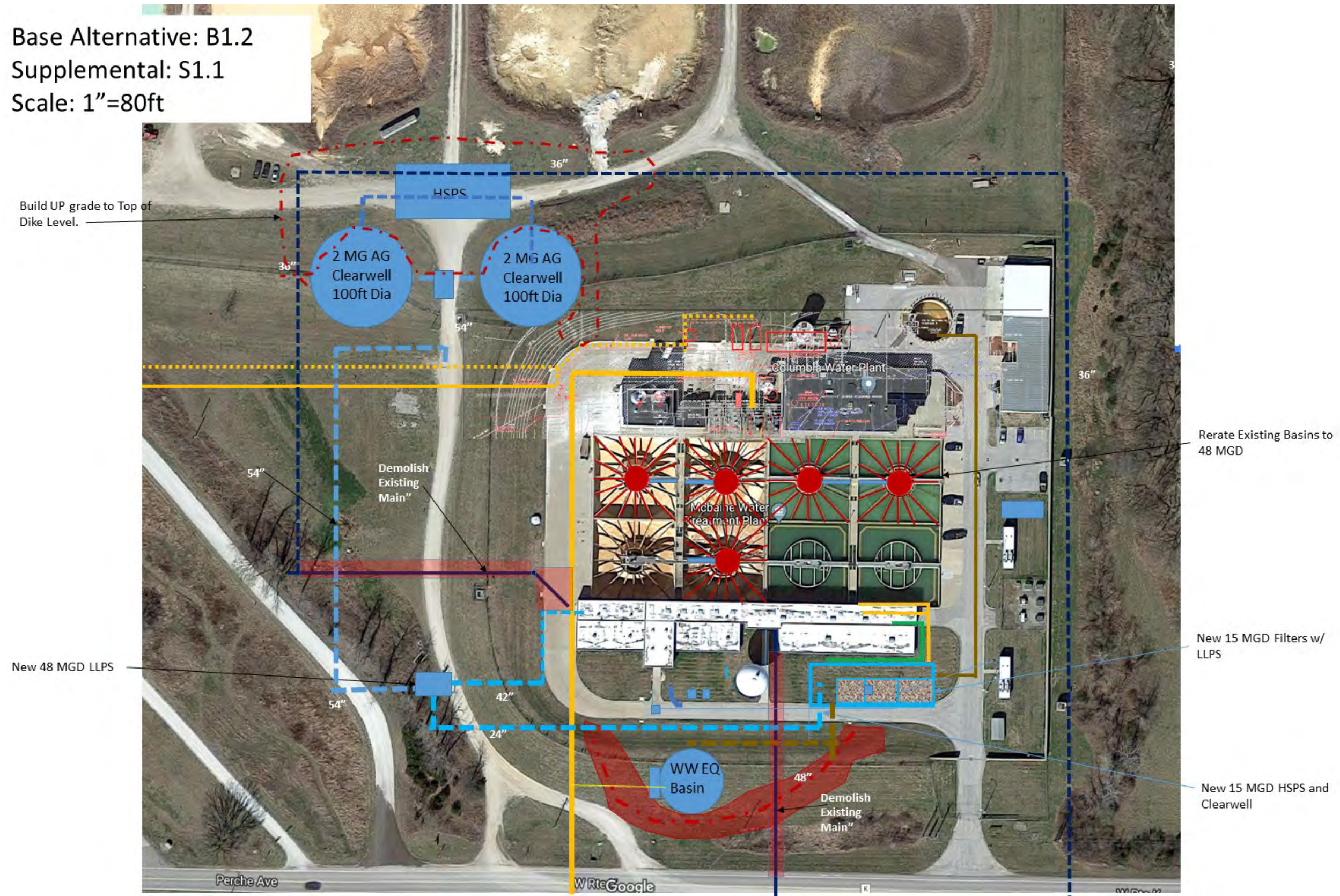


Figure 22 Alternative B1.2, S1.1 Layout

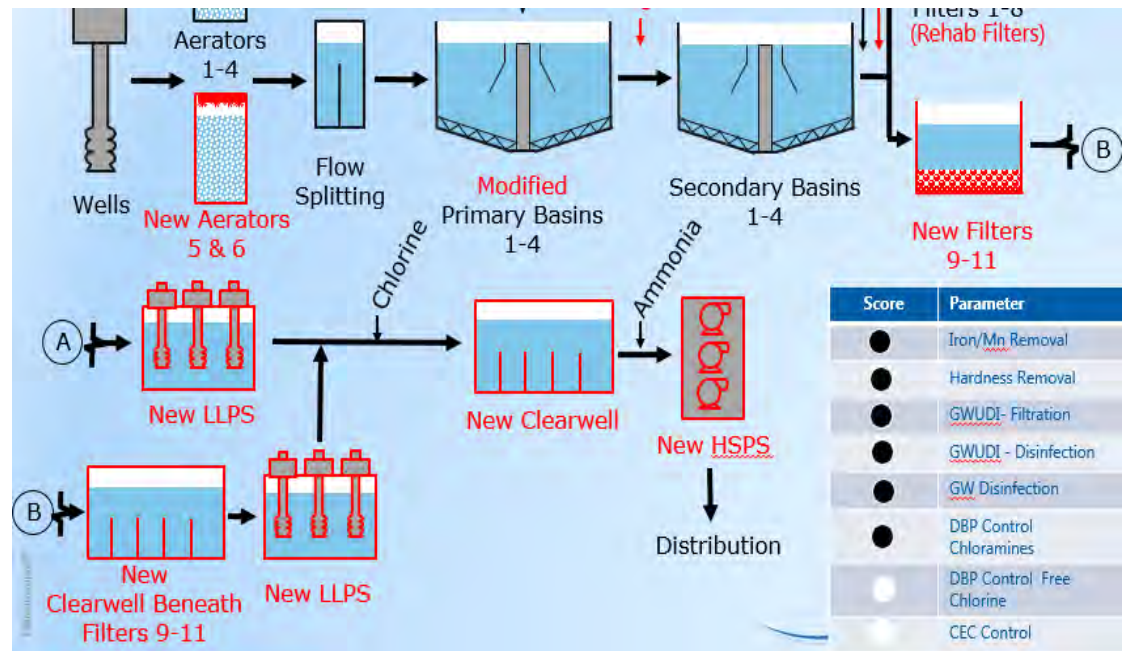


Figure 23 Alternative B1.2, S1.1 Process Flow Schematic

4.5.4 Alternative B1.2, S1.1, S2.1 - Expand Existing Plant (New Filter Train) and Add Post Filter GAC Contactors

This alternative includes the same improvements included in Alternative B1.2, S1.1 with the addition of construction of GAC contactors. A summary of the highlights included with this alternative are presented below. An overall layout along with a process flow diagram for this alternative is presented in Figure 24 and Figure 25, respectively.

- Water Quality:
 - Ability to design finished water quality to meet DBP regulations without relying on chloramines.
 - Robust process that will remove some CECs. Operating cost may be impacted by future regulations due to process inefficiencies.
- Operability:
 - Additional staffing.
 - Staffing education for new processes (DBP control).
 - Increased maintenance (new pumps, filters, and process).
 - Moderate complexity.
- Constructability:
 - Moderate disruption to plant operations.
 - Large space requirements.
- GWUDI Facility:
 - Fully compliant.
- Project Costs:
 - Capital = \$166 million.
 - O&M = \$4.7 million.
 - Life Cycle = \$236 million.

Base Alternative: B1.2
 Supplemental: S1.1,S2.1
 Scale: 1"=80ft

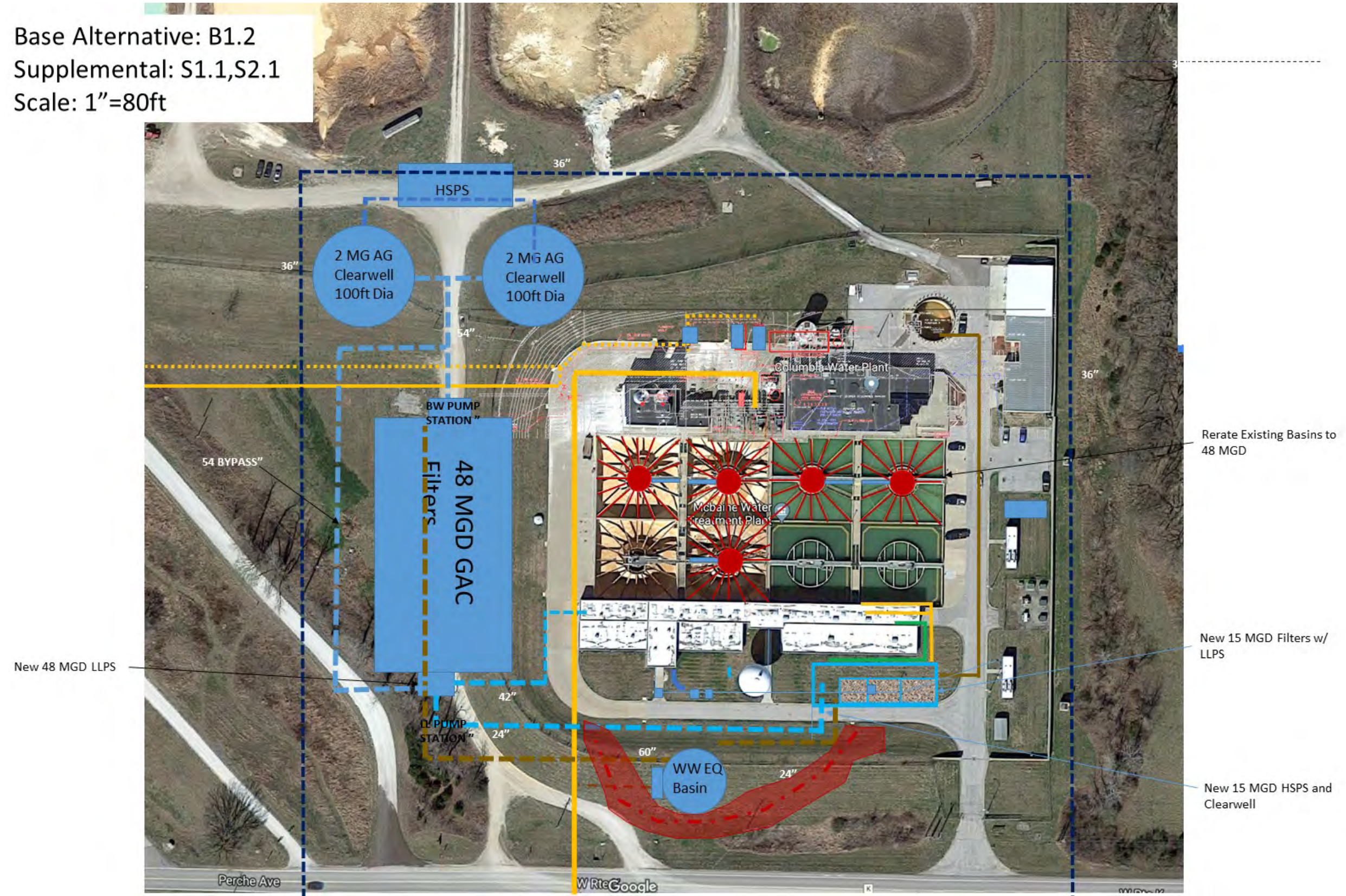


Figure 24 Alternative B1.2, S1.1, S2.1 Layout

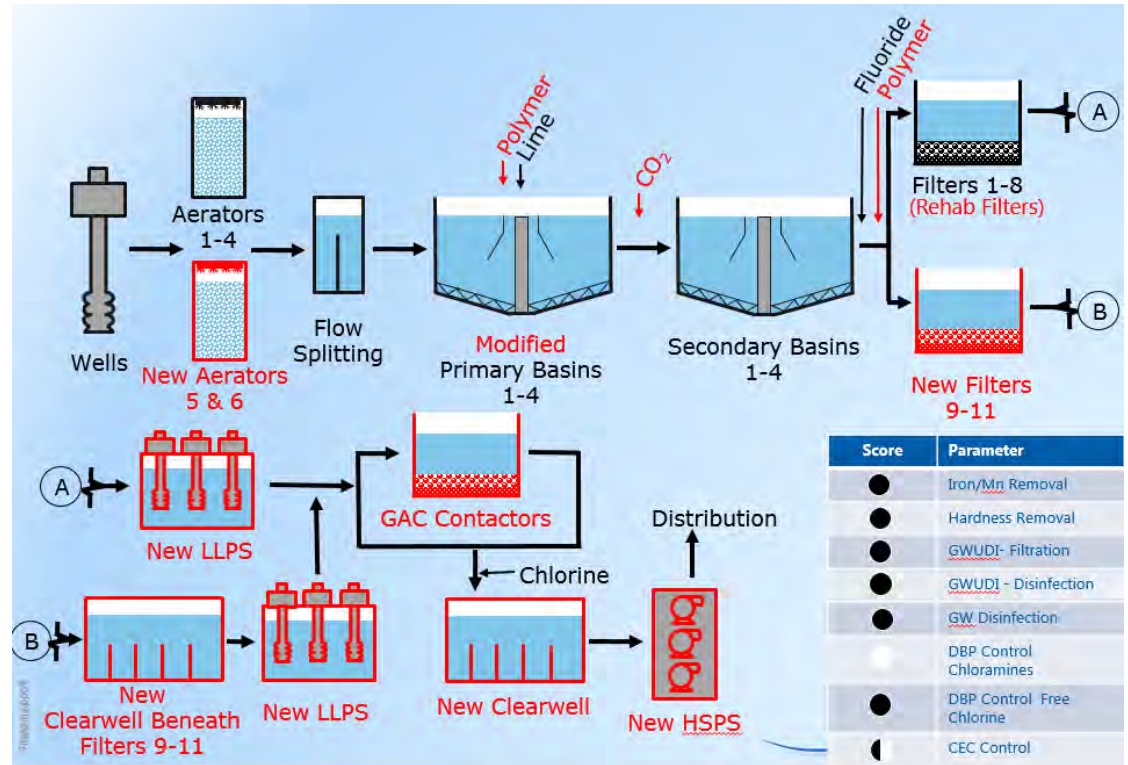


Figure 25 Alternative B1.2, S1.1, S2.1 Process Flow Schematic

4.5.5 Alternative B2, S1.1, S2.1, S3.2 - Expand Existing Plant (New Treatment Train), Post Treatment Ozone/Biofiltration, and Post Filter GAC Contactors

This alternative includes construction of a new treatment train consisting of two new aerators, a softening basin, a secondary basin, an ozone contactor, filters, and a low lift pump station. In addition, modifications to the existing train need to be performed, including modifications to Primary Basin No. 1 and No. 2, multiple new low lift pump stations, an ozone contactor, modifications to the filters for GWUDI compliance, new GAC contactors, new clearwells and a new high service pump station for delivery of finished water to the distribution system. A summary of the highlights included with this alternative are presented below. An overall layout along with process flow diagrams for this alternative is presented in Figure 26, Figure 27, and Figure 28, respectively.

- Water Quality:
 - Ability to design finished water quality to meet DBP regulations without relying on chloramines.
 - Best Available Technology for CEC removal. Synergistic impacts with post filter GAC.
- Operability:
 - Additional staffing.
 - Staffing education for new processes.
 - Increased maintenance (new pumps, filters, and process).
 - Most complex alternative to operate (two trains with multiple processes).

- Constructability:
 - Minimal disruption to plant operations.
 - Large space requirements.
- GWUDI Facility:
 - Fully compliant.
- Project Costs:
 - Capital = \$223 million.
 - O&M = \$5.1 million.
 - Life Cycle = \$298 million.

Base Alternative: B2
 Supplemental: S1.1, S2.1, S3.2
 Scale: 1"=80ft

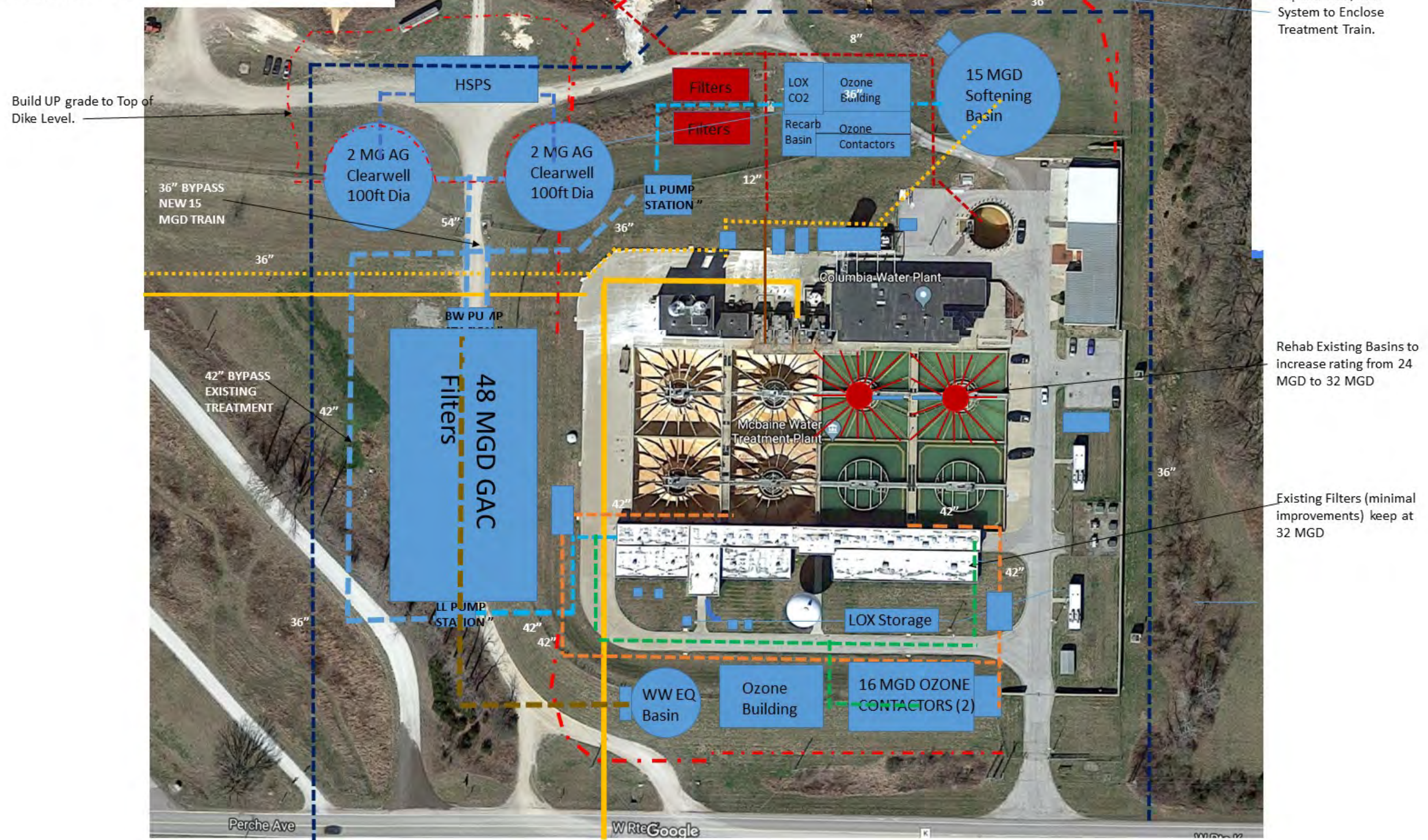


Figure 26 Alternative B2, S1.1, S2.1, S3.2 Layout

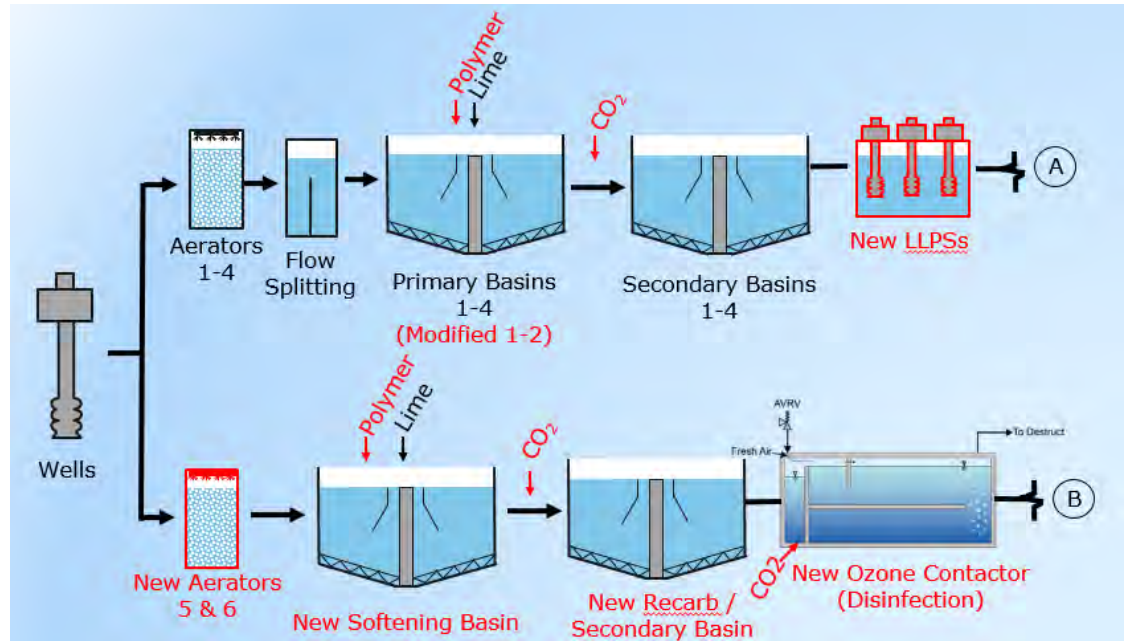


Figure 27 Alternative B2, S1.1, S2.1, S3.2 Process Flow Schematic Part I

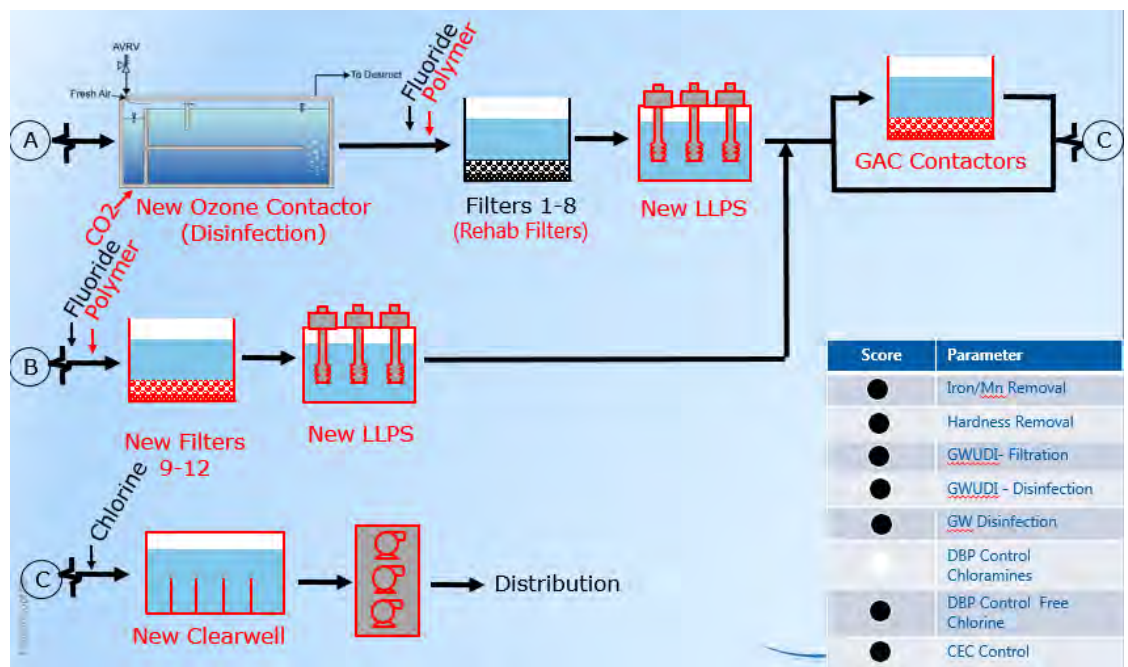


Figure 28 Alternative B2, S1.1, S2.1, S3.2 Process Flow Schematic Part II

4.6 Final Rankings

Using the layouts, refined costs, and updated scores, the shortlisted alternatives were evaluated and re-ranked. The updated rankings were presented to the DWPWG during the Final Ranking Workshop held on January 29, 2018. A summary of the final rankings with respect to the updated non-economic and economic criterion are presented in Figure 29.

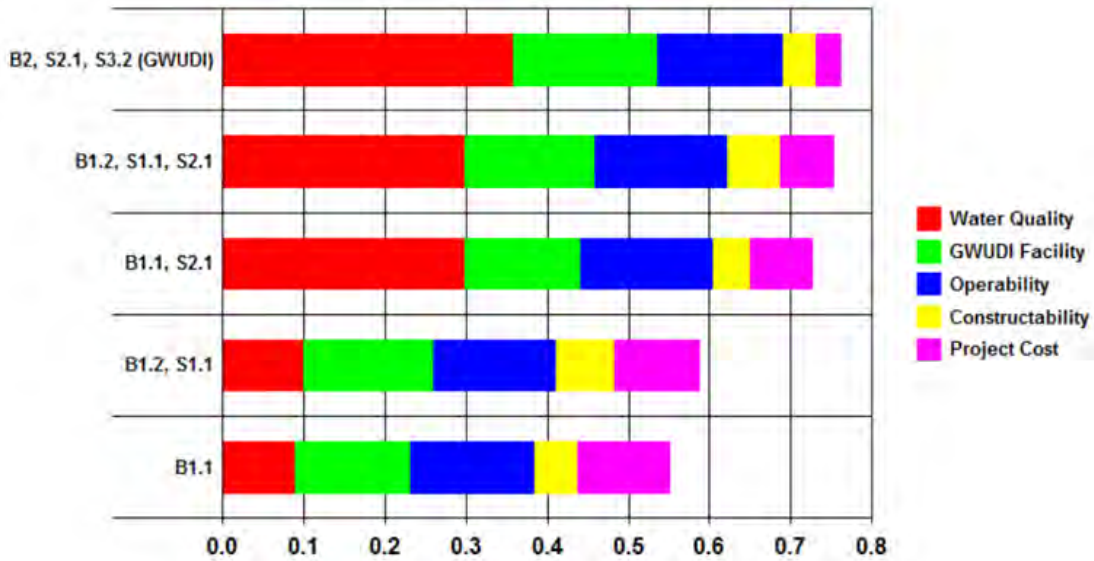


Figure 29 Final Ranking of Shortlisted Alternatives

Similar to the initial evaluation, because of the high weight given to Water Quality and GWUDI, it was the higher cost alternatives that scored highest and provided the most benefit. The benefit/cost ratios were again analyzed for the shortlisted alternatives and a summary is presented in Figure 30.

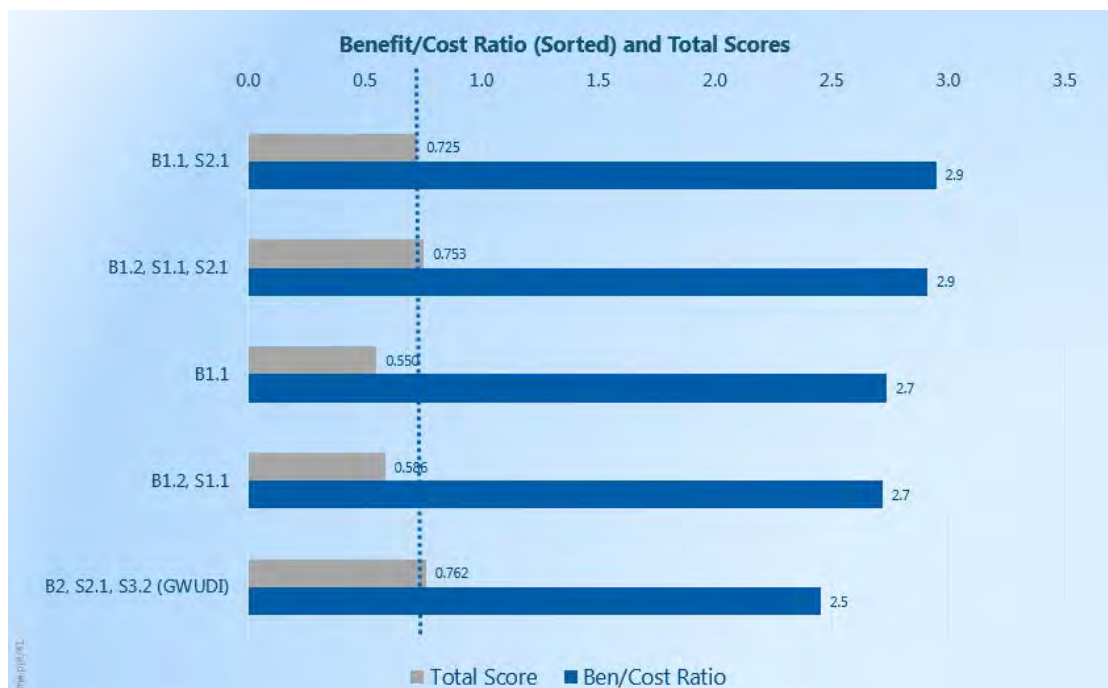


Figure 30 Benefit/Cost Ratios for Shortlisted Alternatives

The benefit/cost ratios showed that although the alternative containing ozone/Biofiltration (B2, S1.1, S2.1, S3.2), scored incrementally higher than the other alternatives, it had the lowest benefit/cost ratio. Because of this, removing this alternative from consideration was recommended. This left the group with two very viable sets of alternatives that can each be implemented in phases. Alternative B1.1 offers the lowest cost at \$160 million with a total score of 0.550 and can be upgraded to B1.1, S2.1 with a score of 0.725 for an extra \$61 million. Alternative B1.2, S1.1, on the other hand, offers a similar pattern at a slightly higher score (0.586) for \$178 million and it can be upgraded to B1.2, S1.1, S2.1 with a score of 0.753 for an extra \$58 million. This concept of phasing the recommended alternatives is presented in Figure 31.



Figure 31 Recommended Alternatives Scores vs. Life Cycle Cost

4.7 Recommendations of Drinking Water Planning Work Group

The DWPWG met on February 26, 2018 to review the final ranking results and provide the final recommendations. The findings and recommendations of the DWPWG are as follows:

1. DWPWG Findings:
 - a. The McBaine WTP should consider processes that meet the requirements for a GWUDI Facility.
 - b. The McBaine WTP should utilize treatment technologies to achieve Disinfection By-Products (DBP) compliance without the need for chloramines and to also assist in removal of Contaminants of Emerging Concern (CEC's).

2. DWPWG Recommendations:
 - a. Priority should be given to first restoring the plant to its 32 MGD capacity prior to increasing capacity to 48 MGD.
 - b. The base alternatives of B1.1, B1.2, and B2 should be evaluated with the supplemental processes to achieve improved water quality through a phased approach.
 - c. The design on the selected alternative should begin no later than 2020, as indicated in Carollo's analysis, to be in operation no later than 2024, unless design and construction are able to be accomplished sooner.
 - d. In order to improve water quality while the new process train is in design, and construction, repair and/or enhancement of the current filters and pilot testing done to make every effort to return to free chlorine disinfection.
 - e. The rehabilitation and/or enhancement initiatives outlined in the Condition Assessment will address deficiencies in the facility and system and request an updated timeline for these initiatives be produced by Water and Light.

Appendix A

DWPWG ORDINANCE

Introduced by Treece Council Bill No. R 48-17 A

Permanent Record
Filed in Clerk's Office

A RESOLUTION

establishing a Drinking Water Planning Work Group to assist in an update of the 2011 Water Treatment Plant Expansion Preliminary Design Report.

BE IT RESOLVED BY THE CITY COUNCIL OF THE CITY OF COLUMBIA, MISSOURI, AS FOLLOWS:

SECTION 1. There is hereby established a Drinking Water Planning Work Group to assist in an update of the 2011 Water Treatment Plant Expansion Preliminary Design Report and to provide guidance to the Water and Light Advisory Board and City Council on the following:

- Review current drinking water regulations, including what types of disinfection methods comply with regulations.
- Review Columbia's current water supply conditions.
- Assess the current state of utility industry and customer-side water treatment technology and cost.
- Review and provide input on developed recommendations.
- Develop drinking water planning recommendations.

SECTION 2. The Drinking Water Planning Work Group shall consist of seven (7) members comprised as follows:

- One (1) member shall be a City Council member appointed by the City Council. The initial City Council member appointee is Karl Skala.
- Six (6) members shall be appointed by the City Utilities – Water and Light Director from the drinking water customer user groups set forth herein. The initial six (6) appointees are as follows:
 1. Residential customer member – Julie Ryan (CoMo Safe Water)
 2. Commercial customer member – Matt Off (Director, Rockbridge HyVee)
 3. Industrial customer member – Ron Pruett (3M, Plant Engineering)
 4. Water industry professional member – Terry Merritt (Alliance Water Resources)

5. Educational institution member – Randy Jackson (Environmental Engineer, Columbia Public School District)
6. Healthcare industry member – Michael Szewczyk, MD (Chair, Columbia/Boone County Board of Health)

SECTION 3. The Drinking Water Planning Work Group shall also include the following non-voting members:

- Two (2) ad hoc non-voting members shall be members of the Water and Light Advisory Board to be appointed by the Water and Light Advisory Board.
- One (1) ad hoc non-voting member shall be from the Office of Sustainability to be appointed by the Sustainability Manager.


SECTION 4. A quorum to hold a meeting shall consist of four (4) voting members. All meetings shall be open to involvement and participation by as many additional community members who desire to attend.

SECTION 5. The Drinking Water Planning Work Group shall make a final report to the Water and Light Advisory Board of its findings and recommendations by December 31, 2017. The Work Group shall be dissolved upon submitting its final report.

SECTION 6. The Drinking Water Planning Work Group shall be provided reasonable staff support.

ADOPTED this 3rd day of April, 2017.

ATTEST:




City Clerk



Mayor and Presiding Officer

APPROVED AS TO FORM:



City Counselor

Appendix B

KICKOFF WORKSHOP



Visioning Workshop I
City of Columbia, MO
Water and Light Department
Drinking Water Planning Workgroup
July 17, 2017, 5:30 pm
701 E Broadway Council Chambers

WATER
OUR FOCUS
OUR BUSINESS
OUR PASSION

Columbia
Engaging...Meeting...Working With Water®



Purpose and Goals of
Planning Workgroup

Draft Mission Statement of Planning Workgroup

- "To enhance the quality of life for Columbia, Missouri Citizens by providing direction to Columbia Water and Light on the best means to continue its mission to provide at an affordable price; high-quality water and dependable service that exceed customer expectations; protects and ensures a long-term water supply for future generations; and serves as responsible stewards of public health, utility resources, and the environment."

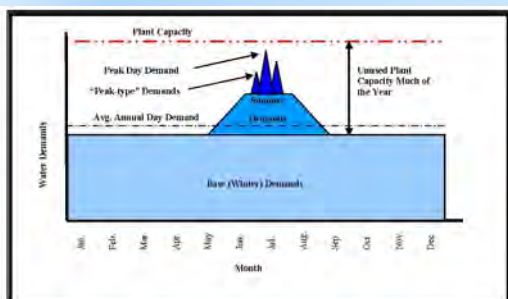
Challenges to Accomplishing Mission

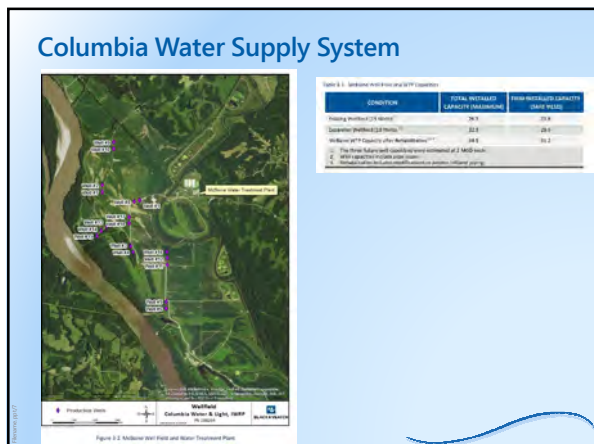
- Affordability: % of Median Household Income
- Capacity: Satisfy Future Water Demands
- Water Quality:
- Environmental Stewardship:

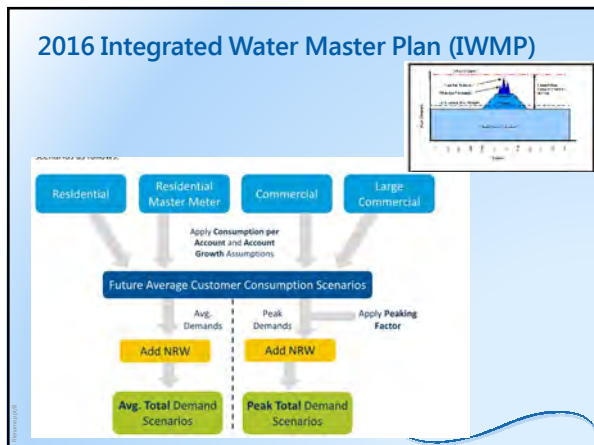
Capacity Studies

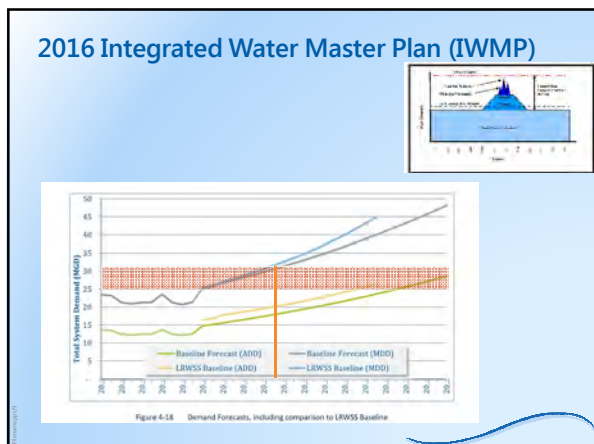
- **2007 Water System Study (Jacobs)**
- **2007 Ground Water Flow in McBaine Bottoms (USGS)**
- 2010 University of Missouri Columbia Report
- 2011 Preliminary Expansion Study (Carollo)
- 2012 Well Siting Study (Black and Veatch)
- **2015 Long Range Planning Study (Jacobs)**
- 2016 Water Treatment Plant Condition Assessment (Black and Veatch)
- **2016 Integrated Water Supply Plan (Black and Veatch)**
- **2017 Integrated Management Plan (HDR)**

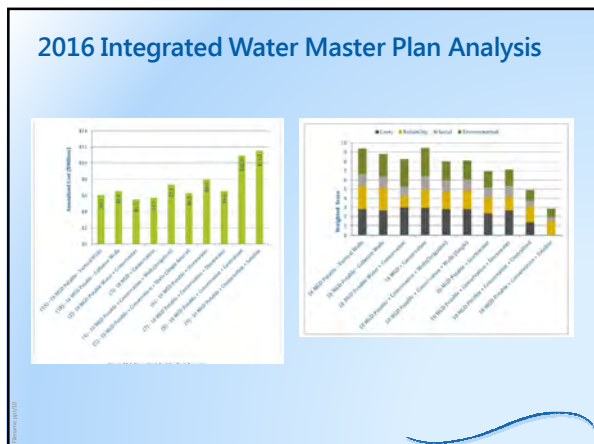
Capacity: Water Demand Basics





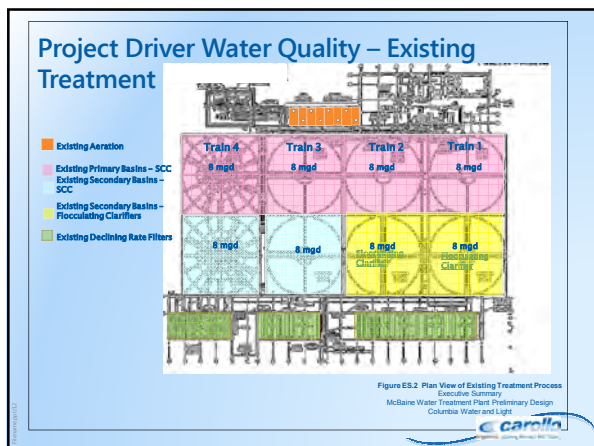


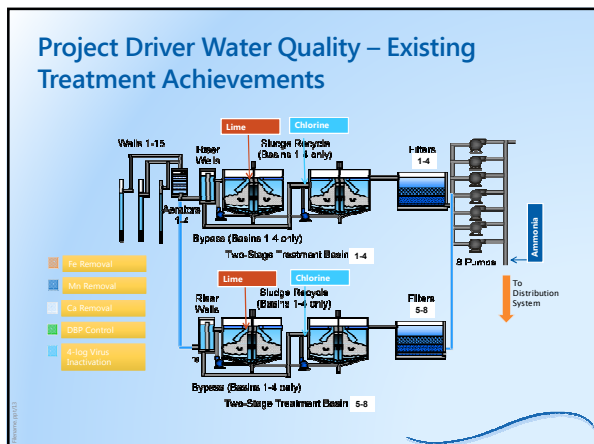




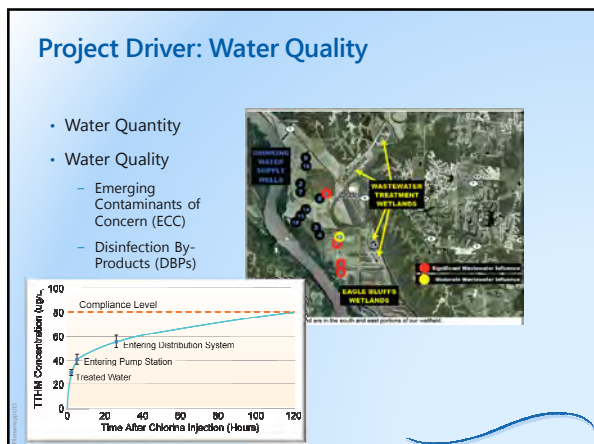
2016 Integrated Water Master Plan Recommendations

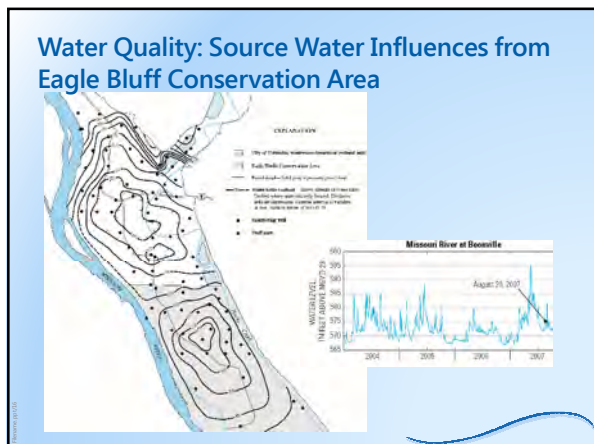
- Expand Existing Wellfield by 16 mgd
- Continued Use of Deep Wells For Non Potable Irrigation
- Continued Use of ASR wells
- Review Conservation Program and Expand Outreach
- No IPR or DPR
- No Non-Potable System (Stormwater reuse)

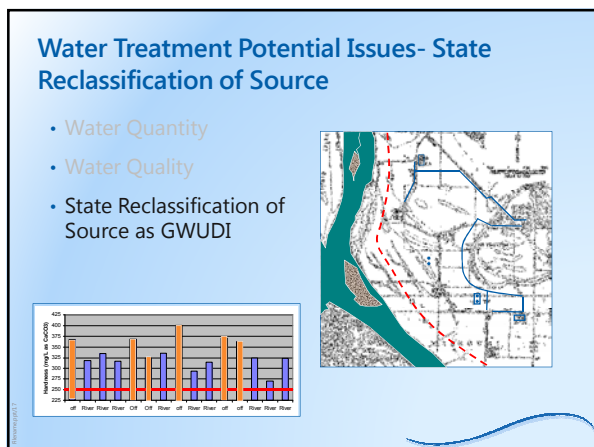


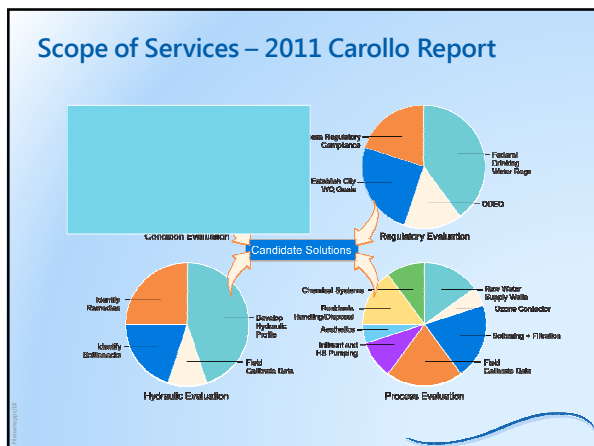


- ### Water Quality Studies
- 2007 Water System Study (Jacobs)
 - **2007 Ground Water Flow in McBaine Bottoms (USGS)**
 - **2010 University of Missouri Columbia Report**
 - **2011 Preliminary Expansion Study (Carollo)**
 - **2012 Well Siting Study (Black and Veatch)**
 - 2015 Long Range Planning Study (Jacobs)
 - **2016 Water Treatment Plant Condition Assessment (Black and Veatch)**
 - 2016 Integrated Water Supply Plan (Black and Veatch)
 - 2017 Integrated Management Plan (HDR)



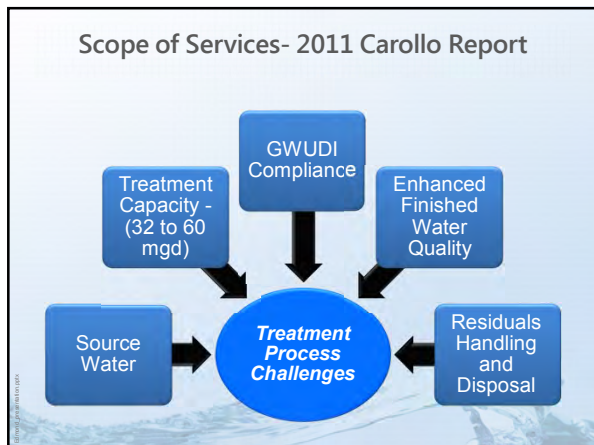






Scope of Services- 2011 Carollo Report

- Task 1 – Project Inception ✓
- Task 2 – Data Collection and Analysis ✓
- Task 3 – Regulatory Evaluation ✓
- Task 4 – Process Evaluation ✓
- Task 5 – Hydraulic Evaluation ✓
- Task 6 – Develop Alternatives ✓
- Task 7 – Analysis and Recommendations ✓



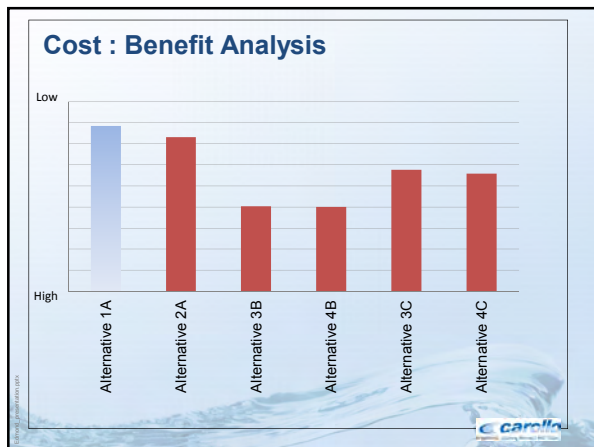
Treatment Alternative Identification

- “Base” Treatment Trains
 - Conventional Softening
 - Split Treatment
- “Supplemental” Processes
 - GAC
 - MIEX
 - Deep Bed Filtration
 - Secondary Aeration
 - UV, Ozone

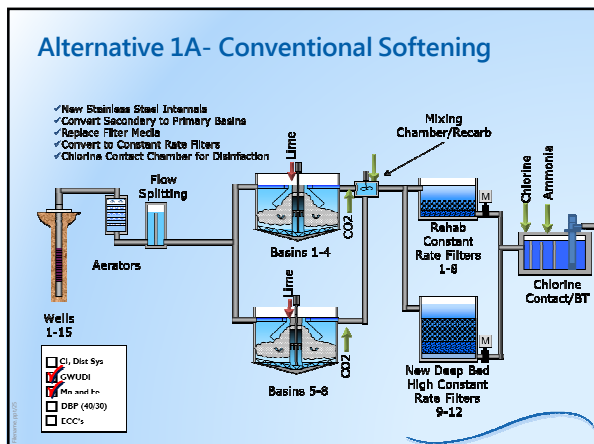
```
graph TD; A[Base Train] -- "+" --> B[Supplemental Processes]; B -- "=" --> C[Complete Process];
```

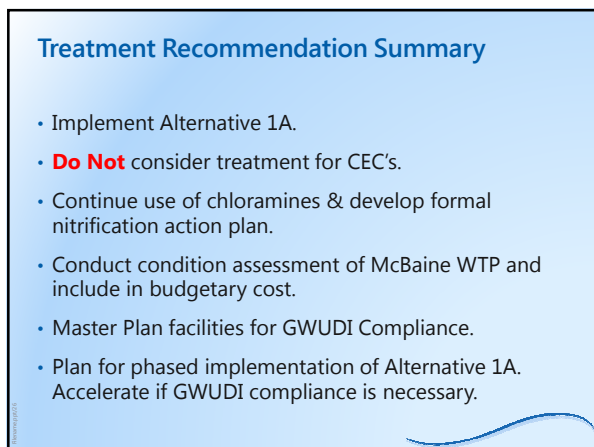
Final Selection: Cost Benefit Analysis

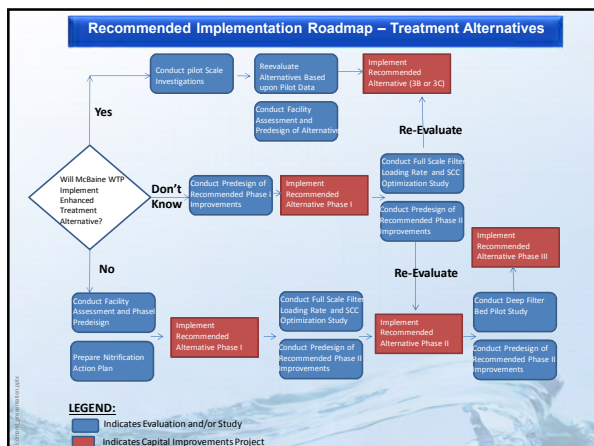
Alternative	ECC Reduction	Free Chlorine	Permitting	MOPD	Ability to Communicate To Public	Life-Cycle Cost (\$M)	Cost Differential (\$M)
1A Existing	-	-	++	++	-	95	-
3C Ozone BAF	++	+	--	-	+++	122	27
3B GAC Filters	+	+	+	++	++	159	64

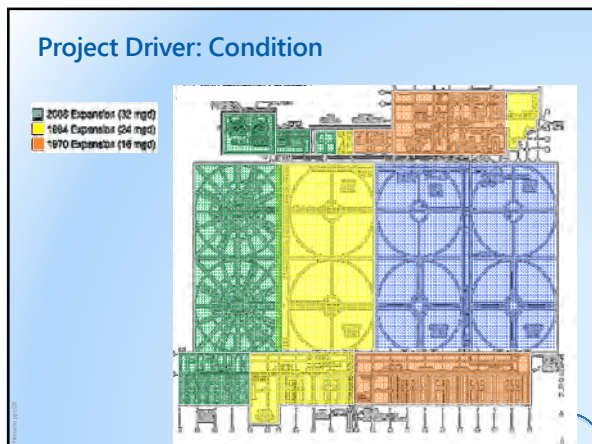


- ### Water Quality Studies
- 2007 Water System Study (Jacobs)
 - **2007 Ground Water Flow in McBaine Bottoms (USGS)**
 - **2010 University of Missouri Columbia Report**
 - **2011 Preliminary Expansion Study (Carollo)**
 - **2012 Well Siting Study (Black and Veatch)**
 - 2015 Long Range Planning Study (Jacobs)
 - **2016 Water Treatment Plant Condition Assessment (Black and Veatch)**
 - 2016 Integrated Water Supply Plan (Black and Veatch)
 - 2017 Integrated Management Plan (HDR)



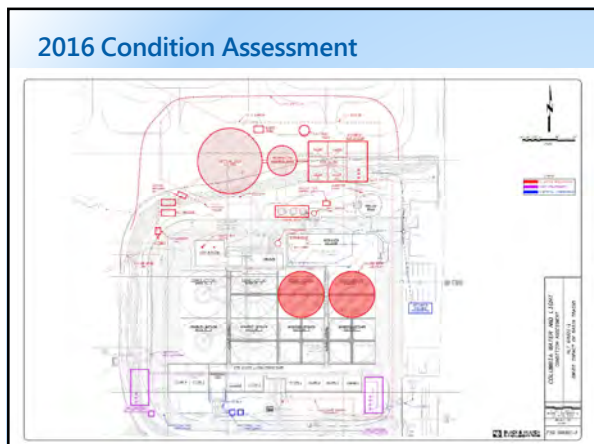






- ### Water Quality Studies
- 2007 Water System Study (Jacobs)
 - 2007 Ground Water Flow in McBaine Bottoms (USGS)
 - 2010 University of Missouri Columbia Report
 - 2011 Preliminary Expansion Study (Carollo)
 - 2012 Well Siting Study (Black and Veatch)
 - 2015 Long Range Planning Study (Jacobs)
 - **2016 Water Treatment Plant Condition Assessment (Black and Veatch)**
 - 2016 Integrated Water Supply Plan (Black and Veatch)
 - 2017 Integrated Management Plan (HDR)

- ### 2016 Condition Assessment
- New Water Demand/Capacity Results – 2015 LRSS eliminate need for 65 mgd.
 - Capacity Downgraded from 32 to 24 mgd.
 - Growth of wintertime demands may not permit Expansion within Basins when needed.
 - Water Quality Considerations:
 - Continue existing treatment process goals
 - Locate Wells to avoid State Classification of Water as GWUDI



2016 Condition Assessment

Columbia Water and Light - 2016 CONDITION ASSESSMENT REPORT

Table 9-4 Costs for Expansion Alternatives (in \$1,000s of Dollars)

ALTERNATIVE	EXP 45-1		EXP 45-2		EXP 45-3		EXP 45-4		EXP 45-5		EXP 45-6	
	85 Basis	90 Basis	85 Basis	90 Basis	85 Basis	90 Basis	85 Basis	90 Basis	85 Basis	90 Basis	85 Basis	90 Basis
Water Supply												
Wells	\$1,640	\$1,640	\$1,640	\$1,780	\$1,780	\$1,780	\$1,780	\$1,780	\$1,780	\$1,780	\$1,780	\$1,780
Riser Water Piping	\$2,730	\$2,730	\$2,730	\$3,152	\$3,152	\$3,152	\$3,152	\$3,152	\$3,152	\$3,152	\$3,152	\$3,152
Water Supply Construction Total	\$4,370	\$4,370	\$4,370	\$4,932	\$4,932	\$4,932	\$4,932	\$4,932	\$4,932	\$4,932	\$4,932	\$4,932
Treatment Plant Expansion												
General Requirements	\$1,945	\$1,285	\$1,824	\$4,063	\$4,230	\$1,424	\$4,518	\$4,518	\$4,518	\$4,518	\$4,518	\$4,518
Site Structures/On-Site Piping	\$4,421	\$3,016	\$3,418	\$4,224	\$4,110	\$6,493	\$4,371	\$4,883	\$4,883	\$4,883	\$4,883	\$4,883
Access	\$2,330	\$2,488	\$2,281	\$3,812	\$1,730	\$2,544	\$3,812	\$1,230	\$1,230	\$1,230	\$1,230	\$1,230
Utilities	\$8,281	\$1,538	\$4,101	\$11,138	\$10,496	\$18,201	\$12,118	\$12,118	\$12,118	\$12,118	\$12,118	\$12,118
Construction (Pumping)	\$1,831	\$1,311	\$2,348	\$2,793	\$2,508	\$3,684	\$3,684	\$3,684	\$3,684	\$3,684	\$3,684	\$3,684
Construction	\$0	\$0	\$1,909	\$0	\$0	\$1,865	\$0	\$0	\$0	\$0	\$0	\$0
High Voltage Piping	\$2,278	\$2,278	\$2,278	\$4,345	\$4,418	\$4,418	\$7,238	\$7,238	\$7,238	\$7,238	\$7,238	\$7,238
Optical Fiber Systems	\$1,748	\$1,848	\$1,328	\$3,362	\$2,014	\$2,760	\$2,512	\$4,418	\$4,418	\$4,418	\$4,418	\$4,418
Electrical and Instrumentation	\$5,138	\$3,403	\$3,375	\$7,367	\$4,135	\$8,723	\$4,135	\$4,135	\$4,135	\$4,135	\$4,135	\$4,135
Treatment Plant Subtotal	\$27,858	\$28,771	\$30,271	\$56,287	\$57,628	\$71,098	\$64,108	\$64,108	\$64,108	\$64,108	\$64,108	\$64,108
Construction Total	\$31,728	\$34,151	\$34,641	\$61,219	\$61,638	\$81,656	\$71,703	\$71,703	\$71,703	\$71,703	\$71,703	\$71,703
Engineering/Administration	\$3,971	\$5,425	\$4,112	\$11,052	\$10,293	\$21,248	\$10,750	\$11,293	\$11,293	\$11,293	\$11,293	\$11,293
PROJECT TOTAL	\$39,727	\$45,927	\$48,994	\$82,532	\$81,969	\$104,960	\$82,454	\$82,454	\$82,454	\$82,454	\$82,454	\$82,454



2016 Condition Assessment

Columbia Water and Light - 2016 CONDITION ASSESSMENT REPORT

Table 9-5 provides an implementation schedule for the recommended enhancement alternatives identified in Section 9.

Table 9-5-1 Recommended Implementation Schedule

ALTERNATIVE	2016	2017	2018	2019	2020
Wells	\$1,640	\$1,640	\$1,640	\$1,640	\$1,640
Riser Water Piping	\$2,730	\$2,730	\$2,730	\$2,730	\$2,730
Water Supply Construction Total	\$4,370	\$4,370	\$4,370	\$4,370	\$4,370
General Requirements	\$1,945	\$1,285	\$1,824	\$4,063	\$4,230
Site Structures/On-Site Piping	\$4,421	\$3,016	\$3,418	\$4,224	\$4,110
Access	\$2,330	\$2,488	\$2,281	\$3,812	\$1,730
Utilities	\$8,281	\$1,538	\$4,101	\$11,138	\$10,496
Construction (Pumping)	\$1,831	\$1,311	\$2,348	\$2,793	\$2,508
Construction	\$0	\$0	\$1,909	\$0	\$0
High Voltage Piping	\$2,278	\$2,278	\$2,278	\$4,345	\$4,418
Optical Fiber Systems	\$1,748	\$1,848	\$1,328	\$3,362	\$2,014
Electrical and Instrumentation	\$5,138	\$3,403	\$3,375	\$7,367	\$4,135
Treatment Plant Subtotal	\$27,858	\$28,771	\$30,271	\$56,287	\$57,628
Construction Total	\$31,728	\$34,151	\$34,641	\$61,219	\$61,638
Engineering/Administration	\$3,971	\$5,425	\$4,112	\$11,052	\$10,293
PROJECT TOTAL	\$39,727	\$45,927	\$48,994	\$82,532	\$81,969

Table 9-5-2 Recommended Implementation Schedule

ALTERNATIVE	2016	2017	2018	2019	2020
Wells	\$1,640	\$1,640	\$1,640	\$1,640	\$1,640
Riser Water Piping	\$2,730	\$2,730	\$2,730	\$2,730	\$2,730
Water Supply Construction Total	\$4,370	\$4,370	\$4,370	\$4,370	\$4,370
General Requirements	\$1,945	\$1,285	\$1,824	\$4,063	\$4,230
Site Structures/On-Site Piping	\$4,421	\$3,016	\$3,418	\$4,224	\$4,110
Access	\$2,330	\$2,488	\$2,281	\$3,812	\$1,730
Utilities	\$8,281	\$1,538	\$4,101	\$11,138	\$10,496
Construction (Pumping)	\$1,831	\$1,311	\$2,348	\$2,793	\$2,508
Construction	\$0	\$0	\$1,909	\$0	\$0
High Voltage Piping	\$2,278	\$2,278	\$2,278	\$4,345	\$4,418
Optical Fiber Systems	\$1,748	\$1,848	\$1,328	\$3,362	\$2,014
Electrical and Instrumentation	\$5,138	\$3,403	\$3,375	\$7,367	\$4,135
Treatment Plant Subtotal	\$27,858	\$28,771	\$30,271	\$56,287	\$57,628
Construction Total	\$31,728	\$34,151	\$34,641	\$61,219	\$61,638
Engineering/Administration	\$3,971	\$5,425	\$4,112	\$11,052	\$10,293
PROJECT TOTAL	\$39,727	\$45,927	\$48,994	\$82,532	\$81,969

2016 Condition Assessment

Columbia Water and Light - 2016 CONDITION ASSESSMENT REPORT

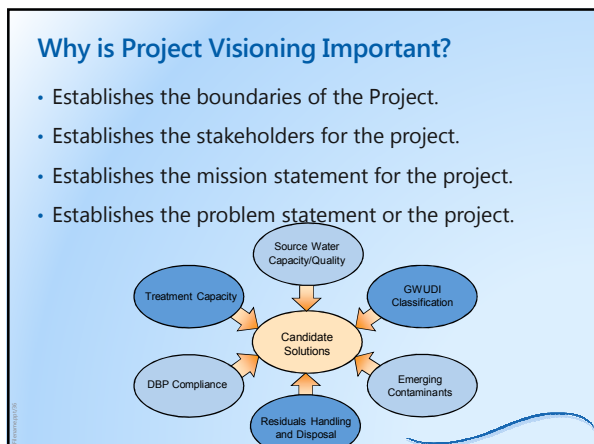
Table 9-6 provides an implementation schedule for the recommended enhancement alternatives identified in Section 9.

Table 9-6-1 Recommended Implementation Schedule

ALTERNATIVE	2016	2017	2018	2019	2020
Wells	\$1,640	\$1,640	\$1,640	\$1,640	\$1,640
Riser Water Piping	\$2,730	\$2,730	\$2,730	\$2,730	\$2,730
Water Supply Construction Total	\$4,370	\$4,370	\$4,370	\$4,370	\$4,370
General Requirements	\$1,945	\$1,285	\$1,824	\$4,063	\$4,230
Site Structures/On-Site Piping	\$4,421	\$3,016	\$3,418	\$4,224	\$4,110
Access	\$2,330	\$2,488	\$2,281	\$3,812	\$1,730
Utilities	\$8,281	\$1,538	\$4,101	\$11,138	\$10,496
Construction (Pumping)	\$1,831	\$1,311	\$2,348	\$2,793	\$2,508
Construction	\$0	\$0	\$1,909	\$0	\$0
High Voltage Piping	\$2,278	\$2,278	\$2,278	\$4,345	\$4,418
Optical Fiber Systems	\$1,748	\$1,848	\$1,328	\$3,362	\$2,014
Electrical and Instrumentation	\$5,138	\$3,403	\$3,375	\$7,367	\$4,135
Treatment Plant Subtotal	\$27,858	\$28,771	\$30,271	\$56,287	\$57,628
Construction Total	\$31,728	\$34,151	\$34,641	\$61,219	\$61,638
Engineering/Administration	\$3,971	\$5,425	\$4,112	\$11,052	\$10,293
PROJECT TOTAL	\$39,727	\$45,927	\$48,994	\$82,532	\$81,969







Project Visioning – Defining Sustained and Tipping Point Capacities



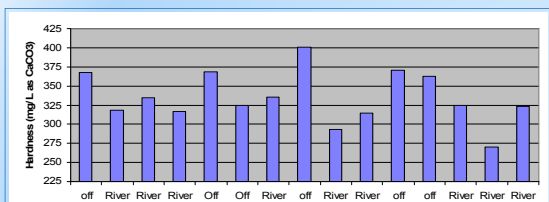
Project Visioning – Attaining GWUDI Compliance @ McBaine

- Turbidity Removal
- Disinfection By Product Precursor Removal
- Disinfection

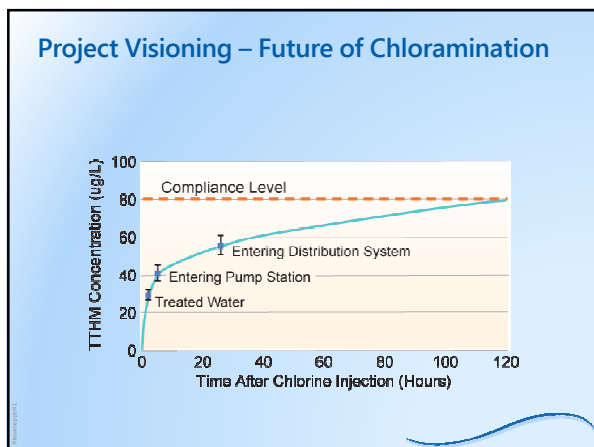
Comparison of Groundwater versus Surface Water or GWUDI Monthly Reporting Requirements

Parameter	Groundwater Reporting	Surface Water or GWUDI Reporting
Water Temperature	+	+
Water Turbidity	+	+
Water Chlorine Residual	+	+
Water Chlorine Dioxide Residual	+	+
Water pH	+	+
Water Total Hardness	+	+
Water Total Dissolved Solids	+	+
Water Total Suspended Solids	+	+
Water Total Phosphate	+	+
Water Total Nitrate	+	+
Water Total Ammonia Nitrogen	+	+
Water Total Nitrite	+	+
Water Total Nitrogen	+	+
Water Total Phosphorus	+	+
Water Total Copper	+	+
Water Total Lead	+	+
Water Total Cadmium	+	+
Water Total Chromium	+	+
Water Total Manganese	+	+
Water Total Zinc	+	+
Water Total Barium	+	+
Water Total Selenium	+	+
Water Total Silver	+	+
Water Total Mercury	+	+
Water Total Arsenic	+	+
Water Total Boron	+	+
Water Total Fluoride	+	+
Water Total Chloride	+	+
Water Total Sulfate	+	+
Water Total Iron	+	+
Water Total Aluminum	+	+
Water Total Silicon	+	+
Water Total Calcium	+	+
Water Total Magnesium	+	+
Water Total Potassium	+	+
Water Total Sodium	+	+
Water Total Chlorine	+	+
Water Total Bromine	+	+
Water Total Iodine	+	+
Water Total Fluorine	+	+
Water Total Phosphorus	+	+
Water Total Nitrogen	+	+
Water Total Ammonia Nitrogen	+	+
Water Total Nitrite	+	+
Water Total Nitrate	+	+
Water Total Phosphate	+	+
Water Total Copper	+	+
Water Total Lead	+	+
Water Total Cadmium	+	+
Water Total Chromium	+	+
Water Total Manganese	+	+
Water Total Zinc	+	+
Water Total Barium	+	+
Water Total Selenium	+	+
Water Total Silver	+	+
Water Total Mercury	+	+
Water Total Arsenic	+	+
Water Total Boron	+	+
Water Total Fluoride	+	+
Water Total Chloride	+	+
Water Total Sulfate	+	+
Water Total Iron	+	+
Water Total Aluminum	+	+
Water Total Silicon	+	+
Water Total Calcium	+	+
Water Total Magnesium	+	+
Water Total Potassium	+	+
Water Total Sodium	+	+

Project Visioning – Continue Softening Goals







Project Visioning – Future of Existing Water Source

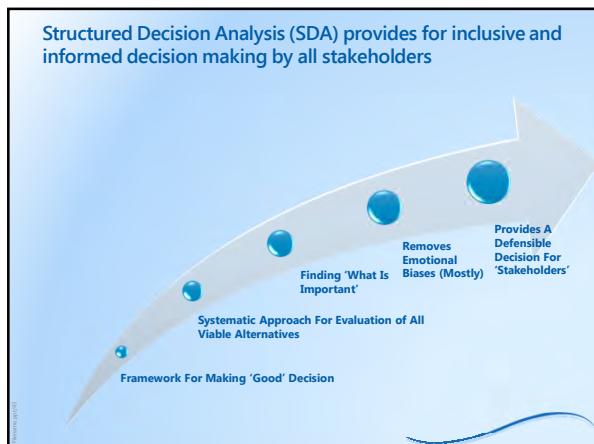
Ground Water Flow, 2004-05, and Water Quality, 1992-2007, in the East System, Columbia, Missouri

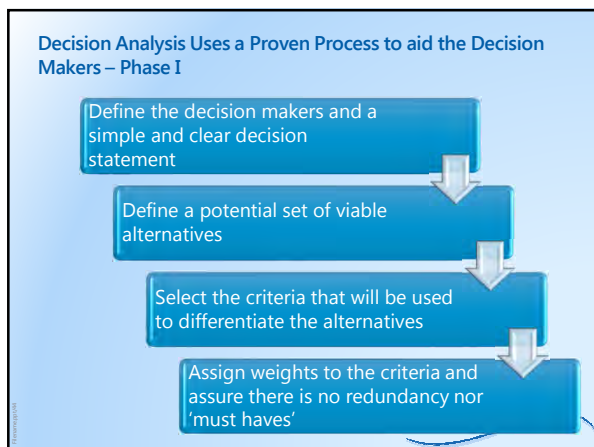
Table 2. Pharmaceutical compounds analyzed, minimum reporting limit, and concentration in samples from the city surface and monitoring wells, MGS and others, 2007.

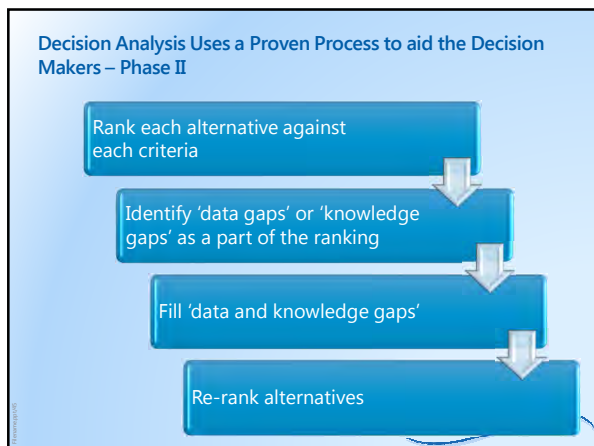
(MLD concentrations are in micrograms per liter (µg/L), and MRLs are in micrograms per liter (µg/L))

Compound	Minimum reporting limit	Detected in city surface sample (µg/L concentration)	Detected in monitoring well samples (µg/L concentration)
1,3-Dichlorobenzene	0.024	0.114	MRL (ML, 0.000)
Acetaminophen	0.05	—	MRL (ML, 0.000)
Caffeine	0.08	—	MRL (ML, 0.000)
Chloroacetylene	0.02	0.025	MRL (ML, 0.000)
Clozapine	0.02	—	—
Diazepam	0.04	—	MRL (ML, 0.000)
Diphenhydramine	0.04	—	—
Ethanol	0.04	—	—
Fluoxetine	0.05	—	—
Hydrochloric acid	0.04	—	—
Hydrocodone bitartrate	0.04	0.118	—
Hydroxyacetone	0.05	—	—
Hydroxybenzoin	0.06	—	—
Propylgallate	0.04	—	—
Warfarin	0.07	0.06	MRL (ML, 0.000)

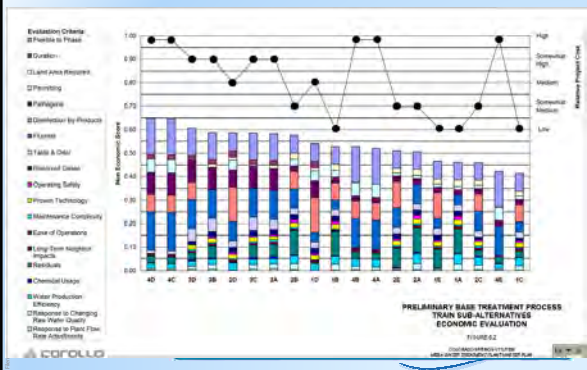
A water or wastewater issue? (EDC's, Pharm, Nitrate, etc.)







Decision Analysis Uses a Proven Process to aid the Decision Makers – Phase III



Define Project Stakeholders and Discuss Roles

Define Project Stakeholders and Discuss Roles

Discuss/Review Contents of Visioning Questionnaire

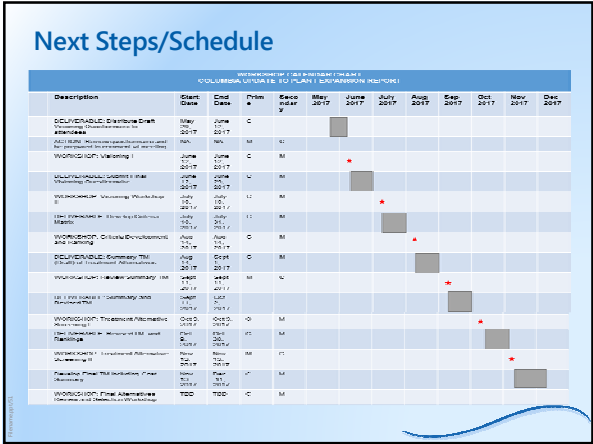
- Plant Capacity
- Potential Alternate Plant Site Locations
- Chloramination Future
- Microcontaminant Removal Future
- Facilities That Are Not to be Retained
- Limitation of existing facility
- Budget/Schedule Constraints
- Others?

Discuss/Review Contents of Visioning Questionnaire

- Plant Capacity
- Potential Alternate Plant Site Locations
- Chloramination Future
- Microcontaminant Removal Future
- Facilities That Are Not to be Retained
- Limitation of existing facility
- Budget/Schedule Constraints
- Others?











Appendix C

SUMMARY OF VISIONING QUESTIONNAIRE AND RESULTS

VISIONING QUESTIONNAIRE

PART I - PURPOSE AND INSTRUCTIONS

The purpose of this questionnaire is to establish a vision and identify the boundaries for the Drinking Water Planning Group to assist in the update of the 2011 Water Treatment Plant Preliminary Design Report. As someone who has been identified by the Columbia Water and Light Department as a stakeholder in this process, your input is of value and will result in a more thorough and comprehensive update. Please feel free to attach any additional information to this form. **Please only answer questions in areas that you are familiar with or have knowledge about.**

Any questions regarding this form should be addressed to **Thomas Crowley at tcrowley@carollo.com.**

We will collect and Review this information as part of our Visioning and Kickoff Workshop II to be Conducted On **August 14, 2017.**

PART II – RESPONDENT INFORMATION

1. Please provide the information below regarding the respondent:

Name:

Title:

Occupation:

Phone:

Fax:

Date:

2. Please provide a brief description of your goals for the project.

PART III - QUESTIONNAIRE

Water Treatment Plant Configuration:

1. To reduce anticipated operational expenses, should the current treatment goals to soften the water be abandoned in favor of less expensive treatment measures? (This may cause some consumers to install in-home water softeners)

- Continue Softening Treatment Goals
- Discontinue Softening Treatment Goals

Please list the reasons for your selection:

2. The secondary regulations concern the aesthetic aspects of a drinking water supply rather than the health aspects. Should any new treatment processes consider satisfying the current secondary regulations (suggested limits) as well as the primary regulations (required by law)? Satisfying the secondary regulations is currently done at the existing facilities.

- Continue Satisfying Secondary Suggested Limits for Aesthetic Properties
- Discontinue Satisfying Secondary Suggested Limits for Aesthetic Properties

Please list the reasons for your selection:

**City of Columbia, MO WTP
Visioning Questionnaire**

Water Treatment Plant Configuration (cont.):

3. Should the study examine abandoning and demolishing the existing water treatment plant (32 mgd) and constructing an entirely new facility with source water obtained from a different location at a significant cost to current and future customers?

Existing Supply and Treatment Plant Should be abandoned

Continue Use of Current Source and Treatment Facility

Please list the reasons for your selection:

4. The end of this questionnaire provides a glossary of the advanced treatment technology and the potential benefits this technology would provide. Please select which of these advanced technologies you would like to see the study address. Please list the reasons for your selections.

Membrane Filtration

Air Stripping

Nano/Reverse Osmosis

Enhanced Softening

Advanced Oxidation

All of the Above

Ion Exchange

Others (Please List Below)

Advanced Disinfection

Ozone/Infiltration

Advanced Biofiltration

Please list the reasons for your selection:

Water Treatment Plant Configuration (cont.):

5. To satisfy regulations associated with disinfection by products, the City of Columbia converted from free chlorine to chloramines in the distribution system and conducts periodic conversions to chlorine to avoid issues that are associated with nitrification. There are more costly technologies that can be employed to satisfy all disinfection by product regulations **and** permit switching back to chlorine. Given this, how important is it to you that the City of Columbia switches back to the exclusive use of free chlorine in the distribution system? Please state the reasons for your selection:

- Absolutely Critical to Switch Back to Chlorine
- Very Important to Switch Back to Chlorine
- Not Very Important
- Stay with Chloramines
- Other (Please list) _____

In the space allotted below please state your reasons for the selection made above:

Water Treatment Plant Configuration (cont.):

6. Past investigations of surface water and groundwater sources in Missouri and throughout the country have detected the presence of extremely low levels (one drop in 20 Olympic swimming pools) of Endocrine Disrupting (estrogen, etc) and Pharmaceutical (acetaminophen, etc.) compounds in many drinking water supplies. Studies to determine if long-term exposure to the low concentrations of these constituents impact human health are at least 10+ years away and it is not certain when (if at all) some or all of these constituents will be regulated. Technologies that remove or destroy these compounds from the supply are available but are significantly more costly to implement than the current treatment process. Given this, how important is it to you that this study considers processes that remove or destroy these compounds? Please state the reasons for your selection.

- Absolutely Critical to Remove or Destroy these Compounds No Matter the Expense.
- Study Should Evaluate the Costs/Benefits of Technologies that Remove or Destroy these Compounds.
- Not Very Important that Study Considers Removal/Destruction of these Compounds.
- Study **Should Not** Consider Removal/Destruction of these Compounds.
- Other (Please list)_____

In the space allotted below please state your reasons for the selection made above:

**City of Columbia, MO WTP
Visioning Questionnaire**

Water Treatment Plant Configuration (cont.):

7. Green elements at a water facility are elements that minimize chemical use and maximize energy efficiency. Should a “green” element be a consideration for ranking and analysis of treatment alternatives?

- Yes
- No
- Other (Please List) _____

In the space allotted below please list the reasons for your response:

8. Are there any other issues regarding treatment that should be addressed?

- Yes (please list) _____
- No

In the space allotted below please list the reasons for your response:

**City of Columbia, MO WTP
Visioning Questionnaire**

*****END OF QUESTIONNAIRE*****

PART IV GLOSSARY OF WATER TREATMENT TECHNOLOGIES

- Advanced Biofiltration:** Technologies that utilize an exterior carbon source and other nutrients in lieu of Ozone to establish and maintain a biofiltration process (a filter bed laden with microorganisms that break down organic matter into carbon dioxide, water and salts). These processes have proven effective in reducing the extremely low levels (one drop in 20 Olympic swimming pools) of some Endocrine Disrupting (estrogen, etc) and Pharmaceutical (acetaminophen, etc.) compounds found in many of the nations drinking water supplies. This treatment may provide enhanced removal of disinfection by product precursors and may permit the re-establishment of free chlorine as a secondary (distribution) system disinfectant.
- Advanced Disinfection:** Technologies (Ozone, chlorine dioxide, UV, low pressure membrane filtration) that are approved by the US EPA to provide primary disinfection of drinking water that meet or exceed national standards without the use of free chlorine. This does not eliminate the use of chlorination in the process. Chlorination or Chloramination will be required by the Missouri Department of Natural resources following this process to produce a measurable residual disinfectant in the distribution system. Some of these technologies may provide enhanced removal of disinfection by product precursors and may permit the re-establishment of free chlorine as a secondary (distribution) system disinfectant.
- Advanced Oxidation:** The process of adding or generating powerful oxidants to oxidize trace levels of organic or microbiological organisms in water. These processes have proven effective in reducing the extremely low levels (one drop in 20 Olympic swimming pools) of some Endocrine Disrupting (estrogen, etc) and Pharmaceutical (acetaminophen, etc.) compounds found in many of the nations drinking water supplies.
- Air Stripping:** Technologies involving the transferring of volatile components of a liquid into an air stream. Some of the disinfection by-products generated from drinking water chlorination can be safely removed from drinking water through this process. This treatment may provide enhanced removal of disinfection by products and may permit the re-establishment of free chlorine as a secondary (distribution) system disinfectant.
- Enhanced Softening:** The process of adding an excess of alkaline agent (lime, caustic soda, etc.) to water to remove hardness (calcium and magnesium ions) via precipitation. This treatment may provide enhanced removal of disinfection by product precursors and may permit the re-establishment of free chlorine as both a primary and secondary (distribution) system disinfectant.

PART IV GLOSSARY OF WATER TREATMENT TECHNOLOGIES (CONT.)

- Ion Exchange: A reversible chemical reaction between an insoluble solid and a solution during which ions may be interchanged. This separation process, as it applies to Columbia, would be to examine fixed bed or dispersed magnetic resins to fix some organic ions to the resins. This treatment may provide enhanced removal of disinfection by product precursors and may permit the re-establishment of free chlorine as both a primary and secondary (distribution) system disinfectant.
- Ozone/Biofiltration: A combined water treatment process to reduce natural organic matter (NOM) which is a water disinfectant byproduct precursor. Water is first assonated (ozone is mixed into the water flow to oxidize organic matter, iron and manganese) and then passed through a biofilter (a filter bed laden with microorganisms that break down organic matter into carbon dioxide, water and salts). These processes have proven effective in reducing the extremely low levels (one drop in 20 Olympic swimming pools) of some Endocrine Disrupting (estrogen, etc) and Pharmaceutical (acetaminophen, etc.) compounds found in many of the nations drinking water supplies. This treatment may provide enhanced removal of disinfection by product precursors and may permit the re-establishment of free chlorine as a secondary (distribution) system disinfectant.
- Micro/Ultra Filtration: Water under moderate pressure (25-50 psig) is forced through a membrane, a thin material with very small pores, stopping small particles (including bacteria). This is proven to provide an effective barrier to most pathogens but is not effective in removing ions (softening) or most organic compounds.
- Nano/Reverse Osmosis: Water under high pressure (75-120 psig) is forced through a membrane using a separation process that employs the principles of reverse osmosis to remove dissolved contaminants from water; typically applied for membrane softening or the removal of dissolved organic contaminants. This treatment may provide enhanced removal of disinfection by product precursors and may permit the re-establishment of free chlorine as both a primary and secondary (distribution) system disinfectant. In addition, these processes have proven effective in reducing the extremely low levels (one drop in 20 Olympic swimming pools) of some Endocrine Disrupting (estrogen, etc) and Pharmaceutical (acetaminophen, etc.) compounds found in many of the nations drinking water supplies.

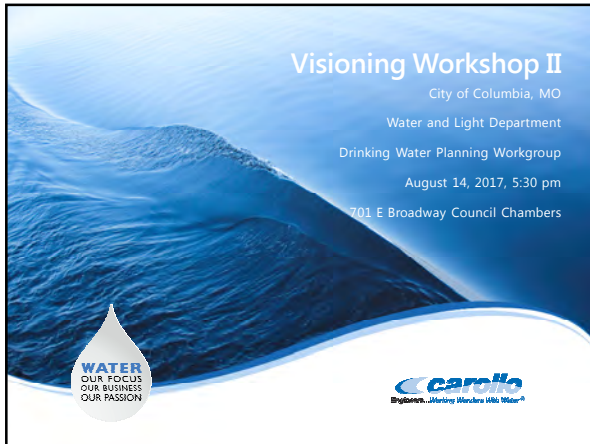
PART IV GLOSSARY OF WATER TREATMENT TECHNOLOGIES (CONT.)

Softening (precipitative): The process of adding an alkaline agent (lime, caustic soda, etc.) to water to remove hardness (calcium) via precipitation. This is done to reduce scaling in water heaters and otherwise improve other aesthetic aspects of drinking water.

Ion Exchange: A reversible chemical reaction between an insoluble solid and a solution during which ions may be interchanged. This separation process, as it applies to Columbia, would be to examine fixed bed or dispersed magnetic resins to fix some organic ions to the resins. This treatment may provide enhanced removal of disinfection by product precursors and may permit the re-establishment of free chlorine as both a primary and secondary (distribution) system disinfectant.

Appendix D

SUMMARY OF VISIONING WORKSHOPS



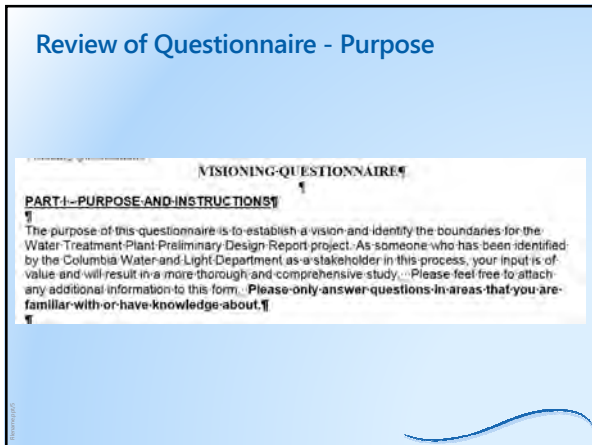
Workshop Agenda

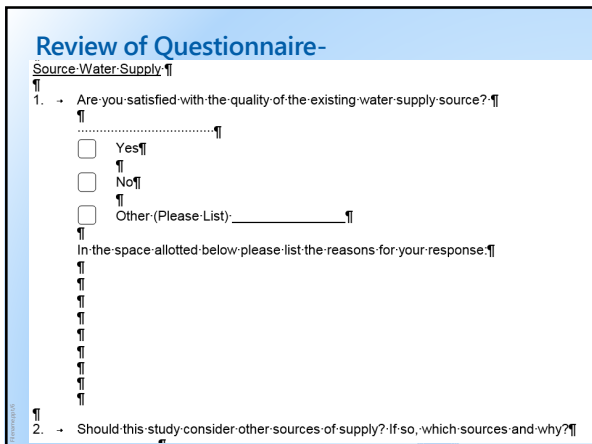
- Review of Questionnaire
- Treatment Technologies Overview
- Primary and Secondary Drinking Water Regulations
- Softening Presentation
- CEC Presentation
- Disinfection By Products Presentation
- Treatment Technologies Overview
- Review Action/Decision Logs
- Review Next Steps
- General Comments by Public, Members, and Staff
- Next Meeting Date

Draft Mission Statement of Planning Workgroup

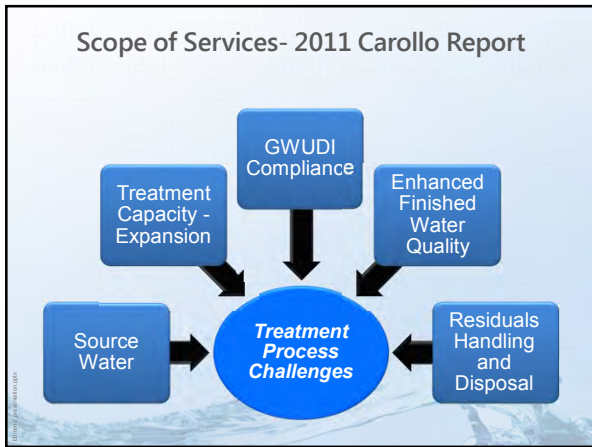
- "To enhance the quality of life for Columbia, Missouri Citizens by providing direction to Columbia Water and Light on the best means to continue its mission to provide at an affordable price; high-quality water and dependable service that exceeds customer expectations; protects and ensures a long-term water supply for future generations; and serves as responsible stewards of public health, utility resources, and the environment."

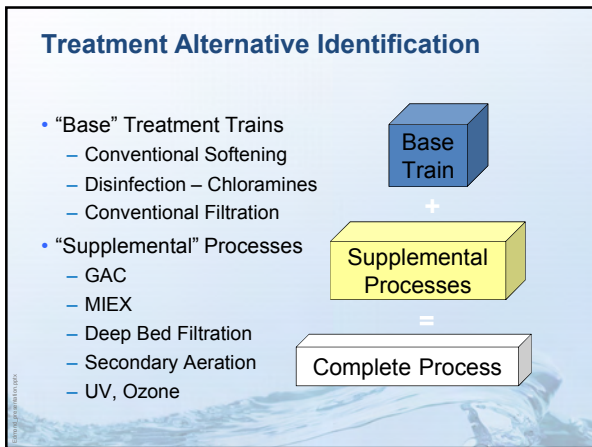














Primary Drinking Water Regulations

- What are primary Drinking water regulations and how do they vary based upon source water classification?
- What are Secondary Drinking Water Regulations?

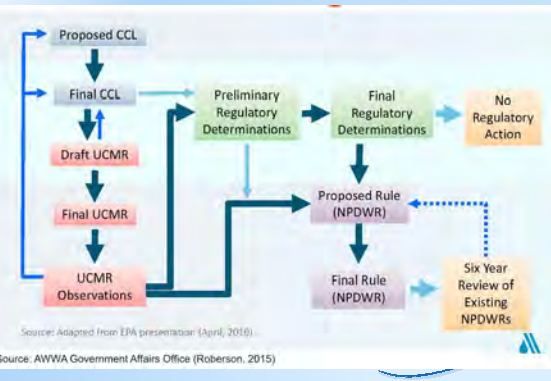
Primary Drinking Water Standards

- The National **Primary Drinking Water Regulations** (NPDWR) are legally enforceable **primary standards** and treatment techniques that apply to public **water** systems. **Primary standards** and treatment techniques protect public health by limiting the levels of contaminants in **drinking water**.
- These levels are based on consideration of health risks, technical feasibility of treatment, and cost-benefit analysis. (MCLs) which are established to protect the public against consumption of drinking water contaminants that present a risk to human health. An MCL is the maximum allowable amount of a contaminant in drinking water which is delivered to the consumer.

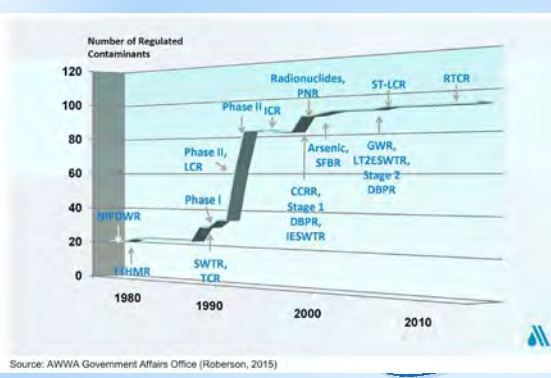
Primary Drinking Water Standards – EPA Regulatory Framework

- Under the Safe Drinking Water Act, promulgated in 1974, the USEPA has established drinking water regulations for more than 90 contaminants
- 1986 amendments:
 - Required that EPA review existing regulations every six years, termed the “Six year Review” process
 - Established the Contaminant Candidate List (CCL) process for identifying new contaminants for regulatory determination every five years

SDWQ Standard Setting Process



SDWA Regulatory Timeline



Contaminant Candidate List Process

	Year Published	Contaminants Included	Regulatory Determinations
CCL1	1998	• 10 microbial • 50 chemical	• Not to regulate 8 chemicals (incl. manganese) and 1 microorganism (<i>Acanthamoeba</i>)
CCL2	2005	• 9 microbial • 42 chemical	• Not to regulate 11 chemicals; • More information needed on perchlorate
CCL3	2009	• 12 microbial • 104 chemicals	• Preliminary determination to regulate strontium • Not to regulate 4 chemicals

Primary Drinking Water Regulations

- What are primary Drinking water regulations and **how do they vary based upon source water classification?**
- What are Secondary Drinking Water Regulations?

Difference Between GWUDI and GW Boils Down to Three Major Parameters

Comparison of Groundwater versus Surface Water or CWUDI Measurement Reporting Requirements	Groundwater	Surface Water or CWUDI
Turbidity Reporting Requirements	✓	✓
Microbial Reporting Requirements	✓	✓
Chlorination Disinfection Byproduct Reporting	✓	✓
Lead Reporting Requirements	✓	✓
Copper Reporting Requirements	✓	✓
Chloride Reporting Requirements	✓	✓
Fluoride Reporting Requirements	✓	✓
Iron Reporting Requirements	✓	✓
Manganese Reporting Requirements	✓	✓
Nitrate Reporting Requirements	✓	✓
Radon Reporting Requirements	✓	✓
Sulfate Reporting Requirements	✓	✓
Total Dissolved Solids Reporting Requirements	✓	✓
Total Hardness Reporting Requirements	✓	✓
Total Suspended Solids Reporting Requirements	✓	✓
Total Chlorine Reporting Requirements	✓	✓
Total Chlorine Demand Reporting Requirements	✓	✓
Total Chlorine Residual Reporting Requirements	✓	✓
Total Chlorine Residual Chlorine Demand Reporting Requirements	✓	✓

- Turbidity Removal
- Disinfection By Product Precursor Removal
- Disinfection

Primary Drinking Water Regulations

- What are primary Drinking water regulations and how do they vary based upon source water classification?
- **What are Secondary Drinking Water Regulations?**

Notable Regulations – Safe Drinking Water Act

- EPA has established National Secondary Drinking Water Regulations (NSDWRs) that set non-mandatory water quality standards for 15 contaminants. EPA does not enforce these "secondary maximum contaminant levels" (SMCLs). They are established as guidelines to assist public water systems in managing their drinking water for aesthetic considerations, such as taste, color, and odor. These contaminants are not considered to present a risk to human health at the SMCL.
- While SMCLs are not federally enforceable, EPA requires a special notice for exceedance of the fluoride SMCL of 2.0 mg/L. Community water systems that exceed the fluoride SMCL of 2 mg/L, but do not exceed the MCL of 4.0 mg/L for fluoride, must provide public notice to persons served no later than 12 months from the day the water system learns of the exceedance (40 CFR 141.208).

Secondary Standard Philosophy

- These problems can be grouped into three categories:
 - Aesthetic effects — undesirable tastes or odors;
 - Cosmetic effects — effects which do not damage the body but are still undesirable
 - Technical effects — damage to water equipment or reduced effectiveness of treatment for other contaminants

Table of Secondary Standards		
Contaminant	Secondary MCL	Noticeable Effects above the Secondary MCL
Aluminum	0.05 to 0.2 mg/L*	colored water
Chloride	250 mg/L	salty taste
Color	15 color units	visible tint
Copper	1.0 mg/L	metallic taste; blue-green staining
Corrosivity	Non-corrosive	metallic taste; corroded pipes/ fixtures staining
Fluoride	2.0 mg/L	tooth discoloration
Foaming agents	0.5 mg/L	frothy, cloudy; bitter taste; odor
Iron	0.3 mg/L	rusty color; sediment; metallic taste; reddish or orange staining
Manganese	0.05 mg/L	black to brown color; black staining; bitter metallic taste
Odor	3 TON (threshold odor number)	"rotten-egg", musty or chemical smell
pH	6.5 - 8.5	low pH: bitter metallic taste; corrosion high pH: slippery feel; soda taste; deposits
Silver	0.1 mg/L	skin discoloration; graying of the white part of the eye
Sulfate	250 mg/L	salty taste
Total Dissolved Solids (TDS)	500 mg/L	hardness; deposits; colored water; staining; salty taste
Zinc	5 mg/L	metallic taste

Continue Secondary Standards

2. - The secondary regulations concern the aesthetic aspects of a drinking water supply rather than the health aspects. Should any new treatment processes consider satisfying the current secondary regulations (suggested limits) as well as the primary regulations (required by law)? Satisfying the secondary regulations is currently done at the existing facilities.

Continue Satisfying Secondary Suggested Limits for Aesthetic Properties

Discontinue Satisfying Secondary Suggested Limits for Aesthetic Properties

Please list the reasons for your selection:

Softening Presentation

Softening in Visioning Workshop

1. To reduce anticipated operational expenses, should the current treatment goals to soften the water be abandoned in favor of less expensive treatment measures? (This may cause some consumers to install in-home water softeners?)

Continue Softening Treatment Goals

Discontinue Softening Treatment Goals

Please list the reasons for your selection.

Softening Basics

- Removal of Calcium and Magnesium
 - Divalent cations

CONCENTRATION OF DIATOMS AS CALCIUM CARBONATE IN MILLIGRAMS PER LITER

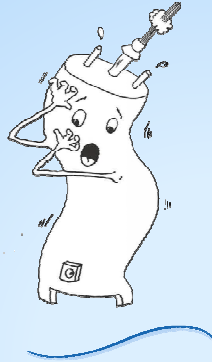
USGS 2005 Streamflow

Why Remove Hardness ?

- Aesthetics
 - American Institute of Laundering
 - Costs are 2X for hard versus soft
 - Synthetic detergents
 - Better than fatty acids (basic)
 - Builders - consumed by hard water
 - Purdue University
 - Fabrics - wear out 15% quicker
 - Colors fade
 - Whites darken
 - Reduced equipment life
 - 30% reduction - washing machines
 - Hot water heaters

Water Hardness is a Balance for Hot Water Heaters

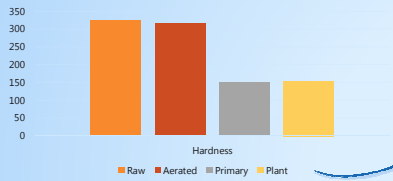
- Low hardness – Corrosion
 - Soft water 2x or 3X anode consumption
- Hard water – Calcium carbonate build up
 - Slows heat transfer – overheating of tank bottom
 - Over temperature – dissolved glass
 - Insulates tank from anode



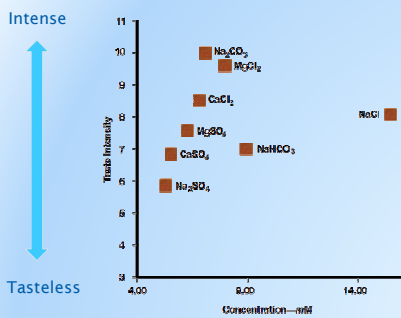
What is Considered Soft ?

Hardness Range (mg/L as CaCO ₃)	Hardness Description
0-75	Soft
75-150	Moderately Hard
150-300	Hard
> 300	Very Hard

1 grains of CaCO₃/gallon = 17.1 mg/L



When Do Customers Complain ?



When Do Customers Complain ?

Potability Grade	TDS mg/L
Excellent	< 100
Good	101-300
Fair	301-700
Poor	701-1,000
Unacceptable	> 1,001

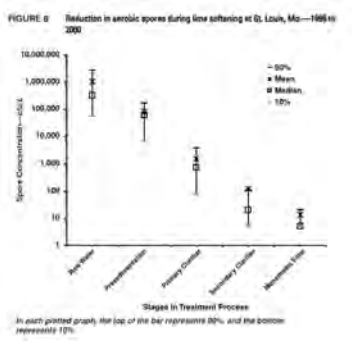
Variability of water quality and temperature have big effects

What can Softening Do ?

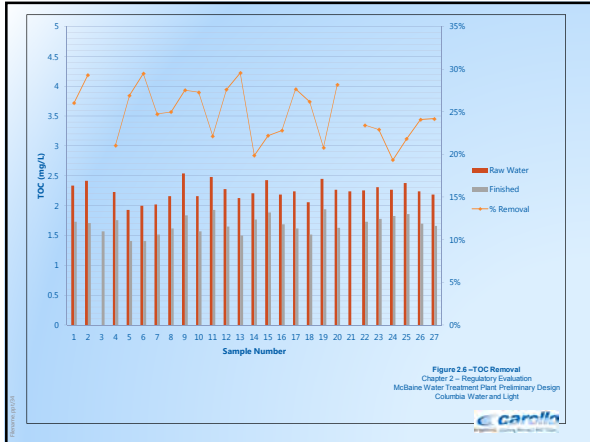
- Removes
 - Hardness
 - Heavy metals (lead, cadmium, copper, zinc, chromium mercury, arsenic)
 - Barium
 - Silica
 - Fluoride
 - Iron
 - Manganese
 - Turbidity
 - Organics (color)
 - Oil
 - Algae, bacteria and viruses
 - Radium, uranium, gross alpha, beta
 - Reduces corrosion
 - Will not remove Iocane

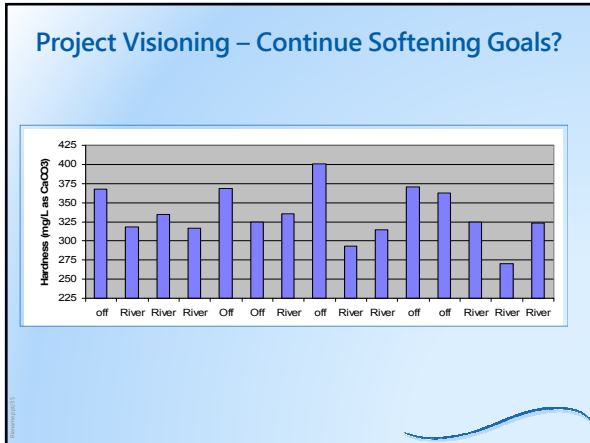


Pathogen Removal Is Significant in Softening Process



LT2ESWTR grants an additional 0.5 log Cryptosporidium Removal







Contaminant Candidate List Process

Draft CCL4 – February 14, 2015

- Remainders from CCL3, minus
 - Positives for perchlorate (2011) and strontium (preliminary 2014)
 - Four negative preliminary determinations in 2014
- 110 chemical contaminants, including
 - Cyanotoxins
 - Manganese
- 12 microbial contaminants

UCMR Monitoring Approach

Monitoring Frequency:

- GW systems: 2x in a year
- SW systems: Quarterly in a year
- UCMR4 will follow seasonal sampling approach for cyanotoxins

Monitoring Locations:

- Can vary depending on contaminant
- UCMR1 – all entry points
- UCMR2 – included distribution system samples for nitrosamines
- UCMR3 – included distribution system samples for Cr(VI)

CWS Participants:

- List 1 monitored in all PWSs serving more than 10,000 people and a subset (800) of PWSs serving less than 10,000
- List 2 monitored in all PWSs serving more than 100,000 people and subset of PWSs serving less people

UCMR4 – Monitoring between 2018 - 2020

Contaminant	Sampling Point(s)	Method
Cyanotoxins: total microcystin & 5 congeners, anatoxin-a, cylindrospermopsin, nodularin	Entry point	EPA 546, EPA 544 and 545
Germanium	Entry point	EPA 200.8, SM 3125
Manganese	Entry point	EPA 525.3
8 pesticides	Entry point	EPA 541
3 alcohols	Entry point	EPA 530
3 other semivolatle compounds	Entry point	EPA 552.3 or 557
3 brominated DBPs ¹ & indicator compounds ²	Distribution system	

¹ HAA5, HAA6Br, HAA9
² TOC, bromide, temperature and pH

3rd Six Year Review Identified 8 NPDWRs for Regulatory Revision

- Stage 1 and 2 D/DBPR (TTHM, HAA5, Chlorite)
- *Cryptosporidium*
- Heterotrophic Bacteria
- *Giardia lamblia*
- *Legionella*
- Viruses

<https://www.epa.gov/dwsixyearreview/six-year-review-3-drinking-water-standards>

Executive Order 13771 and 13777 on Reducing Regulatory Burden

- January 30, 2017 EO 13771 Reducing Regulation and Controlling Regulatory Costs
 - Any new regulation must be coupled with two de-regulations
- February 24, 2017 EO 13777
 - Within 60 days of order, agencies must designate Regulatory Reform Officers to oversee regulatory reform initiatives, including compliance with EO 13771

<https://www.whitehouse.gov/the-press-office/2017/02/24/presidential-executive-order-enforcing-regulatory-reform-agenda>

Regulatory Horizon

Contaminant	Regulatory Framework	Probability*
Perchlorate	2011 decision to regulate; NRDC settlement	Likely
Lead	Proposed Long Term-LCR rule expected 2017	Likely
Cyanotoxins	2015 health advisories (HA); UCMR4; CCL4	Likely
Strontium	2014 preliminary decision to regulate	Likely
Chlorate	3 rd Six Year Review; Pesticide Office	Possible
NDMA	3 rd Six Year Review	Possible
Cr(VI)	UCMR3; CCL4	Possible
1,4-dioxane	UCMR3; CCL4	Maybe
Perfluorocompounds	2016 revised HA; UCMR3; CCL4	Maybe
Brominated DBPs	UCMR4; 3 rd Six Year Review	Maybe
Manganese	UCMR4; CCL4	Maybe

* Based on AWWA Government Affairs (Roberson, 2015); "Likely" – regulation in 5 years; "Possible" – 50/50 chance of final regulation in 5-10 years; "Maybe" – anything can happen

Project Visioning – Presence of CEC’s in Supply

Ground Water Flow, 2004-07, and Water Desalting, 1992-2007, in McBaine Bottoms, Columbia, Missouri

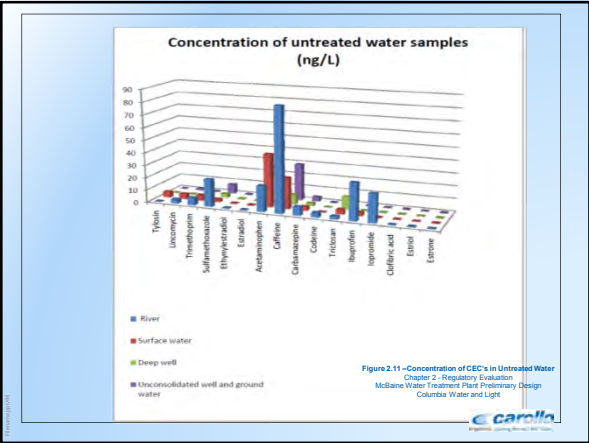
Table 7. Pharmaceutical compounds analyzed, minimum reporting limit, and concentration in samples from the city outflow and monitoring wells, McBaine Bottoms, 2007

[All concentrations are in micrograms per liter (µg/L), unless noted. — = not detected (n.d.)]

Compound	Minimum reporting limit	Detected in city outflow sample (concentration)	Detected in monitoring well sample (well concentration)
L7-Diethylstilbestrol	0.024	0.118	MW-10, E100007
Acetaminophen	0.15	—	MW-11K, E10000
			MW-13, E10000
			MW-11A, E10000
Caffeine	0.18	144	MW-26, E1007
Carbamazepine	0.22	0.029	—
Citalopram	0.28	—	—
Clonidine	0.22	—	—
Colchicine	0.24	—	MW-11A, E10000
Diphenhydramine	0.18	—	—
Diltiazem	0.16	—	—
Fluoxetine	0.05	—	—
Hydrocodone	0.14	—	—
Sulfamonomethoxazole	0.04	0.05	—
Sulfonamide	0.05	—	—
Thioridazine	0.09	—	—
Warfarin	0.51	0.06	MW-11A, E10000

Snapshot in time.

Extent and types are unknown.

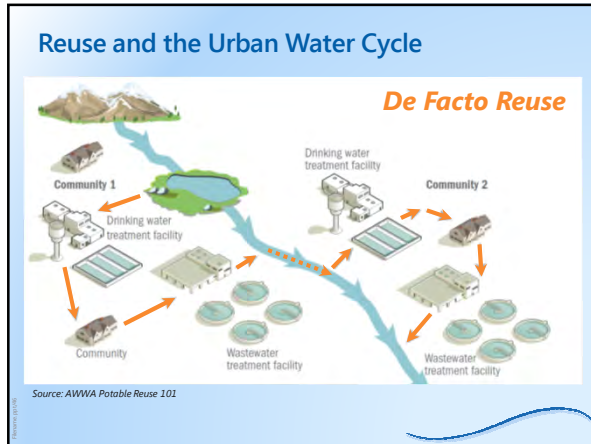


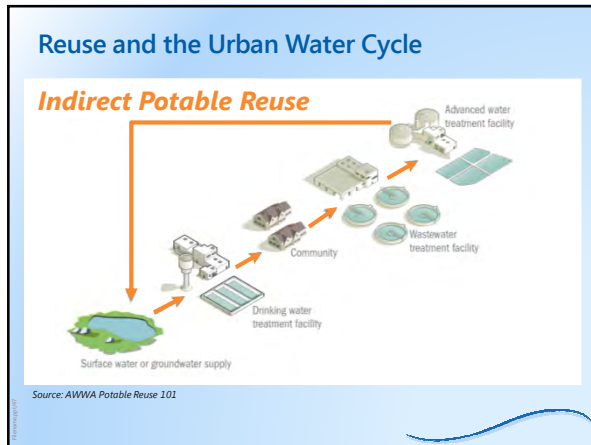
Visioning – CEC Treatment

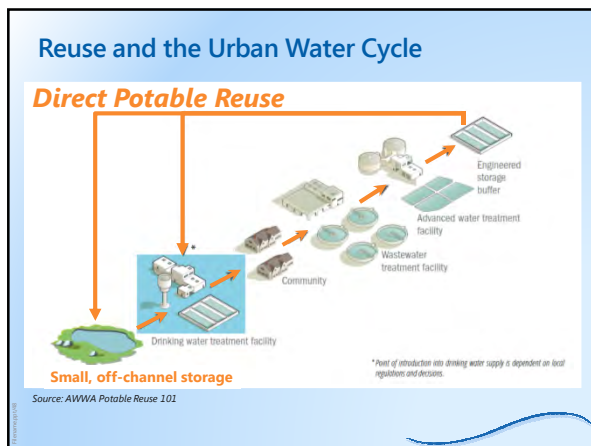
6. → Past investigations of surface-water and groundwater sources in Missouri and throughout the country have detected the presence of extremely low levels (one drop in 20 Olympic swimming pools) of Endocrine Disrupting (estrogen, etc.) and Pharmaceutical (acetaminophen, etc.) compounds in many drinking water supplies. Studies to determine if long-term exposure to the low concentrations of these constituents impact human health are at least 10+ years away and it is not certain when (if at all) some or all of these constituents will be regulated. Technologies that remove or destroy these compounds from the supply are available but are significantly more costly to implement than the current treatment process. Given this, how important is it to you that this study considers processes that remove or destroy these compounds? Please state the reasons for your selection. ¶

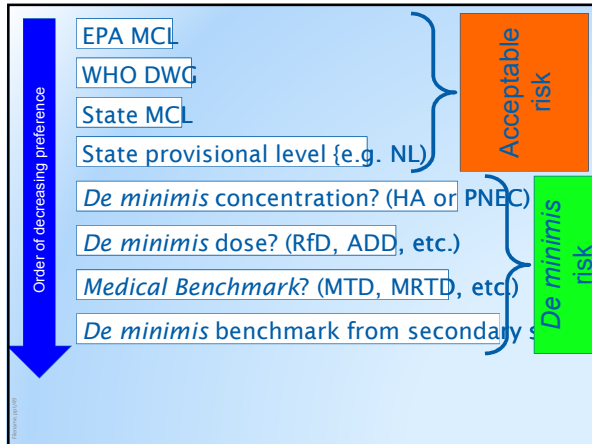
- Absolutely Critical to Remove or Destroy these Compounds No Matter the Expense. ¶
- Study Should Evaluate the Costs/Benefits of Technologies that Remove or Destroy these Compounds. ¶
- Not Very Important that Study Considers Removal/Destruction of these Compounds. ¶
- Study Should Not Consider Removal/Destruction of these Compounds. ¶
- Other (Please list) _____ ¶

In the space allotted below please state your reasons for the selection made above. ¶









NWRI Expert Panel Recommendations (WaterReuse-11-02)

Contaminant of Emerging Concern	Public Health Criterion	Secondary Effluent Concentration
N-nitrosodimethylamine (NDMA)	10 ng/L	Varies
Perfluorooctanoic acid (PFOS)	200 ng/L*	Not Measured
ng/L		
Estrone (E1)	320 ng/L	14 ng/L
17β-estradiol (E2)	N/A	< 5 ng/L
17α-ethinylestradiol (EE2)	N/A	< 5 ng/L
Perfluorooctanoic acid (PFOA)	400 ng/L*	Not Measured
1,4-dioxane	1 µg/L	Not Measured
Cotinine	1 µg/L	0.049 µg/L
Phenytoin (Dilantin)	2 µg/L	0.210 µg/L
Atenolol	4 µg/L	0.450 µg/L
µg/L		
TCEP	5 µg/L	0.110 µg/L
Carbamazepine	10 µg/L	0.320 µg/L
Primidone	10 µg/L	0.440 µg/L
DEET	200 µg/L	0.046 µg/L
Meprobamate	200 µg/L	0.190 µg/L
mg/L		
Triclosan	2 mg/L	0.000063 mg/L
Sucralose	150 mg/L	0.017 mg/L

Indicator TOxCs

- Frequent Occurrence at 'High' Concentrations (relative to detection limits)
- Availability and Reliability of Analytical Methods (LC-MS/MS → expensive!)
- Performance validation
 - **Bioretransformation** → Activated Sludge, Biofiltration, Environmental Buffer
 - High = Caffeine, Naproxen, Ibuprofen
 - Low = Carbamazepine, Meprobamate, Sucralose
 - **Adsorption** → Activated Sludge, Granular Activated Carbon, Environmental Buffer
 - High = Triclosan, Triclocarban, Bisphenol A
 - Low = Caffeine, Meprobamate, Sucralose
 - **Oxidation** → Chlorine, Ozone, Hydroxyl Radicals
 - High = Carbamazepine, Triclosan, Bisphenol A
 - Low = TCEP, Meprobamate, Sucralose
 - **Photolysis** → UV, Environmental Buffer
 - High = Diclofenac, Triclosan, NDMA
 - Low = Primidone, Meprobamate, Sucralose
 - **Wastewater influence**
 - Primidone, Meprobamate, Sucralose

Pharmaceuticals Make Good Headlines...




<http://www.dailymail.co.uk/health/article-3339996/Top-scientist-warns-health-timebomb-caused-prescription-drugs-washed-drains.html>

Pharmaceuticals Make Good Headlines...

In Big Spring, we found...

- Anti-anxiety drug
- Blood pressure med!
- Anti-convulsant!
- Insect repellent!
- Anti-microbial!

...and more!

Chemical	Health Criterion	WWTP Effluent	DPR Product Water
Carbamazepine	10 µg/L	<0.01 µg/L	<0.0005 µg/L
Estrone	320 ng/L	<0.2 ng/L	<0.2 ng/L
Meprobamate	200 µg/L	0.23 µg/L	0.00045 µg/L
Atenolol	4 µg/L	0.33 µg/L	<0.001 µg/L
Primidone	10 µg/L	0.19 µg/L	<0.0005 µg/L
PFOA	70 ng/L ¹	12 ng/L	< 5 ng/L
PFOS	70 ng/L ¹	5.4 ng/L	< 1 ng/L
1,4-dioxane	1 µg/L	0.36 µg/L ²	<0.07 µg/L ³
DEET	200 µg/L	0.19 µg/L	0.15 µg/L
Triclosan	2.1 mg/L	0.0018 µg/L	< 0.01 µg/L
Saccharose ⁴	150 mg/L	0.041 mg/L	0.000150 mg/L
TCEP	5 µg/L	2.1 µg/L	< 0.01 µg/L

Stavitskiy, D., et al. (2016). *Drugs in Public Water: Monitoring, Final Report to Texas Water Development Board (also WRSR 14-17)*.

...but they Do NOT Drive Public Health Risk!

Chemical	Health Criterion	WWTP Effluent	DPR Product Water
Carbamazepine	10 µg/L	<0.01 µg/L	<0.0005 µg/L
Estrone	320 ng/L	<0.2 ng/L	<0.2 ng/L
Meprobamate	200 µg/L	0.23 µg/L	0.00045 µg/L
Atenolol	4 µg/L	0.33 µg/L	<0.001 µg/L
Primidone	10 µg/L	0.19 µg/L	<0.0005 µg/L
PFOA	70 ng/L ¹	12 ng/L	< 5 ng/L
PFOS	70 ng/L ¹	5.4 ng/L	< 1 ng/L
1,4-dioxane	1 µg/L	0.36 µg/L ²	<0.07 µg/L ³
DEET	200 µg/L	0.19 µg/L	0.15 µg/L
Triclosan	2.1 mg/L	0.0018 µg/L	< 0.01 µg/L
Saccharose ⁴	150 mg/L	0.041 mg/L	0.000150 mg/L
TCEP	5 µg/L	2.1 µg/L	< 0.01 µg/L

Stavitskiy, D., et al. (2016). *Drugs in Public Water: Monitoring, Final Report to Texas Water Development Board (also WRSR 14-17)*.

Other DPR Research Concludes the Same

Compound (ng/L)	Typical Effluent	Guidance Value
Atenolol	710	70,000
Atrazine	28	1,000
DEET	140	2,500,000
Gemfibrozil	31	45,000
Naproxen	<25	220,000

Data from Reuse-05-05, 08-05, 11-02, and Bonelli et al 2009, ES&T 43 (2), 597-603

	Max Secondary WWTFC Conc. (ng/L)	Max LP-Dose-BAQ Conc. (ng/L)	Max Drinking Water Conc. (ng/L)	DWEL (ng/L)	Liters per day to meet DWEL
Fluoxetine	0.71	<0.001	0.019	6.8	792
Chloramphenicol	0.14	<0.0005	0.019	12	1,300
Fluazolidone	Not Reported	<0.0005	0.082	34	62,000
Diazepam	Not Reported	<0.0003	0.00033	35	270,000
Codeine	0.025	<0.0003	0.0021	48	43,000
Ampicillin	0.71	<0.001	0.019	70	7,800
Morphine	0.041	0.008	0.062	260	13,000
Hydrocodone	<0.05	<0.001	0.025	1,850	140,000
Difenhydramine	0.97	<0.0003	0.003	18,000	12,000,000



...and Texas doesn't regulate them anyway.

See Water Environment & Reuse Foundation Project No. 11-02 and 15-01 for details.

Said another way:

"Not everything that counts can be counted, and not everything that can be counted counts."

Note: This quote is often attributed to Albert Einstein, but credit should more likely go to sociologist William Bruce Cameron, who wrote this in paper published in 1963. Source: <http://quoteinvestigator.com/2010/05/26/everything-counts-einstein/>

Project Visioning – Future of Existing Water Source

Ground Water Flow, 2004-05, and Water Quality, 1992-2007, in Middlesex System, Colorado, Missouri

Table 1. Pharmaceutical compounds analyzed, minimum reporting limit, and concentration in samples from the city surface and monitoring wells, Middlesex System, 2007.

(ND) = not detected; (M) = maximum; (L) = limit; (D) = detection; (S) = sample; (C) = concentration.

Compound	Minimum reporting limit	Detected in city surface sample (low concentration)	Detected in monitoring well samples (high concentration)
1,3-Dichlorobenzene	0.024	0.114	MW-1, MW-2, MW-3, MW-4, MW-5, MW-6, MW-7, MW-8, MW-9, MW-10, MW-11, MW-12, MW-13, MW-14, MW-15, MW-16, MW-17, MW-18, MW-19, MW-20, MW-21, MW-22, MW-23, MW-24, MW-25, MW-26, MW-27, MW-28, MW-29, MW-30, MW-31, MW-32, MW-33, MW-34, MW-35, MW-36, MW-37, MW-38, MW-39, MW-40, MW-41, MW-42, MW-43, MW-44, MW-45, MW-46, MW-47, MW-48, MW-49, MW-50, MW-51, MW-52, MW-53, MW-54, MW-55, MW-56, MW-57, MW-58, MW-59, MW-60, MW-61, MW-62, MW-63, MW-64, MW-65, MW-66, MW-67, MW-68, MW-69, MW-70, MW-71, MW-72, MW-73, MW-74, MW-75, MW-76, MW-77, MW-78, MW-79, MW-80, MW-81, MW-82, MW-83, MW-84, MW-85, MW-86, MW-87, MW-88, MW-89, MW-90, MW-91, MW-92, MW-93, MW-94, MW-95, MW-96, MW-97, MW-98, MW-99, MW-100
Acetaminophen	0.05	—	—
Caffeine	0.05	0.141	—
Chloramphenicol	0.02	0.025	—
Cloxacillin	0.02	—	—
Cocaine	0.02	—	—
Diazepam	0.02	—	—
Diphenhydramine	0.02	—	—
Fluoxetine	0.02	—	—
Fluazolidone	0.02	—	—
Hydrocodone	0.02	—	—
Hydrocodone bitartrate	0.02	—	—
Hydroxyzine	0.02	—	—
Propoxyphene	0.02	—	—
Warfarin	0.02	—	—

A water or wastewater issue? (EDC's, Pharm, Nitrate, etc.)

Project Visioning – Considering Treatment for CEC's

Ground Water Flow, 2004-05, and Water Quality, 1992-2007, in McEneaney Bottoms, Columbia, Missouri

Table 1. Pharmaceutical compounds analyzed, detection reporting limit, and concentration in samples from the city taplines and reporting wells, McEneaney Bottoms, 2007

(ND) concentrations are not detected and (L) is less than (L) (see footnote)

Compound	Maximum reporting limit	Detected in city well or sample (see concentration)	Detected in monitoring well sample (see concentration)
4,4'-Dichlorodiphenyl ether	0.024	0.118	NW-1 (N-11000)
Acetaminophen	0.05	—	NW-1 (N-11000) NW-1 (N-11000)
Citalopram	0.08	0.147	NW-2 (N-11000)
Cloxacillin	0.02	0.025	—
Clozapine	0.08	—	—
Cyclosporin	0.02	—	—
Diclofenac sodium	0.04	—	NW-1 (N-11000)
Diphenhydramine	0.04	—	—
Diphenhydramine	0.04	—	—
Ethinylestradiol	0.03	—	—
Metoprolol	0.04	—	—
Metoprolol (chiral)	0.04	0.118	—
Nitrofurantoin	0.03	—	—
Phenacetin	0.06	—	—
Propoxyphene	0.04	—	—
Warfarin	0.01	0.06	NW-1 (N-11000)

A water or wastewater issue? (EDC's, Pharm, Nitrate, etc.)



Disinfection By Products

Visioning - Disinfection By Products

Water Treatment Plant Configuration (cont.)

5. → To satisfy regulations associated with disinfection by products, the City of Columbia converted from free chlorine to chloramines in the distribution system and conducts periodic conversions to chlorine to avoid issues that are associated with nitrification. There are more costly technologies that can be employed to satisfy all disinfection by product regulations and permit switching back to chlorine. Given this, how important is it to you that the City of Columbia switches back to the exclusive use of free chlorine in the distribution system? Please state the reasons for your selection.

Absolutely Critical to Switch Back to Chlorine

Very Important to Switch Back to Chlorine

Not Very Important

Stay with Chloramines


Other (Please list) _____

In the space allotted below please state your reasons for the selection made above.

Page Break

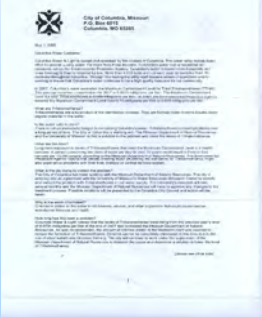
Maximum Contaminant Levels for Disinfection Byproducts

TTHM MCL = 0.080 mg/L
HAA5 MCL = 0.060 mg/L




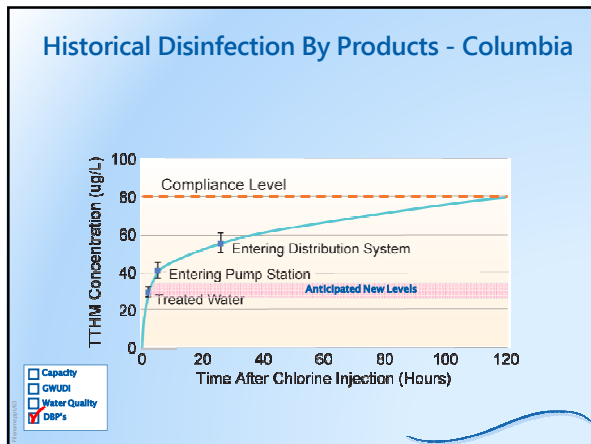
- Apply to CWSs and NTNCWSs that add a disinfectant to their water
- Reduce risks of cancer, liver and kidney damage, reproductive problems associated with elevated levels of byproducts

MDNR Notice of Violation



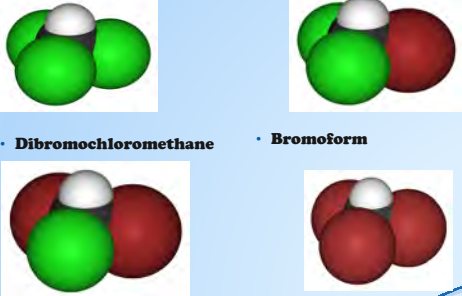
- In 2007 Columbia's water supply exceeds Federal MCL for TTHMs
- Average concentration of 82.3 ppb
- April 2008 - MDNR notice of violation





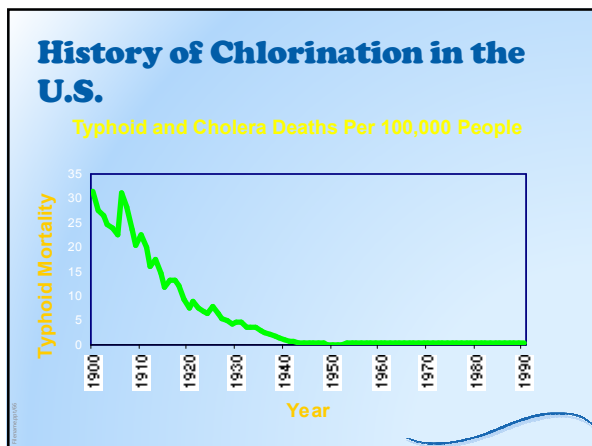
Total Trihalomethanes

- Chloroform
- Bromodichloromethane
- Dibromochloromethane
- Bromoform



Why Chlorinate if It Produces Byproducts?





Problem Description

$\text{Cl}_2 + \text{NOM} \rightarrow \text{Halogenated Organics}$

Pathogens

DBPs

Source Water

Flocculation/Sedimentation

Filtration

Clearwell

Distribution System

Problem Description

$\text{Cl}_2 + \text{NOM} \rightarrow \text{Halogenated Organics}$

Pathogens

DBPs

Cl₂

Source Water

Flocculation/Sedimentation

Filtration

Clearwell

Distribution System

Problem Description

$\text{Cl}_2 + \text{NOM} \rightarrow \text{Halogenated Organics}$

Pathogens

DBPs

Cl₂

Source Water

Flocculation/Sedimentation

Filtration

Clearwell

Distribution System

Why Chloramines? Chloramination vs. Chlorination

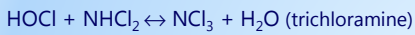
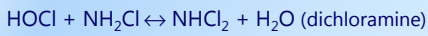
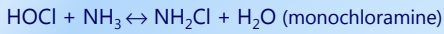
Advantages

- Lower HAA and THM formation
- More stable disinfectant

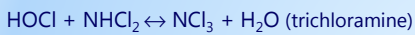
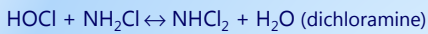
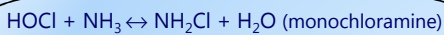
Disadvantages

- Poorer disinfectant
- May lead to nitrification in the distribution system

What are Chloramines?



What are Chloramines?



Chloramine chemistry is complicated, but we know a lot about it

No.	Reaction	Rate or Equilibrium Constant	Reference
1	$\text{HOCl} + \text{NH}_3 \rightarrow \text{NH}_2\text{Cl} + \text{H}_2\text{O}$	$4.2 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$	Jahromi and Valentine (1995)
2	$\text{NH}_2\text{Cl} + \text{H}_2\text{O} \rightarrow \text{NH}_3 + \text{HOCl}$	$2.1 \times 10^6 \text{ s}^{-1}$	Morris and Isaac (1981)
3	$\text{NH}_2\text{Cl} + \text{HOCl} \rightarrow \text{NHCl}_2 + \text{H}_2\text{O}$	$2.8 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$	Margreth et al. (1976)
4	$\text{NHCl}_2 + \text{H}_2\text{O} \rightarrow \text{HOCl} + \text{NH}_2\text{Cl}$	$6.4 \times 10^6 \text{ s}^{-1}$	Margreth et al. (1976)
5	$\text{NH}_2\text{Cl} + \text{NH}_2\text{Cl} \rightarrow \text{NHCl}_2 + \text{NH}_3$	pH dependent	Vitousek et al. (2004)
6	$\text{NH}_2\text{Cl} + \text{NH}_3 \rightarrow \text{NHCl}_2 + \text{NH}_4\text{Cl}$	$8.1 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$	Banal and Margreth (1981)
7	$\text{NH}_2\text{Cl} + \text{NHCl}_2 \rightarrow \text{N}_2 + \text{HCl} + \text{HCl}$	$1.5 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$	Lenz (1981)
8	$\text{NHCl}_2 + \text{H}_2\text{O} \rightarrow \text{NH}_3 + \text{HOCl} + \text{HCl}$	$1.1 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$	Jahromi and Valentine (1995)
9	$\text{NH}_3 + \text{NHCl}_2 \rightarrow \text{N}_2 + \text{HOCl} + \text{HCl}$	$2.8 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$	Lenz (1981)
10	$\text{NH}_3 + \text{NHCl}_2 \rightarrow \text{N}_2 + \text{H}_2\text{O} + \text{HCl}$	$8.3 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$	Lenz (1981)
11	$\text{HOCl} \rightleftharpoons \text{H}^+ + \text{OCl}^-$	$K_a = 3.5 \times 10^{-8}$	Baker and Pardo (1995)
12	$\text{NH}_3 \rightleftharpoons \text{NH}_4^+ + \text{H}^+$	$K_a = 5.6 \times 10^{-10}$	Baker and Pardo (1995)
13	$\text{H}_2\text{CO}_3 \rightleftharpoons \text{HCO}_3^- + \text{H}^+$	$K_a = 4.3 \times 10^{-7}$	Baker and Pardo (1995)
14	$\text{HCO}_3^- \rightleftharpoons \text{CO}_3^{2-} + \text{H}^+$	$K_a = 4.7 \times 10^{-11}$	Baker and Pardo (1995)
15	$\text{H}_2\text{O} \rightleftharpoons \text{H}^+ + \text{OH}^-$	$K_w = 10^{-14}$	Baker and Pardo (1995)

$K_a = \text{H}^+[\text{OCl}^-] / [\text{HOCl}] = 3.5 \times 10^{-8}$ when $\text{H}_2\text{CO}_3 = 1 \text{ M}$
 $K_w = 10^{-14}$ when $[\text{H}^+] = [\text{OH}^-] = 10^{-7} \text{ M}$
 NHCl is the unchlorinated monochloramine auto-decomposition parameter

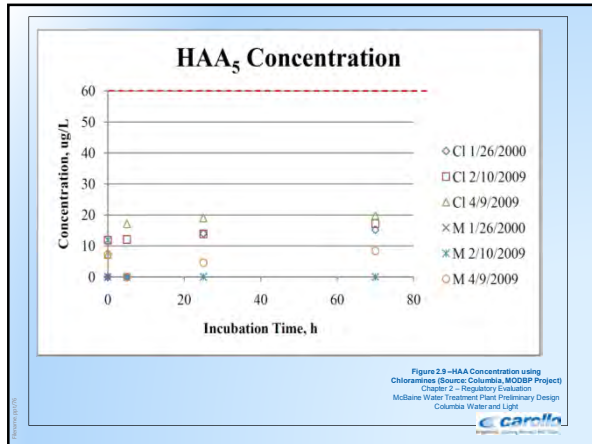
No.	Reaction	Rate or Equilibrium Constant	Reference
13	$\text{HOCl} + \text{Br}^- \rightarrow \text{HOBr} + \text{Cl}^-$	$1.51 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$	Kramer and Margreth (1995)
16	$\text{HOBr} + \text{NH}_3 \rightarrow \text{NH}_2\text{Br} + \text{H}_2\text{O}$	$7.5 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$	Wynn and Morris (1989)
17	$\text{OBr}^- + \text{NH}_3 \rightarrow \text{NH}_2\text{Br} + \text{OH}^-$	$7.6 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$	Wynn and Morris (1989)
18	$\text{NH}_2\text{Br} + \text{H}_2\text{O} \rightarrow \text{HOBr} + \text{NH}_3$	$1.5 \times 10^6 \text{ s}^{-1}$	Wynn and Lusk (1989)
19	$\text{NH}_2\text{Br} + \text{NH}_2\text{Br} \rightarrow \text{N}_2 + \text{H}_2\text{O} + \text{H}^+$	pH dependent	Lenz et al. (2004)
20	$\text{NH}_2\text{Br} + \text{NH}_3 \rightarrow \text{NH}_2\text{Br} + \text{NH}_4\text{Br}$	pH dependent	Lenz et al. (2004)
21	$\text{NH}_2\text{Br} + \text{NH}_2\text{Br} \rightarrow \text{N}_2 + \text{H}^+ + \text{H}_2\text{O}$	pH dependent	Lenz et al. (2004)
22	$\text{NH}_2\text{Br} + \text{NH}_2\text{Br} + \text{H}_2\text{O} \rightarrow \text{N}_2 + \text{H}^+ + \text{H}_2\text{O}$	$4.9 \text{ M}^{-1} \text{ s}^{-1}$	Lenz et al. (2004)
23	$\text{HOBr} + \text{NH}_2\text{Cl} \rightarrow \text{NH}_2\text{Br} + \text{HOCl}$	$2.8 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$	Gandy and Margreth (1994)
24	$\text{OBr}^- + \text{NH}_2\text{Cl} \rightarrow \text{NH}_2\text{Br} + \text{OH}^-$	$2.2 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$	Gandy and Margreth (1994)
25	$\text{NH}_2\text{Cl} + \text{NH}_2\text{Cl} + \text{Br}^- \rightarrow \text{NH}_2\text{Br} + \text{Cl}^- + \text{NH}_3$	pH dependent	Todd et al. (1989), This work
26	$\text{NH}_2\text{Cl} + \text{NH}_2\text{Cl} + \text{H}_2\text{O} \rightarrow \text{N}_2 + \text{H}^+ + \text{H}_2\text{O}$	$17 \text{ M}^{-1} \text{ s}^{-1}$	Valentine 1983, This work
27	$\text{HOBr} + \text{OH}^- \rightleftharpoons \text{OBr}^- + \text{H}_2\text{O}$	$K_a = 5.8 \times 10^{-9}$	Hogg and Hogg (1982)
28	$\text{NH}_2\text{Cl} + \text{NH}_2\text{Cl} + \text{H}_2\text{O} \rightarrow \text{N}_2 + \text{H}^+ + \text{H}_2\text{O}$	$K_a = 1.4 \times 10^{-11}$	Hogg and Hogg (1982)
29	$\text{NH}_2\text{Cl} + \text{NH}_2\text{Cl} + \text{H}_2\text{O} \rightarrow \text{N}_2 + \text{H}^+ + \text{H}_2\text{O}$	$K_a = 4.2 \times 10^{-11}$	Hogg and Hogg (1982)
30	$\text{NH}_2\text{Cl} + \text{NH}_2\text{Cl} + \text{H}_2\text{O} \rightarrow \text{N}_2 + \text{H}^+ + \text{H}_2\text{O}$	$K_a = 3.1 \times 10^{-11}$	Hogg and Hogg (1982)

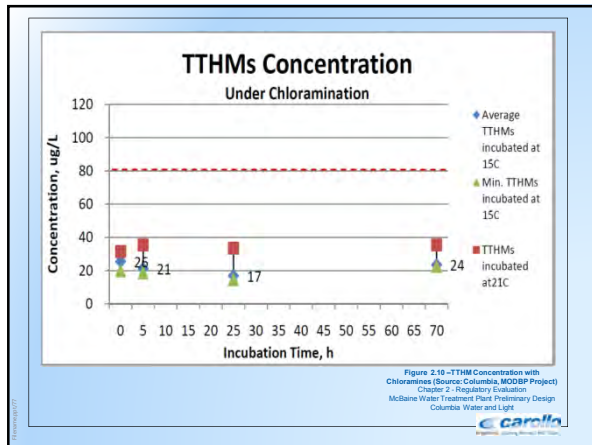
Chloramines – Other Considerations

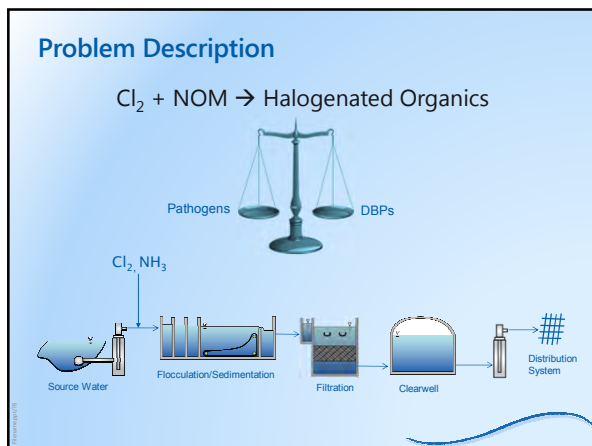
- Chloramine has been around for 90 years
- One in five Americans has chloraminated water
- EPA stated in its 1994 review that: *"In humans, health effects do not appear to be associated with levels of residual monochloramines typically found in drinking water"*
- Some individuals and groups may be inalterably opposed to the introduction of chloramines

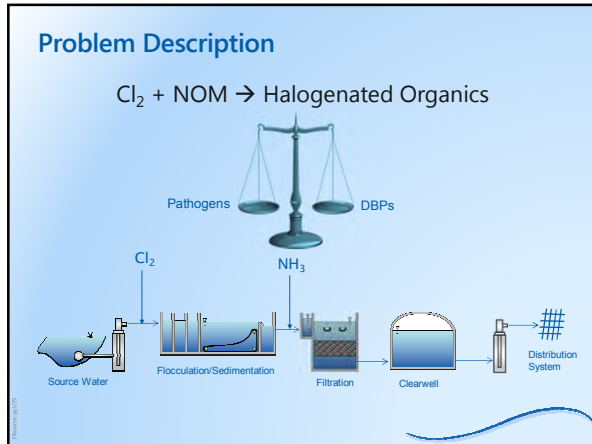
Columbia Conversion to Chloramination

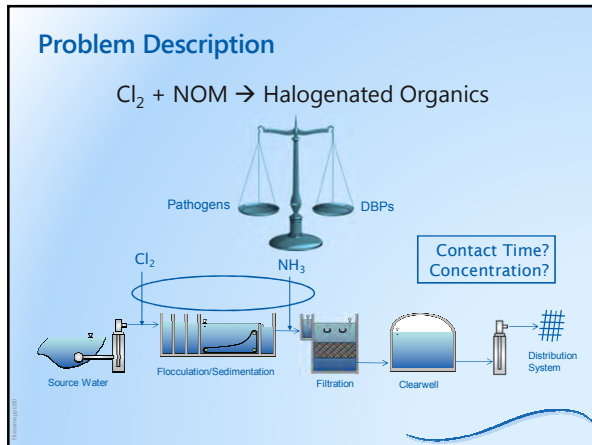
- Conversion from free chlorine disinfection to chloramination.
- Free Chlorine "burns" to limit nitrification

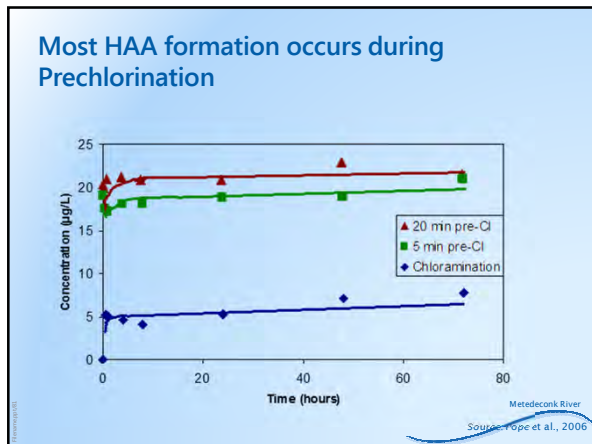


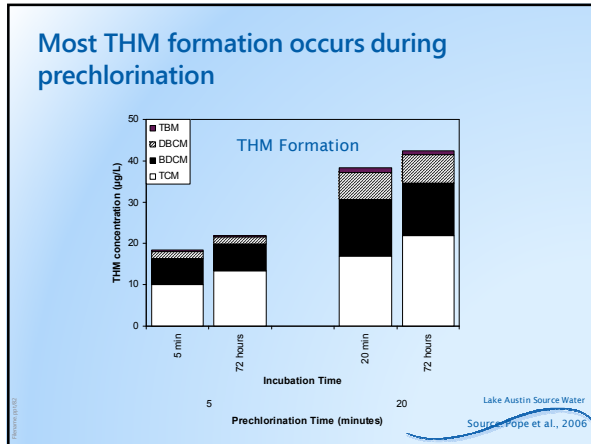








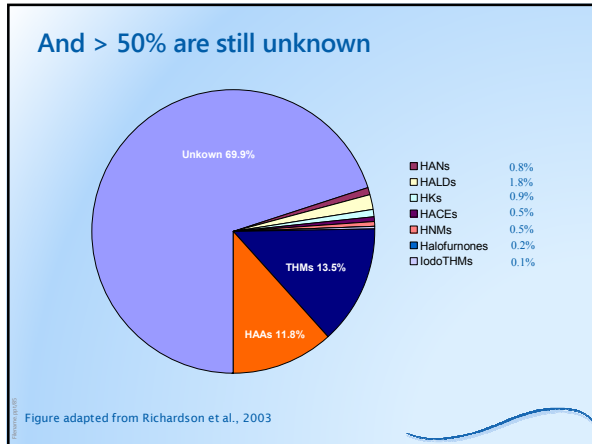




HAA formation during chloramination:

Factors that Impact HAA Formation	
pH	HAA ↑ as pH ↓
Bromide	HAA ↑ as Bromide ↑
Total Organic Carbon (TOC)	HAA ↓ as TOC ↓
Chlorine/Nitrogen Ratio	HAA ↑ as Cl ₂ /N ↑
Temperature	HAA ↑ as Temperature ↑
Residual	HAA ↑ as Residual ↑

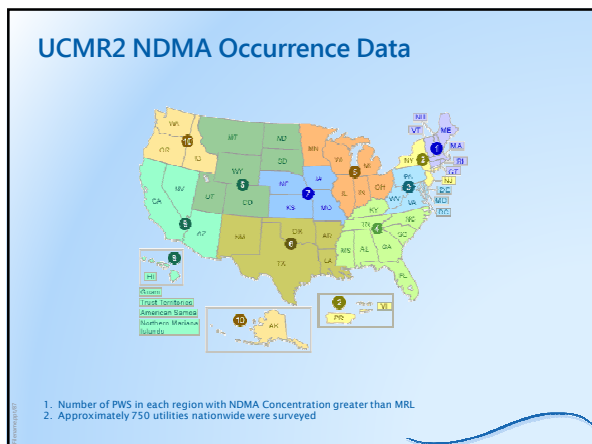
- ### The EPA Currently Regulates 11 DBPs
- 4 THMs (80 µg/L)
 - 5 HAAs (60 µg/L)
 - Chlorite (1 mg/L)
 - Bromate (10 µg/L)
- But, > 600 DBPs Have Been Identified**

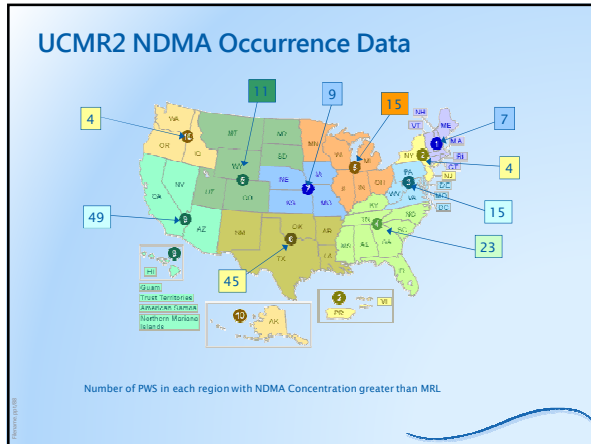


Several of emerging DBPs are on the EPA Contaminant Candidate List (CCL3)

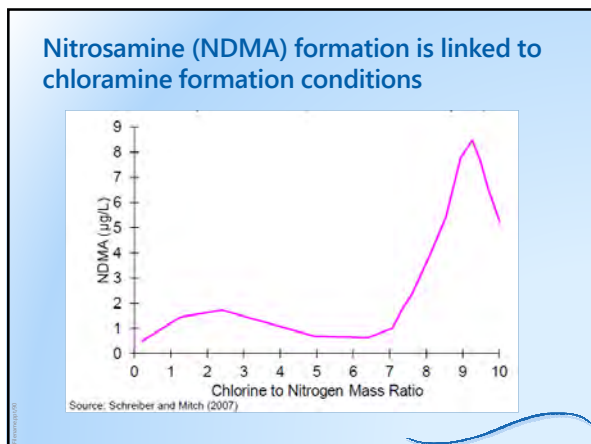
- 6 Nitrosamines (e.g., NDMA)
- Formaldehyde
- Bromochloromethane
- Chlorate

The 6 Nitrosamines were screened as part of the Unregulated Contaminant Monitoring Rule (UCMR2)





- ### NDMA
- Chlorination
 - Cationic Coagulation Polymers and Coagulant Aids (i.e., poly-DADMAC and epi-DMA)
 - Chloramination
 - Formation is increased near breakpoint
 - Preoxidation with chlorine or ozone may decrease
 - California Action Level = 10 ng/L



NDMA formation may be reduced by:

- 1. Reducing dichloramine formation during chloramination
 - a) Add chlorine upstream of ammonia at WTP
 - b) Elevate pH
 - c) Minimize Chlorine to Nitrogen Ratio
 - i. Trade-offs with nitrification control
- 2. Add oxidants (e.g. free chlorine, ozone) prior to ammonia addition
- 3. Manage polymer addition
- 4. Source water protection (wastewater impacted source waters may form more NDMA)



Treatment Technologies Evaluation

Visioning – Treatment Technologies

4 - The end of this questionnaire provides a glossary of the advanced treatment technology and the potential benefits this technology would provide. Please select which of these advanced technologies you would like to see the study address. (Please list the reasons for your selections.)

- | | | |
|--|---|---|
| <input type="checkbox"/> Membrane Filtration | - | <input type="checkbox"/> Air Stripping |
| <input type="checkbox"/> Nano/Reverse Osmosis | - | <input type="checkbox"/> Enhanced Softening |
| <input type="checkbox"/> Advanced Coagulation | - | <input type="checkbox"/> All of the Above |
| <input type="checkbox"/> Ion Exchange | - | <input type="checkbox"/> Others (Please List Below) |
| <input type="checkbox"/> Advanced Disinfection | - | _____ |
| <input type="checkbox"/> Ozone/Infiltration | - | _____ |
| <input type="checkbox"/> Advanced Bio/Strat | - | _____ |

Please list the reasons for your selection.

**Alternative
Development**



“Fatal Flaw” and “Must Include” List

- “Must Include” or the Alternative will be eliminated from consideration
 - Capacity without Purchasing Water
 - Satisfy Regulatory Requirements
 - Meets Secondary Standards (Fe and Mn)
 - Meets Hardness Goal of 150 mg/L
 - Uses existing well field
 - Optimize existing infrastructure
 - Satisfy GWUDI compliance



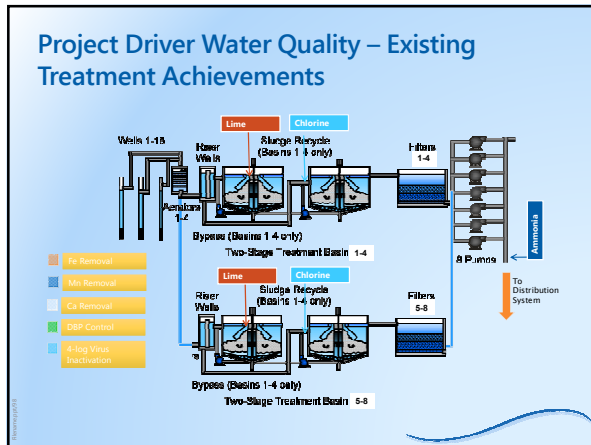
“Fatal Flaw” and “Must Include” List

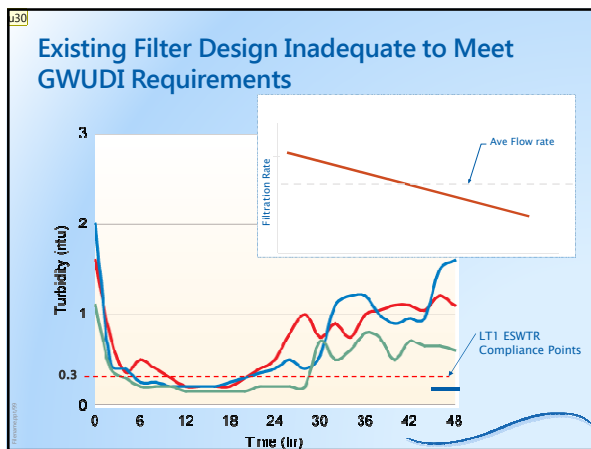
- “Fatal Flaw” will eliminate Potential Alternative from consideration
 - Technology has never been built at this scale
 - Inappropriate technology
 - Extremely inflated costs
 - Not acceptable to the Community



Technologies for Evaluation

Oxidation Technologies				
Ferrate	Chlorine UV / H2O2	Chlorine dioxide UV / TIO2	Ozone P. Acid / UV	Ozone / H2O2 Permanganate
Hardness Removal Technologies				
Conventional Softening High Rate Softening	Enhanced Softening Anion Exchange	Softening with caustic	Split Treatment	Pelletized Lime Reactor Nanofiltration Reverse Osmosis
Filtration Technologies				
Nanofiltration Conventional Filtration	RO	Membranes (low pressure) Deep bed with constant rate filtration	Biological filtration Manganese coated filter media	Alternative filtration (bag, earth, slow sand) Greensand Filtration
Disinfection By Product Control				
GAC Filter Contactors	PAC Contactors – Acticarb	Post Filtration GAC Columns	Ozone/Biofiltration	Nanofiltration/RO EC Bromide Removal TOC Specific Resin
Enhanced Coagulation	Chlorine Dose Control	PAC MIEX	Air Stripping	
Disinfection Technologies				
Chlorine	UV	Chloramines Chlorine Dioxide	Ozone Ferrate	Permanganate Periacetic Acid






Slide 99

- u30** Comment on the declining rate mode. Not appropriate for what they have. Find alot in Iowa because Cleasby. Slow Start concept. Maximum filtration rate.
user, 4/27/2009

Filtration Improvements

- Option I – Deep Bed Filtration
- Option II – Membranes

Micro/Ultra Filtration:- Water under moderate pressure (25-50-psig) is forced through a membrane, a thin material with very small pores, stopping small particles (including bacteria). This is proven to provide an effective barrier to most pathogens but is not effective in removing ions (softening) or most organic compounds.

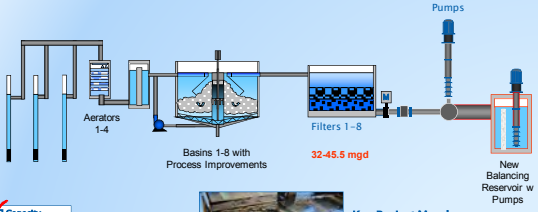


Deep Bed
Austin, TX (50 mgd)

Membrane Retrofit Pilot
Kansas City, MO (230 mgd)

Membrane Expansion
Olathe, KS (30 mgd)

Option 1 – Convert To Constant Rate Filtration & Increase Production



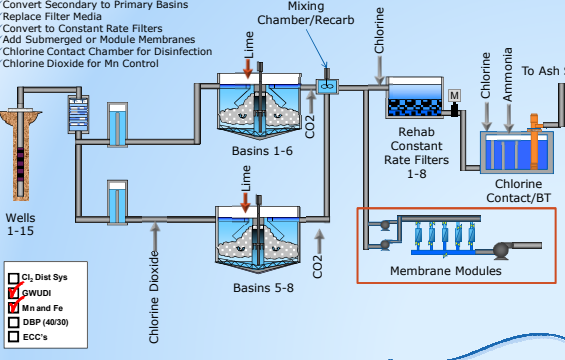
Capacity
 CWUDI
 Water Quality
 DBP's

Key Project Members:
Robert Morrioni
Bryant Bench

Colorado Springs

Alternative No. 1B Membranes

- ✓ New Stainless Steel Internals
- ✓ Convert Secondary to Primary Basins
- ✓ Replace Filter Media
- ✓ Convert to Constant Rate Filters
- ✓ Add Submerged or Module Membranes
- ✓ Chlorine Contact Chamber for Disinfection
- ✓ Chlorine Dioxide for Mn Control



Legend:
 Cl₂ Dist Sys
 CWUDI
 Mn and Fe
 DBP (40/30)
 ECC's

Technologies for Evaluation

Oxidation Technologies				
Ferrate	Chlorine UV / H2O2	Chlorine dioxide UV / TIO2	Ozone P. Acid / UV	Ozone / H2O2 Permanganate

Hardness Removal Technologies

Nano/Reverse-Osmosis: → Water under high pressure (75-120 psig) is forced through a membrane using a separation process that employs the principles of reverse osmosis to remove dissolved contaminants from water; typically applied for membrane softening or the removal of dissolved organic contaminants. This treatment may provide enhanced removal of disinfection by product precursors and may permit the re-establishment of free chlorine as both a primary and secondary (distribution) system disinfectant. In addition, these processes have proven effective in reducing the extremely low levels (one drop in 20 Olympic swimming pools) of some Endocrine Disrupting (estrogen, etc.) and Pharmaceutical (acetaminophen, etc.) compounds found in many of the nations drinking water supplies.

Chlorine Dose Control	MIEX	Air Stripping	TOC Specific Resin
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Disinfection Technologies			
Chlorine	Chloramines	Ozone	Permanganate
UV	Chlorine Dioxide	Ferrate	Periacetic Acid

Technologies for Evaluation

Oxidation Technologies				
Ferrate	Chlorine UV / H2O2	Chlorine dioxide UV / TIO2	Ozone P. Acid / UV	Ozone / H2O2 Permanganate

Softening (precipitative): → The process of adding an alkaline agent (lime, caustic soda, etc.) to water to remove hardness (calcium) via precipitation. This is done to reduce scaling in water heaters and otherwise improve other aesthetic aspects of drinking water.

Ion Exchange: → A reversible chemical reaction between an insoluble solid and a solution during which ions may be interchanged. This separation process, as it applies to Columbia, would be to examine fixed bed or dispersed magnetic resins to fix some organic ions to the resins. This treatment may provide enhanced removal of disinfection by product precursors and may permit the re-establishment of free chlorine as both a primary and secondary (distribution) system disinfectant.

GAC Filter Contactors	PAC Contactors - Activated	Columns	Nanofiltration/RO
Enhanced Coagulation	PAC	Ozone/Biofiltration	EC Bromide Removal
Chlorine Dose Control	MIEX	Air Stripping	TOC Specific Resin

Disinfection Technologies			
Chlorine	Chloramines	Ozone	Permanganate
UV	Chlorine Dioxide	Ferrate	Periacetic Acid

DPR Pilot Consists of Five Process Steps

Ozone/Biofiltration: → A combined water treatment process to reduce natural organic matter (NOM) which is a water disinfectant byproduct precursor. Water is first assanated (ozone is mixed into the water flow to oxidize organic matter, iron and manganese) and then passed through a biofilter (a filter bed laden with microorganisms that break down organic matter into carbon dioxide, water and salts). These processes have proven effective in reducing the extremely low levels (one drop in 20 Olympic swimming pools) of some Endocrine Disrupting (estrogen, etc.) and Pharmaceutical (acetaminophen, etc.) compounds found in many of the nations drinking water supplies. This treatment may provide enhanced removal of disinfection by product precursors and may permit the re-establishment of free chlorine as a secondary (distribution) system disinfectant.

DPR Pilot Consists of Five Process Steps

Advanced Disinfection: Technologies (Ozone, chlorine dioxide, UV, low-pressure membrane filtration) that are approved by the US EPA to provide primary disinfection of drinking water that meet or exceed national standards without the use of free chlorine. This does not eliminate the use of chlorination in the process. Chlorination or Chloramination will be required by the Missouri Department of Natural Resources following this process to produce a measurable residual disinfectant in the distribution system. Some of these technologies may provide enhanced removal of disinfection by-product precursors and may permit the re-establishment of free chlorine as a secondary (distribution) system disinfectant.

Advanced Oxidation: The process of adding or generating powerful oxidants to oxidize trace levels of organic or microbiological organisms in water. These processes have proven effective in reducing the extremely low levels (one drop in 20 Olympic swimming pools) of some Endocrine Disrupting (estrogen, etc.) and Pharmaceutical (acetaminophen, etc.) compounds found in many of the nation's drinking water supplies.

Ozone (O₃): Looks Like This

O₃ Contactor **O₃ Generator / Panel**

Ozone (O₃): Disinfects Virus and Destroys Many Organics

Before Ozonation **After Ozonation**

Figure 11 Comparison of MIPRO™ MS2 Log Reduction-Ozone(TOC+NO₂-) Relationship with Results of Different Studies


Biologically Active Filtration (BAF): Looks Like This

BAF


UF

CAE

UV/AOP

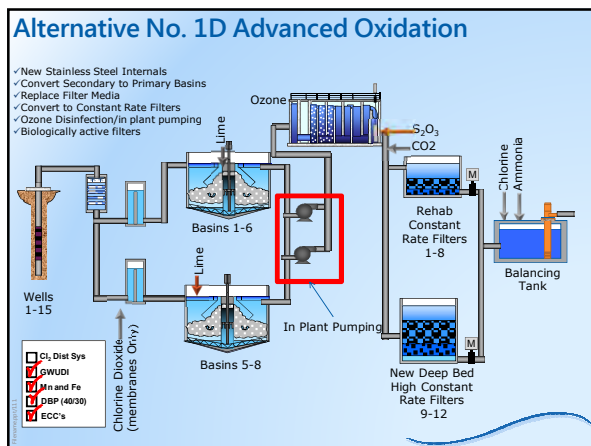


"Oxelia" is Xylem's Combination of Wedeco Ozone and Leopold BAF



BAF: Breaks Down Organics and Mitigates NDMA Formed

Compound	Max. Recommended Value, ng/L	Secondary Effluent, ng/L	Tertiary Effluent with UV, ng/L	O ₃ BAF Filtrate, ng/L
Atenolol	70,000	710	120	<25
Atrazine	1,000	28	<10	<10
Bisphenol A	200,000	<50	<50	<50
Carbamazepine	1,000	140	192	<10
DEET	2,500,000	54	232	<25
Diclofenac	1,800	62	57	<25
Gemfibrozil	45,000	31	12	<10
Ibuprofen	400,000	<25	<25	<25
Meprobamate	260,000	41	362	190
Musk Ketone	350,000	<100	<100	<100
Naproxen	220,000	<25	<25	<25
Phenytoin	6,800	110	113	33
Primidone	10,000	67	168	31
Sulfamethoxazole	35,000	570	1,150	<25
Triclosan	350	26	38	<25
Trimethoprim	70,000	280	43	<10
TCEP	1,000	540	349	<200



Ultrafiltration (UF): Looks like this... with no Membrane Module

Toray Hollow Fiber Module

Ultrafiltration (UF): Removes Particles and Protozoa Pathogens

Size (µm)	Molecular Weight (Daltons)	Pathogens/Processes
0.0001	200	UF
0.001	20,000	UF, NF
0.01	200,000	UF, NF, RO
0.1		UF, MF, RO
1.0		MF, RO

Drinking Water Pathogens: Bacteria, Giardia, Cryptosporidium, Viruses

Membrane Filtration Process: UF, MF, NF, RO

Alternative No. 1C UV Disinfection

- ✓ New Stainless Steel Internals
- ✓ Convert Secondary to Primary Basins
- ✓ Replace Filter Media
- ✓ Convert to Constant Rate Filters
- ✓ Add Filtration
- ✓ UV Disinfection

Wells 1-15

Basins 1-6

Basins 5-8

Mixing Chamber/Recarb

Rehab Constant Rate Filters 1-8

New Deep Bed High Constant Rate Filters 9-12

UV Disinfection

Balancing Tank

Chlorine Dioxide (membranes Only)

Chlorine

Ammonia

CO₂

Legend:

- ☐ Cl₂ Dist Sys
- ☑ GWUDI
- ☑ Mn and Fe
- ☑ DBP (40/30)
- ☑ ECC's

Granular Activated Carbon (GAC): Looks Like This


Coagulation/Physical Separation

DAF

MF/UF

GAC

UV/AOP



GAC: Provides Polishing and "Backup" Treatment

Coagulation/Physical Separation

DAF

MF/UF

GAC

UV/AOP

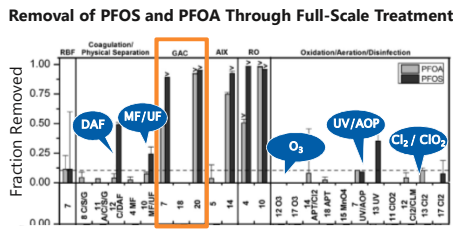


Figure 1. in Appleman et al. 2014. *Water Research*, 51, 246-255.

Ultraviolet Light / Advanced Oxidation Process (UV/AOP)


Coagulation/Physical Separation

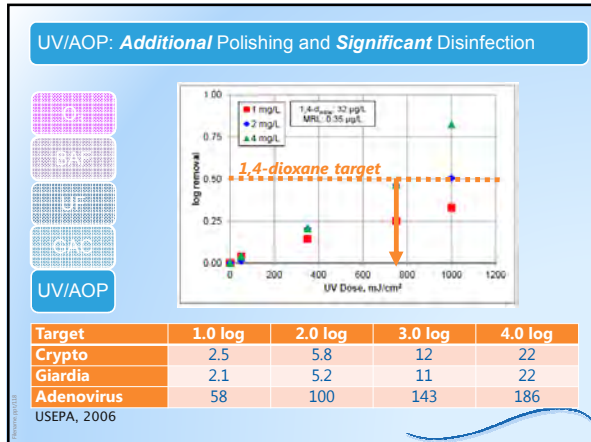
DAF

MF/UF

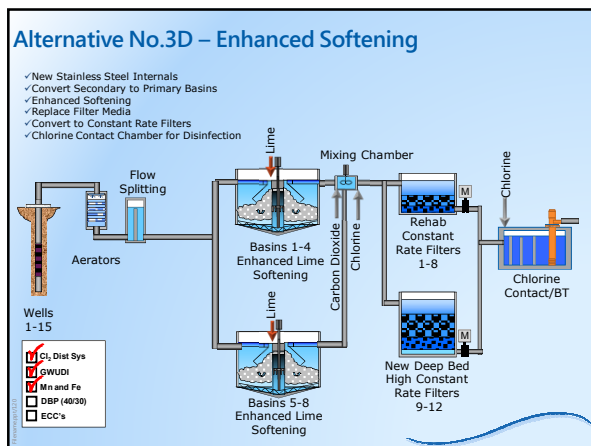
GAC

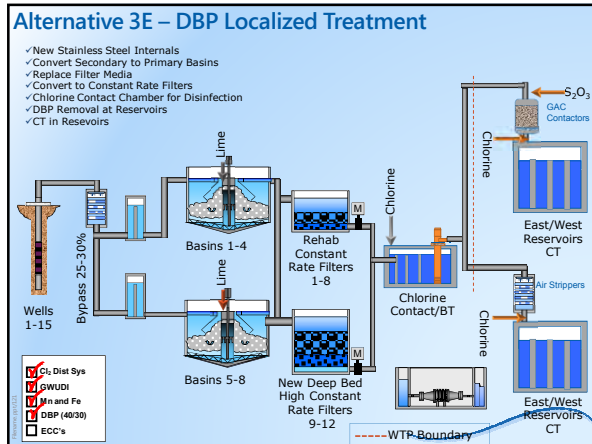
UV/AOP

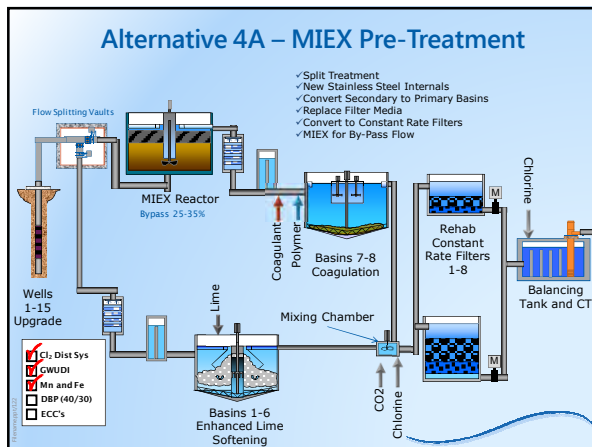


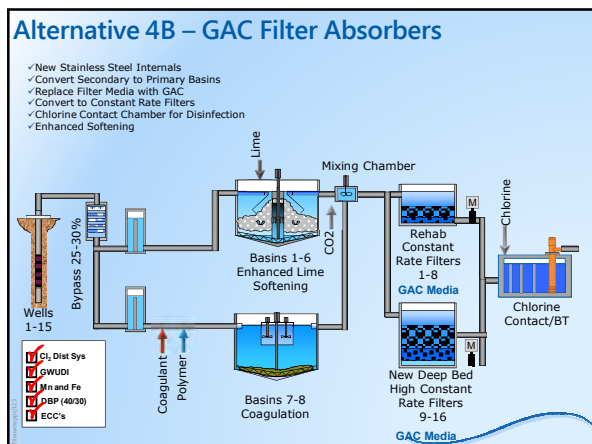


- ### Other Technologies – DBP Control
- Enhanced Softening
 - Post Treatment Aeration/Stripping
 - Post Treatment Adsorption – GAC
 - Pretreatment – MIEX
 - Treatment – GAC Filter Absorbers











Updated Action/Decision Log

DECISION LOG

DECISION LOG

Project: 0
Client: City of Columbia, MD
Job #: 0
Contract #: 0

UPDATED 5/14/2017
BY: DL

ITEM No.	DECISION BY	DECISION FOR/AUSE	DECISION DESCRIPTION	DECISION DATE	COMMENTS
1	City	Townhall Meeting	Terry is appointed the chairman for the group. no one was opposed.	10-Jul-17	Vice chair is still open and will be filled in the future.
2	City	Townhall Meeting	Decision/Action log to include decisions made, date of the decision, who made the decision, etc. if there was a vote, the voting results are to be included.	10-Jul-17	
3	City	Townhall Meeting	All cost impacts to be disclosed in anticipated rate increase in a typical year.	10-Jul-17	Charge rate increases associated with planer improvements.
4	City/Camallo	Townhall Meeting	Develop a systematic approach for evaluation of all alternatives. Score each of the alternatives as they relate to water quality, not monetary value, to distinguish the goals of the municipality.	10-Jul-17	Try and remove all emotional biases.

ACTION LOG

ACTION ITEM LOG

Project: 0
Client: City of Columbia, MD
Job #: 0
Contract #: 0

DATE: 5/14/2017
BY: DL

ITEM No.	RESPONSIBLE PARTY	ACTION ITEM	ITEM DATE	TARGET RESOLUTION DATE	ITEM COMPLETION DATE	COMMENTS
1	Camallo	Communicated the emerging developments of concern (ECOC) and their scope.	10-Jul-17			
2	Camallo	Provide support for the public regarding model development and the model's capabilities.	10-Jul-17			
3	City/Police	Ask about what is most concerning to Camallo and how to best support the things that are difficult to understand.	10-Jul-17			



Next Steps

- Summarize Visioning Questionnaire
- Set Boundaries for Project
- Conduct Fatal Flaw Analysis and Present Recommendations
- Introduce Structured Decision Analysis
- Next Meeting: September 11, 2017









Workshop Purpose

- Finalize Visioning Exercise
 - Boundaries for Investigations
 - Establish Finished Water Quality Goals
- Introduce Structured Decision Analysis
 - Background
 - Homework – Criteria Development

Workshop Agenda

- Review Visioning Questionnaire Responses
- Review Missioning Statement
- Set Project Boundaries
- Fatal Flaw Analysis Review/Discussion
- Introduction to Structured Decision Analysis
- Review Action/Decision Logs
- Review Next Steps
- General Comments by Public, Members, and Staff
- Next Meeting Date



Water Treatment Plant Configuration

1. To reduce anticipated operational expenses, should the current treatment goals to soften the water be abandoned in favor of less expensive treatment measures? (This may cause some consumers to install in-home water softeners)

Continue Softening Treatment Goals

Discontinue Softening Treatment Goals

- Citizens are accustomed to softened water
- Softening delivers a higher quality product that customers expect

Water Treatment Plant Configuration

2. The secondary regulations concern the aesthetic aspects of a drinking water supply rather than the health aspects. Should any new treatment processes consider satisfying the current secondary regulations (suggested limits) as well as the primary regulations (required by law)? Satisfying the secondary regulations is currently done at the existing facilities.

Continue Satisfying Secondary Suggested Limits for Aesthetic Properties

Discontinue Satisfying Secondary Suggested Limits for Aesthetic Properties

- Good to be ahead of the game. Secondary limits could be future regulations.
- Customers expect this quality of product

Water Treatment Plant Configuration

3. Should the study examine abandoning and demolishing the existing water treatment plant (32 mgd) and constructing an entirely new facility with source water obtained from a different location at a significant cost to current and future customers?

Existing Supply and Treatment Plant Should be abandoned
 Continue Use of Current Source and Treatment Facility

- Abandon:**
 - The investment in the existing facilities would be beyond our reasonable ability to pay.
- Continue Use:**
 - Potential source issues (GW v GWUDI) can be met with treatment options as they arise.

Water Treatment Plant Configuration

4. The end of this questionnaire provides a glossary of the advanced treatment technology and the potential benefits this technology would provide. Please select which of these advanced technologies you would like to see the study address. Please list the reasons for your selections.

<input checked="" type="checkbox"/> Membrane Filtration	<input type="checkbox"/> Air Stripping
<input checked="" type="checkbox"/> Nano/Reverse Osmosis	<input type="checkbox"/> Enhanced Softening
<input type="checkbox"/> Advanced Oxidation	<input checked="" type="checkbox"/> All of the Above
<input checked="" type="checkbox"/> Ion Exchange	<input type="checkbox"/> Others (Please List Below)
<input checked="" type="checkbox"/> Advanced Disinfection	<input type="checkbox"/> GAC
<input checked="" type="checkbox"/> Ozone/Infiltration	<input type="checkbox"/> _____
<input checked="" type="checkbox"/> Advanced Biofiltration	<input type="checkbox"/> _____

Water Treatment Plant Configuration

5. To satisfy regulations associated with disinfection by products, the City of Columbia converted from free chlorine to chloramines in the distribution system and conducts periodic conversions to chlorine to avoid issues that are associated with nitrification. There are more costly technologies that can be employed to satisfy all disinfection by product regulations and permit switching back to chlorine. Given this, how important is it to you that the City of Columbia switches back to the exclusive use of free chlorine in the distribution system? Please state the reasons for your selection:

Absolutely Critical to Switch Back to Chlorine
 Very Important to Switch Back to Chlorine
 Not Very Important
 Stay with Chloramines
 Other (Please list) _____

- Other:**
 - Would like to use free chlorine if we could still meet the DBP rule.
 - Prefer the solution that provides the most flexibility and benefits.

Water Treatment Plant Configuration

6. Past investigations of surface water and ground-water sources in Missouri and throughout the country have detected the presence of extremely low levels (one drop in 20 Olympic swimming pools) of Endocrine Disrupting (estrogen, etc) and Pharmaceutical (acetaminophen, etc.) compounds in many drinking water supplies. Studies to determine if long-term exposure to the low concentrations of these constituents impact human health are at least 10+ years away and it is not certain when (if at all) some or all of these constituents will be regulated. Technologies that remove or destroy these compounds from the supply are available but are significantly more costly to implement than the current treatment process. Given this, how important is it to you that this study considers processes that remove or destroy these compounds? Please state the reasons for your selection.

- 1 Absolutely Critical to Remove or Destroy these Compounds No Matter the Expense.
- 4 Study Should Evaluate the Costs/Benefits of Technologies that Remove or Destroy these Compounds.
- Not Very Important that Study Considers Removal/Destruction of these Compounds.
- Study **Should Not** Consider Removal/Destruction of these Compounds.
- Other (Please list) _____

Water Treatment Plant Configuration

7. Green elements at a water facility are elements that minimize chemical use and maximize energy efficiency. Should a "green" element be a consideration for ranking and analysis of treatment alternatives?

- 4 Yes
- No
- Other (Please List) _____

- Columbia is a "green" town.
- Energy efficiency is important to the plant's bottom line.

Water Treatment Plant Configuration

8. Are there any other issues regarding treatment that should be addressed?

- 3 Yes (please list) _____
- 1 No

- **YES:**
 - Cost/benefit assessment of treatment options if classification changes to GWUDI.
 - Staffing.
 - Continued use or discontinuation of fluoride.



Draft Mission Statement of Planning Workgroup

- "To enhance the quality of life for Columbia, Missouri Citizens by providing direction to Columbia Water and Light on the best means to continue its mission to provide at an affordable price; high-quality water and dependable service that exceeds customer expectations; protects and ensures a long-term water supply for future generations; and serves as responsible stewards of public health, utility resources, and the environment."

Do we want to make this more specific? I.e. best treatment process at the existing WTP?



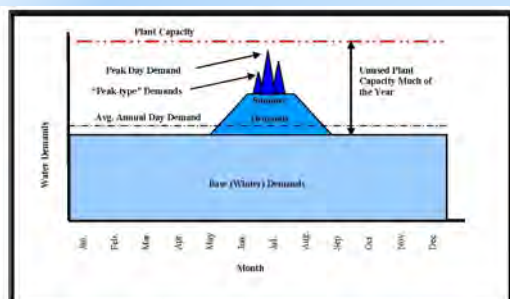
Project Boundary Exercise

- Water Supply
- Finished Water Quality Goals
- Project Framework

Project Boundary Exercise

- Water Supply
- Finished Water Quality Goals
- Project Framework

Water Supply Exercise – Basic Definitions



Water Supply Exercise – 2016 IWRP Recommendations

- Establish Future Demand Scenarios

- Basic Assumptions – Well Field:

- Wells will continue to be a source of supply (29.6 mgd).
- Wells will be expanded based upon maximizing supply.
 - 1300 feet between well "pairs"
 - 200 feet from "surface water" source
- Well Field has "space" for 52 mgd (30 wells, 2 standby)



Water Supply Exercise – 2016 IWRP Recommendations

- Basic Assumptions – Water Quality:

- Utilize Chloride to Monitor
- Bias against high chloride wells (blend)
- Consider repurposing Close wells as "cutoff" wells
- Consider possibility of reclassification as GWUDI to allow flexibility to move wells closer to river



Water Supply Exercise- 2016 IWRP Recommendations

- Maximize Local Supply for Non Potable Use
 - Deep Wells for large irrigating/industrial supply
- Continue but do not expand ASR program



Water Supply Exercise-2016 IWRP Recommendations

- Continue to expand and refine Conservation Program but harsh measures are not required due to abundance of Supply sources.
- Continue resolution with Integrated Stormwater Plan recommendations.

Water Supply Exercise Boundaries

Statement	YES	NO	MAYBE
The DWPWG Accepts the Recommendation of the IWRP	<input checked="" type="checkbox"/>		
GWUDI Compliant Facility is Required			

GWUDI vs GW Only

- Survey Results
- Decision Impacts

Water Supply Exercise Boundaries

Statement	YES	NO	MAYBE
The DWPWG Accepts the Recommendation of the IWRP	<input checked="" type="checkbox"/>		
GWUDI Compliant Facility is Required			
Others?			

Project Boundary Exercise

- Water Supply
- Finished Water Quality Goals
- Project Framework

Finished Water Quality Goals – Raw Water Quality

Table 8-1 Water Quality Goal Summary (2010 - 2012)

Parameter (mg/L or CFU/100 mL)	2010	2011	2012
Ammonia, NH₃	0.29	0.14	0.28
Raw Water	0.31	0.13	0.29
Project Best Estimate	0.28	0.14	0.28
Bioassay	1.14	1.46	1.34
Raw Water	1.12	1.46	1.34
Project Best Estimate	1.14	1.46	1.34
Chlorophyll a	0.77	0.77	0.77
Raw Water	0.77	0.77	0.77
Project Best Estimate	0.77	0.77	0.77
Coliform (fecal) (mg/L or CFU/100 mL)	0.02	0.02	0.02
Raw Water	0.02	0.02	0.02
Project Best Estimate	0.02	0.02	0.02
Iron	0.02	0.02	0.02
Raw Water	0.02	0.02	0.02
Project Best Estimate	0.02	0.02	0.02
Phosphate	0.02	0.02	0.02
Raw Water	0.02	0.02	0.02
Project Best Estimate	0.02	0.02	0.02
Turbidity (NTU)	0.02	0.02	0.02
Raw Water	0.02	0.02	0.02
Project Best Estimate	0.02	0.02	0.02
Total Dissolved Solids (mg/L or CFU/100 mL)	0.02	0.02	0.02
Raw Water	0.02	0.02	0.02
Project Best Estimate	0.02	0.02	0.02
Total Suspended Solids (mg/L or CFU/100 mL)	0.02	0.02	0.02
Raw Water	0.02	0.02	0.02
Project Best Estimate	0.02	0.02	0.02
Total Phosphorus (mg/L or CFU/100 mL)	0.02	0.02	0.02
Raw Water	0.02	0.02	0.02
Project Best Estimate	0.02	0.02	0.02
Total Nitrogen (mg/L or CFU/100 mL)	0.02	0.02	0.02
Raw Water	0.02	0.02	0.02
Project Best Estimate	0.02	0.02	0.02
Total Chlorine Residual (mg/L or CFU/100 mL)	0.02	0.02	0.02
Raw Water	0.02	0.02	0.02
Project Best Estimate	0.02	0.02	0.02

Occurrence of Pharmaceuticals in McBane Bottoms

Pharmaceutical	2010	2011	2012
1,7-Diaminobenzene (Metabolite of Caffeine)	0.118	0.020	0.020
Caffeine	0.143	0.020	0.020
Carbamazepine (Anti-epileptic)	0.022	0.020	0.020
Clopidogrel	0.020	0.020	0.020
Cytidine	0.020	0.020	0.020
Deltamethrin	0.020	0.020	0.020
Diphenhydramine	0.020	0.020	0.020

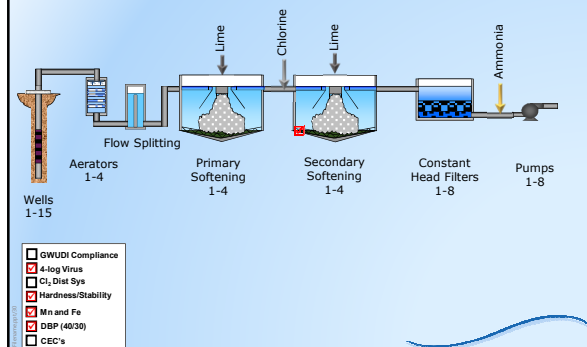
Regulatory Horizon

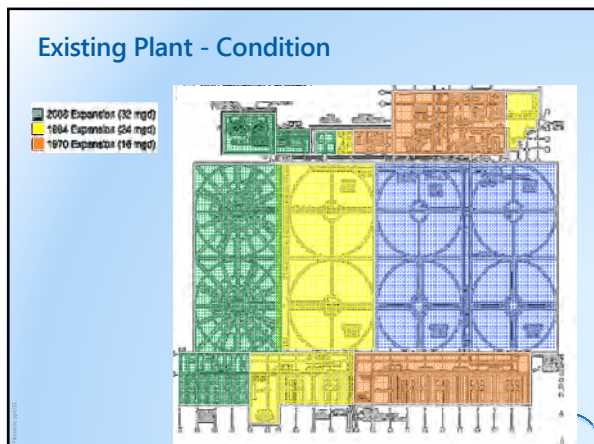
Contaminant	Regulatory Framework	Probability*
Perchlorate	2011 decision to regulate; NRDC settlement	Likely
Lead	Proposed Long Term-LCR rule expected 2017	Likely
Cyanotoxins	2015 health advisories (HA); UCMR4; CCL4	Likely
Strontium	2014 preliminary decision to regulate	Likely
Chlorate	3 rd Six Year Review, Pesticide Office	Possible
NDMA	3 rd Six Year Review	Possible
Cr(VI)	UCMR3; CCL4	Possible
1,4-dioxane	UCMR3; CCL4	Maybe
Perfluorocompounds	2016 revised HA; UCMR3; CCL4	Maybe
Brominated DBPs	UCMR4; 3 rd Six Year Review	Maybe
Manganese	UCMR4; CCL4	Maybe

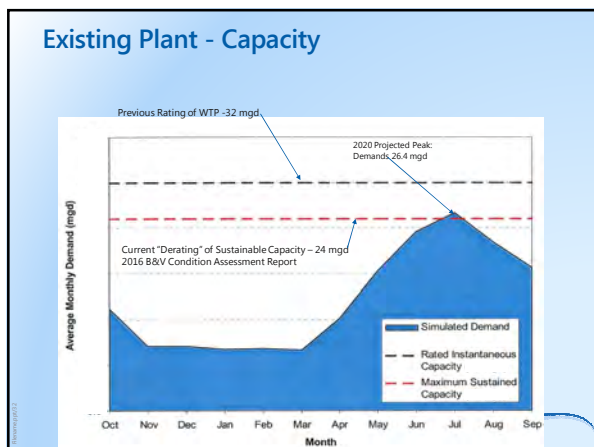
* Based on AWWA Government Affairs (Roberson, 2015); "Likely" - regulation in 5 years; "Possible" - 50/50 chance of final regulation in 5-10 years; "Maybe" - anything can happen

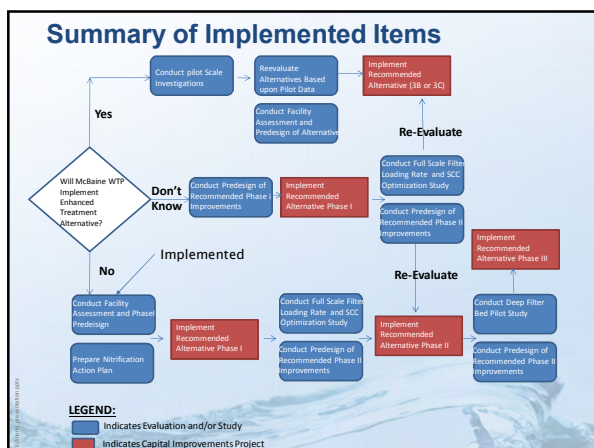
2016 Finished Water Quality Report

Existing Plant









Water Treatment Plant Configuration

3. Should the study examine abandoning and demolishing the existing water treatment plant (32 mgd) and constructing an entirely new facility with source water obtained from a different location at a significant cost to current and future customers?

- 1 Existing Supply and Treatment Plant Should be abandoned
- 2 Continue Use of Current Source and Treatment Facility

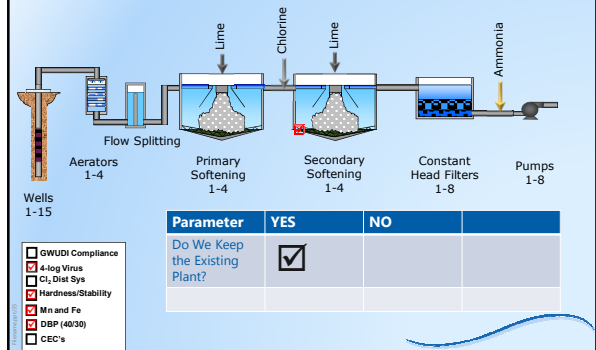
Abandon:

- The investment in the existing facilities would be beyond our reasonable ability to pay.

Continue Use:

- Potential source issues (GW v GWUDI) can be met with treatment options as they arise.

Existing Plant - Schematic



Finished Water Quality Goals:

Parameter	Regulatory Value	Enhanced WQ Value	YES	NO	MAYBE
Turbidity	≤ 0.3 NTU for 95% of Individual Filter Readings ≤ 1.0 NTU in 100% of Individual Filter Readings	Eventual Goal of Partnership Standards for New Designs ≤ 0.1 NTU for 95% of Individual Filter Readings ≤ 0.3 NTU in 100% for Individual Filter Readings.		<input checked="" type="checkbox"/>	
Disinfection	Giardia – 2 log Virus – 4 log Cryptosporidium – 2 log (bin 1)	NONE		<input checked="" type="checkbox"/>	
TTHM HAA	≤ 80ug/L RAA ≤ 60 ug/L RAA	≤ 64 ug/L RAA ≤ 48 ug/L RAA		<input checked="" type="checkbox"/>	
Total Chlorine entering System	< 4.0 mg/L	1.2-1.5 mg/L		<input checked="" type="checkbox"/>	
NDMA	NR	< 10 ng/L		<input checked="" type="checkbox"/>	
Chlorate	NR	NR		<input checked="" type="checkbox"/>	
Brominated DBP's	NR	(See TTHM/HAA)		<input checked="" type="checkbox"/>	

Water Treatment Plant Configuration

5. To satisfy regulations associated with disinfection by products, the City of Columbia converted from free chlorine to chloramines in the distribution system and conducts periodic conversions to chlorine to avoid issues that are associated with nitrification. There are more costly technologies that can be employed to satisfy all disinfection by product regulations and permit switching back to chlorine. Given this, how important is it to you that the City of Columbia switches back to the exclusive use of free chlorine in the distribution system? Please state the reasons for your selection:

Absolutely Critical to Switch Back to Chlorine

Very Important to Switch Back to Chlorine

Not Very Important

Stay with Chloramines

Other (Please list) _____

• Other:

- Would like to use free chlorine if we could still meet the DBP rule.
- Prefer the solution that provides the most flexibility and benefits.

Water Treatment Plant Configuration

6. Past investigations of surface water and groundwater sources in Missouri and throughout the country have detected the presence of extremely low levels (one drop in 20 Olympic swimming pools) of Endocrine Disrupting (estrogen, etc) and Pharmaceutical (acetaminophen, etc) compounds in many drinking water supplies. Studies to determine if long-term exposure to the low concentrations of these constituents impact human health are at least 10+ years away and it is not certain when (if at all) some or all of these constituents will be regulated. Technologies that remove or destroy these compounds from the supply are available but are significantly more costly to implement than the current treatment process. Given this, how important is it to you that this study considers processes that remove or destroy these compounds? Please state the reasons for your selection.

Absolutely Critical to Remove or Destroy these Compounds No Matter the Expense.

Study Should Evaluate the Costs/Benefits of Technologies that Remove or Destroy these Compounds.

Not Very Important that Study Considers Removal/Destruction of these Compounds.

Study Should Not Consider Removal/Destruction of these Compounds.

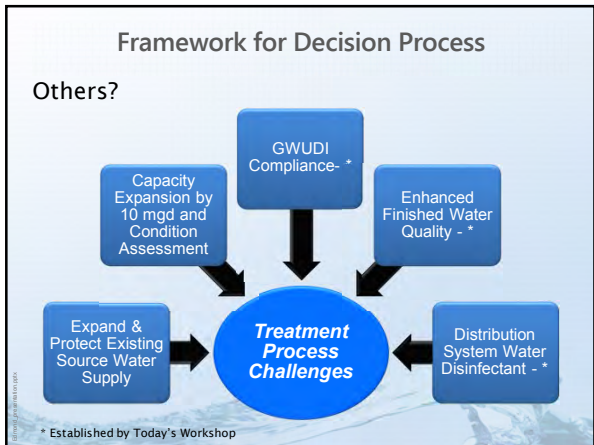
Other (Please list) _____

Finished Water Quality Goals:

Parameter	Regulatory Value	Enhanced WQ Value	YES	NO	MAYBE
CECs	Not Regulated	Treatment Process to Maximize Removal of Type of Compounds detected.			<input checked="" type="checkbox"/>
Chloramines	Not Regulated	Eliminate Need for Chloramines in System			<input checked="" type="checkbox"/>
Fluoride	4.0 mg/L MCL 0.7 mg/L MCLg	0.0 mg/L MCLg			

Project Boundary Exercise

- Water Supply
- Finished Water Quality Goals
- Project Framework

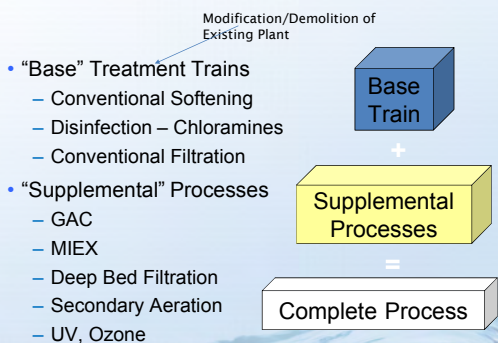




“Fatal Flaw” and “Must Include” List

- “Must Include” or the Alternative will be eliminated from consideration
 - Capacity without Purchasing Water
 - Satisfy Regulatory Requirements
 - Meets Secondary Standards (Fe and Mn)
 - Meets Hardness Goal of 150 mg/L
 - Uses existing well field
 - Optimize existing infrastructure
 - Satisfy GWUDI compliance

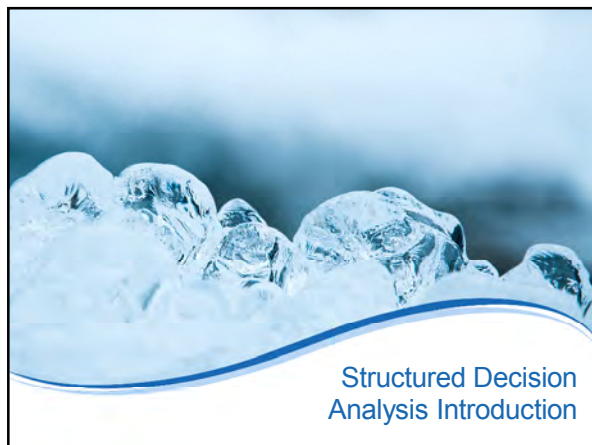
Treatment Alternative Identification

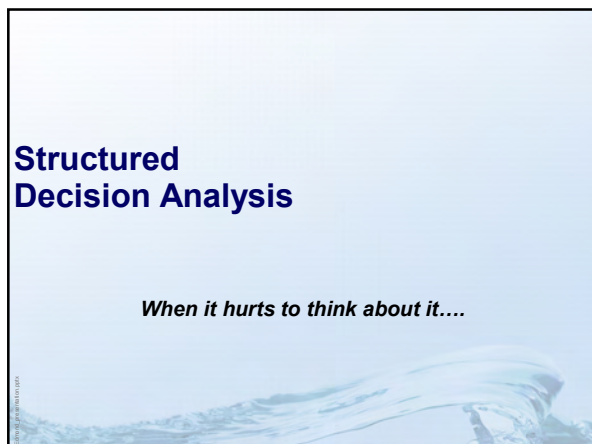


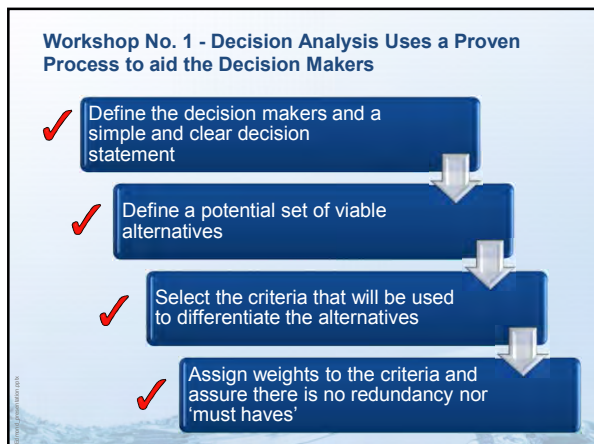
“Fatal Flaw” and “Must Include” List

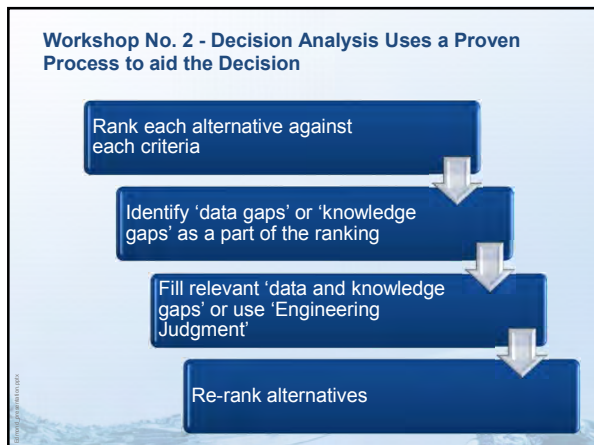
- “Fatal Flaw” will eliminate Potential Alternative from consideration
 - Technology has never been built at this scale
 - Inappropriate technology
 - Extremely inflated costs
 - Not acceptable to the Community

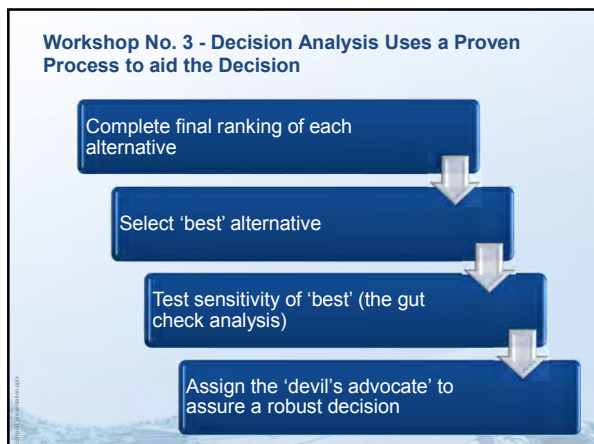
Technologies for Fatal Flaw Evaluation				
CEC Oxidation/Removal Technologies				
Ferrate	Chlorine	Chlorine dioxide	Ozone	Ozone / H2O2
Wet Air Oxidation	UV / H2O2	UV / TIO2	P. Acid / UV	Permanganate
Hardness Removal Technologies				
Conventional Softening	Enhanced Softening	Softening with caustic	Split Treatment	Pelletized Lime Reactor
High Rate Softening	Anion Exchange			Nanofiltration Reverse Osmosis
Filtration Technologies				
Nanofiltration	RO	Membranes (low pressure)	Biological filtration	Alternative filtration (bag, earth, slow sand)
Conventional Filtration		Deep bed with constant rate filtration	Manganese coated filter media	Greensand Filtration
Disinfection By Product Control				
GAC Filter Contactors	PAC Contactors – Acticarb	Post Filtration GAC Columns	Nanofiltration/RO	
Enhanced Coagulation	PAC	Ozone/Biofiltration	EC Bromide Removal	
Chlorine Dose Control	MIEX	Air Stripping	TOC Specific Resin	
Disinfection Technologies				
Chlorine	Chloramines	Ozone	Permanganate	
UV	Chlorine Dioxide	Ferrate	Periacetic Acid	













Updated Action/Decision Log

DECISION LOG					
ITEM No.	DECISION BY	DECISION FORUM	DECISION DESCRIPTION	DECISION DATE	COMMENTS
1	City	Townhall Meeting	Pete or appointed the chairman for the group, no one was opposed	14-Aug-17	Vote Chair has been filed.
2	City	Townhall Meeting	Decision/Action log to include decisions made, date of the decision, who made the decision, etc. if there was a vote, the voting results are to be included	15-Jul-17	
3	City	Townhall Meeting	All cost impacts to be displayed as anticipated rate increase to typical user	15-Jul-17	Usage rate increases associated with planned improvements.
4	City/Carelo	Townhall Meeting	Develop a systematic approach for evaluation of all alternatives. Score each of the alternatives as they relate to water quality, not monetary value, to distinguish the goals of the municipality	15-Jul-17	Try and remove all emotional biases.
5	City	Townhall Meeting	Take an appointed vote chair for the group with no objections	14-Aug-17	
6	City	Townhall Meeting	Questions are to be filed out by members of the committee and city staff	14-Aug-17	Public should be involved in the future when decisions are narrowed down.
7					
8					

ACTION LOG						
ITEM No.	RESPONSIBLE PARTY	ACTION ITEM	ITEM DATE	STATUS/RESOLUTION DATE	ITEM COMPLETION DATE	COMMENTS
1	Carelo	Compare/merck the emerging contaminants of concern (ECCs) and their source	15-Jul-17	14-Aug-17	14-Aug-17	
2	Carelo	Provide input to the public regarding model development and the model capabilities	15-Jul-17	15-Sep-17	15-Sep-17	Carelo working on Model/Fact Sheet
3	City/Public	Ask about a report concerning the Carelo open narrow land around the shops that are affected by underflow	15-Jul-17	15-Sep-17	15-Sep-17	
4	Carelo	Confer meeting with Mayor, members for review and approval of next meeting	16-Aug-17	15-Sep-17	15-Sep-17	Confirmed Action statement at 9/13/17 meeting.
5	City/Public	All questionnaire, Heat out and to Shevon by the 25th	16-Aug-17	25-Aug-17	25-Aug-17	Carelo received 6 surveys and summarized in 8/31/17 meeting.
6	Shevon	Make available monitoring and data, updated to systems	16-Aug-17	11-Sep-17	11-Sep-17	
7	Shevon	Develop business license of where Columbia has been and include the map with treatment	16-Aug-17	11-Sep-17	11-Sep-17	
8	Carelo	Send out copies of the presentation to everybody that provided the approval	16-Aug-17	15-Aug-17	15-Aug-17	Carelo working on binder for all and provide at 8/31/17 meeting.
9	Carelo	Summarize recommendations of Carelo study that has already been performed concerning what is being implemented soon	16-Aug-17	11-Sep-17	11-Sep-17	
10	Carelo	Provide either power quality report in next presentation	16-Aug-17	11-Sep-17	11-Sep-17	
11	Carelo	Prepare Project Binder with all previously presented information including critical stakeholders	11-Sep-17	9-Oct-17	11-Sep-17	Carelo to distribute at next meeting



Next Steps



- Carollo:
 - Complete Fatal Flaw Analysis Based Upon Visioning framework.
 - Develop Base Treatment Alternatives
 - Develop Additional Treatment Alternatives
 - Present Potential Treatment Alternatives for Shortlisting
- Workgroup:
 - Review Criteria and add/subtract
- Carollo/Workshop
 - Paired Comparison of Criteria to establish importance.
 - Shortlist of Treatment Alternatives
- Next Meeting: October 10th, 18th, 23rd







Appendix E
SUMMARY OF STRUCTURED DECISION
ANALYSIS WORKSHOPS

Structured Decision Analysis –Criteria Selection Workshop
City of Columbia, MO
Water and Light Department
Drinking Water Planning Workgroup
October 10, 2017, 5:30 pm
Water Treatment Plant Conference Room



The New Look of Carollo
AN INTRODUCTION OF OUR UPDATED TEMPLATES



Agenda

- Review Mission Statement
- Review Water Quality Goals
- Summarize Visioning/Project Boundaries
- Fatal Flaw Analysis Review/Discussion
- Treatment Process Review and Shortlist Discussion
- Introduction to Structured Decision Analysis (SDA)
- Criteria Selection
- Criteria Ranking
- Review Action/Decision Logs
- Review Next Steps
- General Comments by Public, Members and Staff
- Next Meeting Date
- Adjournment



Agenda

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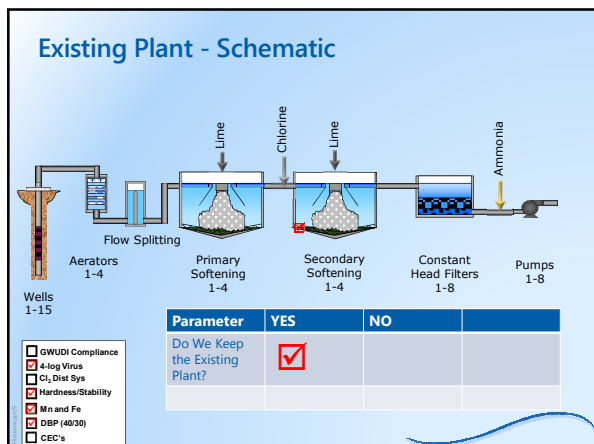
Finished Water Quality Goals:

Parameter	Regulatory Value	Enhanced WQ Value	YES	NO	MAYBE
Turbidity	≤ 0.3 NTU for 95% of Individual Filter Readings ≤ 1.0 NTU in 100% of Individual Filter Readings	Eventual Goal of Partnership Standards for New Designs ≤ 0.1 NTU for 95% of Individual Filter Readings ≤ 0.3 NTU in 100% for Individual Filter Readings			<input checked="" type="checkbox"/>
Disinfection	Giardia – 2 log Virus – 4 log Cryptosporidium – 2 log (bin 1)	NONE			<input checked="" type="checkbox"/>
TTHM HAA	≤ 80ug/L RAA ≤ 60 ug/L RAA	≤ 64 ug/L RAA ≤ 48 ug/L RAA	<input checked="" type="checkbox"/>		
Total Chlorine entering System	< 4.0 mg/L	1.2-1.5 mg/L			<input checked="" type="checkbox"/>
NDMA	NR	< 10 ng/L	<input checked="" type="checkbox"/>		
Chlorate	NR	NR	<input checked="" type="checkbox"/>		
Brominated DBPs	NR	(See TTHM/HAA)	<input checked="" type="checkbox"/>		

Finished Water Quality Goals:

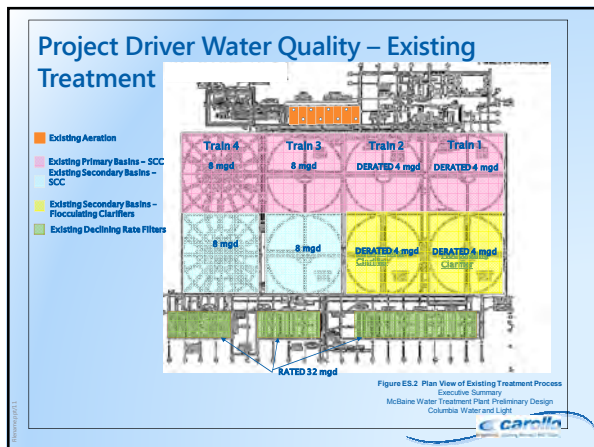
Parameter	Regulatory Value	Enhanced WQ Value	YES	NO	MAYBE
CECs	Not Regulated	Treatment Process to Maximize Removal of Type of Compounds detected.			<input checked="" type="checkbox"/>
Chloramines	Not Regulated	Eliminate Need for Chloramines in System			<input checked="" type="checkbox"/>
Fluoride	4.0 mg/l, MCL 0.7 mg/l, MCLg	0.0 mg/l, MCLg		<input checked="" type="checkbox"/>	

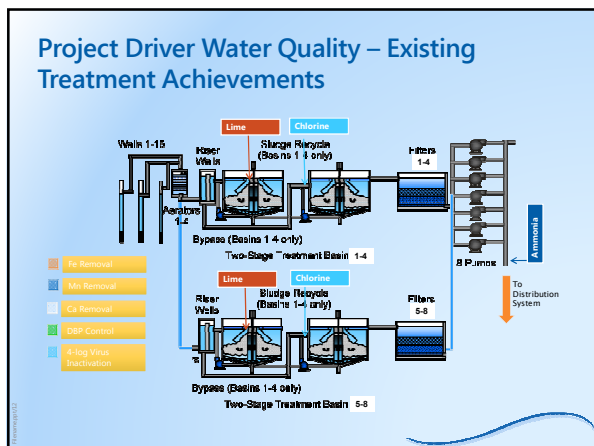
- ### Agenda
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Water Supply Exercise Boundaries

Statement	YES	NO	MAYBE
The DWPWG Accepts the Recommendation of the IWRP	<input checked="" type="checkbox"/>		
GWUDI Compliant Facility is Required			<input checked="" type="checkbox"/>
Others?			





Project Visioning- "Must Include List"

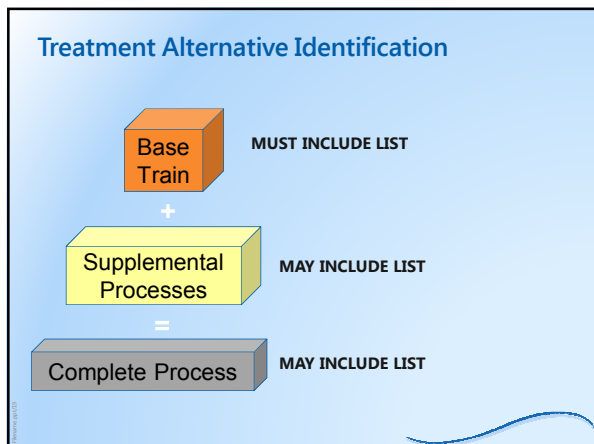
- "Must Include" or the Alternative will be eliminated from consideration
 - Reuse Existing Plant Infrastructure
 - Continued Expansion of Wellfield per IWRP
 - Meets all water quality goals for Groundwater Facility (current treatment level- softening).
 - Addresses Ageing Infrastructure as Identified in 2016 Condition Assessment to restore capacity of 32 mgd in short term (next 3 years).
 - Expansion of Plant to 48 mgd per IWRP by 2024

Project Visioning- "May Include List"

- "May Include" will be distinguished as a second or third tier alternative
 - Meets all water quality goals for a GWUDI Facility
 - Will enable plant to eliminate chloramines as a disinfectant in the distribution system.
 - Will maximize reduction of CEC's

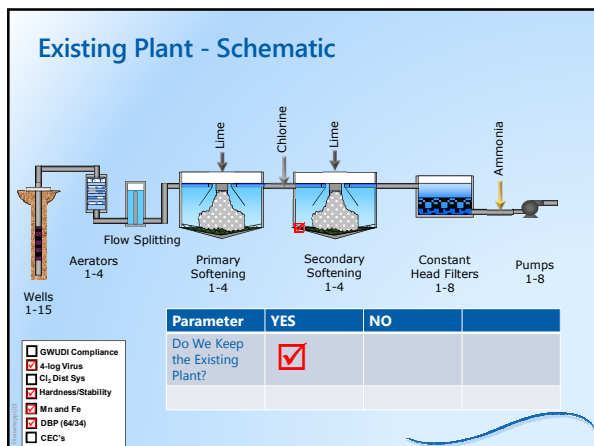
Agenda

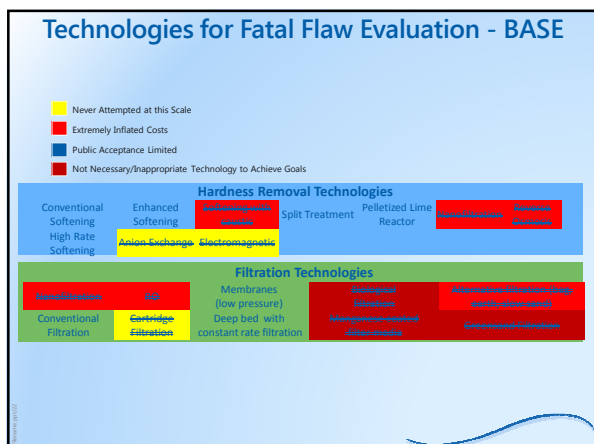
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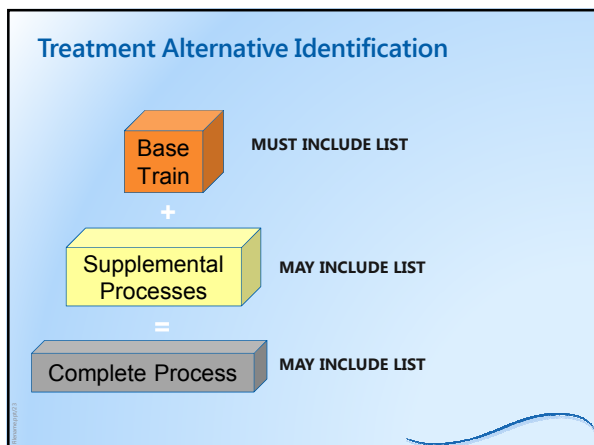


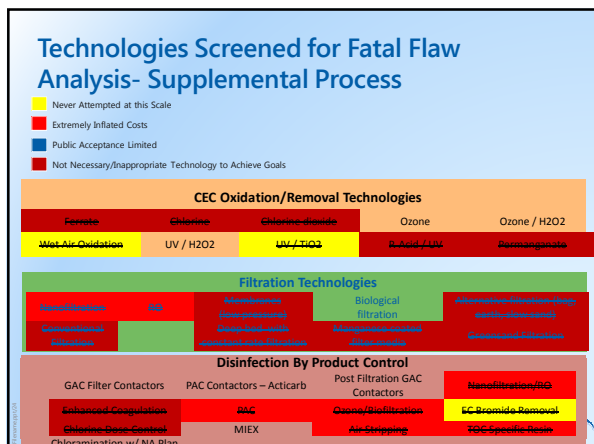
"Fatal Flaw" and "Must Include" List

- "Fatal Flaw" will eliminate Potential Alternative from consideration
 - Technology has never been built at this scale
 - Inappropriate technology
 - Extremely inflated costs
 - Not acceptable to the Community









Agenda

- Review Mission Statement
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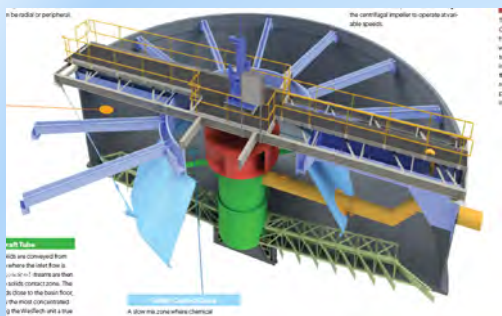
Base Treatment Alternatives

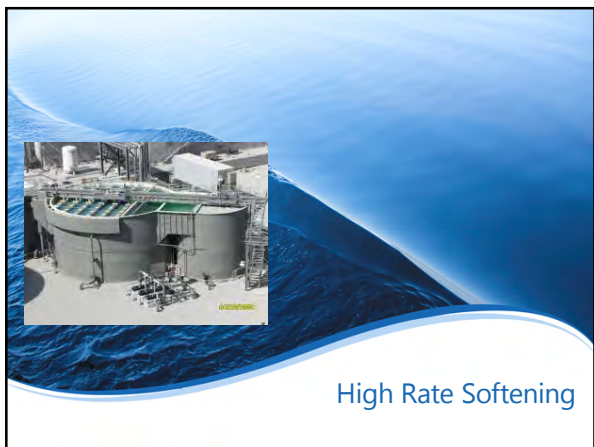
- Softening:
 - Conventional Softening (B1)
 - High Rate Softening (B2)
 - Pellet Softening (B3)
 - Nanofiltration/RO (B4)
- Filtration:
 - None
 - Conventional
 - High Rate Conventional
 - Membrane
- DBP Control:
 - Chloramines
- Disinfection:
 - Chlorine



Conventional Softening

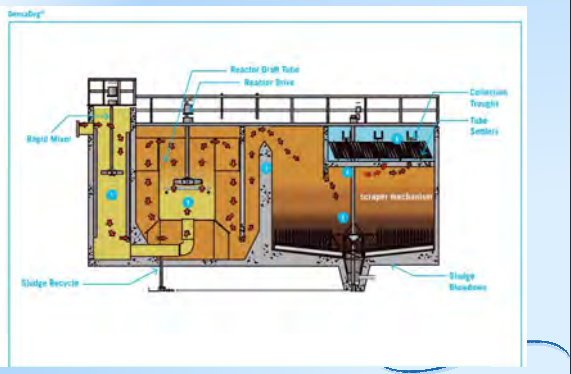
Conventional Softening Units






High Rate Softening

High Rate Softening






Conventional Softening and Pellet Softening Utilizes Same Chemistry but Physically and Hydraulically Different



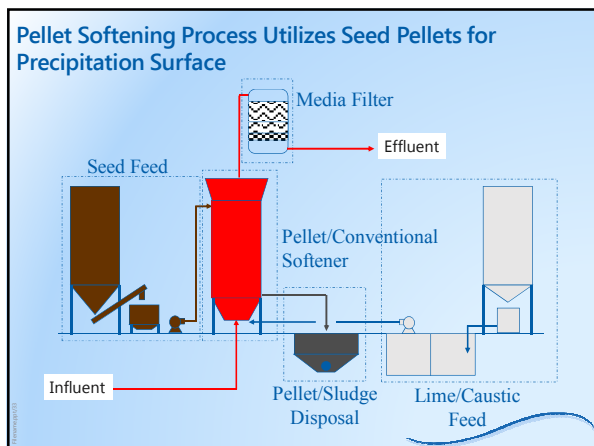
CONVENTIONAL SOFTENING

- Proven US Technology
- Low rate (1.75 gpm/sf) = large foot print
- Requires open tank = energy loss
- Residuals require drying ponds or mechanical dewatering

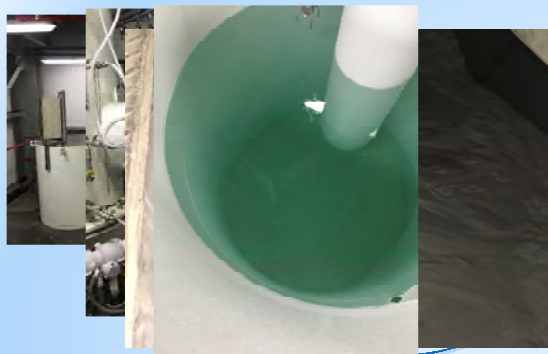


PELLET SOFTENING

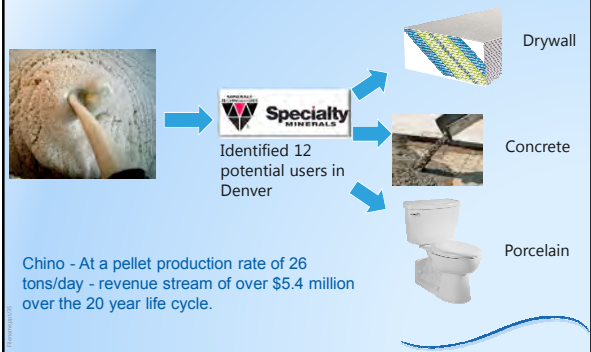
- Fluidized bed using sand/calcium carbonate seed
- Can utilize lime or caustic
- High rate (35 gpm/sf) = small footprint
- Can be operated in a pressure vessel = save energy
- Residuals easily dewatered by gravity

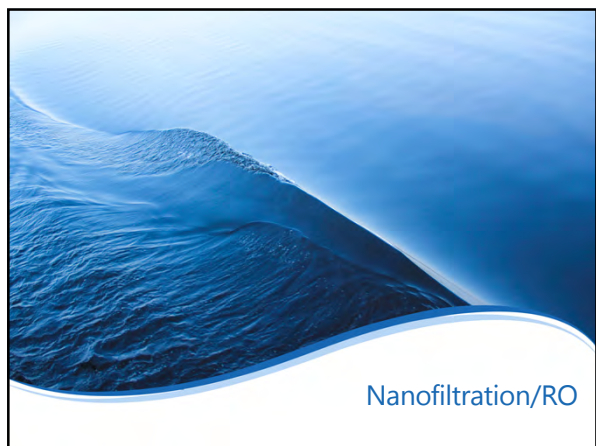


Chino CRF Utilizes Pellet Softening



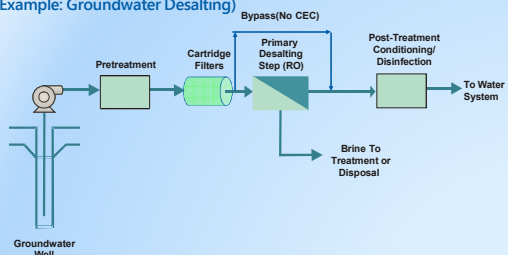
Pure Calcium Carbonate Has Missouri Market Value





A Primary Desalting RO System has Several Components

(Example: Groundwater Desalting)



Horizontal Cartridge Filter Orientation Provides Easier Access for Operators



Vertical Turbine High Pressure Feed Pumps are Commonly Used in RO Systems



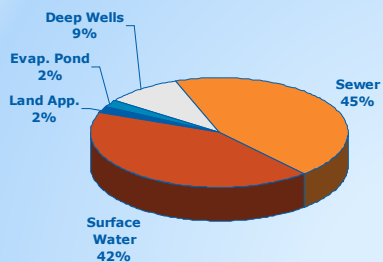
This RO plant in Hilton Head, SC Treats 3-mgd in Four RO Trains

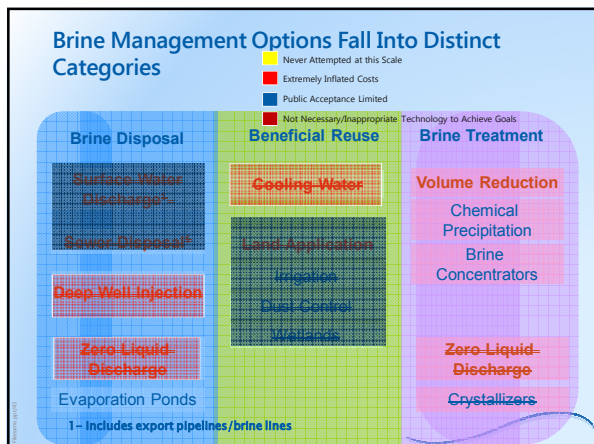


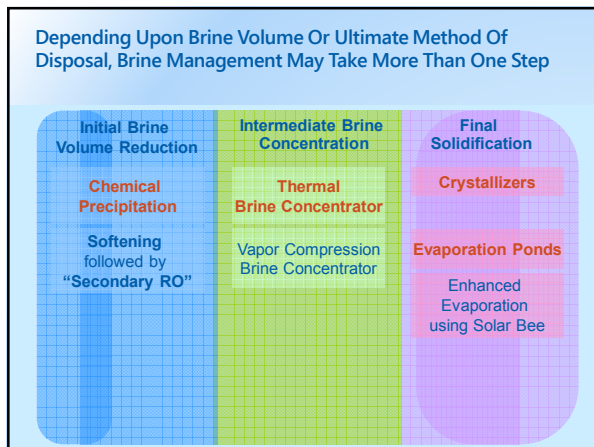
Depending on Feed Water Chemistry, Post-Treatment may include Decarbonation



Current Practice Of Brine Management In The USA



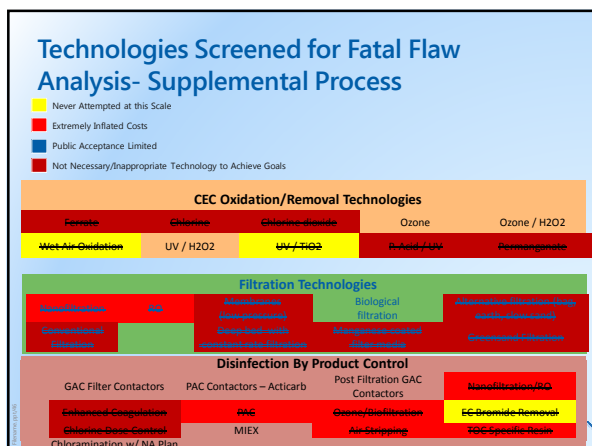




Potential Base Treatment Alternatives

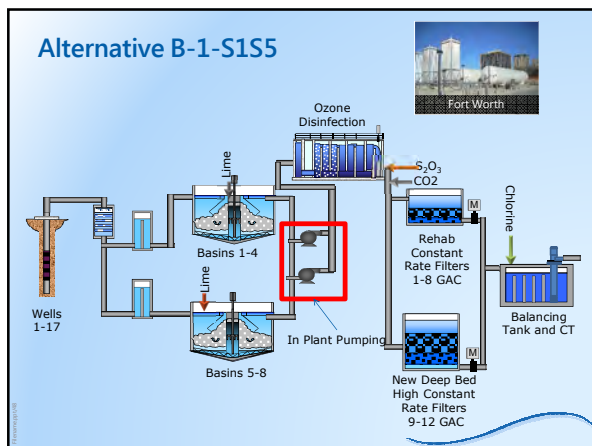
Base	Softening				Filtration				DBP Control		Disinfection		Relative Cost
	Conv	HR	Pellet	RO	Conv	HR	Mem	None	Chloramines	No additional	Chlorine		
B1-1	X				X				X		X		Low
B1-2	X					X			X		X		Low
B1-3	X						X		X		X		M/H
B2-1		X			X				X		X		Low
B2-2		X				X			X		X		Med
B2-3		X					X		X		X		M/H
B3-1			X					X	X		X		Med
B4-1				X				X	X		X		Highest
OTHER													

■ Groundwater Treatment Plant ONLY



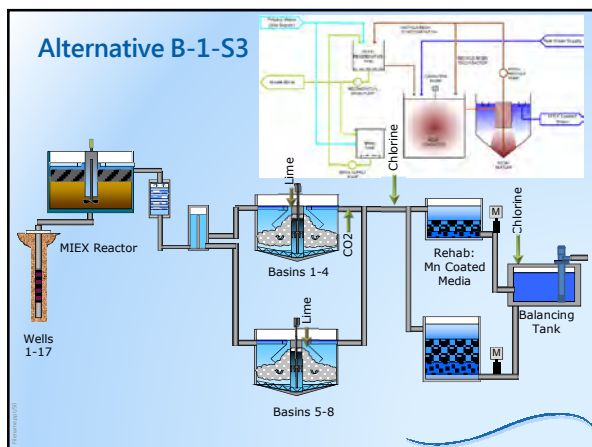
Supplemental Process

Suppli	CEC Removal			DBP Control						Relative Cost	
	Ozone/Pe- roxide (S1)	UV/Pe- roxide (S2)	None	MIEX (S3)	GAC Contactors (S4)	GAC Filters (S5)	Acticarb (PAC) (S6)				
B1-1-S155	X					X					Lower
B1-1-S255		X				X					M-H
B1-1-S355	X			X							Highest
B1-1-S3			X	X							M-H
B1-1-S4			X		X						Lower
B1-1-S6			X				X				M-H
B1-1-S154	X				X						High
B1-3-S4						X					M-H
B1-3-S6							X				High
B3-1-S155	X					X					High
B3-1-S5						X					M-H
B4-1											Highest



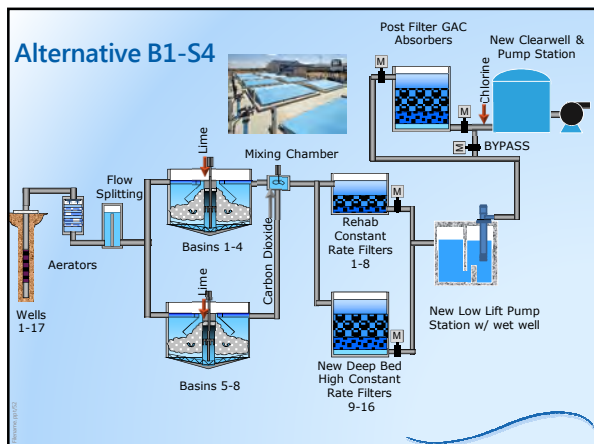
Supplemental Process

Alt.	CEC Removal			DBP Control				Relative Cost
	Ozone/Peroxide (S1)	UV/Peroxide (S2)	None	MIEX (S3)	GAC Contactors (S4)	GAC Filters (S5)	Acticarb (PAC) (S6)	
B1-1-S1S5	X					X		Lower
B1-1-S2S5		X				X		M-H
B1-1-S3S5	X			X				Highest
B1-1-S3			X	X				M-H
B1-1-S4			X		X			Lower
B1-1-S6			X				X	M-H
B1-1-S1S4	X				X			High
B1-3-S4						X		M-H
B1-3-S6							X	High
B3-1-S1S5	X					X		High
B3-1-S5						X		M-H
B4-1								Highest
OTHER								



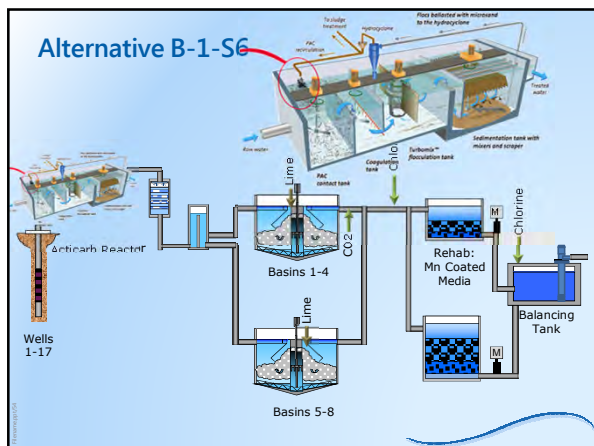
Supplemental Process

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	Ozone/Peroxide (S1)	UV/Peroxide (S2)	None	MIEX (S3)	GAC Contactors (S4)	GAC Filters (S5)	Acticarb (PAC) (S6)	
B1-1-S1S5	X					X		Lower
B1-1-S2S5		X				X		M-H
B1-1-S3S5	X			X				Highest
B1-1-S4			X		X			Lower
B1-1-S6			X				X	M-H
B1-1-S1S4	X				X			High
B1-3-S4						X		M-H
B1-3-S6							X	High
B3-1-S1S5	X					X		High
B3-1-S5						X		M-H
B4-1								Highest
OTHER								



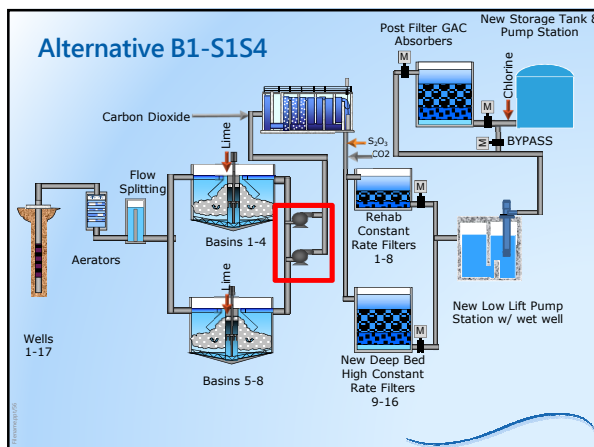
Supplemental Process

Alt.	CEC Removal				DBP Control				Relative Cost
	Ozone/Peroxide (S3)	UV/Peroxide (S2)	None	MIEX (S3)	GAC Contactors (S4)	GAC Filters (S5)	Acticarb (PAC) (S6)		
B1-1-S155	X					X			Lower
B1-1-S365		X					X		M-H
B1-1-S365	X				X				Highest
B1-1-S3			X		X				M-H
B1-1-S4			X			X			Lower
B1-1-S6			X				X		M-H
B1-1-S154	X				X				High
B1-3-S4						X			M-H
B1-3-S6							X		High
B3-1-S155	X					X			High
B3-1-S5						X			M-H
B4-1									Highest
OTHER									



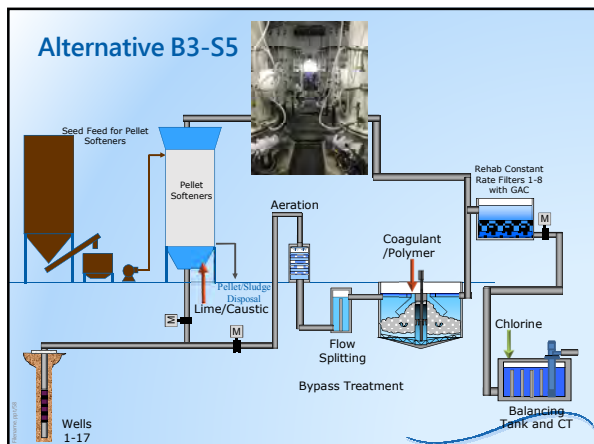
Supplemental Process

Alt.	CEC Removal			DBP Control				Relative Cost
	Ozone/Peroxide (S1)	UV/Peroxide (S2)	None	MIEX (S3)	GAC Contactors (S4)	GAC Filters (S5)	Acticarb (PAC) (S6)	
B1-1-S1S5	X					X		Lower
B1-1-S2S5		X				X		M-H
B1-1-S3S5	X			X				Highest
B1-1-S3			X	X				M-H
B1-1-S4			X		X			Lower
B1-1-S6		X	X				X	M-H
B1-1-S1S4	X				X			High
B1-3-S4						X		M-H
B1-3-S6							X	High
B3-1-S1S5	X					X		High
B3-1-S5						X		M-H
B4-1								Highest
OTHER								

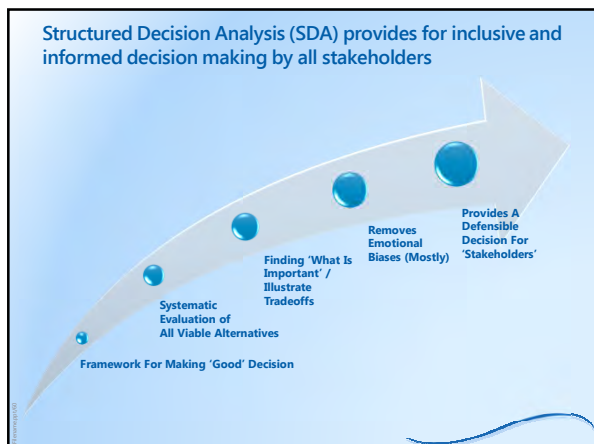


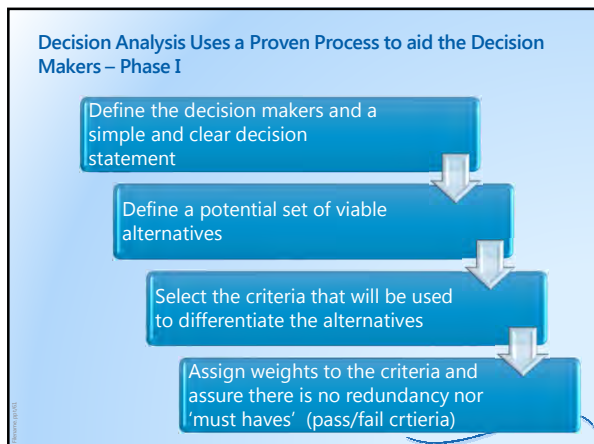
Supplemental Process

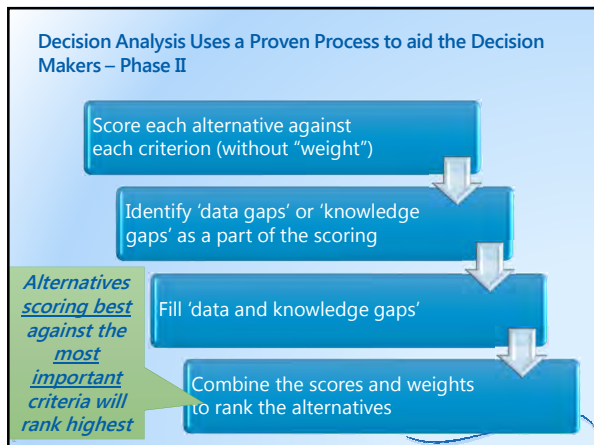
Alt.	CEC Removal			DBP Control				Relative Cost
	Ozone/Peroxide (S1)	UV/Peroxide (S2)	None	MIEX (S3)	GAC Contactors (S4)	GAC Filters (S5)	Acticarb (PAC) (S6)	
B1-1-S1S5	X					X		Lower
B1-1-S2S5		X				X		M-H
B1-1-S3S5	X			X				Highest
B1-1-S3			X	X				M-H
B1-1-S4			X		X			Lower
B1-1-S6		X	X				X	M-H
B1-1-S1S4	X				X			High
B1-3-S4						X		M-H
B1-3-S6							X	High
B3-1-S1S5	X					X		High
B3-1-S5						X		M-H
B4-1								Highest
OTHER								

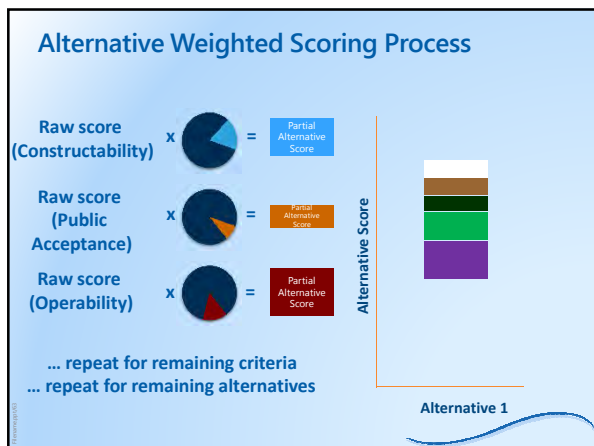


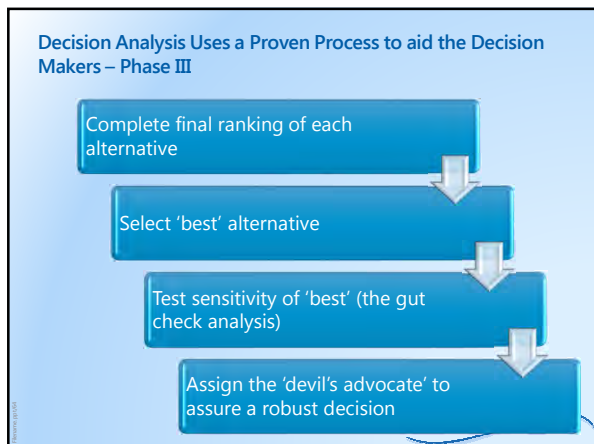
- ### Agenda
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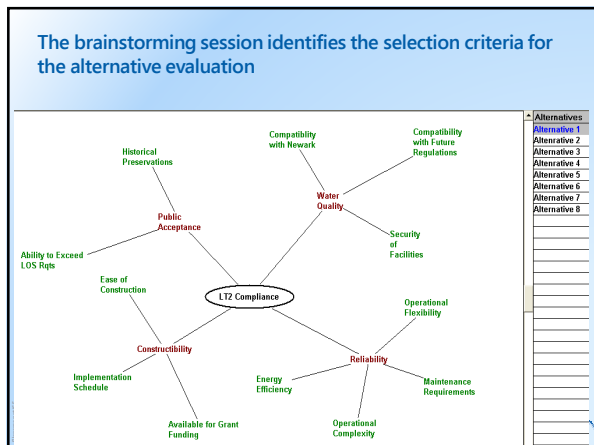


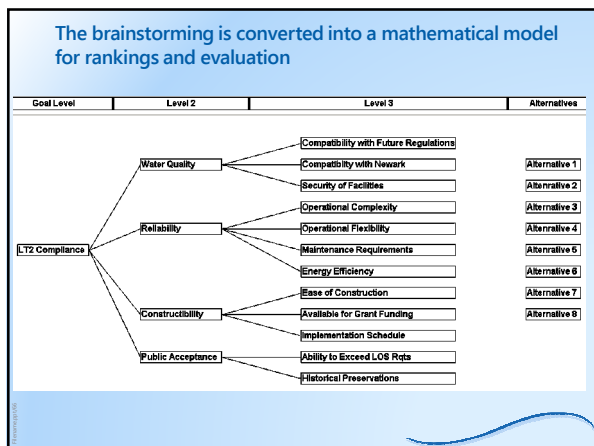




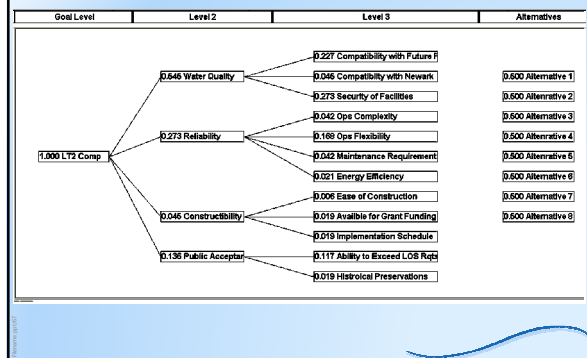




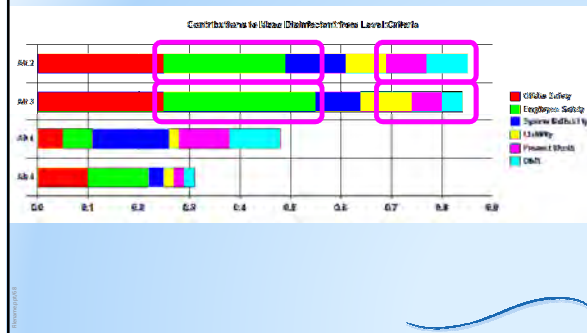




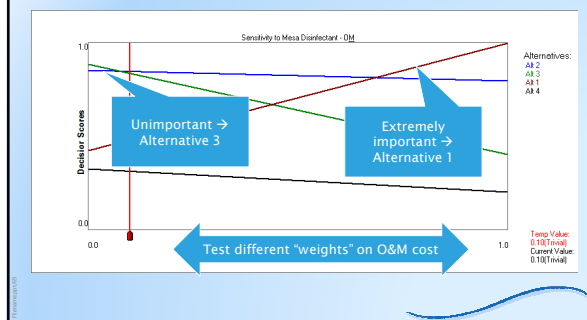
The brainstorming is converted into a mathematical model for rankings and evaluation



Model Results Help Screen Alternatives and Understand Tradeoffs



Sensitivity Analyses Help Make Robust Decisions



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Current Evaluation Criteria & Scores

A - Constructability		
Maintenance of plant operation	Plant must be able to produce finished water during construction activities.	0 - Unable to phase process with multiple plant shutdowns. 10 - Many options for phasing process alternative with minimal disruption to existing plant operations.
Schedule	Construction duration in months, shorter duration is desired.	0 - Very long construction period. 10 - Short construction period.
Space Requirements	Square feet, Smaller footprint is better.	0 - Largest footprint required to accommodate WTP structures (not including residuals handling). 10 - Smallest footprint required to accommodate WTP structures (not including residuals handling).
Permitting	Number of permits required and difficulty to obtain.	0 - Numerous permits needed requiring significant involvement from multiple stakeholders. 10 - Minimal permitting requirements with limited stakeholder involvement.

Current Evaluation Criteria & Scores

Public Acceptance		
Water Quality	Minimize formation of DBPs	0 - DBP concentrations in the distribution system comply with regulatory requirements but are not reduced from existing DBP concentrations. 10 - DBP concentrations in distribution system is reduced and meets the goal of 80% THMs and 80% HAA MCLs.
Sustainability	Minimize carbon footprint Minimize chemical usage Maximize energy efficiency Opportunities for reuse	0 - Process is not energy efficient and uses large quantities of chemicals for treatment. No opportunities for reusing waste materials. 10 - Process is efficient and uses small quantities of chemicals, uses less energy and offers opportunities for reusing waste materials.
Future Regulations	A process that can remove ECCs is good	0 - No removal of ECCs 10 - Highest removal of ECC compounds based upon Best Available Control Technology.
Communication	A process that is easily communicated to and accepted by the public and the decision makers is good	0 - Process alternative is difficult to demonstrate to stakeholders and is difficult to obtain stakeholder buy-in. 10 - Process alternative is easy to explain and widely acceptable to stakeholders.

Current Evaluation Criteria and Scores

C. Operability		
Residuals Production	Tons per year Smaller quantities of residuals are desired	0 - High residuals production. 10 - Low residuals production.
Staffing Requirements	Alternatives that do not require intensive training and large numbers of operators are desirable	0 - Extensive training is required and the process requires several operators at any given time. 10 - Training requirements are less complicated and fewer operators are required to operate the process.
Proven Technology	Alternatives including processes with a proven track record score higher than newer, less proven technologies.	0 - No full-scale installations. 10 - Extensive full-scale experience both in number of installations and number of years in service.
Maintenance Complexity	Mechanical intensity. Alternatives with more processes and/or a higher degree of sophistication are less desirable	0 - Numerous processes with extensive short- and long-term maintenance needs. 10 - Fewer processes with low level of sophistication.
Source water Treatability	Alternatives includes processes that can handle large variability in source water quality without impact to finished water quality is good.	0 - Many processes sensitive to water quality changes requiring frequent operator intervention. 10- Fewer processes sensitive to water quality changes requiring less operator intervention.

Current Evaluation Criteria and Scores

- Others:
 - Operational Costs
 - Maintenance Costs
 - Life Cycle Costs
 - Capital Costs
 - Impact on Rates as compared to ??? (MHI???, Fixed income customer???)
 - GWUDI Compliance



Pairwise Comparison Exercise

Sub-criteria Pairwise - Constructability

CONSTRUCTABILITY COMPARISON					
	Maintain Plant Operations	Schedule	Space Requirements	Permitting	
Maintain Plant Operations	NA				
Schedule	NA	NA			
Space Requirements	NA	NA	NA		
Permitting	NA	NA	NA	NA	
					NA

COST COMPARISON					
	Life Cycle	Operational	Maintenance	Capital	
Life Cycle	NA				
Operational	NA	NA			
Maintenance	NA	NA	NA		
Capital	NA	NA	NA	NA	

Sub-criteria Pairwise – Water Quality

WATER QUALITY COMPARISON					
	Water Quality Goals - TTHMS	Sustainability	Water Quality - CEC's	Communication	
Water Quality Goals - TTHMS	NA				
Sustainability	NA	NA			
Water Quality - CEC's	NA	NA	NA		
Communication	NA	NA	NA	NA	
					NA

Sub-criteria Pairwise – Operability

OPERABILITY COMPARISON					
	Residuals Production	Staffing Requirements	Proven Technology	Complexity	Source Water Quality
Residuals Production	NA				
Staffing Requirements	NA	NA			
Proven Technology	NA	NA	NA		
Complexity	NA	NA	NA	NA	
Source Water Quality	NA	NA	NA	NA	NA

Pairwise Comparison

Criteria	Constructability	Water Quality	Operability	GWUDI	COST	
Constructability	NA					
Water Quality	NA	NA				
Operability	NA	NA	NA			
GWUDI	NA	NA	NA	NA		
COST	NA	NA	NA	NA	NA	

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Next Steps

- Development of Shortlisted Alternatives
 - Process Schematic
 - Description with respect to criteria
 - Estimated Costs: Capital and Life Cycle
- Issue TM prior to Meeting
- Meeting to review and rank alternatives with respect to criteria: (Shorten Shortlist)

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- **Next Meeting Date – Monday November 13, 2017 5:30 pm Broadway**
- Adjournment

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- **Adjournment**

Pairwise Comparison and Preliminary Ranking Workshop
City of Columbia, MO
Water and Light Department
Drinking Water Planning Workgroup
November 13, 2017, 5:30 pm
Water Treatment Plant Conference Room



Agenda

- Finalize Mission Statement
- Review Pairwise Comparison Result
- Review Project Boundaries
- Discuss/Review Alternatives and Carollo Shortlist
- SDA Model
- Discuss and Rank Shortlisted Alternatives
- Review Data Gaps
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Finalize Mission Statement and Goals

FINAL DRAFT Mission Statement for Drinking Water Planning Workgroup:

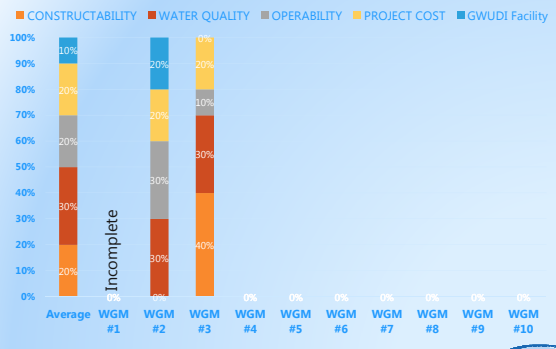
Mission Statement: Provide planning recommendations to the Water and Light Advisory Board and the City Council regarding the replacement of the water treatment system by establishing water quality goals, determining construction criteria and, conducting a thorough, objective, assessment of industry accepted treatment technologies to determine the process or processes that best meet those criteria.

- The Goals of the Drinking Water Planning Workgroup are as follows:**
- Review current planning strategies for water supply and verify current goals and planning horizon for water treatment capacity expansion.
 - Consider current regulations, potential future regulations, and potential future water reuse and recycling potential long-term water quality goals.
 - Assess the state of the industry and identify potential treatment strategies that meet or exceed some or all of the potential long-term water quality goals based upon industry acceptance and long-term (present and future) costs.
 - Formulate a set of water quality goals with potential treatment strategies to meet or exceed potential goals in the area.
 - Objectively evaluate and rank potential treatment strategies that meet planning horizon goals using a structured decision analysis model.
 - Conduct a sensitivity analysis of decisions to review decisions and identify alternatives to potential changes in criterion assessments.
 - Through the decision process, develop planning recommendations to guide the Water and Light Advisory Board and City Council regarding the water treatment system.

Agenda

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Criteria Weighting Results



Voting to Accept Pairwise Comparisons

- Accept pairwise comparisons as is?
- Potentially delay schedule to incorporate pairwise comparisons from this workshop?

Final Schedule



Constructability Pairwise Comparison

I. CONSTRUCTABILITY PAIRWISE COMPARISON WORKSHEET					
	Maintain Plant Operations	Schedule	Space Requirements	Permitting	
Maintain Plant Operations	NA	Maintain Plant Operations	67% Space 33% Maint. O.	Maintain Plant Operations	
Schedule	NA	NA	Space Requirements	Permitting	
Space Requirements	NA	NA	NA	67% Permit 33% Space	
Permitting	NA	NA	NA	NA	

Notes:
1. Do not use Shaded Spaces

Water Quality Pairwise Comparison

B. WATER QUALITY PAIRWISE COMPARISON					
	Water Quality Goals - TTHMs	Sustainability	Water Quality - CEC's	Communication	
Water Quality Goals - TTHMs	NA	TTHMs	TTHMs	TTHMs	
Sustainability	NA	NA	Sustainability	Sustainability	
Water Quality- CEC's	NA	NA	NA	CECs	
Communication	NA	NA	NA	NA	

Notes:
1. Do not use Shaded Spaces

Operability Pairwise Comparison

C. OPERABILITY PAIRWISE COMPARISON WORKSHEET					
	Residuals Production	Staffing Requirements	Proven Technology	Complexity	Source Water Quality
Residuals Production	NA	67% Staffing 33% Res.	Proven Tech	Complexity	67% Source WQ 33% Residuals
Staffing Requirements	NA	NA	67% Tech. 33% Staffing	67% Staffing 33% Complexity	67% Staffing 33% Source WQ
Proven Technology	NA	NA	NA	67% Complexity 33% Tech.	Proven Tech
Complexity	NA	NA	NA	NA	Complexity
Source Water Quality	NA	NA	NA	NA	NA

Notes:
1. Do not use shaded spaces.

Cost Comparison Pairwise Comparison

D. COST PAIRWISE COMPARISON WORKSHEET				
	Life Cycle	Operational	Maintenance	Capital
Life Cycle	NA	67% Operational 33% Life Cycle	67% Maintenance 33% Life Cycle	67% Capital 33% Life Cycle
Operational	NA	NA	Operational	67% Operational 33% Capital
Maintenance	NA	NA	NA	67% Capital 33% Maintenance
Capital	NA	NA	NA	NA

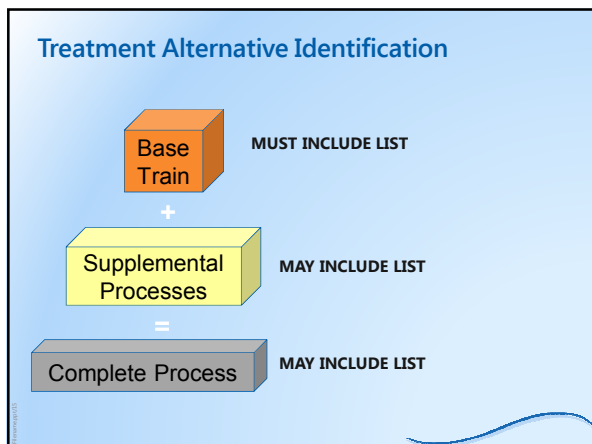
Notes:
1. Do not use shaded spaces.

GWUDI/Major Pairwise Comparison

E. GWUDI/MAJOR PAIRWISE COMPARISON WORKSHEET					
	A. Constructability	B. Water Quality	C. Operability	D. Cost	E. GWUDI
A. Constructability	NA	67% Water Quality 33% Const.	67% Op. 33% Const.	50% Cost 50% Const.	50% GWUDI 50% Const.
B. Water Quality	NA	NA	Water Quality	67% WQ 33% Cost	WQ
C. Operability	NA	NA	NA	50% Op. 50% Cost	Op.
D. Cost	NA	NA	NA	NA	50% GWUDI 50% Cost
E. GWUDI	NA	NA	NA	NA	NA

Notes:
1. Do not use shaded spaces.

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“Fatal Flaw” and “Must Include” List

- “Fatal Flaw” will eliminate Potential Alternative from consideration
 - Technology has never been built at this scale
 - Inappropriate technology
 - Extremely inflated costs
 - Not acceptable to the Community

Fatal Flaw Analysis Base Treatment Trains

- Never Attempted at this Scale
- Extremely Inflated Costs
- Public Acceptance Limited
- Not Necessary/Inappropriate Technology to Achieve Goals

Hardness Removal Technology		Hardness Removal Technology	
Fatal Flaw	Treatment Technology	Fatal Flaw	Treatment Technology
	Conventional Softening		Conventional Softening
	High Rate Softening		High Rate Softening
■	Enhanced Softening		
■	Softening with Caustic		
■	Anion Exchange		
■	Split Treatment		
	Nanofiltration/RO		Nanofiltration/RO
	Pelletized Lime Reactor		Pelletized Lime Reactor
■	Electromagnetic		
■	Home POU devices		

Fatal Flaw Analysis Base Treatment Trains

- Never Attempted at this Scale
- Extremely Inflated Costs
- Public Acceptance Limited
- Not Necessary/Inappropriate Technology to Achieve Goals

Filtration Technology		Filtration Technology	
Fatal Flaw	Treatment Technology	Fatal Flaw	Treatment Technology
	Conventional Filtration – Constant Rate		Conventional Filtration – Constant Rate
	Ultrafiltration Membranes		Ultrafiltration Membranes
	Deep bed filtration – Constant Rate		Deep Bed Filters – Constant Rate
■	Alternative (Slow Sand Diatomaceous Earth)		
	MnO2 Coated Media Filtration		
■	Manganese Greensand		
	Nanofiltration/RO		Nanofiltration/RO
■	Cartridge Filtration		
	Declining Rate Filtration		Declining Rate Filtration

Fatal Flaw Analysis Advanced Treatment

■ Never Attempted at this Scale
■ Extremely Inflated Costs
■ Public Acceptance Limited
■ Not Necessary/Inappropriate Technology to Achieve Goals

CEC Removal/Oxidation Technology	
Fatal Flaw	Treatment Technology
■	Ferrate
■	Free Chlorine
	Chlorine Dioxide
	Ozone or Ozone/Peroxide
■	Wet Air Oxidation
	UV/Peroxide
■	UV/Titanium Dioxide
■	UV/Peracetic Acid
■	Permanganate

➔

CEC/Oxidation Removal Technology	
Fatal Flaw	Treatment Technology
	Chlorine Dioxide (Mn Only)
	Ozone or Ozone Peroxide
	UV/Peroxide
	Nanofiltration/RO

Fatal Flaw Analysis Advanced Treatment

■ Never Attempted at this Scale
■ Extremely Inflated Costs
■ Public Acceptance Limited
■ Not Necessary/Inappropriate Technology to Achieve Goals

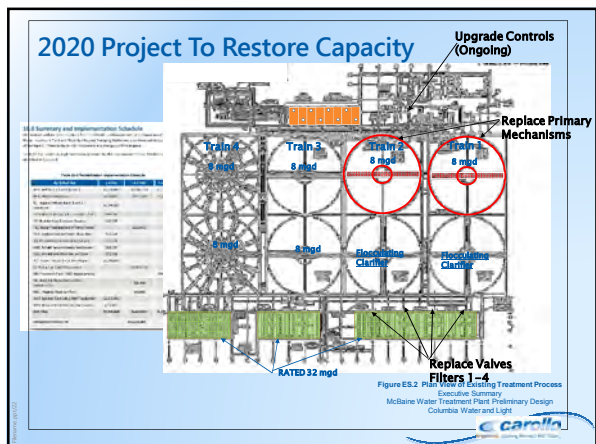
DBP Precursor Removal Technology	
Fatal Flaw	Treatment Technology
■	GAC Filter Contactors
	PAC Contactors (Actiflow CARBm)
	Post Filter GAC Contactors
	Nanofiltration/RO
	Enhanced Coagulation
■	Ozone Biofiltration
■	Chlorine Dose Control
■	Anion Exchange Beds
	Chloramination (w/ Nitrification Action Plan)
	MIEX (magnetic Ion Exchange)
■	Air Stripping
■	Electrodialysis

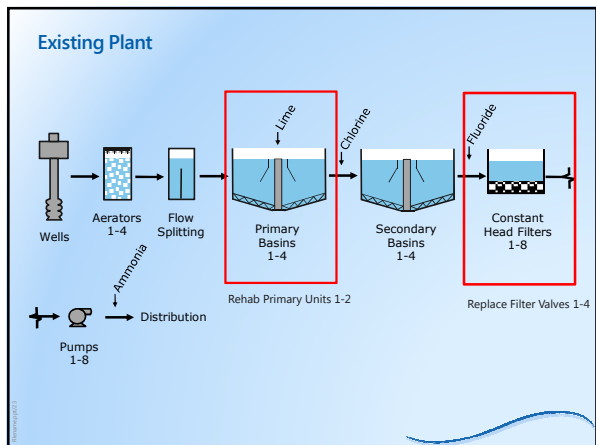
➔

DBP Precursor Removal Technology	
Fatal Flaw	Treatment Technology
	PAC Contactors (Actiflow CARBm)
	Post Filter GAC Contactors
	Nanofiltration/RO
	Enhanced Coagulation (only in Bypass)
	Chloramination (w/ Nitrification Action Plan)
	MIEX (magnetic Ion Exchange)

Project Visioning- "Must Include List"

- "Must Include" or the Alternative will be eliminated from consideration
 - Reuse Existing Plant Site
 - Continued Expansion of Wellfield per IWRP
 - Meets all water quality goals for Groundwater Facility (current treatment level- softening).
 - Addresses Aging Infrastructure as Identified in 2016 Condition Assessment to restore capacity of 32 mgd in short term (next 3 years).
 - Expansion of Plant to 48 mgd per IWRP by 2024





- Project Visioning- "May Include List"**
- "May Include" will be distinguished as a second or third tier alternative
 - Meets all water quality goals for a GWUDI Facility
 - Will enable plant to eliminate chloramines as a disinfectant in the distribution system.
 - Will maximize reduction of CEC's

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Treatment Alternative Identification

Base Train MUST INCLUDE LIST

Supplemental Processes MAY INCLUDE LIST

Complete Process MAY INCLUDE LIST

Existing Plant

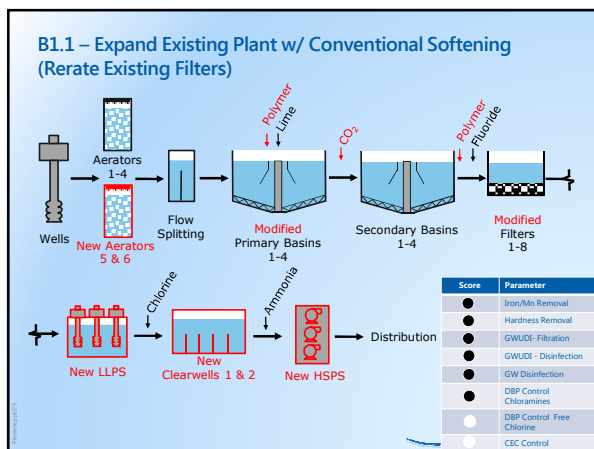
Score	Parameter
●	Iron/Mn Removal
●	Hardness Removal
●	GWUDI- Filtration
●	GWUDI - Disinfection
●	GW Disinfection
●	DBP Control Chloramines
●	DBP Control Free Chlorine
●	CEC Control

Columbia WTP Expansion Alternatives

Alternatives			
Base Alternative	GWUDI Compliance	DBP Control	CEC Removal
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○	○	○
B2 – New 15 mgd Treatment Train	○	○	○
B3 – Replace Filters w/ UF Membranes	●	○	○
B4 – Replace Plant w/RO Facility	●	●	○
B5 – Replace Conventional Softening w/Pellet Softening	●	○	○

● Yes, ○ Partial, ○ No

Adder for GWUDI
 · S1.1 – Expansion to GWUDI
 Adder for DBP Control
 · S2.1 – GAC
 · S2.2 – MBEX
 · S2.3 – Actiflo™ CARB
 Adder for CEC Removal
 · S3.1 – UV Disinfection
 · S3.2 – Ozone

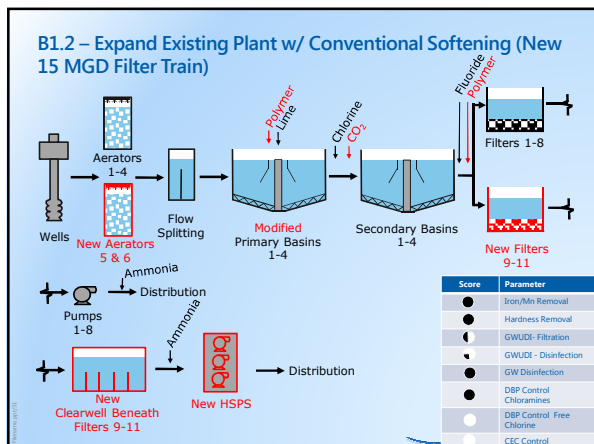


Columbia WTP Expansion Alternatives

Alternatives			
Base Alternative	GWUDI Compliance	DBP Control	CEC Removal
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○	○	○
B2 – New 15 mgd Treatment Train	○	○	○
B3 – Replace Filters w/ UF Membranes	●	○	○
B4 – Replace Plant w/RO Facility	●	●	○
B5 – Replace Conventional Softening w/Pellet Softening	●	○	○

● Yes, ○ Partial, ○ No

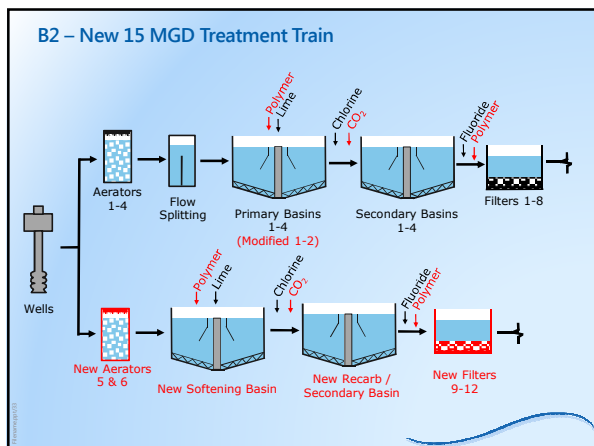
Adder for GWUDI
 · S1.1 – Expansion to GWUDI
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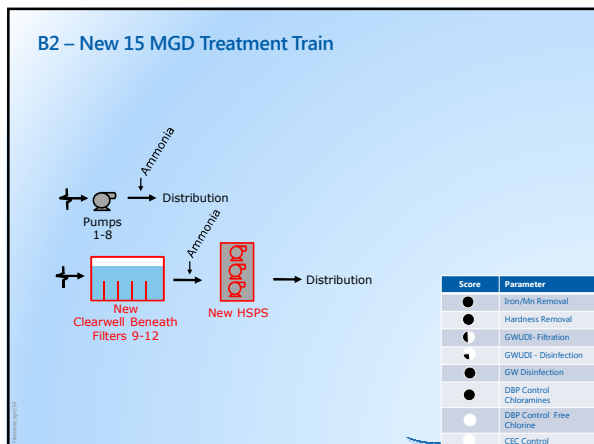


Columbia WTP Expansion Alternatives

Base Alternative	GWUDI Compliance	DBP Control	CEC Removal	Adder for GWUDI
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○	S1.1 – Expansion to GWUDI
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○	○	○	Adder for DBP Control S1.1 – GAC S2.2 – MEX S2.3 – Actiflo™ CARB
B2 – New 15 mgd Treatment Train	Add S1.1	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	Adder for CEC Removal S3.1 – UV Disinfection S3.2 – Ozone
B3 – Replace Filters w/ UF Membranes	●	○	○	
B4 – Replace Plant w/RO Facility	●	●	●	
B5 – Replace Conventional Softening w/Pellet Softening	●	○	○	

● Yes, ○ Partial, ○ No

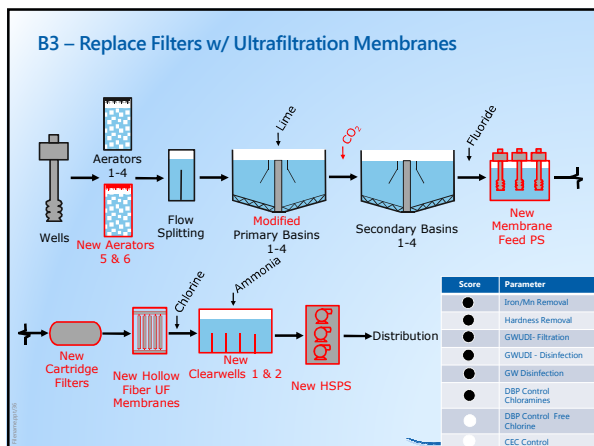




Columbia WTP Expansion Alternatives

Base Alternative	GWUDI Compliance	DBP Control	CEC Removal	
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○	Adder for GWUDI • S1.1 – Expansion to GWUDI
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○	○	○	Adder for DBP Control • S2.1 – GAC • S2.2 – MEX • S2.3 – Actiflo™ CARB
B2 – New 15 mgd Treatment Train	Add S1.1	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	Adder for CEC Removal • S3.1 – UV Disinfection • S3.2 – Ozone
B3 – Replace Filters w/ UF Membranes	●	○	○	
B4 – Replace Plant w/RO Facility	●	●	●	
B5 – Replace Conventional Softening w/Pellet Softening	●	○	○	

● Yes, ● Partial, ○ No



Columbia WTP Expansion Alternatives

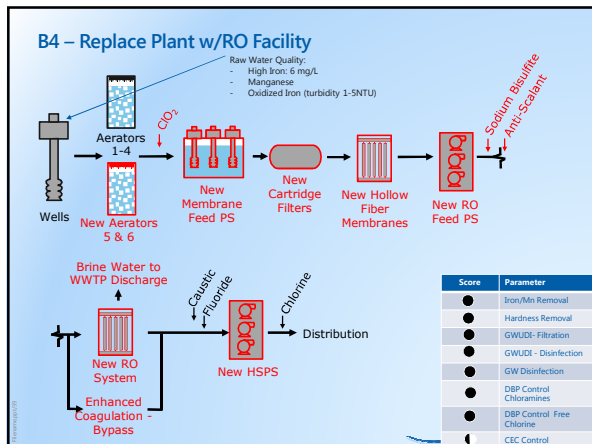
Alternatives				
Base Alternative	GWUDI Compliance	DBP Control	CEC Removal	
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○	Adder for GWUDI • S1.1 – Expansion to GWUDI
		Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○	○	○	Adder for CEC Removal • S3.1 – UV Disinfection • S3.2 – Ozone
	Add S1.1	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B2 – New 15 mgd Treatment Train	○	○	○	
	Add S1.1	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B3 – Replace Filters w/ UF Membranes	●	○	○	
		Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B4 – Replace Plant w/RO Facility	●	●	●	
			Add S3.1 or S3.2	
B5 – Replace Conventional Softening w/Pellet Softening	●	○	○	
		Add S2.1, S2.2, S2.3	Add S3.1 or S3.2	

● Yes, ● Partial, ○ No

Source Water Quality

Parameter	Units	Range (Wells)
Hardness, Total	mg/L as CaCO ₃	218 – 534
Calcium	mg/L as CaCO ₃	189 – 265
Magnesium	mg/L as CaCO ₃	61 – 79
Iron (Total)	mg/L	2.8 – 14.2
Manganese (Total)	mg/L	0.197 – 1.33
Turbidity	NTU	0.14-2.5

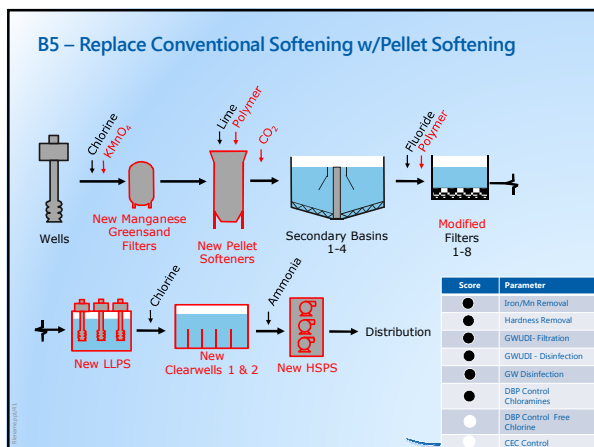
*Historical raw water quality from McBaine WTP Expansion Preliminary Design Report (Carollo, 2012)

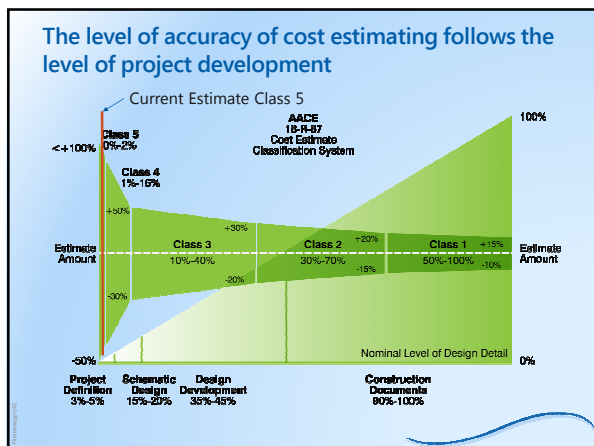


Columbia WTP Expansion Alternatives

Base Alternative	GWUDI Compliance	DBP Control	CEC Removal	
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○	Adder for GWUDI • S1.1 – Expansion to GWUDI
		Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○	○	○	Adder for CEC Removal • S3.1 – UV Disinfection • S3.2 – Ozone
	Add S1.1	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B2 – New 15 mgd Treatment Train	○	○	○	
	Add S1.1	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B3 – Replace Filters w/ UF Membranes	●	○	○	
		Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B4 – Replace Plant w/RO Facility	●	●	○	
			Add S3.1 or S3.2	
B5 – Replace Conventional Softening w/Pellet Softening	●	○	○	
		Add S2.1, S2.2, S2.3	Add S3.1 or S3.2	

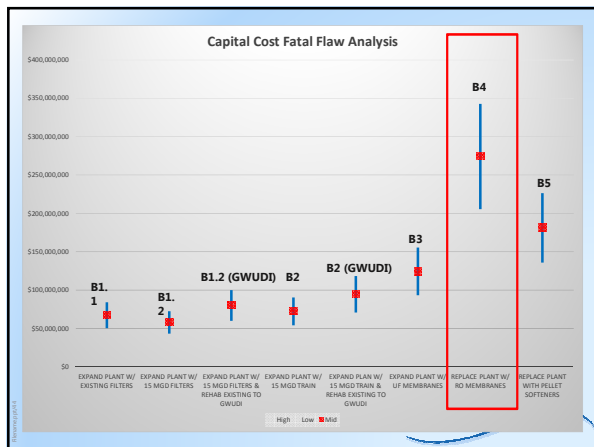
● Yes, ○ Partial, ○ No

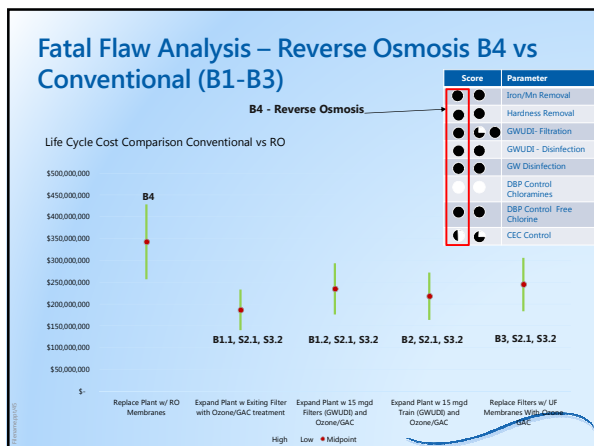


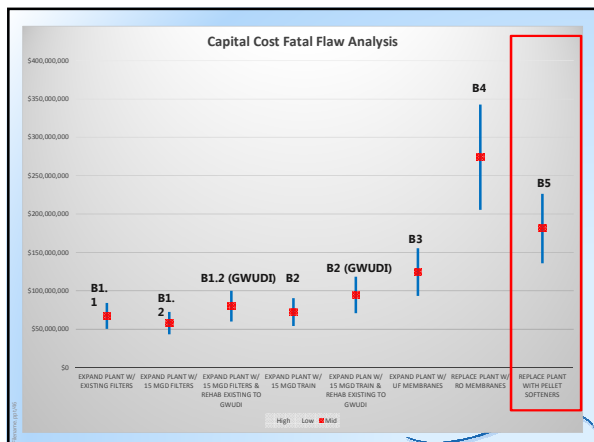


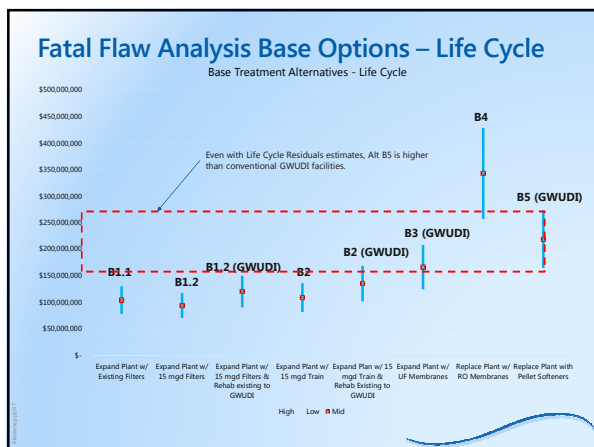
Cost Estimate

- Class 5 AACE – Order of Magnitude
- Markups –
 - General Conditions – 8%
 - Contractor Overhead and Profit – 10%
 - General Conditions – 8%
 - Engineering and Admin – 12%
 - Contingency – 50%
- All alternatives provide a plant capacity of 48 mgd
- Cost Development
 - 2016 Condition Assessment
 - Historical data
 - Market Trends
 - Vendor Quotes
 - Cost Estimating Manuals
- O&M
 - 13 MGD Average Annual Flow
 - Current Dosages
 - \$0.08 per kWh
 - 0.25% of Capital for O&M



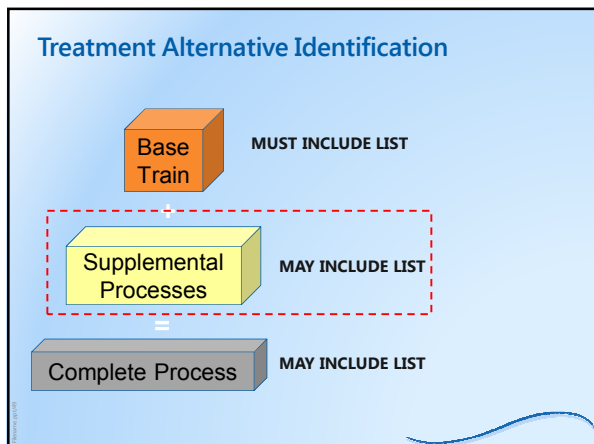






Fatal Flaw Analysis

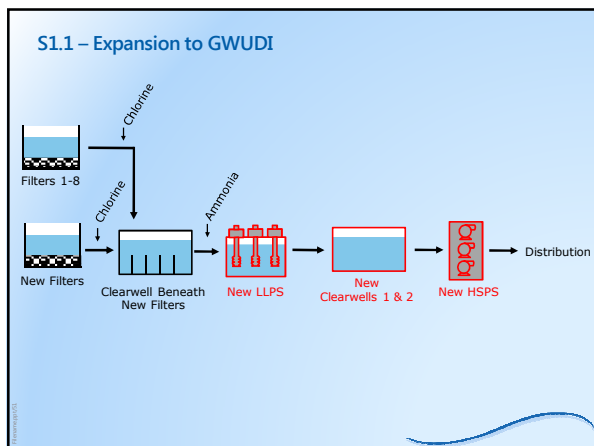
- Eliminate B4 from Consideration:
 - RO membranes too expensive
 - Permitting of Brine disposal problematic
 - Well water quality (oxidized iron, turbidity, silica) not conducive to RO treatment, requires pre-treatment prior to membranes.
 - Conventional technologies with advanced treatment still less expensive to achieve same goals.
- Eliminate B5 from Consideration:
 - Pellet softeners too expensive (capital)
 - Insufficient sales revenue to tip operational costs in favor of pellet softening
 - Well water quality (iron, manganese) not conducive to Pellet softeners. Require pretreatment to remove iron/manganese to prevent fouling.
 - Other base alternatives achieve same goals with lower costs (hardness removal)



Columbia WTP Expansion Alternatives

Base Alternative	GWUDI Compliance	DBP Control	CEC Removal	
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○	Add for GWUDI S1.1 – Expansion to GWUDI
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○ Add S1.1	○ Add S2.1, S2.2, or S2.3	○ Add S3.1 or S3.2	Add for DBP Control S1.1 – GAC S2.2 – MEX S2.3 – Actiflo™ CARB
B2 – New 15 mgd Treatment Train	○ Add S1.1	○ Add S2.1, S2.2, or S2.3	○ Add S3.1 or S3.2	Add for CEC Removal S3.1 – UV Disinfection S3.2 – Ozone
B3 – Replace Filters w/ UF Membranes	●	○ Add S2.1, S2.2, or S2.3	○ Add S3.1 or S3.2	
B4 – Replace Plant w/RO Facility	●	●	●	Add S3.1 or S3.2
B5 – Replace Conventional Softening w/Dual Softening	●	●	●	Add S3.1 or S3.2

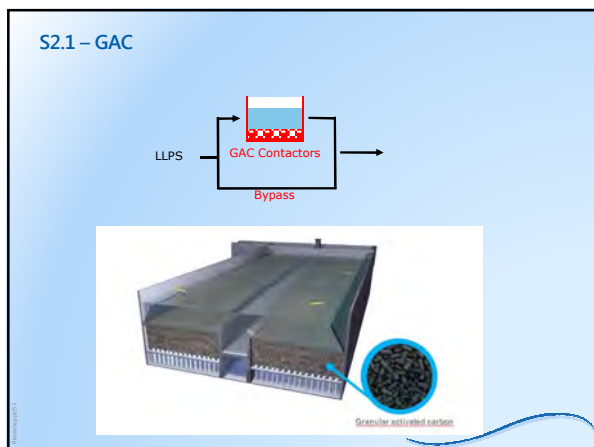
● Yes, ○ Partial, ○ No



Columbia WTP Expansion Alternatives

Base Alternative	GWUDI Compliance	DBP Control	CEC Removal	
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○	Adder for GWUDI • S1.1 – Expansion to GWUDI Adder for DBP Control • S2.1 – GAC • S2.2 – MIBK • S2.3 – Actiflo™ CARB
		Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○	○	○	Adder for CEC Removal • S1.1 – UV Disinfection • S1.2 – Ozone
	Add S1.1	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B2 – New 15 mgd Treatment Train	○	○	○	
	Add S1.1	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B3 – Replace Filters w/ UF Membranes	●	○	○	
		Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B4 – Replace Plant w/RO Facility	⚡	⚡	⚡	Add S2.1 or S2.3
B5 – Replace Conventional Softening w/Dolomite Softening	⚡	⚡	⚡	Add S2.1 or S2.3

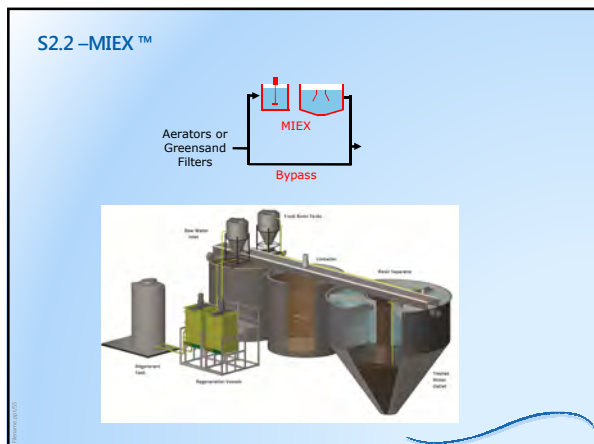
● Yes, ○ Partial, ○ No



Columbia WTP Expansion Alternatives

Base Alternative	GWUDI Compliance	DBP Control	CEC Removal	
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○	Adder for GWUDI • S1.1 – Expansion to GWUDI Adder for DBP Control • S2.1 – GAC • S2.2 – MIBK • S2.3 – Actiflo™ CARB
		Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○	○	○	Adder for CEC Removal • S1.1 – UV Disinfection • S1.2 – Ozone
	Add S1.1	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B2 – New 15 mgd Treatment Train	○	○	○	
	Add S1.1	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B3 – Replace Filters w/ UF Membranes	●	○	○	
		Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	
B4 – Replace Plant w/RO Facility	⚡	⚡	⚡	Add S2.1 or S2.3
B5 – Replace Conventional Softening w/Dolomite Softening	⚡	⚡	⚡	Add S2.1 or S2.3

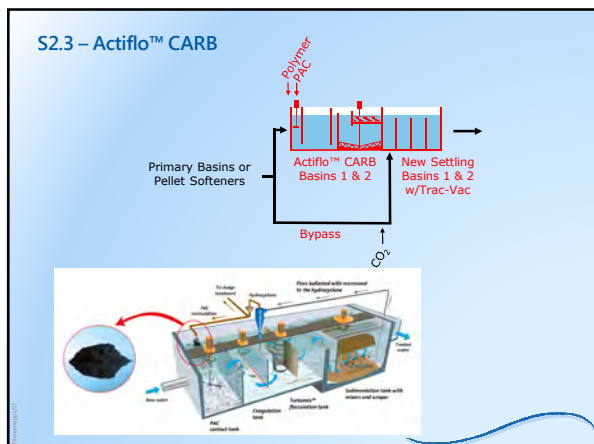
● Yes, ○ Partial, ○ No

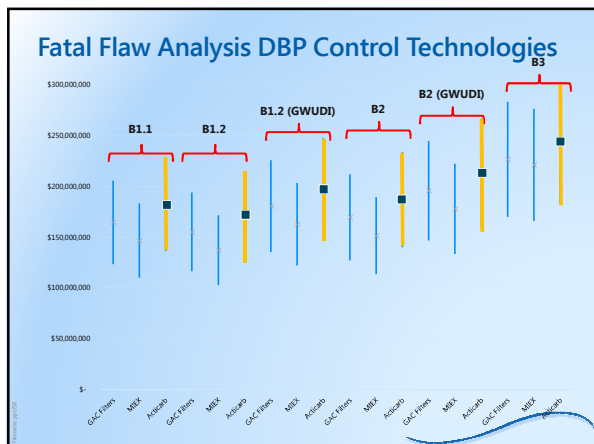


Columbia WTP Expansion Alternatives

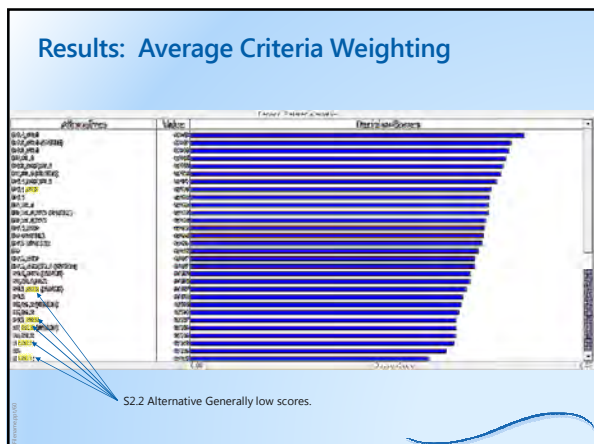
Base Alternative	GWUDI Compliance	DBP Control	CEC Removal	
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○	Add for GWUDI S1.1 – Expansion to GWUDI
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○	○	○	Add for DBP Control S1.1 – GAC S2.2 – MIEX S2.3 – Actiflo™ CARB
B2 – New 15 mgd Treatment Train	Add S1.1	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2	Add for CEC Removal S3.1 – UV Disinfection S3.2 – Ozone
B3 – Replace Filters w/ UF Membranes	●	○	○	
B4 – Replace Plant w/RO Facility	●	●	●	
B5 – Replace Conventional Softening w/Pellet Softening	●	○	○	

● Yes, ○ Partial, ○ No





- ### Fatal Flaw Analysis
- Eliminate S2.3 (Actiflo Carb) from Consideration:
 - Incorporation into existing treatment train more difficult
 - Higher operating costs due to solids disposal and Chemical (PAC) costs
 - GAC and/or MIE are better alternative to controlling DBP's.



Fatal Flaw Analysis

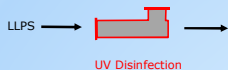
- Eliminate MIEC S2.2:
 - Permitting- Brine Stream Disposal
 - Operability- More complicated control than other DBP control technology.
 - Constructability – Difficult integration within existing processes.

Columbia WTP Expansion Alternatives

Base Alternative	GWUDI Compliance	DBP Control	CEC Removal	
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○	Add for GWUDI S1.1 – Expansion to GWUDI
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○	○	○	Add for DBP Control S3.1 – GAC S2.2 – MIEC S2.3 – AmBic-10 CASB
B2 – New 15 mgd Treatment Train	○	○	○	Add for CEC Removal S3.1 – UV Disinfection S3.2 – Ozone
B3 – Replace Filters w/ UF Membranes	●	○	○	
B4 – Replace Plant w/RO facility	●	●	●	
B5 – Replace Conventional Softening w/Dual Softening	●	●	●	

● Yes, ○ Partial, ○ No

S3.1 – UV Disinfection

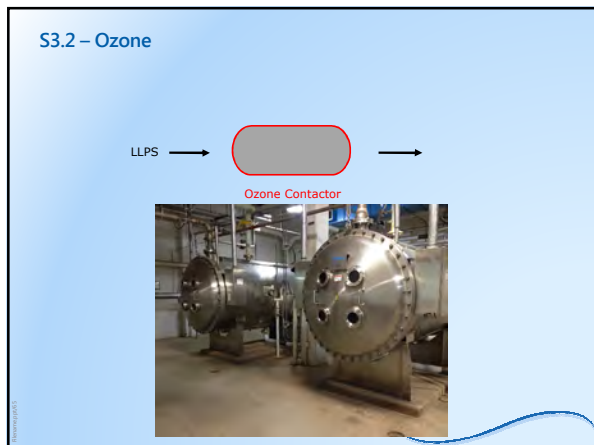


Columbia WTP Expansion Alternatives

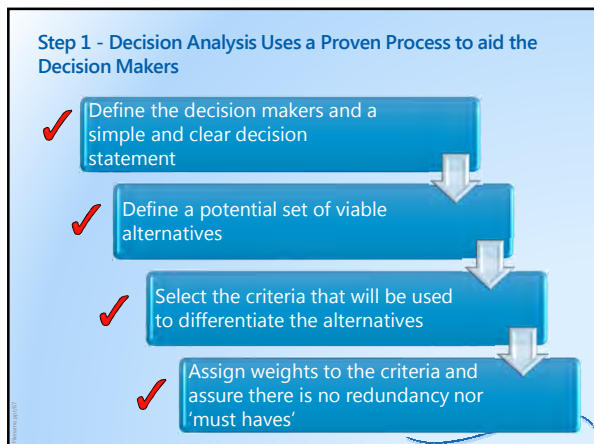
Alternatives			
Base Alternative	GWUDI Compliance	DBP Control	CEC Removal
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○
		Add S2.1, S2.2, or S3.2	Add S3.1 or S3.2
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○	○	○
	Add S1.1	Add S2.1, S2.2, or S3.2	Add S3.1 or S3.2
B2 – New 15 mgd Treatment Train	○	○	○
	Add S1.1	Add S2.1, S2.2, or S3.2	Add S3.1 or S3.2
B3 – Replace Filters w/ UF Membranes	●	○	○
		Add S2.1, S2.2, or S3.2	Add S3.1 or S3.2
B4 – Replace Plant w/RO Facility	●	●	○
			Add S2.1 or S2.2
B5 – Replace Conventional Softening w/Reverse Osmosis	●	●	○
			Add S2.1 or S2.2

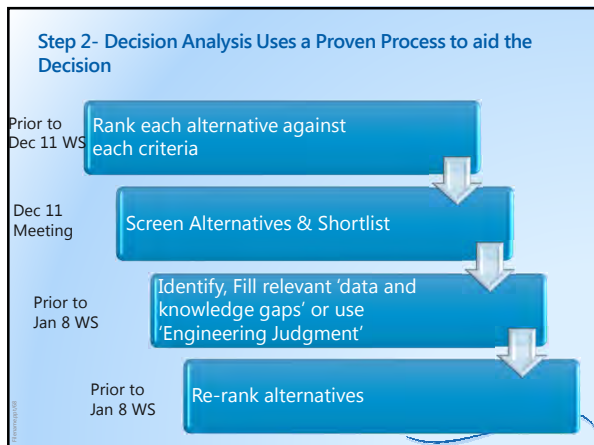
Adder for GWUDI: S1.1 – Expansion to GWUDI
 Adder for DBP Control: S2.1 – GAC, S2.2 – AAFB, S2.3 – Activated Carbon
 Adder for CEC Removal: S3.1 – UV Disinfection, S3.2 – Ozonation

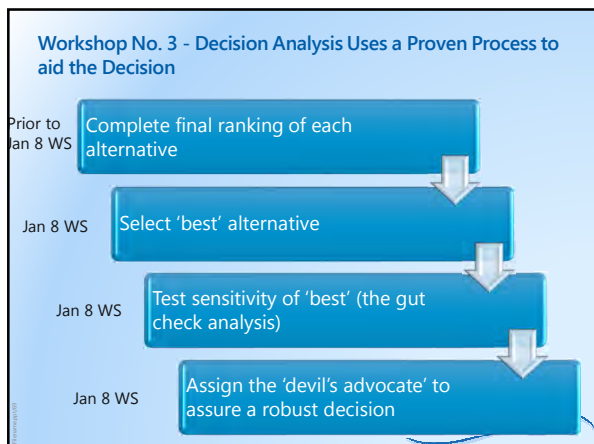
● Yes, ○ Partial, ○ No



- ### Agenda
- Finalize Mission Statement
 - Review Pairwise Comparison Result
 - Review Project Boundaries
 - Discuss/Review Alternatives and Carollo Shortlist
 - **SDA Model**
 - Discuss and Rank Shortlisted Alternatives
 - Review Data Gaps
 - Review Action/Decision Logs
 - Review Next Steps
 - General Comments by Public, Members and Staff
 - Next Meeting Date
 - Adjournment







Agenda

- Finalize Mission Statement
- Review Pairwise Comparison Result
- Review Project Boundaries
- Discuss/Review Alternatives and Carollo Shortlist
- SDA Model
- **Discuss and Rank Shortlisted Alternatives – Tabled Until December 11, 2017?**
- Review Data Gaps
- Review Action/Decision Logs
- Review Next Steps
- General Comments by Public, Members and Staff
- Next Meeting Date
- Adjournment

Columbia WTP Expansion Alternatives

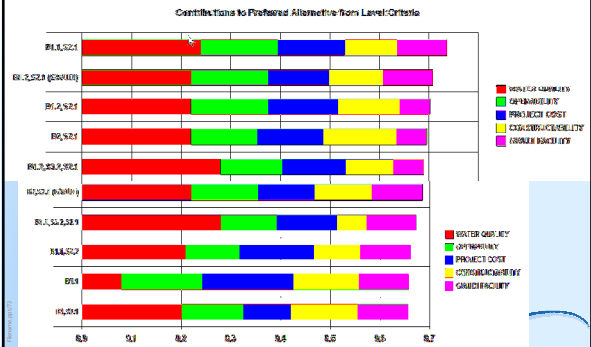
Base Alternative	GWUDI Compliance	DBP Control	CEC Removal	
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○	Adder for GWUDI • S1.1 – Expansion to GWUDI
		Add S2.1, S2.2 , or S2.3	Add S3.1 or S3.2	Adder for DBP Control • S1.1 – GAC • S2.2 – MEX • S2.3 – Amlicin-CAD
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○	○	○	
	Add S1.1	Add S2.1, S2.2 , or S2.3	Add S3.1 or S3.2	Adder for CEC Removal • S3.1 – UV Disinfection • S3.2 – Ozone
B2 – New 15 mgd Treatment Train	○	○	○	
	Add S1.1	Add S2.1, S2.2 , or S2.3	Add S3.1 or S3.2	
B3 – Replace Filters w/ UF Membranes	●	○	○	
		Add S2.1, S2.2 , or S2.3	Add S3.1 or S3.2	
B4 – Replace Plant w/RO Facility	●	●	●	
			Add S3.1 or S3.2	
B5 – Replace Conventional Softening w/Dual Softening	●	●	●	
		Add S2.1 , S2.2 , S2.3	Add S3.1 or S3.2	

● Yes, ○ Partial, ○ No

Shortlisted Alternatives

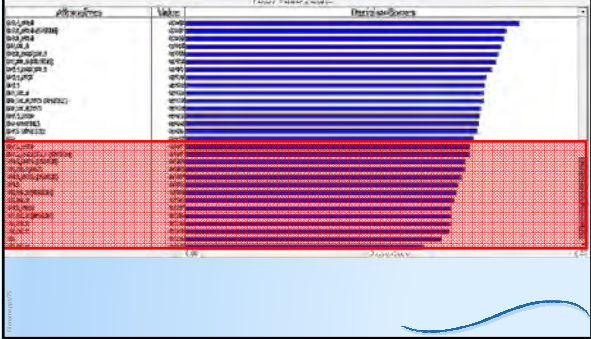
#	Base Alt.	Title	Sup. Alt.	Title
1	B1.1	Expand Plant w/ Existing Filters	NA	
2	B1.1	Expand Plant w/ Existing Filters	S2.1	GAC Filters
3	B1.1	Expand Plant w/ Existing Filters	S3.2	Ozone/Biof.
4	B1.1	Expand Plant w/ Existing Filters	S2.1, S3.1	GAC Filters, UV Disinfection
5	B1.1	Expand Plant w/ Existing Filters	S2.1, S3.2	GAC Filters, Ozone/Biof.
6	B1.2	Expand Plant w/ New 15 mgd Filters	NA	
7	B1.2	Expand Plant w/ New 15 mgd Filters	S1.1	GWUDI
8	B1.2	Expand Plant w/ New 15 mgd Filters	S1.1, S2.1	GWUDI, GAC Filters
9	B1.2	Expand Plant w/ New 15 mgd Filters	S1.1, S3.2	GWUDI, Ozone/Biof.
10	B1.2	Expand Plant w/ New 15 mgd Filters	S1.1, S2.1, S3.2	GWUDI, GAC Filters, Ozone/Biof.
11	B2	Expand Plant w/ New 15 mgd Train	NA	
12	B2	Expand Plant w/ New 15 mgd Train	S1.1	GWUDI
13	B2	Expand Plant w/ New 15 mgd Train	S1.1, S2.1	GWUDI, GAC Filters
14	B2	Expand Plant w/ New 15 mgd Train	S1.1, S3.2	GWUDI, Ozone/Biof.
15	B2	Expand Plant w/ New 15 mgd Train	S1.1, S2.1, S3.2	GWUDI, GAC Filters, Ozone/Biof.
16	B3	Replace Filters w/ UF Membranes	NA	
17	B3	Replace Filters w/ UF Membranes	S2.1	GAC Filters
18	B3	Replace Filters w/ UF Membranes	S3.2	Ozone/Biof.
29	B3	Replace Filters w/ UF Membranes	S2.1, S3.2	GAC Filters, Ozone/Biof.

Results (Top 10) : Average Criteria Weighting (Hempel, Pruett)



Preliminary Ranking	ALTERNATIVE	AVERAGE WEIGHT	MERRITT -	HEMPEL	PRUETT	SKALA -	RYAN - NA	SZEWZYK -	FALLS -	CONWAY -	OFF - NA	JACKSON -
			NA missing weights			NA missing weights	NA missing weights	NA missing weights	NA missing weights	NA missing weights	NA missing weights	NA missing weights
1	B1.1.S2.1	1		1	6							
2	B1.2.S2.1 (GWUDI)	2		2	9							
3	B1.1.S2.1	3		8	2							
4	B2.S2.1	4		15	1							
5	B1.2.S3.2.S2.1	5		6	5							
6	B1.2.S3.1 (GWUDI)	6		5	4							
7	B1.1.S3.2.S2.1	7		3	19							
8	B1.1.S2.2	8		10	24							
9	B1.1	9		11	20							
10	B1.2.S3.1	10		13	7							
11	B2.S2.1.S3.2 (GWUDI)	11		4	14							
12	B2.S2.1.S3.2	12		12	10							
13	B1.1.S3.2	13		9	21							
14	B2 (GWUDI)	14		17	8							
15	B1.2 (GWUDI)	15		19	12							
16	B2	16		24	3							
17	B1.2.S3.2	17		23	11							
18	B1.2.S2.2.S2.1 (GWUDI)	18		7	28							
19	B1.2.S3.2 (GWUDI)	19		16	25							
20	B3.S2.1.S3.2	20		14	15							
21	B1.2.S2.2 (GWUDI)	21		20	29							
22	B1.2	22		27	17							
23	B2.S3.2 (GWUDI)	23		18	22							
24	B2.S3.2	24		26	13							
25	B1.2.S2.2	25		28	27							
26	B1.2.S3.1 (GWUDI)	26		21	26							
27	B3.S3.2	27		22	18							
28	B2.S2.2	28		29	16							
29	B3	29		25	23							
30	B3.S2.2	30		30	30							

Results: Average Criteria Weighting (Hempel, Pruett)



Shortlisted Alternatives

#	Base Alt.	Title	Sup. Alt.	Title
1	B1.1	Expand Plant w/ Existing Filters	NA	
2	B1.1	Expand Plant w/ Existing Filters	S2.1	GAC Filters
3	B1.1	Expand Plant w/ Existing Filters	S3.2	Ozone/Biof.
4	B1.1	Expand Plant w/ Existing Filters	S2.1, S3.1	GAC Filters, UV Disinfection
5	B1.1	Expand Plant w/ Existing Filters	S2.1, S3.2	GAC Filters, Ozone/Biof.
6	B1.2	Expand Plant w/ New 15 mgd Filters	NA	
7	B1.2	Expand Plant w/ New 15 mgd Filters	S1.1	GWUDI
8	B1.2	Expand Plant w/ New 15 mgd Filters	S1.1, S2.1	GWUDI, GAC Filters
9	B1.2	Expand Plant w/ New 15 mgd Filters	S1.1, S3.2	GWUDI, Ozone/Biof.
10	B1.2	Expand Plant w/ New 15 mgd Filters	S1.1, S2.1, S3.2	GWUDI, GAC Filters, Ozone/Biof.
11	B2	Expand Plant w/ New 15 mgd Train	NA	
12	B2	Expand Plant w/ New 15 mgd Train	S1.1	GWUDI
13	B2	Expand Plant w/ New 15 mgd Train	S1.1, S2.1	GWUDI, GAC Filters
14	B2	Expand Plant w/ New 15 mgd Train	S1.1, S3.2	GWUDI, Ozone/Biof.
15	B2	Expand Plant w/ New 15 mgd Train	S1.1, S2.1, S3.2	GWUDI, GAC Filters, Ozone/Biof.
16	B3	Replace Filters w/ UF Membranes	NA	
17	B3	Replace Filters w/ UF Membranes	S2.1	GAC Filters
18	B3	Replace Filters w/ UF Membranes	S3.2	Ozone/Biof.
19	B3	Replace Filters w/ UF Membranes	S2.1, S3.2	GAC Filters, Ozone/Biof.

- ### Agenda
- Finalize Mission Statement
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- ### Identify and Review Data Gaps
- General:
 - Develop Layouts to clarify constructability ratings.
 - Modify alternatives to address potential permitting issues (if possible).
 - Modify alternative to address potential operability issues. (if possible).
 - B1.1, B1.2 (GWUDI), and B2 (GWUDI) Alternatives
 - (B1.1) Rerating of Filters to > 6 gpm/sqft for 45 mgd
 - Improvement of existing filters (32 mgd) for GWUDI
 - GAC S1.2 Alternatives
 - GAC cost and replacement frequency
 - Revisit MIEC (if necessary) as potential for some options
 - Ozone Alternatives:
 - Develop Bromate control strategies and costs
 - UV alternatives:
 - Update costs for Transmittance values.

Agenda

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3/22/2018



DECISION LOG

DECISION LOG

Project: Preliminary Design Report Update - Project Proceedings DATE: 10/10/2017
Client: City of Columbia, MD BY: [initials]
Job #: C:\Users\ [user] \Documents\ [file name]

ITEM No.	RESPONSIBLE PARTY	DECISION	DECISION DATE	STATUS	COMMENTS
7	City	Finalist Meeting		Finalist Meeting	The group agreed to the alternative design solution for... (RF) for the design to be supplied via email to the... meeting... The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
8	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
9	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
10	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
11	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
12	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
13	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
14	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
15	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
16	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
17	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
18	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
19	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
20	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
21	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
22	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...
23	City	Finalist Meeting		Finalist Meeting	The group decided to accept the... (RF) as the... The group decided to accept the... (RF) as the...

3/22/2018



ACTION LOG

ACTION ITEM

Project: Preliminary Design Report Update - Project Proceedings DATE: 10/10/2017
Client: City of Columbia, MD BY: [initials]
Job #: C:\Users\ [user] \Documents\ [file name]

ITEM No.	RESPONSIBLE PARTY	ACTION	TERM	START DATE	ITEM COMPLETION DATE	COMMENTS
11	Carroll	Provide binder containing past and future material to committee members.	11-Sep-17	09-Sep-17	09-Sep-17	
12	Carroll	Provide and present mission statement at the next meeting for approval.	11-Sep-17	09-Sep-17	09-Sep-17	
13	Carroll	Send out post to group for next meeting date with October 11th as the preferred date.	11-Sep-17	09-Sep-17	12-Sep-17	
14	Carroll	Send out updated mission statement.	10-Oct-17	09-Oct-17	12-Oct-17	
15	Carroll/Drause	Send out meeting agenda for sub-criteria cross-examination meeting.	10-Oct-17	09-Oct-17	12-Oct-17	
16	City	Print and return voting sheets for sub-criteria cross-examination meeting.	10-Oct-17	1 week before next meeting		Committee Members will select which sub-criteria are more important than others.
17	Carroll/Drause	Send out post to group for next meeting date.	10-Oct-17	13-Oct-17	13-Oct-17	

3/22/2018



Agenda

- Finalize Mission Statement
- Review Pairwise Comparison Result
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- Discuss/Review Alternatives and Carollo Shortlist
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- General Comments by Public, Members and Staff
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Next Steps

- Carollo:
 - Preliminary Ranking of Remaining Alternatives
 - Identify Data Gaps and Resolve
 - Update Costs and Rankings Based upon Data gaps
- Workgroup:
 - Review Preliminary Ranking of Remaining Alternatives
 - Develop list of questions/concerns 1 week prior to meeting.
- Carollo/Workshops – December 11/January 8
 - Review final shortlist and criteria ranking
 - Conduct sensitivity analysis
 - Determine final recommendation/draft summary

Agenda

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- **Next Meeting Date: December 11, 2017 5:30 pm**
- Adjournment



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- Next Meeting Date
- **Adjournment**



Pairwise Comparison and Preliminary Ranking Workshop

City of Columbia, MO
Water and Light Department
Drinking Water Planning Workgroup
January 8, 2018, 5:30 pm
Water Treatment Plant Conference Room



Agenda

- Pairwise Comparison
- Base Alternatives:
 - Discuss/Review Alternatives and Carollo Shortlist
 - SDA Model Development
 - Discuss and Rank Shortlisted Alternatives
- Supplemental Alternatives:
 - Discuss/Review Alternatives and Carollo Shortlist
 - SDA Model Development
 - Discuss and Rank Shortlisted Alternatives
- Review Data Gaps & Action/Decision Logs
- Review Final Steps
- General Comment by Public, Members, and Staff
- Next Meeting Date – FINAL DECISION MAKING AND PUBLIC SUMMARY WORKSHOPS

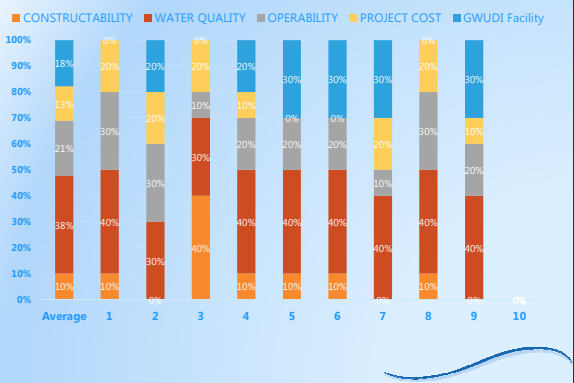
Agenda

- **Pairwise Comparison**
- Base Alternatives:
 - Discuss/Review Alternatives and Carollo Shortlist
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 - Discuss and Rank Shortlisted Alternatives
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 - Discuss/Review Alternatives and Carollo Shortlist
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Pairwise Comparison Surveys

- Distributed ranking worksheets to members of Drinking Water Planning Workgroup.
- Received 10 out of 10 fully completed responses – Thank you!!!

Criteria Weighting Results

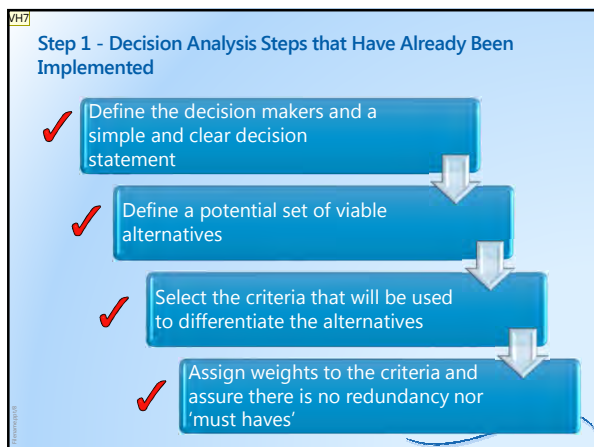


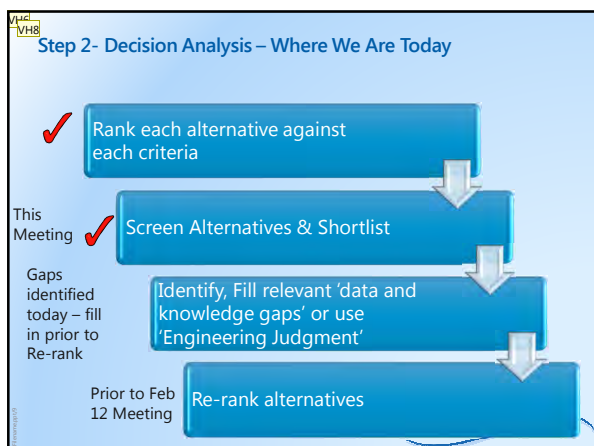
Summary of Pairwise Comparisons

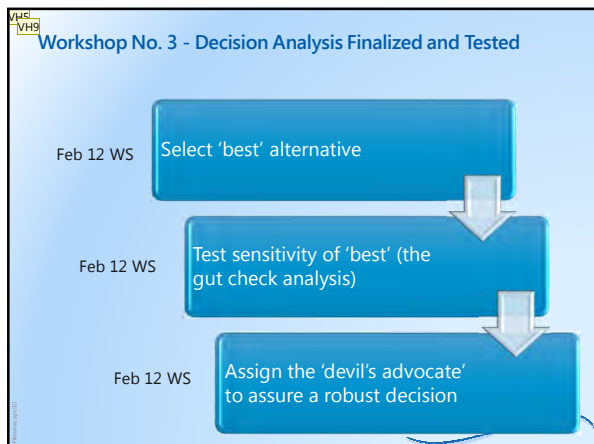
- Most participants scored water quality highest
- Most participants scored cost and GWUDI higher.
- Operability was more important than constructability to most participants.



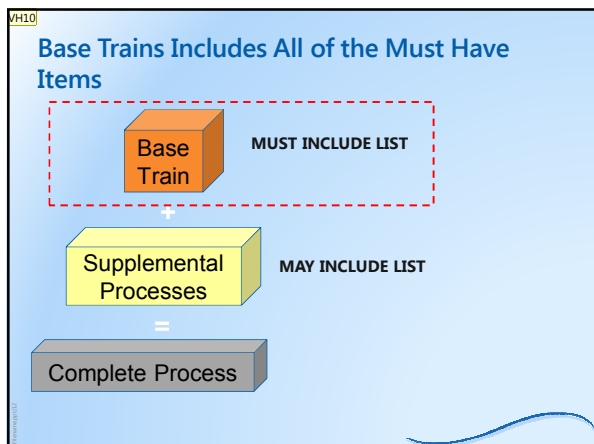


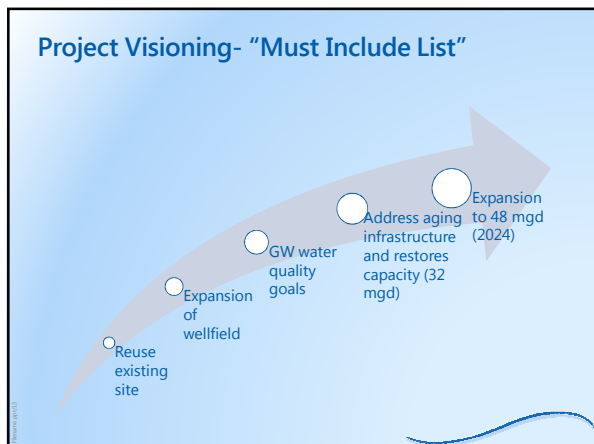


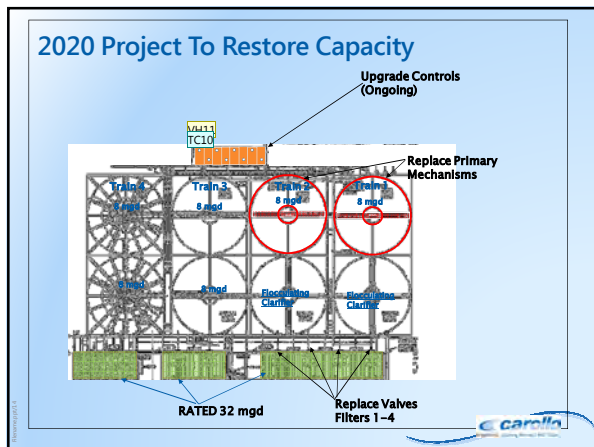


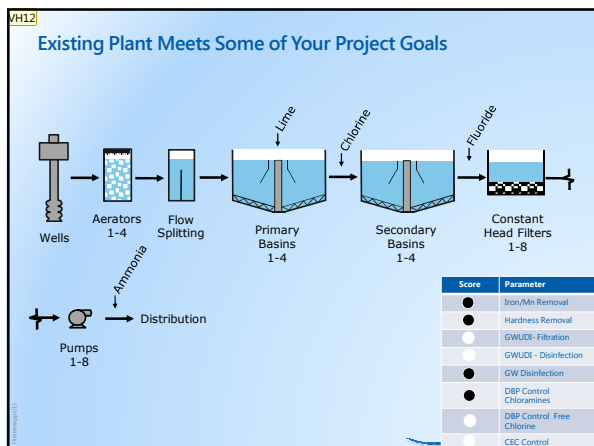


- ### Agenda
- Pairwise Comparison
 - **Base Alternatives:**
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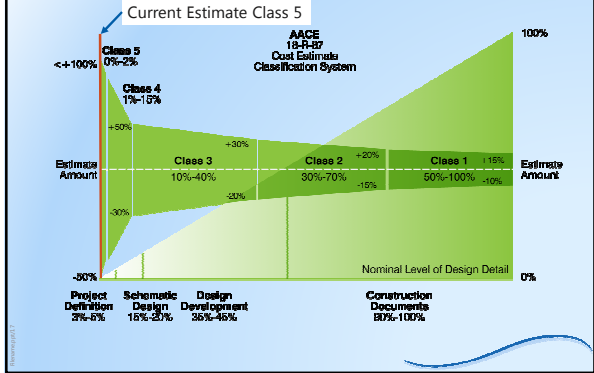


Some of the Base Train Expansion Alternatives Meet GWUDI Requirements

Base Alternative	GWUDI Compliance
B1.1 – Expand Existing Plant w/Conventional Softening (Parallel Filters)	●
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○
B7 – New 15 mgd Treatment Train	○
B9 – Replace filters w/ UF Membranes	●
B4 – Replace Plant w/RO Facility	●
B5 – Replace Conventional Softening w/Pellet Softening	●

● Yes, ○ Partial, ○ No

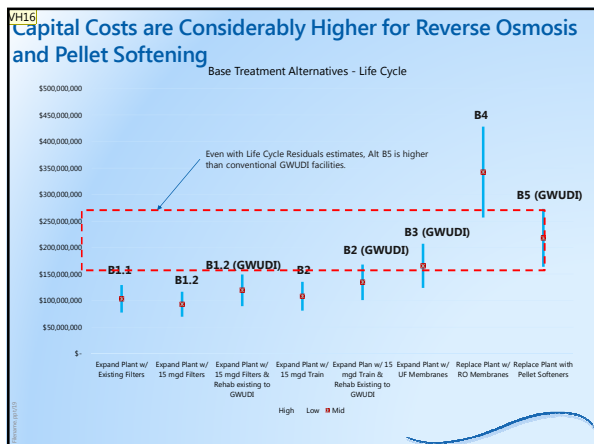
The level of accuracy of cost estimating follows the level of project development

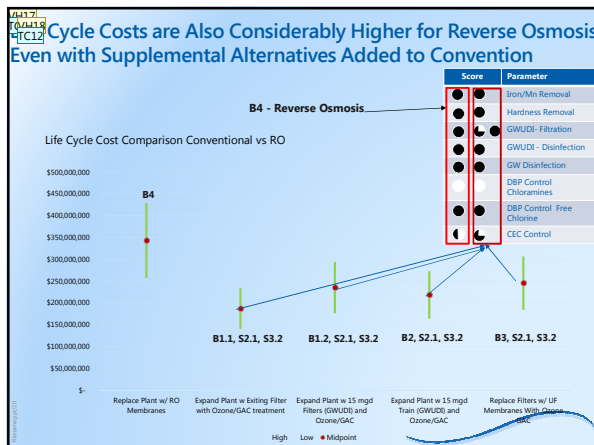


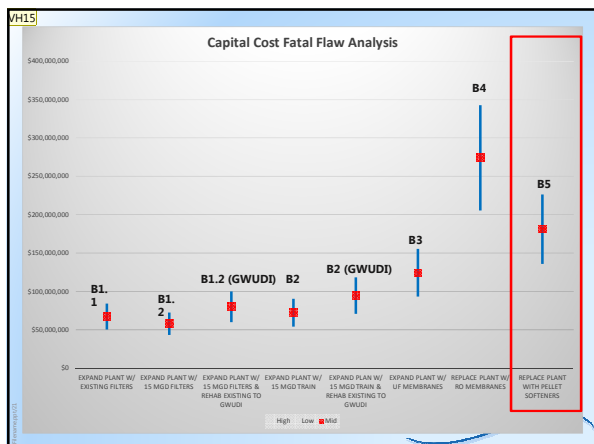
VH13 Class 5 AACE Cost Estimate - Order of Magnude

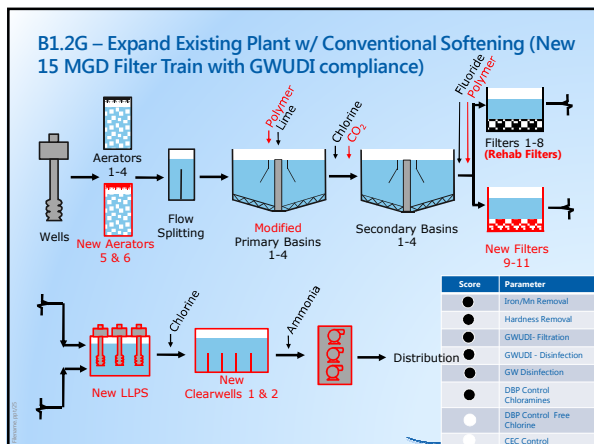
- Markups
 - GCs – 8%
 - Contractor O&P – 10%
 - Eng. and Admin – 12%
 - Contingency – 50%
- O&M
 - 13 MGD Average Annual Flow
 - Current Dosages
 - \$0.08 per kWh
 - 0.25% of Capital for O&M
- Cost Development
 - 2016 Condition Assessment
 - Historical data
 - Market Trends
 - Vendor Quotes
 - Cost Estimating Manuals

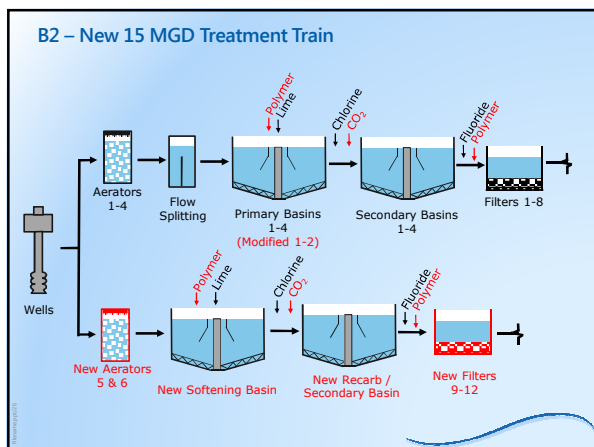
All base alternatives provide a plant capacity of 48 mgd

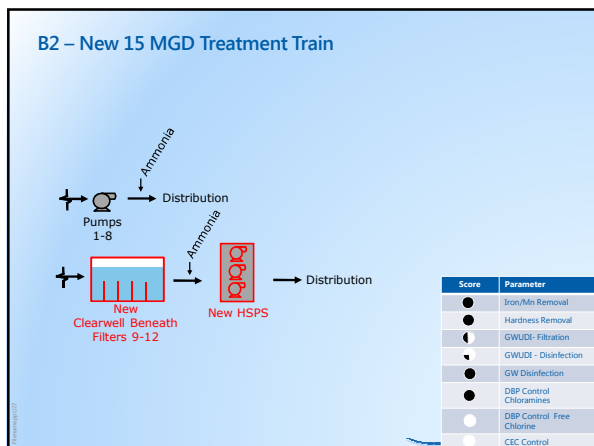


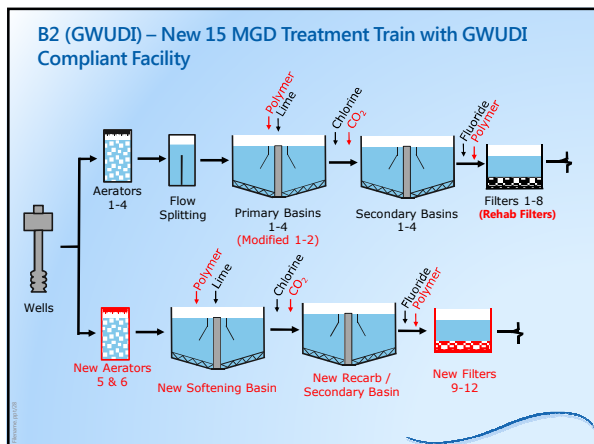


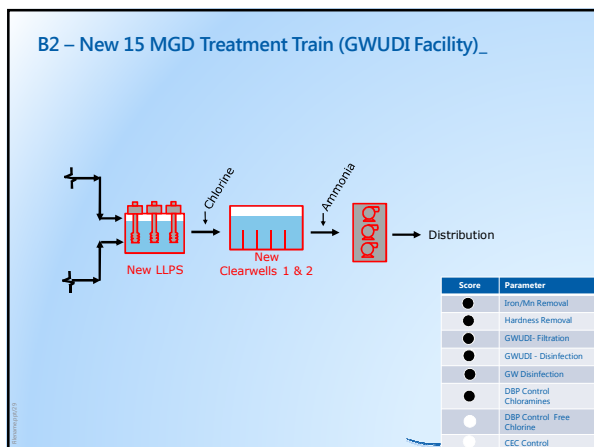


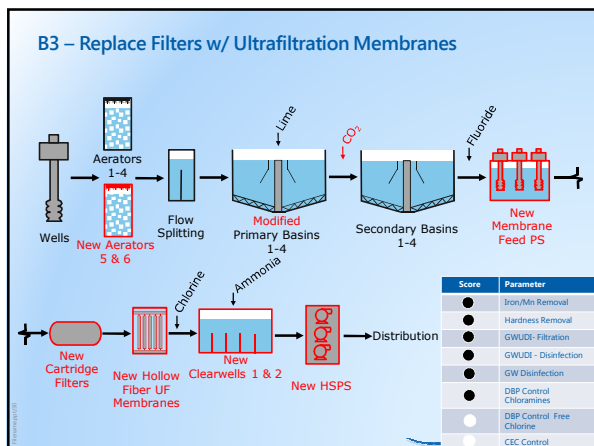


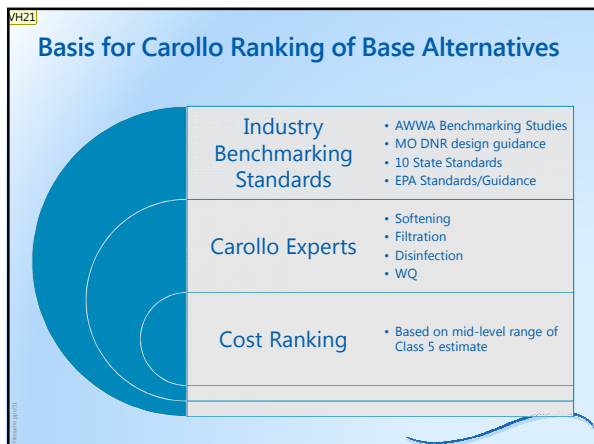


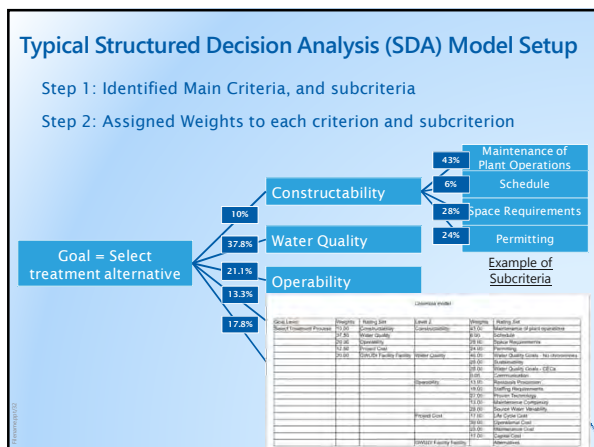


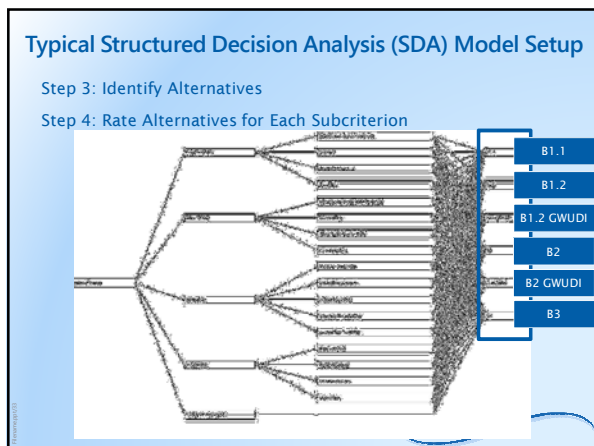


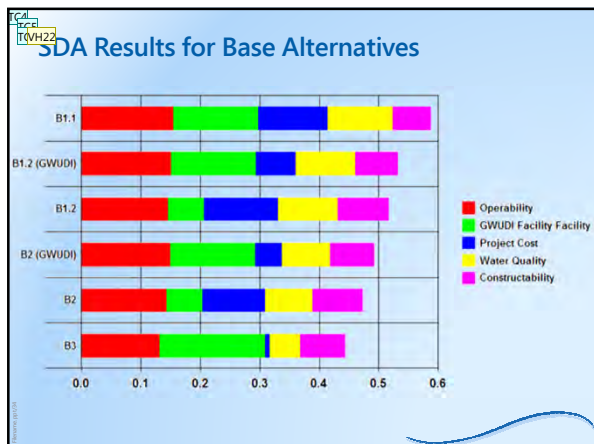


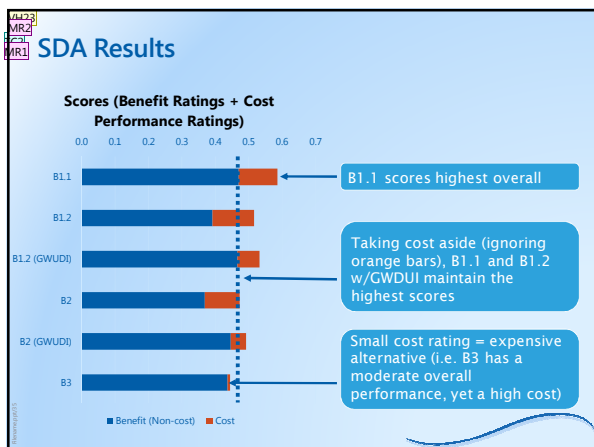


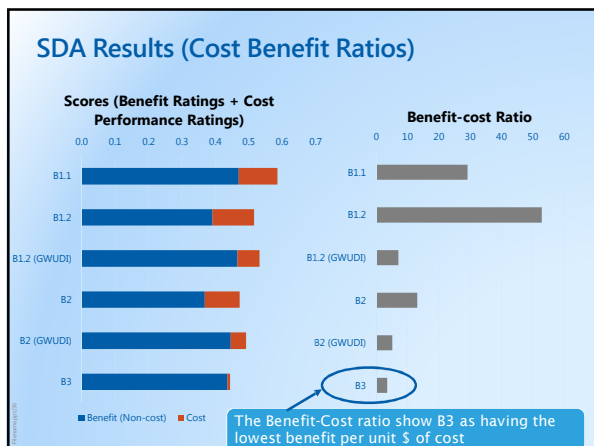


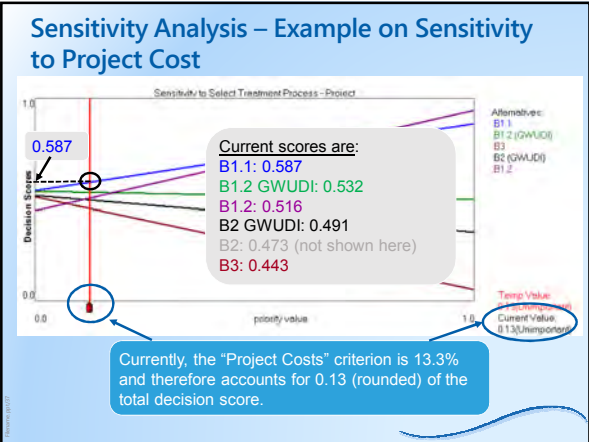


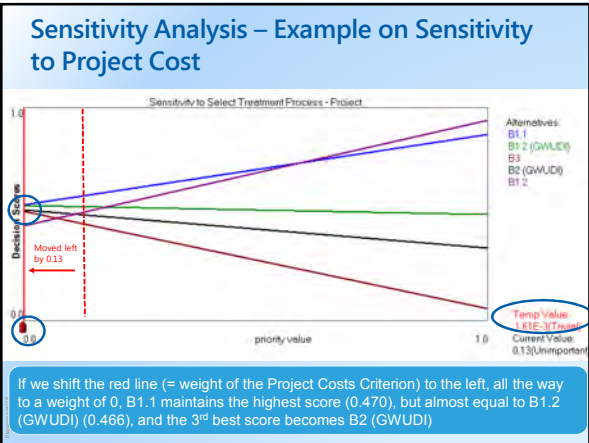


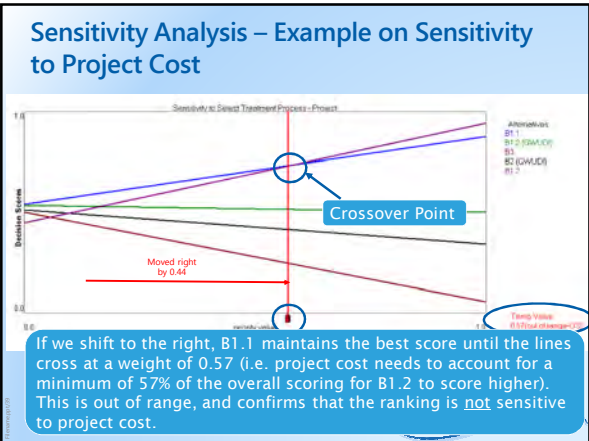












Definition of Criticality

- The smallest shift necessary to affect the ranking of the 2 highest alternatives gauges the sensitivity
- That amount is called the criticality
- Project cost example:
 - Mathematically, a shift of 0.147 (to the left) would be necessary
 - The criticality is 14.7% for Project Costs. The model is therefore not sensitive to the weight on Project Costs.
- The criticality is assessed for all criteria weights. The higher the criticality number, the less sensitive the model is to the subject criteria.

Criticality of Most Sensitive Criteria

Criticality	Criterion Name	Explanation
14.7%	Project Costs	Not sensitive. The Project Cost weight would need to be negative to make B1.2 GWUDI rank higher than B1.1
14.9%	GWUDI Facility	Not sensitive. The GWUDI Facility weight would need to be reduced from 18% to 3.1% to make B1.2 rank higher than B1.1
21.7%	Constructability	Not sensitive. The Constructability weight would need to increase from 10% to 31.7% for B1.2 to rank higher than B1.1
43.5%	Sustainability	Not sensitive at all. There are no different weight that changes the ranking

Ranking Questions/Discussions

- SDA Model manipulation

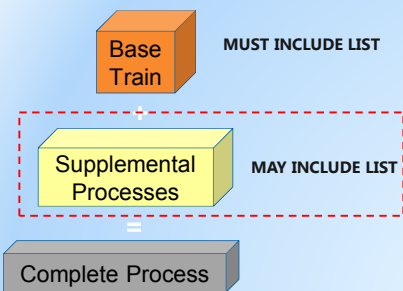
Conclusions of SDA Analysis

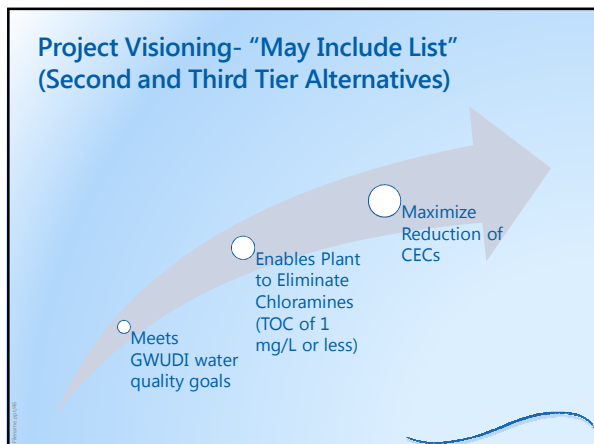
- Eliminate B3 (UF membranes) from further consideration.
- Move forward with other base alternatives to pair with supplemental alternatives.

Agenda

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- Base Alternatives:
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Treatment Alternative Identification





VH26

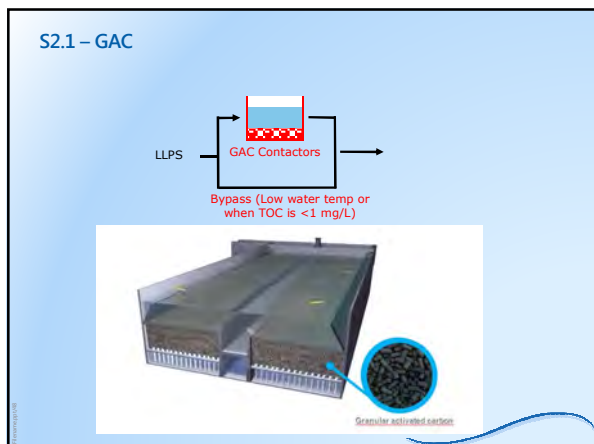
GAC Can Be Added to Any of the Three Base Alternatives

Base Alternative	DBP Control	CEC Removal
B1.1 - Expand Existing Plant w/Conventional Softening (Rerate filters)	<input type="checkbox"/> Add S2.1, S2.2, S2.3, or S2.4	<input type="checkbox"/> Add S3.1 or S3.2
B1.2 - Expand Existing Plant w/Conventional Softening (New 15 MGD filter train)	<input type="checkbox"/> Add S2.1, S2.2, S2.3, or S2.4	<input type="checkbox"/> Add S3.1 or S3.2
H7 - New 15 mgd Treatment Train	<input type="checkbox"/> Add S2.1, S2.2, S2.3, or S2.4	<input type="checkbox"/> Add S3.1 or S3.2
S2 - Replace filters w/ UF Membranes	<input type="checkbox"/> Add S2.1, S2.2, or S2.3	<input type="checkbox"/> Add S3.1 or S3.2
U2 - Replace filter w/TO softening	<input type="checkbox"/>	<input type="checkbox"/> Add S3.1 or S3.2
S3 - Replace conventional softening w/rapid softening	<input type="checkbox"/> Add S2.1, S2.2, S2.3	<input type="checkbox"/> Add S3.1 or S3.2

Yes, Partial, No

Adder for DBP Control
 S2.1 - GAC
 S2.2 - PAC
 S2.3 - Activated CARB
 S2.4 - Ozone/Biofiltration

Adder for CEC Removal
 S3.1 - UV Disinfection/Peroxide
 S3.2 - Ozone/Biofiltration



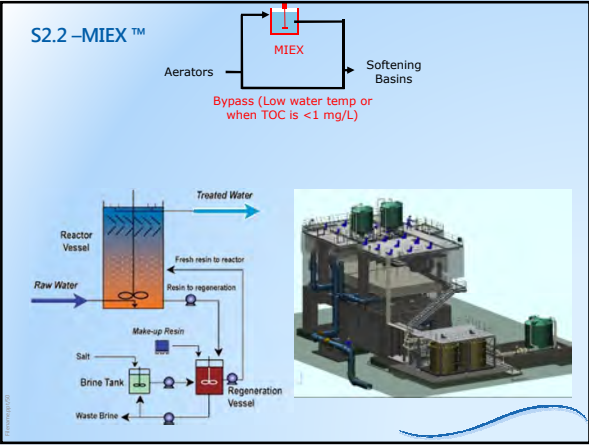
MIEX Can Be Added to Any of the Three Base Alternatives

Alternatives		
Base Alternative	DBP Control	CEC Removal
B1.1 – Expand Existing Plant w/Conventional Softening (Reroute Filters)	<input type="radio"/> Add S2.1, S2.2, S2.3, or S2.4	<input type="radio"/> Add S3.1 or S3.2
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	<input type="radio"/> Add S2.1, S2.2, S2.3, or S2.4	<input type="radio"/> Add S3.1 or S3.2
B2 – New 15 mgd Treatment Train	<input type="radio"/> Add S2.1, S2.2, S2.3, or S2.4	<input type="radio"/> Add S3.1 or S3.2
B3 – Replace Filters w/ UF Membranes	<input type="checkbox"/> Add S2.1, S2.2, or S2.4	<input type="checkbox"/> Add S3.1 or S3.2
B4 – Replace Plant w/RO Facility	<input type="checkbox"/>	<input type="checkbox"/> Add S3.1 or S3.2
B5 – Replace Conventional Softening w/Pellet Softening	<input type="checkbox"/> Add S2.1, S2.2, S2.3	<input type="checkbox"/> Add S3.1 or S3.2

Yes, Partial, No

Adder for DBP Control
 - S2.1 – GAC
 - S2.2 – MIEX
 - S2.3 – Actiflo™ CARB
 - S2.4 – Ozone/Biofiltration

Adder for CEC Removal
 - S3.1 – UV Disinfection/Peroxide
 - S3.2 – Ozone/Biofiltration



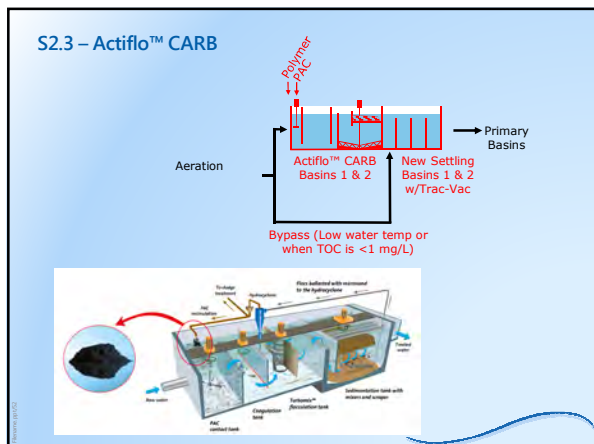
Actiflo™ Carb Can Be Added to Any of the Three Base Alternatives

Alternatives		
Base Alternative	DBP Control	CEC Removal
B1.1 – Expand Existing Plant w/Conventional Softening (Reroute Filters)	<input type="radio"/> Add S2.1, S2.2, S2.3, or S2.4	<input type="radio"/> Add S3.1 or S3.2
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	<input type="radio"/> Add S2.1, S2.2, S2.3, or S2.4	<input type="radio"/> Add S3.1 or S3.2
B2 – New 15 mgd Treatment Train	<input type="radio"/> Add S2.1, S2.2, S2.3, or S2.4	<input type="radio"/> Add S3.1 or S3.2
B3 – Replace Filters w/ UF Membranes	<input type="checkbox"/> Add S2.1, S2.2, or S2.3	<input type="checkbox"/> Add S3.1 or S3.2
B4 – Replace Plant w/RO Facility	<input type="checkbox"/>	<input type="checkbox"/> Add S3.1 or S3.2
B5 – Replace Conventional Softening w/Pellet Softening	<input type="checkbox"/> Add S2.1, S2.2, S2.3	<input type="checkbox"/> Add S3.1 or S3.2

Yes, Partial, No

Adder for DBP Control
 - S2.1 – GAC
 - S2.2 – MIEX
 - S2.3 – Actiflo™ CARB
 - S2.4 – Ozone/Biofiltration

Adder for CEC Removal
 - S3.1 – UV Disinfection/Peroxide
 - S3.2 – Ozone/Biofiltration



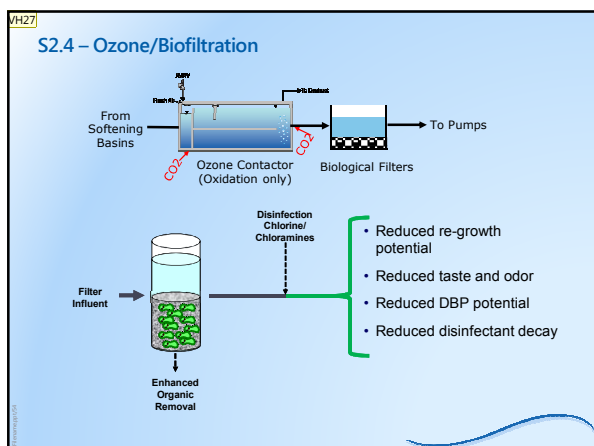
Ozone/BAF Can Be Added to Any of the Three Base Alternatives

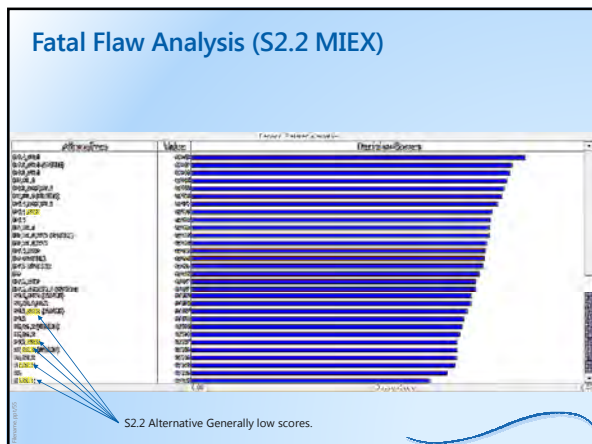
Base Alternative	DBP Control	CEC Removal
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	<input type="checkbox"/> Add S2.1, S2.2, S2.3, or S2.4 <input type="checkbox"/> S2.4	<input type="checkbox"/> Add S3.1 or S3.2
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	<input type="checkbox"/> Add S2.1, S2.2, S2.3, or S2.4	<input type="checkbox"/> Add S3.1 or S3.2
U2 – New 15 mgd Treatment Train	<input type="checkbox"/> Add S2.1, S2.2, S2.3, or S2.4	<input type="checkbox"/> Add S3.1 or S3.2
D3 – Replace Filters w/UF Membranes	<input type="checkbox"/> Add S2.1, S2.2, or S2.3	<input type="checkbox"/> Add S3.1 or S3.2
D4 – Replace Plant w/RO Facility	<input type="checkbox"/> Add S2.1, S2.2, or S2.3	<input type="checkbox"/> Add S3.1 or S3.2
D5 – Replace Conventional Softening w/Partial Softening	<input type="checkbox"/> Add S2.1, S2.2, S2.3	<input type="checkbox"/> Add S3.1 or S3.2

Adder for DBP Control
 • S2.1 – GAC
 • S2.2 – MEX
 • S2.3 – Actiflo™ CARB
 • S2.4 – Ozone/Biofiltration

Adder for CEC Removal
 • S3.1 – UV Disinfection/Peroxide
 • S3.2 – Ozone/Biofiltration

Yes, Partial, No





MIEX Creates a Brine Waste and the Amount of Regeneration Required is Extreme

- Eliminate MIEX S2.2:
 - Permitting- Brine Stream Disposal
 - Operability- More complicated control than other DBP control technology.
 - Potential for resin loss resulting in \$\$\$\$ (overflow)
 - Constructability – Difficult integration within existing processes.
 - Life Cycle Cost: Low Bed Volumes
 - Higher resin replacement rate
 - Higher brine generation

Item	Value
Resin Volume (m³)	100
Resin Cost (\$/m³)	1000
Brine Volume (m³)	1000
Brine Cost (\$/m³)	1000
Resin Replacement Rate	1000
Brine Generation Rate	1000

Fatal Flaw Analysis: S2.4

- High degree of uncertainty regarding the potential for Ozone/Biofiltration Meet TTHM precursor removal goals.
- Requires piloting to determine success.

Typical TOC Removal – 10-15%

For DBP Control GAC and Actiflo™ CARB are the Only Options Without Fatal Flaws

Alternatives		
Base Alternative	DBP Control	CEC Removal
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, S2.3, or S2.4	Add S3.1 or S3.2
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, S2.3, or S2.4	Add S3.1 or S3.2
B2 – New 15 mgd Treatment Train	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, S2.3, or S2.4	Add S3.1 or S3.2
B3 – Replace Filters w/ UF Membranes	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2
B4 – Replace Plant w/RO Facility	<input checked="" type="radio"/>	<input checked="" type="radio"/>
		Add S3.1 or S3.2
B5 – Replace Conventional Softening w/Dual Softening	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, S2.3	Add S3.1 or S3.2

Yes, Partial, No

Adder for DBP Control
 • S2.1 – GAC
 • S2.2 – MBR
 • S2.3 – Actiflo™ CARB
 • S2.4 – Ozone/Biofiltration

Adder for CEC Removal
 • S3.1 – UV Disinfection/Peroxide
 • S3.2 – Ozone/Biofiltration

For DBP Control GAC and Actiflo™ CARB are the Only Options Without Fatal Flaws

Alternatives		
Base Alternative	DBP Control	CEC Removal
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, S2.3, or S2.4	Add S3.1 or S3.2
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, S2.3, or S2.4	Add S3.1 or S3.2
B2 – New 15 mgd Treatment Train	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, S2.3, or S2.4	Add S3.1 or S3.2
B3 – Replace Filters w/ UF Membranes	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2
B4 – Replace Plant w/RO Facility	<input checked="" type="radio"/>	<input checked="" type="radio"/>
		Add S3.1 or S3.2
B5 – Replace Conventional Softening w/Dual Softening	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, S2.3	Add S3.1 or S3.2

Yes, Partial, No

Adder for DBP Control
 • S2.1 – GAC
 • S2.2 – MBR
 • S2.3 – Actiflo™ CARB
 • S2.4 – Ozone/Biofiltration

Adder for CEC Removal
 • S3.1 – UV Disinfection/Peroxide
 • S3.2 – Ozone/Biofiltration

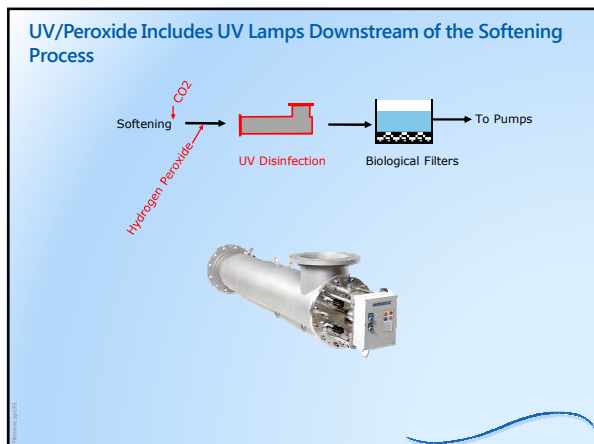
UV/Peroxide Provides CEC Reduction By Generating Free Radicals

Alternatives		
Base Alternative	DBP Control	CEC Removal
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, S2.3, or S2.4	Add S3.1 or S3.2
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, S2.3, or S2.4	Add S3.1 or S3.2
B2 – New 15 mgd Treatment Train	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, S2.3, or S2.4	Add S3.1 or S3.2
B3 – Replace Filters w/ UF Membranes	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, or S2.3	Add S3.1 or S3.2
B4 – Replace Plant w/RO Facility	<input checked="" type="radio"/>	<input checked="" type="radio"/>
		Add S3.1 or S3.2
B5 – Replace Conventional Softening w/Dual Softening	<input type="radio"/>	<input type="radio"/>
	Add S2.1, S2.2, S2.3	Add S3.1 or S3.2

Yes, Partial, No

Adder for DBP Control
 • S2.1 – GAC
 • S2.2 – MBR
 • S2.3 – Actiflo™ CARB
 • S2.4 – Ozone/Biofiltration

Adder for CEC Removal
 • S3.1 – UV Disinfection/Peroxide
 • S3.2 – Ozone/Biofiltration



We Recommend Eliminating UV/Peroxide From Consideration

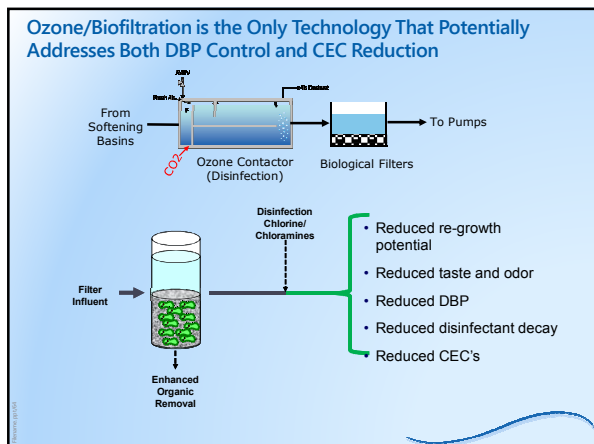
- UV before filtration for removal of assimilable organic carbon (AOC).
- UV Downstream of Softening Has Caused Precipitation Problems (Binney)
- If UV/peroxide is after traditional filtration - GAC Contactors are required (for stabilization).
 - More Costly

Excessive Sleeve Fouling Downstream of Softening

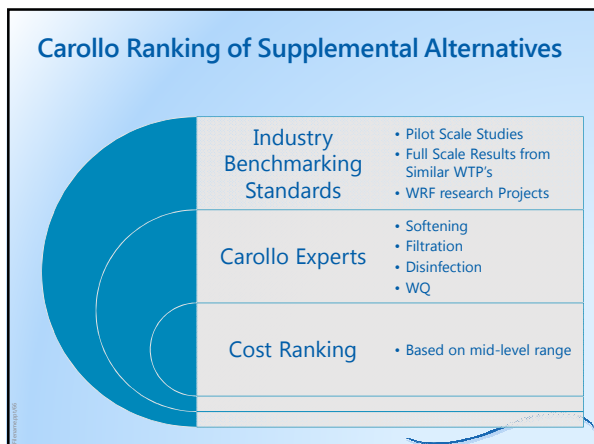
Similar to UV/Peroxide, Ozone Oxidizes CEC

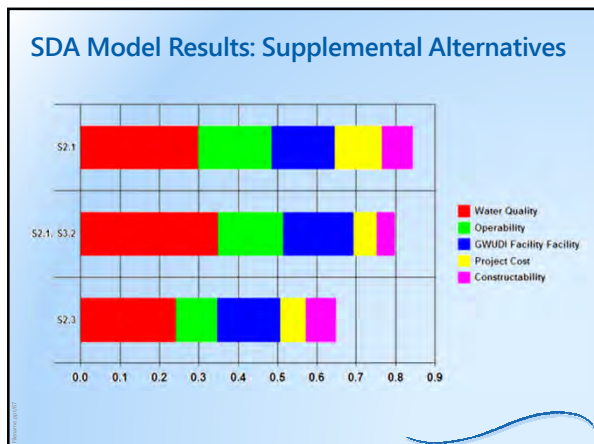
Alternatives	GWUDI Compliance	DBP Control	CEC Removal	
Base Alternative				
B1.1 - Expand Existing Plant w/Conventional Softening (Rerate Filters)	●	○	○	Adder for DBP Control S2.1 - GAC S2.2 - Activlo™ CARB S2.3 - Ozonation/Biofiltration
		Add S2.1, S2.2, or S2.3	Add S2.1 or S2.2	
B1.2 - Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	○	○	○	Adder for CEC Removal S2.1 - GAC S2.2 - Ozonation/Biofiltration
	Add S1.1	Add S2.1, S2.2, or S2.3	Add S2.1 or S2.2	
B2 - New 15 mgd Treatment Train	○	○	○	
	Add S1.1	Add S2.1, S2.2, or S2.3	Add S2.1 or S2.2	
B3 - Replace Filters w/UF Membranes	●	⊖	⊖	
		Add S2.1, S2.2, or S2.3	Add S2.1 or S2.2	
B4 - Replace Plant w/RD Facility	●	⊖	⊖	
			Add S2.1 or S2.2	
B5 - Replace Conventional Softening w/Reverse Softening	●	⊖	⊖	
		Add S2.1, S2.2, S2.3	Add S2.1 or S2.2	

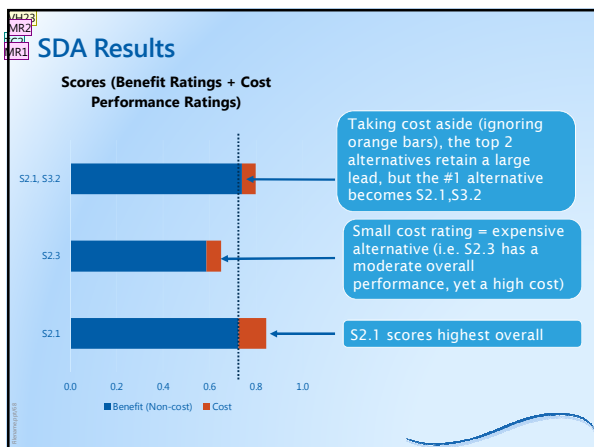
● Yes, ◐ Partial, ○ No

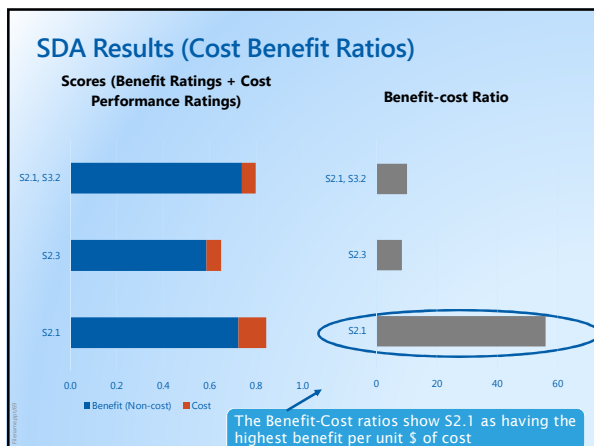


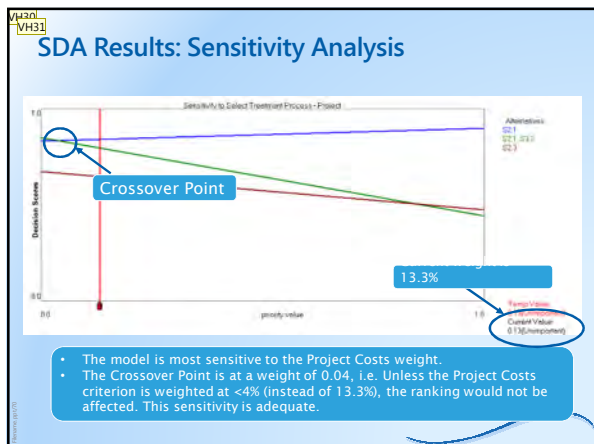
- ### Supplemental Processes Considered
- S2.1 – GAC Filters
 - S2.3 – Actiflo™ CARB Technology
 - S2.1 and S3.2- Ozone/Biofiltration followed by GAC





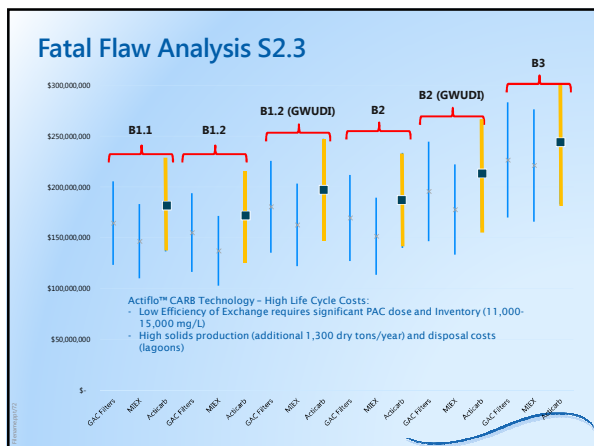






Criticality of Most Sensitive Criteria

Criticality	Criterion Name	Explanation
9.6%	Project Costs	Not very sensitive. The Project Cost weight would need to be reduced from 13% to 3.4% to make S2.1, S3.2 rank higher than S2.1
14.6%	Constructability	Not sensitive. The Constructability weight (10%) would need to go negative to make S2.1, S3.2 rank higher than S2.1
16.4%	Water Quality	Not sensitive. The Water Quality weight would need to increase from 38% to 54% to make S2.1, S3.2 rank higher than S2.1
25.8%	GWUDI Facility	Not sensitive. The GWUDI Facility weight would need to increase from 18% to 42% to make S2.1, S3.2 rank higher than S2.1



Our Recommendation is to Eliminate Actiflo™ Carb from Consideration

The flowchart consists of three blue rectangular boxes connected by white arrows pointing from left to right. The first box contains the text 'Never Built on this Scale' with a vertical note on the left: '.10 mgd largest installation'. The second box contains 'Expensive' with a vertical note on the left: 'PAC Use Results in High Costs'. The third box contains 'Not Sustainable' with a vertical note on the left: 'Extremely High PAC Doses are Not Green'. A small blue wavy line is at the bottom right of the slide.

Ranking Questions/Discussions

- SDA Model manipulation

A blue slide with the title 'Ranking Questions/Discussions' and a single bullet point: '• SDA Model manipulation'. A small blue wavy line is at the bottom right of the slide.

Preliminary Ranking and Alternatives Summary:

Base Concepts:	Supplemental Concepts:
B1.1 – Expand Existing Plant w/Conventional Softening (Rerate Filters)	S1.1– Include improvements for GWUDI Compliance
B1.2 – Expand Existing Plant w/Conventional Softening (New 15 MGD Filter Train)	S2.1 – GAC Filters
B2 – New 15 mgd Treatment Train	S2.1 and S3.2 – Biofiltration with GAC filters

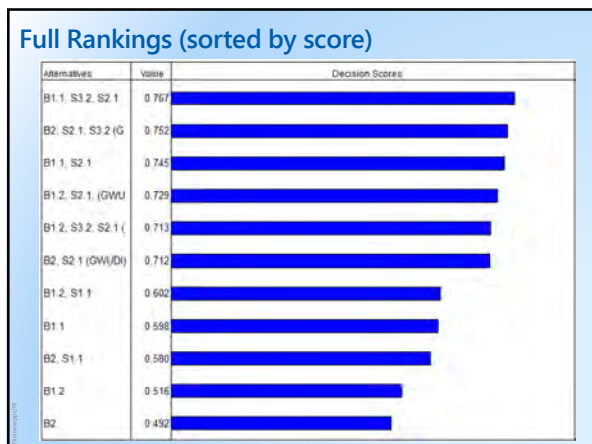
A blue slide with the title 'Preliminary Ranking and Alternatives Summary:'. It contains two columns of text. The left column is under the heading 'Base Concepts:' and lists B1.1, B1.2, and B2. The right column is under the heading 'Supplemental Concepts:' and lists S1.1, S2.1, and S2.1 and S3.2. A small blue wavy line is at the bottom right of the slide.

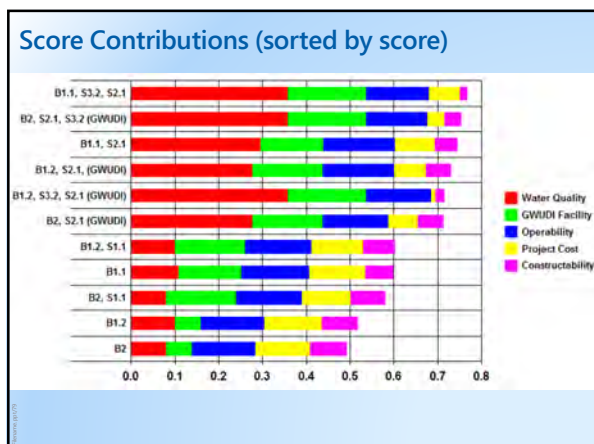
WV-2
VH33

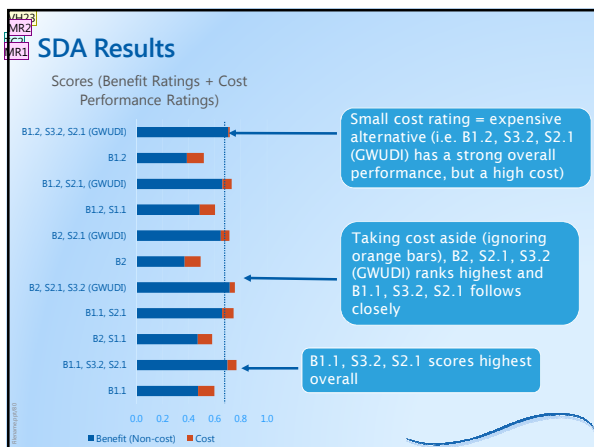
Treatment Alternatives

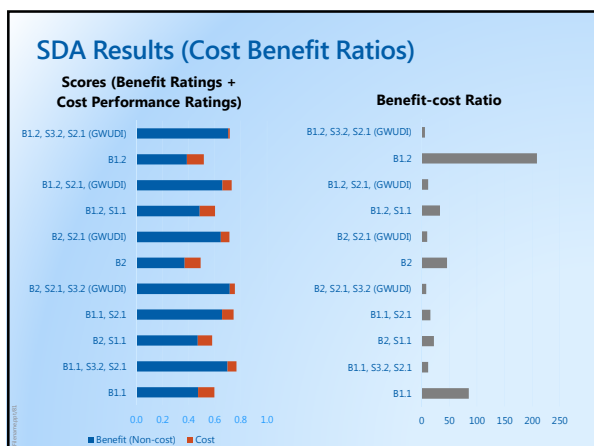
Base	Supplement	Description	Comments
B1.1	No Supplement	Only Upgrade Existing	GWUDI Compliant, Requires Chloramines
B1.1	S2.1	Upgrade Existing With GAC Contactors	GWUDI Compliant Permits use of Free Chlorine
B1.1	S2.1, S3.2	Upgrade Existing with Ozone/BAF and GAC Contactors	GWUDI Compliant Permits use of Free Chlorine
B1.2	No Supplement	New Filters (15mgd)	Not fully GWUDI Compliant Requires Chloramines
B1.2	S1.1	New Filters (15 mgd) with plant upgraded	GWUDI Compliant Requires Chloramines
B1.2	S1.1, S2.1	New Filters (15 mgd) with GAC Contactors	GWUDI Compliant Permits use of Free Chlorine
B1.2	S1.1, S2.1, S3.2	New Filter (15 mgdd) with Ozone/BAF and GAC Contactors	GWUDI Compliant Permits use of Free Chlorine Adds CECs
B2	No Supplement	New Treatment Train (15 mgd)	Not fully GWUDI Compliant Requires Chloramines
B2	S1.1	New Treatment Train (15 mgd) with plant upgraded.	GWUDI Compliant Requires Chloramines
B2	S1.1, S2.1	New Treatment Train (15 mgd) and GAC Contactors	GWUDI Compliant Permits use of Free Chlorine
B2	S1.1, S2.1, S3.2	New Treatment Train (15 mgd) with Ozone/BAF and GAC Contactors	GWUDI Compliant Permits use of Free Chlorine Adds CECs

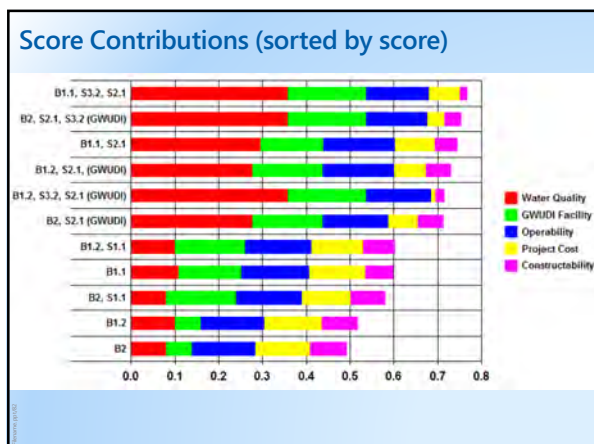




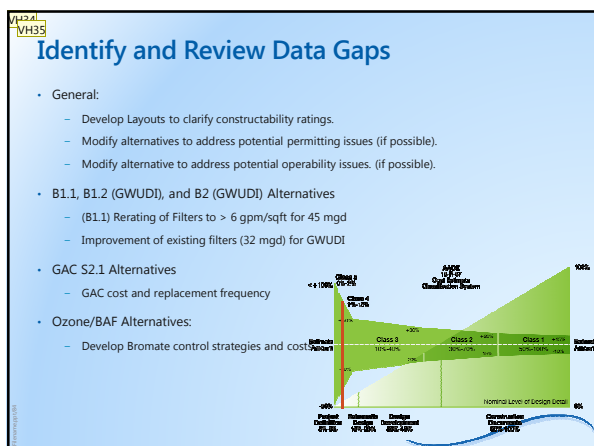








- ### Agenda
- Pairwise Comparison
 - Base Alternatives:
 - Discuss/Review Alternatives and Carollo Shortlist
 - SDA Model Development
 - Discuss and Rank Shortlisted Alternatives
 - Supplemental Alternatives:
 - Discuss/Review Alternatives and Carollo Shortlist
 - SDA Model Development
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 - **Review Data Gaps & Action/Decision Logs**
 - Review Final Steps
 - General Comment by Public, Members, and Staff
 - Next Meeting Date – FINAL DECISION MAKING AND PUBLIC SUMMARY WORKSHOPS



DECISION LOG

DECISION LOG						
Project: Preliminary Design Report Update - Project On/Off/Close						DATE: 10/20/17
Client: City of Columbia, MO						BY: BH
Contract #: 6						
ITEM NO.	DECISION ID#	DECISION DATE	DECISION DESCRIPTION	DECISION DATE	COMMENTS	
13	City	Travel Meeting	Reviewed travel meeting agenda for October 24th over the referenced NO values	14-Sep-17		
14	City	Travel Meeting	Reviewed water quality goal to 100% of the RFP's limit over the referenced NO values	14-Sep-17		
15	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
16	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
17	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
18	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
19	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
20	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
21	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
22	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
23	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
24	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
25	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
26	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
27	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
28	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
29	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
30	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
31	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
32	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
33	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
34	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
35	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
36	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
37	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
38	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
39	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		
40	City	Travel Meeting	Reviewed water quality goals for CEC's management and regulatory values in the referenced NO values	14-Sep-17		

ACTION LOG

ACTION ITEM						
Project: Preliminary Design Report Update - Project On/Off/Close						DATE: 10/20/17
Client: City of Columbia, MO						BY: BH
Contract #: 6						
ITEM NO.	RESPONSIBLE PARTY	ACTION ITEM	START DATE	TARGET / ALLOWED LATE DATE	ITEM COMPLETION DATE	COMMENTS
11	Carroll	Provide binder containing past and future material to committee members	11-Sep-17	09h-17	10-Oct-17	
12	Carroll	Notify and present reason statement at the next meeting for approval	11-Sep-17	09h-17	10-Oct-17	
13	Shaw	Send out poll to group for next meeting meeting date with October 13 being the preferred date	11-Sep-17	Sep-17	12-Sep-17	
14	Carroll	Send out updated reason statement	10-Oct-17	13-Oct-17	12-Oct-17	
15	Carroll/Spaw	Send out voting sheets for sub-criteria stress-examination scenarios	10-Oct-17	13-Oct-17	12-Oct-17	
16	City	Print and return voting sheets for sub-criteria stress-examination exercise	10-Oct-17	13-Oct-17	12-Oct-17	Committee members will select which sub-criteria are more important than others
17	Carroll/Spaw	Send out poll to group for next meeting meeting date	10-Oct-17	13-Oct-17	13-Oct-17	

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- General Comment by Public, Members, and Staff
- Next Meeting Date – FINAL DECISION MAKING AND PUBLIC SUMMARY WORKSHOPS

Final Steps

- Carollo:
 - Update Costs and Rankings Based upon Data gap Resolution
 - Final Ranking
 - Prepare Draft and Final Technical Memorandum Update
- Workgroup:
 - Review Final Ranking and make Recommendation to Water and Light Dept
 - Participate in Public Meeting

Agenda

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- Next Meeting Date – FINAL DECISION MAKING AND PUBLIC SUMMARY WORKSHOPS
 - February 12, 2017 5:30 pm ?

Agenda

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- General Comment by Public, Members, and Staff
- **Next Meeting Date – FINAL DECISION MAKING AND PUBLIC SUMMARY WORKSHOPS**
 - February 12, 2017 5:30 pm ?









Identify and Review Data Gaps

- General:
 - Develop Layouts to clarify constructability ratings.
 - Modify alternatives to address potential permitting issues (if possible).
 - Modify alternative to address potential operability issues. (if possible).
- B1.1, B1.2 (GWUDI), and B2 (GWUDI) Alternatives
 - (B1.1) Rerating of Filters to > 6 gpm/sqft for 45 mgd
 - Improvement of existing filters (32 mgd) for GWUDI
- GAC S2.1 Alternatives
 - GAC cost and replacement frequency
- Ozone/BAF Alternatives:
 - Develop Bromate control strategies and cost

Data Gap Analysis

- B1.1 – Rerating of Existing Filters to 48 mgd.

Concern Regarding Hydraulic Efficiencies:

- Increase Media
- Eliminate Gravel and install IMS Cap

Data Gap Analysis (cont.)

- B1.1 – Rerating of Existing Filters to 48 mgd.

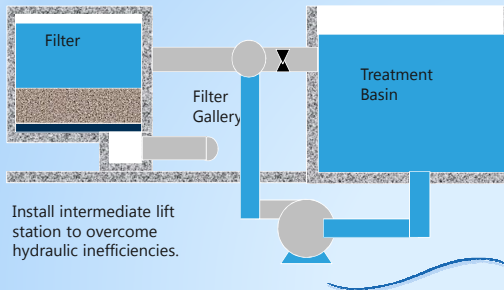
Decreased water level above filters leads to potential problems at high rates.

Concern Regarding Hydraulic Efficiencies:

- Increase Media
- Eliminate Gravel and install IMS Cap

Data Gap Analysis (cont.)

- B1.1 – Rerating of Existing Filters to 48 mgd

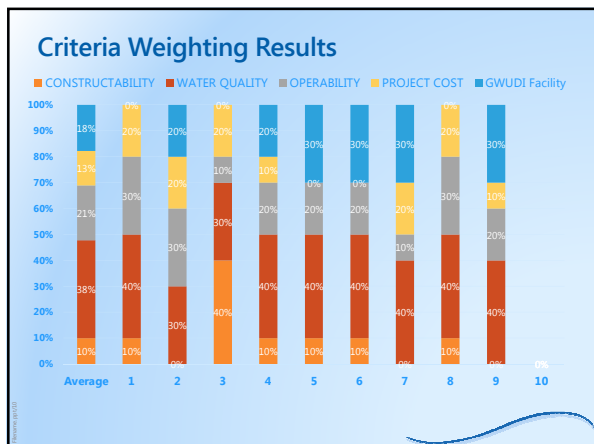


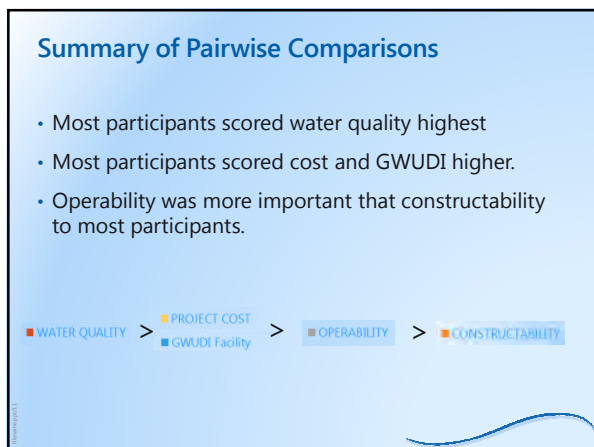
Data Gap Analysis: S2.1 GAC Contactors

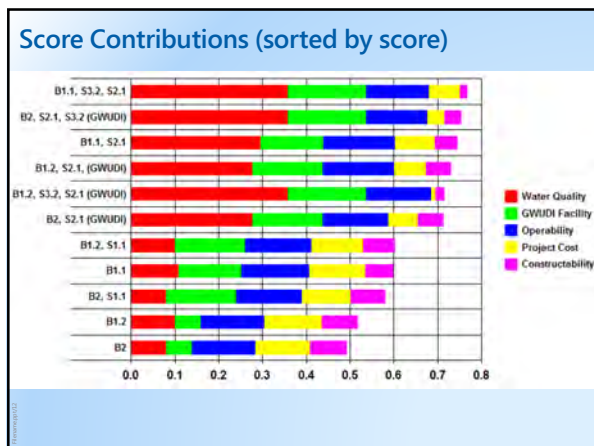
- RSSC (rapid small-scale column) testing required to identify potential Carbon's to test.
- Pilot testing required to determine useful life for DBP management.
- Assumed Carbon Life based upon similar Communities: Every 3 years.

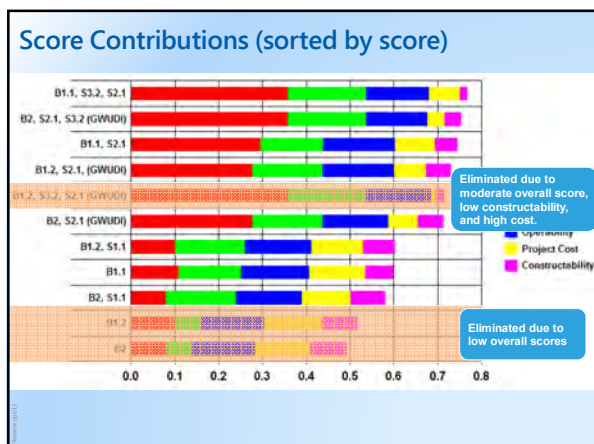
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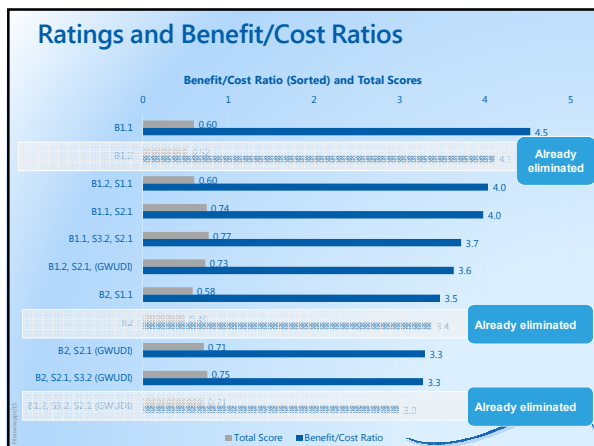


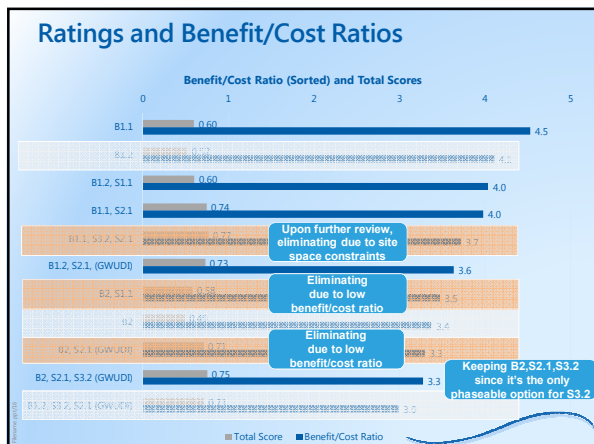


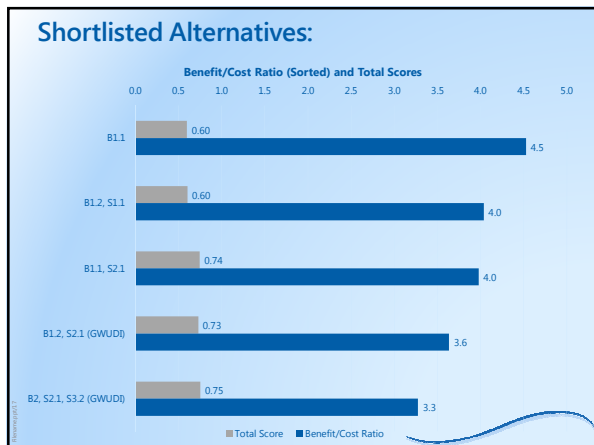


Summary from Last Meeting

- 3 alternatives not short-listed: B2, B1.2, and B1.2,S3.2,S2.1 (GWUDI)
- Because of Water Quality and GWUDI high rating, results ranked highest cost items because those naturally provided highest benefit.
- However... when examining benefit/cost ratios some of these items were clearly offered little additional benefit with high incremental costs.
- Decision was made to re-rank based upon best benefit: cost ratio plus those alternatives most easily phased to the higher cost alternatives.

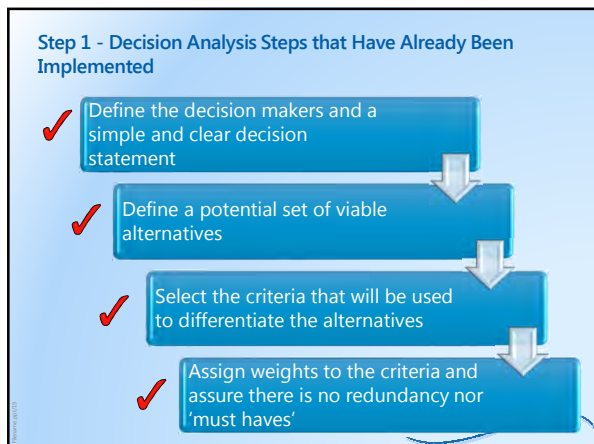


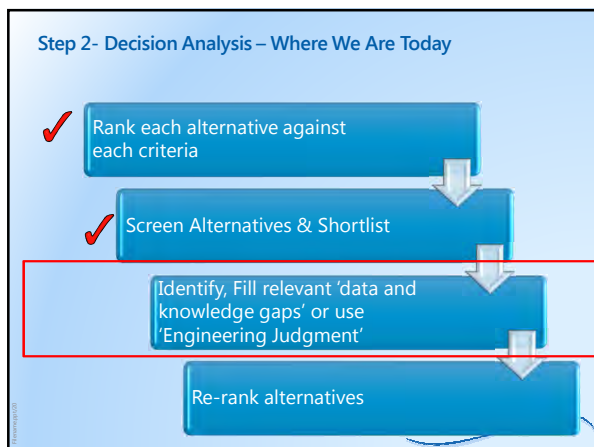


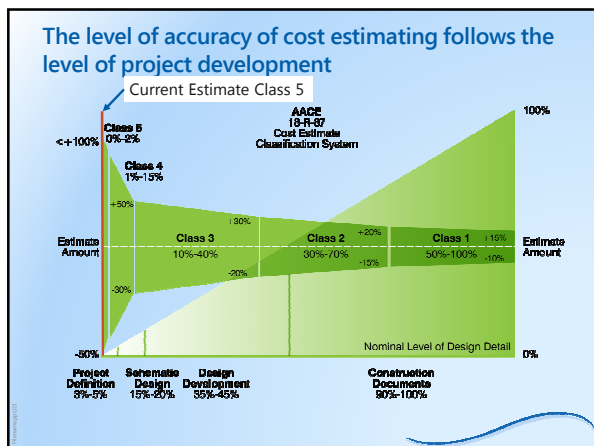


Shortlist Rationale

- All alternatives that did not meet GWUDI Eliminated due to low benefit score.
- Alternatives involving Ozone/biofiltration eliminated:
 - Low Cost/Benefit Ratios
 - Ability to phase is extremely poor (exception B2)

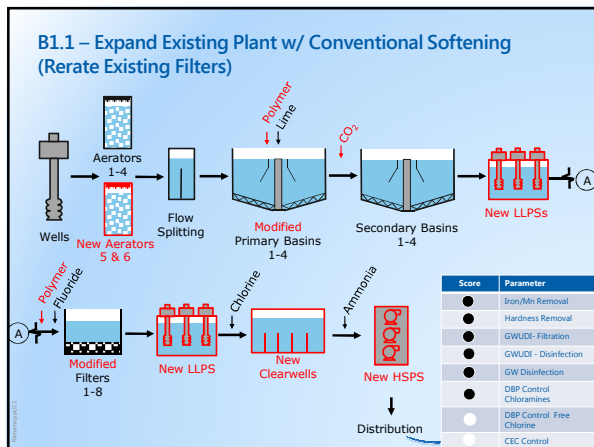


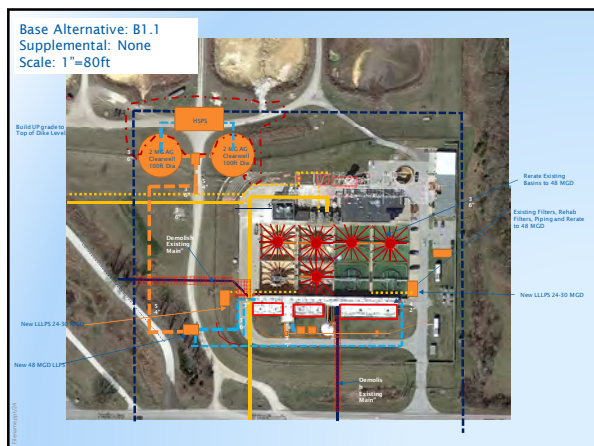




Life Cycle Cost Development:

- Phase 0: 2020
- Phase I: 2024
- Phase II: 2029 (assumes 5 year period to pilot/design/construct)
- End of Life Cycle Period: 2044 (20 years from Phase I)



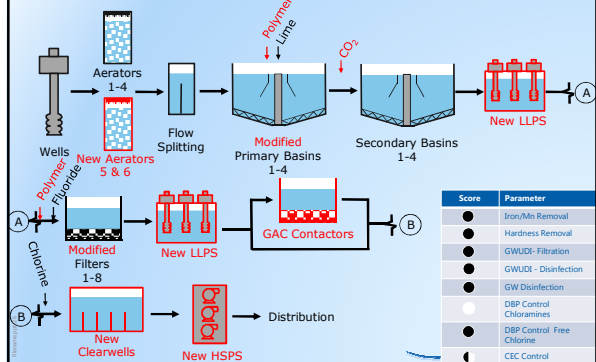


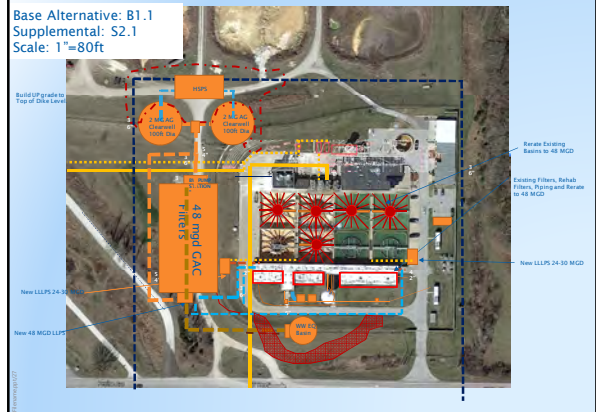
B1.1 Highlights

Description: Expand Existing Plant (Rerate Existing Filters)

<p>Water Quality (37.8%)</p> <ul style="list-style-type: none"> Likely requires chloramines to satisfy current Disinfection By-Product regulations. Potential future regulatory concerns (CEC's) will need additional processes. No significant improvement in overall water quality (Except for GWUDI Compliance) 	<p>Operability (21.1%)</p> <ul style="list-style-type: none"> Increased Maintenance (New Pumps) Low Lift Pumps Required to Control Filtration Process and pump to clearwells, increasing complexity. Most efficient use of space (easier phasing) 	<p>GWUDI Facility (17.8%)</p> <ul style="list-style-type: none"> Improved Filtration Disinfection to meet SWTR Requirements
	<p>Constructability (10%)</p> <ul style="list-style-type: none"> Large Disruption to Plant Ops (Work on Existing Filters) Minimal footprint of new facilities. Rerating Filters Requires Permitting Variance 	<p>Project Cost (13.3%)</p> <ul style="list-style-type: none"> Capital = \$106 million O&M = \$3.6 million Life Cycle = \$160 million <p><small>*Level of Accuracy (+50% to -30%) *Wellfield & Raw Water pipeline improvements not included.</small></p>

B1.1, S2.1 – Expand Existing Plant w/ Conventional Softening (Rerate Existing Filters) + GAC

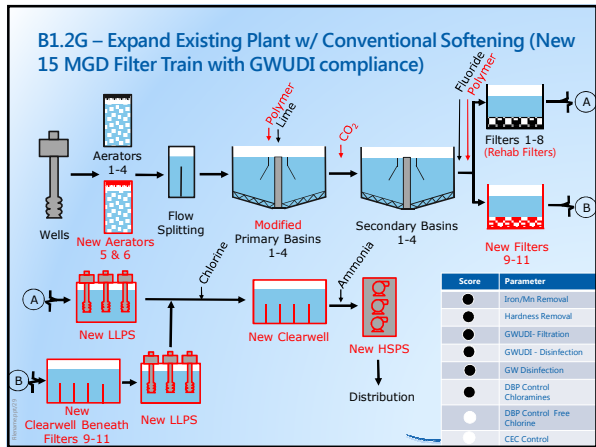


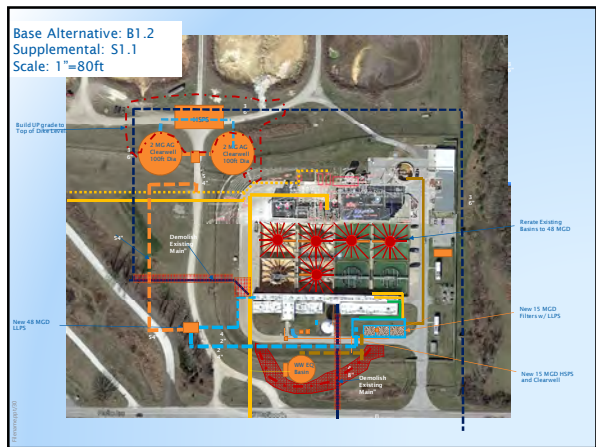


B1.1, S2.1 Highlights

Description: Expand Existing Plant (Rerate Existing Filters) and Add Post Filter GAC Contactors

Water Quality (37.8%)	Operability (21.1%)	GWUDI Facility (17.8%)
<ul style="list-style-type: none"> Ability to design finished water quality to meet DBP regulations without relying on Chloramines. Robust process that will remove some CEC's. Operating Cost may be impacted by future regulations due to process inefficiencies. 	<ul style="list-style-type: none"> Additional Staffing Staffing Education for New Processes (DBP Control) Increased Maintenance (New Pumps and Process) Moderate Complexity 	<ul style="list-style-type: none"> Fully Compliant
	Constructability (10%)	Project Cost (13.3%)
	<ul style="list-style-type: none"> Large Disruption to Plant Ops (Work on Existing Filters) Large Space Requirements will require some use of lagoon space. Rerating Filters Requires Permitting Variance 	<ul style="list-style-type: none"> Capital = \$152 million O&M = \$4.7 million Life Cycle = \$221 million
		<p><small>*Level of Accuracy (+50% to -30%) *Wellfield & Raw Water pipeline improvements not included.</small></p>



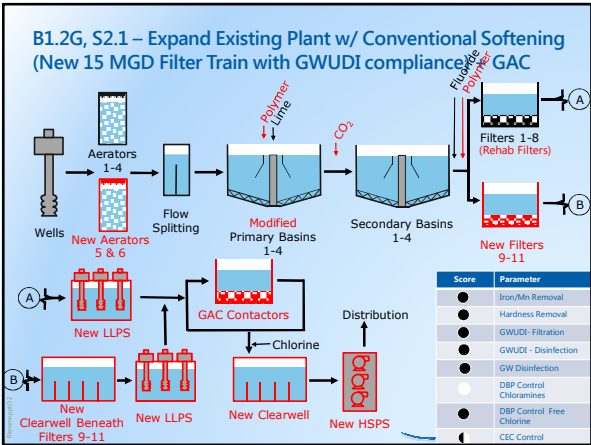


B1.2, S1.1 (GWUDI) Highlights

Description: Expand Existing Plant (New Filter Train)

<p>Water Quality (37.8%)</p> <ul style="list-style-type: none"> Likely requires chloramines to satisfy current Disinfection By-Product regulations. Potential future regulatory concerns (CEC's) will need additional processes. No significant improvement in overall water quality (Except for GWUDI Compliance) 	<p>Operability (21.1%)</p> <ul style="list-style-type: none"> Increased Maintenance (New Pumps and Filters) Minimal Complexity Low Lift Pumping Required for phasing and to minimize future construction costs. A little more difficult to phase. 	<p>GWUDI Facility (17.8%)</p> <ul style="list-style-type: none"> Fully Compliant
<p>Constructability (10%)</p> <ul style="list-style-type: none"> Moderate Disruption to Plant Ops Moderate Space Requirements 	<p>Project Cost (13.3%)</p> <ul style="list-style-type: none"> Capital = \$124 million O&M = \$3.6 million Life Cycle = \$178 million 	

*Level of Accuracy (+50% to -30%)
**Wellfield & Raw Water pipeline improvements not included.



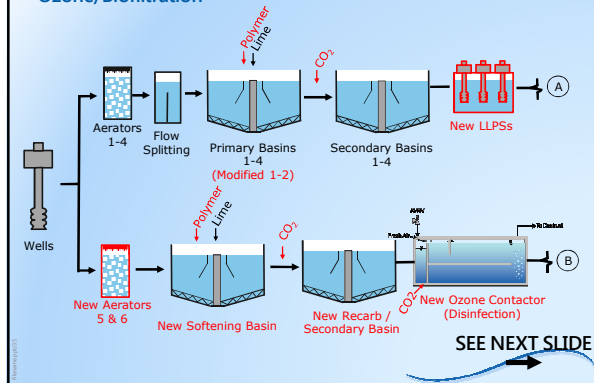


B1.2, S1.1(GWUDI), S2.1 Highlights

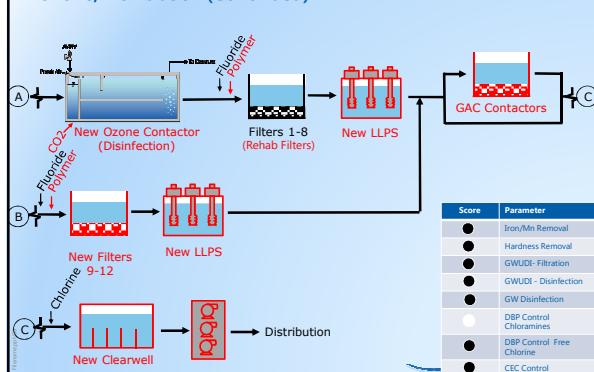
Description: Expand Existing Plant (New Filter Train) and Add GAC Post Filter Contactors.

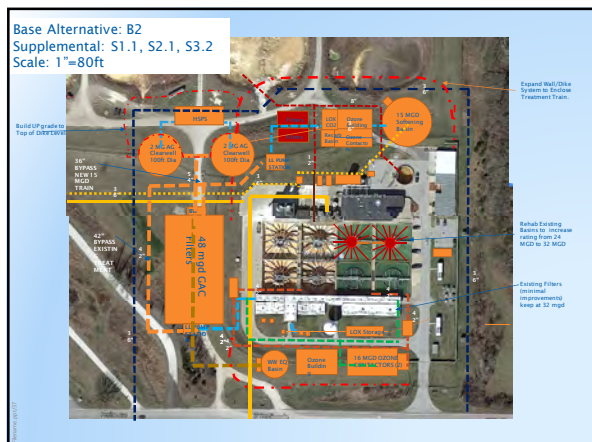
<p>Water Quality (37.8%)</p> <ul style="list-style-type: none"> Ability to design finished water quality to meet DBP regulations without relying on Chloramines. Robust process that will remove some CEC's. Operating Cost may be impacted by future regulations due to process inefficiencies. 	<p>Operability (21.1%)</p> <ul style="list-style-type: none"> Additional Staffing Staffing Education for New Processes Increased Maintenance (New Pumps, Filters, and Process) Moderate Complexity 	<p>GWUDI Facility (17.8%)</p> <ul style="list-style-type: none"> Fully Compliant
<p>Constructability (10%)</p> <ul style="list-style-type: none"> Moderate Disruption to Plant Ops Large Space Requirements 		<p>Project Cost (13.3%)</p> <ul style="list-style-type: none"> Capital = \$166 million O&M = \$4.7 million Life Cycle = \$236 million <p><small>*Level of Accuracy (+50% to -30%) *Wellfield & Raw Water pipeline improvements not included.</small></p>

B2G, S2.1, S3.2 – New 15 MGD Treatment Train + GAC + Ozone/Biofiltration



B2G, S2.1, S3.2 – New 15 MGD Treatment Train + GAC + Ozone/Biofiltration (Continued)

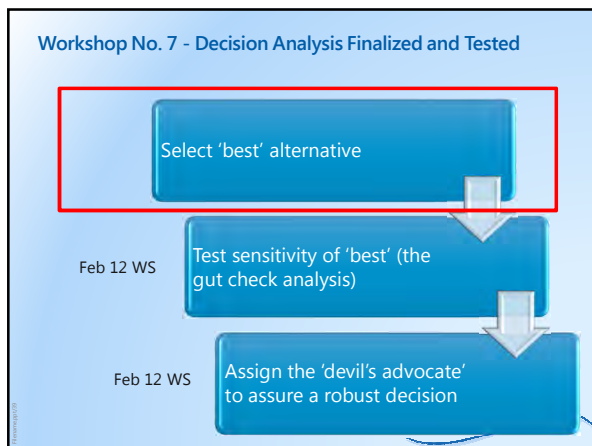




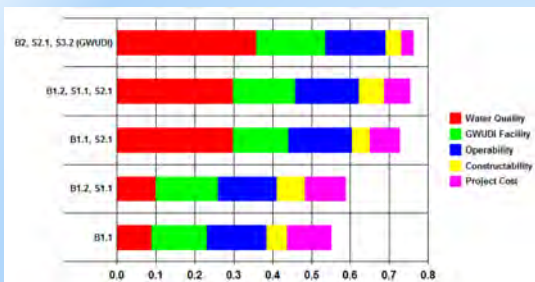
B2 (GWUDI), S2.1, S3.2 Highlights

Description: Expand Existing Plant (New Treatment Train), post treatment Ozone/Biofiltration and post filter GAC contactors.

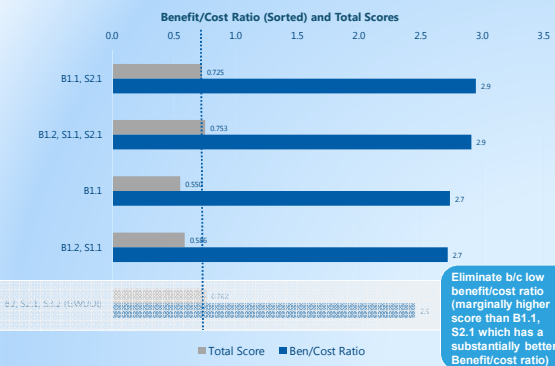
<p>Water Quality (37.8%)</p> <ul style="list-style-type: none"> Ability to design finished water quality to meet DBP regulations without relying on Chloramines. Best Available Technology for CEC removal. Synergistic impacts with Post Filter GAC. 	<p>Operability (21.1%)</p> <ul style="list-style-type: none"> Additional Staffing Staffing Education for New Processes Increased Maintenance (New Pumps, Filters, and Processes) Most Complex Alternative to Operate (two trains with multiple processes) 	<p>GWUDI Facility (17.8%)</p> <ul style="list-style-type: none"> Fully Compliant
<p>Constructability (1.0%)</p> <ul style="list-style-type: none"> Minimal Disruption to Plant Ops High Space Requirements 		<p>Project Cost (13.3%)</p> <ul style="list-style-type: none"> Capital = \$223 million O&M = \$5.1 million Life Cycle = \$298 million <p><small>*Level of Accuracy (+50% to -30%) *Wellfield & Raw Water pipeline improvements not included.</small></p>



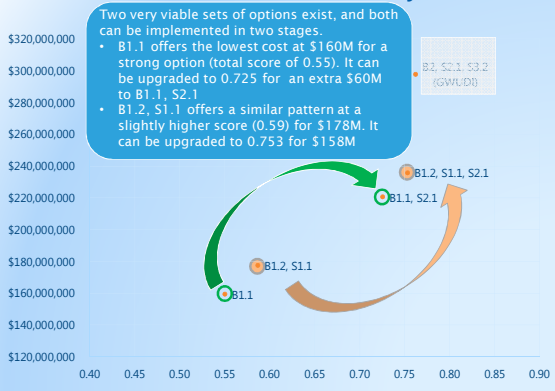
Top 5 Score Contributions (sorted by score)

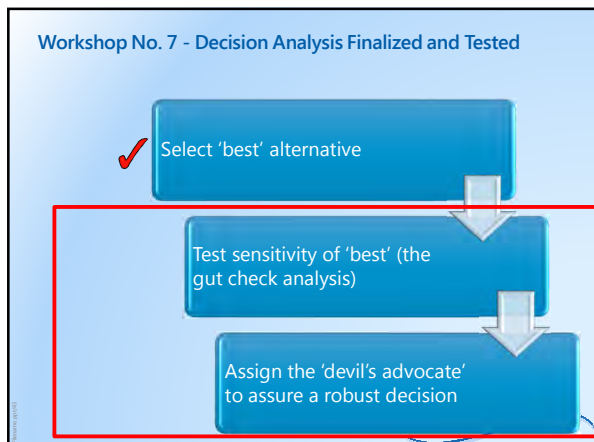


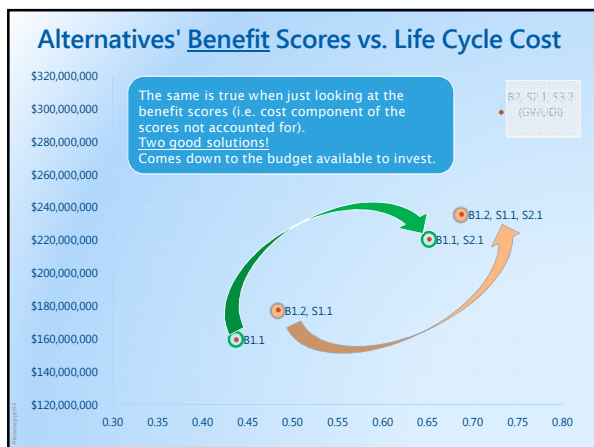
Ratings and Benefit/Cost Ratios



Alternatives' Total Scores vs. Life Cycle Cost







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Adopted Mission Statement and Goals

FINAL Draft Mission Statement for Drinking Water Planning Workgroup:
 Mission Statement: Provide planning recommendations to the Water and Light Advisory Board and the City Council regarding the replacement of the water treatment system by establishing water quality goals, determining treatment criteria, and conducting a thorough, objective assessment of industry accepted treatment technologies to determine the process or processes that best meet those criteria.

The Goals of the Drinking Water Planning Workgroup are as follows:

- Review current planning strategies for water supply and verify current goals and planning horizon for water treatment capacity expansion.
- Consider current regulations, potential future regulations, and potential future water reuse and reuse potential against long-term water quality goals.
- Assess the state of the industry and identify potential treatment strategies that meet or exceed some or all of the potential long-term water quality goals based upon industry acceptance and long-term (present and future) costs.
- Formulate a set of water quality goals that potential treatment strategies to meet or exceed potential goals will be evaluated.
- Objectively evaluate and rank potential treatment strategies that meet planning horizon goals using a structured decision analysis model.
- Conduct a sensitivity analysis of decisions to review decisions and identify all decisions to potential changes in criterion assessments.
- Through this objective process, develop planning recommendations to guide the Water and Light Advisory Board and City Council regarding the water treatment system.

Final Recommendation Statement:

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Appendix F

DWPWG RECOMMENDATIONS



CITY OF COLUMBIA, MISSOURI

COLUMBIA UTILITIES
COLUMBIA TERMINAL RAILROAD

DATE: March 9, 2018

TO: Mayor and City Council
Water and Light Advisory Board

FROM: Terry Merritt, Chair 
Drinking Water Planning Work Group

RE: ***Final Recommendations of the Drinking Water Planning Work Group***

In April 2017, the Drinking Water Planning Work Group was established to assist in the update of the 2011 Water Treatment Plant Expansion Preliminary Design Report and was tasked with the following:

- Reviewing current drinking water regulations, including what types of disinfection methods comply with regulations.
- Reviewing Columbia's current water supply conditions.
- Assessing the current state of utility industry and customer-side water treatment technology and costs.
- Reviewing and providing input on developed recommendations.
- Developing drinking water planning recommendations.

The Work Group met a total of eight times with the final meeting on February 26th, 2018.

The Work Group's findings were as follows:

- The McBaine Water Treatment Plant (McBaine WTP) should consider processes that meet requirements for a Groundwater Under Direct Influence (GWUDI) facility.
- The McBaine WTP should utilize treatment technologies to achieve disinfection byproduct (DBP) compliance without the use of chloramines and to also assist in removal of Contaminants of Emerging Concern (CECs).

The following recommendations were finalized at the meeting on February 26th with all members in favor, excluding Mr. Karl Skala, who abstained his vote:

- Priority should be given to first restoring the plant to its 32 MGD capacity prior to increasing capacity to 48 MGD.

- The base alternatives of B1.1, B1.2, and B2 should be evaluated with the supplemental processes given to achieve improved water quality through a phased approach.
- The design on the selected alternative should begin no later than 2020, as indicated in Carollo's report, to be in operation no later than 2024, unless design and construction are able to be accomplished sooner.
- In order to improve water quality while the new process train is in design and construction, repair and/or enhancement of the current filters and pilot testing done to make every effort to return to free chlorine disinfection.
- The rehabilitation and/or enhancement initiatives outlined in the Condition Assessment will address deficiencies in the facility and system and request an updated timeline for these initiatives be produced by Water and Light.

The Drinking Water Planning Work Group respectfully submits the above recommendations for serious consideration by the Water and Light Advisory Board and Mayor and City Council.